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C L A I M S

1. A method of preparing a supported catalyst, preferably a hydrocracking catalyst, the method at least comprising the steps of:

- 5 a) providing a zeolite Y having a bulk silica to alumina ratio (SAR) of at least 10;
- b) mixing the zeolite Y provided in step a) with a base, water and a surfactant, thereby obtaining a slurry of the zeolite Y;
- 10 c) reducing the water content of the slurry obtained in step b) thereby obtaining solids with reduced water content, wherein the reducing of the water content in step c) involves the addition of a binder;
- d) shaping the solids with reduced water content obtained in step c) thereby obtaining a shaped catalyst carrier;
- 15 e) calcining the shaped catalyst carrier obtained in step d) at a temperature above 300°C in the presence of the surfactant of step b), thereby obtaining a calcined catalyst carrier;
- 20 f) impregnating the catalyst carrier calcined in step e) with a hydrogenation component thereby obtaining a supported catalyst;
- wherein no heat treatment at a temperature of above 500°C takes place between the mixing of step b) and the
- 25 shaping of step d).
2. The method according to claim 1, wherein the zeolite Y provided in step a) has a bulk silica to alumina ratio (SAR) of 20 to 100.
3. The method according to claim 1 or 2, wherein the
- 30 surfactant as used in step b) comprises an alkylammonium halide.

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4. The method according to any one of the preceding claims, wherein in step b) the zeolite Y is mixed with a C₈-C₂₀ alcohol, preferably a C₁₀-C₁₈ alcohol.
5. The method according to any one of the preceding claims, wherein the zeolite Y in the slurry as obtained in step b) has a total mesopore volume in pores with a volume of 2-8 nm as determined according to Ar adsorption according to NLDFT of at least 0.2 ml/g, preferably in the range of 0.30-0.65 ml/g.
- 10 6. The method according to any one of the preceding claims, wherein the calcining in step e) takes places in the presence of oxygen.
7. The method according to any one of the preceding claims, wherein the hydrogenation component comprises a metal selected from the group consisting of Group VIB and Group VIII metals.
- 15 8. The method according to claim 7, wherein the metal is selected from Ni, W and Mo, preferably Ni and W.
9. The method according to any one of the preceding claims, wherein no heat treatment at a temperature of above 300°C takes place between the mixing of step b) and the shaping of step d).
- 20 10. A supported catalyst obtained by the method according to any of the preceding claims.
- 25 11. A process for the conversion of a hydrocarbonaceous feedstock into lower boiling materials, which process comprises contacting the feedstock with hydrogen at elevated temperature and pressure in the presence of a catalyst as obtained in the method according to any of the preceding claims 1-10.
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