

Description**Background of the Invention****1. Field of the Invention**

This invention relates to supported chromium oxide polymerization catalysts, processes for preparing such catalysts and olefin polymerization processes utilizing the catalysts.

2. Description of the Prior Art

It is well known that olefin polymers can be prepared using supported chromium oxide catalysts. The polymerization reactions can be carried out in hydrocarbon solutions in which the polymers are soluble or in diluents in which the polymers are insoluble whereby slurries of suspended solid polymer particles are produced. In such polymerization processes, the melt indexes of the polymers can be varied by varying the polymerization temperatures, i.e., higher reaction temperatures generally result in increased melt indexes. However, in slurry polymerization processes, the reaction temperatures which can be utilized are limited in that at higher temperatures the polymers become swollen and sticky.

Other techniques are known in the art which bring about the production of polymers of higher melt indexes in slurry polymerization processes without increasing the reaction temperatures above normal limits. For example, United States Patent No. 4,384,987 to Hawley discloses a polymerization catalyst comprised of supported chromium oxide which is prepared by a process including the step of treating the catalyst with a permanganate compound. The use of such a catalyst in slurry polymerization processes results in polymers having higher melt indexes.

Another catalyst useful for polymerizing α -olefins is known from EP-A-0 272 553. This catalyst is prepared by impregnating a support containing one or more of silica, titania, and alumina with a chromium compound such as chromium oxide and a metal salt other than the chromium compound and then activating the thus obtained salt-impregnated support by subjecting same to increased temperature in the presence of oxygen. However, this catalyst is suitable for the formation of homopolymers and copolymers of ethylene having high densities.

Supported chromium oxide catalysts have heretofore been comprised of chromium oxide and supports containing one or more of silica, titania, thoria, alumina, zirconia or aluminophosphates. The catalysts are prepared by combining the chromium oxide and the support in a known manner and then activating the catalyst. By the present invention improved supported chromium oxide catalysts and processes for preparing and using such catalysts are provided. The improved catalysts have increased polymerization activities and result in polymers of high melt indexes.

Summary of the Invention

In accordance with the present invention, improved polymerization catalysts comprised of chromium oxide and supports containing one or more of silica, titania, thoria, alumina, zirconia or aluminophosphates are provided. A catalyst of the invention is prepared by first combining chromium oxide and the support utilized in a known manner. The catalyst produced is then impregnated with a metal salt selected from formates, acetates, nitrates, chlorides, chlorates and hydroxides of alkali metals, alkaline earth metals and mixtures thereof and activated. The resulting catalyst has increased polymerization activity and polymers of increased melt indexes can be produced using the catalyst.

The impregnation step of the present invention preferably comprises mixing the catalyst with a non-aqueous solution of the metal salt or salts utilized followed by removing the non-aqueous solvent from the mixture.

In another aspect of the invention, processes for polymerising at least one olefin monomer using the improved catalysts are provided. In a preferred polymerization process, the activated metal salt impregnated catalyst is reduced by contact with carbon monoxide and used with a cocatalyst, i.e., a trialkyl aluminum compound in the presence of hydrogen. Copolymers produced, e.g., ethylene-hexene copolymers, have low density and high comonomer incorporation efficiency.

It is, therefore, a general object of the present invention to provide improved polymerization catalysts and processes for making and using such catalysts.

A further object of the present invention is the provision of improved supported chromium oxide polymerization catalysts having increased activities which can be used to produce olefin polymers having

increased melt indexes.

Other and further objects, features and advantages of the present invention will be readily apparent to those skilled in the art upon a reading of the description of preferred embodiments which follows.

5 **Description of Preferred Embodiments**

In accordance with the present invention, an olefin polymerization catalyst comprised of chromium oxide and a support containing one or more of silica, titania, thoria, alumina, zirconia or aluminophosphates is prepared by a process including the steps of impregnating the catalyst with one or more alkali or alkaline
10 earth metal formates, acetates, nitrates, chlorides, chlorates and hydroxides and activating the thus impregnated catalyst. The resulting catalyst has improved activity and produces a polymer of increased melt index. Melt index is a measure of the viscosity of a polymer at a specified temperature and pressure, and is a function of the molecular weight of the polymer. As referred to herein, Melt Index (MI) and High Load Melt Index (HLMI) are those values determined in accordance with ASTM 1238-65T, conditions E and
15 F, respectively.

A variety of processes and techniques have been developed for producing various supported chromium oxide catalysts useful in olefin polymerization reactions. Such supported chromium oxide catalysts can include silica supports which contain silica admixed with one or more metal compounds of titania, thoria, alumina and/or zirconia. Silica supports are described, for example, in U.S. Patent No. 3,875,079 to Witt.
20 Silica-titania supports on which is dispersed chromium oxide or a chromium compound convertible to chromium oxide by oxidation are described, for example, in United States Patent No. 4,151,122, issued to McDaniel et al. The catalysts produced are activated by a reduction-reoxidation process.

Silica supports employed in supported chromium oxide catalysts can be produced, with or without the metal compounds mentioned above, by introducing an aqueous solution of an alkali metal silicate into an
25 aqueous solution of an acid, either of the solutions optionally containing one or more of the above mentioned metal compounds, aging the hydrogel which forms, washing the hydrogel to reduce the alkali metal content thereof to a minimum, separating the water from the hydrogel to form a xerogel and using the xerogel comprising silica as the chromium oxide support. That is, the xerogel is combined with an anhydrous chromium containing compound and the resulting catalyst is activated.

Supported chromium oxide olefin polymerization catalysts can also be comprised of chromium oxide supported on aluminophosphate supports. Such catalysts are generally used in conjunction with a boron component, either as a part of the support or as a co-catalyst, e.g., a triethylborane co-catalyst. An aluminophosphate supported catalyst is described in United States Patent No. 4,364,842 to McDaniel et al. Various methods can be used to prepare the aluminophosphate base. For example, an aluminum salt can
30 be combined with a source of phosphate ions in an aqueous medium and neutralized with a neutralizing agent to give a hydrogel. Chromium can be co-precipitated or added to the hydrogel. After water is removed from the hydrogel, the resulting chromium-containing xerogel is activated by heating in air.

In accordance with the present invention, a supported chromium oxide catalyst of one of the types described above is treated whereby it is impregnated with a metal salt selected from formates, acetates,
40 nitrates, chlorides, chlorates and hydroxides of alkali metals, alkaline earth metals and mixtures thereof. After such metal salt impregnation, the catalyst is activated. While any of these alkali metal or alkaline earth metal salts or hydroxides and any mixture of such salts or hydroxides can be utilized, the alkali metal salts and hydroxides are preferred, with lithium and sodium formates, acetates and hydroxides being the most preferred. The term "salt(s)" is used hereinafter to mean both the salts and/or hydroxides.

A particularly suitable technique for impregnating the supported catalyst with the metal salt or salts utilized comprises mixing the catalyst with a solution of the salt or salts and then removing the solvent from the mixture. While the solvent can be aqueous or non-aqueous, a non-aqueous solvent is preferred in that the porosity of the support is protected from the high surface tension of water. Of the various non-aqueous solvents which can be utilized, alcohols are preferred with methanol being the most preferred.
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In a preferred preparation process of this invention, a silica-titania supported chromium oxide catalyst of one of the types described above is prepared and calcined at a temperature in the range of from 400 °C to 600 °C. The catalyst is then combined with a methanol solution of a lithium or sodium formate, acetate or hydroxide, or a mixture of such salts, and the resulting mixture is stirred at a temperature in the range of from 25 °C to 70 °C for a time period in the range of from 5 minutes to 60 minutes. The methanol solvent is
50 then removed from the mixture by evaporation followed by the calcination of the treated catalyst in air at a temperature in the range of from 500 °C to 700 °C.

The quantity of metal salt or salts utilized in the non-aqueous solution thereof is such that the catalyst is impregnated with the salt or salts in an amount of from 50 to 500 micromoles per gram of the catalyst,

preferably from 100 to 400 micromoles per gram and most preferably from 150 to 250 micromoles per gram. Generally, the quantity of metal salt or salts required for impregnating the catalyst needs to be increased in the non-aqueous solution only slightly above that to be impregnated in the catalyst or not at all since only a small percentage or none of the salt or salts is lost when the solvent is removed.

While various techniques can be utilized for activating the catalyst, the activation is preferably carried out by calcining the catalyst in an atmosphere containing oxygen, usually dry air. Typically, the activation of the catalyst comprises heating the metal salt impregnated catalyst in air at a temperature in the range of from 400°C to 900°C, preferably from 400°C to 700°C, for a time period of from 1 hour to 10 hours.

The activated metal salt impregnated catalyst can be subjected to at least partial reduction of the hexavalent chromium to a lower valent state by contacting the catalyst with a reducing agent. As will be described hereinbelow, such reduction is beneficial when a cocatalyst is combined with the impregnated catalyst.

The treated catalysts of the present invention, with or without cocatalysts, can be employed in various olefin polymerization processes wherein at least one olefin monomer having from 2 to 8 carbon atoms is contacted with a treated supported chromium oxide catalyst of the present invention under polymerization conditions. The reaction medium can be a dry inert hydrocarbon such as isobutane, n-heptane, methylcyclohexane or benzene at a reactor temperature within the range of from 60°C to 110°C and a reactor pressure of from about 1826 kPa to about 4240 kPa (250 psig to 600 psig). The polymer produced can be recovered, treated with carbon dioxide or water, for example, to deactivate residual catalysts, stabilized with an antioxidant such as butylated hydroxy toluene (BHT), and dried by conventional methods to obtain the final product. Hydrogen can be used in the reactor as known in the art to provide some control of the molecular weight of the polymer.

In a preferred polymerization process wherein a copolymer is produced, the metal salt impregnated catalyst is reduced by high temperature contact with a reducing agent, preferably carbon monoxide, then combined with a cocatalyst and used to polymerize comonomers, e.g., ethylene and hexene. The polymerization reaction is conducted in the presence of hydrogen to produce copolymers of low density and to bring about high comonomer incorporation efficiency. If a reducing agent other than carbon monoxide is used, higher amounts of comonomer are needed in the reaction zone to achieve similar amounts of comonomer incorporation into the resultant copolymer. Generally, the calcined catalyst is directly subjected to the reducing agent at a high temperature although intervening steps may be employed if desired.

When carbon monoxide is utilized, it can be employed at temperatures between 300°C to 500°C although it is preferably employed at temperatures in the range of 350°C to 450°C for best chromium reduction. The partial pressure of the reducing gas in the reduction operation can be varied from subatmospheric pressures to relatively high pressures, but the simplest reducing operation is to utilize essentially pure carbon monoxide at about atmospheric pressure.

The reduction time can vary from a few minutes to several hours or more. The extent of reduction can be followed by visual inspection of catalyst color. The color of the initial activated catalyst is generally orange, indicating the presence of hexavalent chromium. The color of reduced catalyst is blue, indicating that all or substantially all of the initial hexavalent chromium has been reduced to lower oxidation states, generally the divalent state.

The course of the reduction of the air-activated orange catalyst with carbon monoxide can be determined exactly by pulse titration. A known amount of carbon monoxide is added per pulse and the amount of evolved carbon dioxide is measured. When reduction is complete only carbon monoxide will be present and the catalyst will be blue in color. The reduced blue catalyst can be titrated with pulses of oxygen to convert the catalyst to the original orange color. When oxidation is complete, oxygen will be evident in the offgas.

After reduction, the reduced supported catalyst component is cooled to about room temperature, e.g., about 25°C, in an inert atmosphere such as argon or nitrogen to flush out the carbon monoxide. After this flushing treatment the catalyst is kept away from contact with either carbon monoxide or oxygen.

The cocatalyst utilized is preferably a trialkyl aluminum compound wherein the alkyl groups have from 1 to 10 carbon atoms, preferably 2 to 4 carbon atoms. Trialkyl aluminum compounds are preferred for use as cocatalysts because they are effective in improving polymer properties, such as, for example, suppressing polymer density during polymerization. The most preferred cocatalyst is triethyl aluminum.

The trialkyl aluminum cocatalyst is used in an amount within the range of 0.5 to 4 parts per million (ppm), or milligrams per kilogram (mg/kg), based on the amount of diluent in the reactor. Preferably, the cocatalyst is used in an amount within the range of 0.5 to 3 ppm, and most preferably, within the range of 1 to 2 ppm, for cost effectiveness and best polymer properties.

Relatively high levels of hydrogen are used in the polymerization process with the above described reduced catalyst and cocatalyst to achieve high comonomer incorporation efficiency. Preferably, the hydrogen is present in an amount in the range of from 1 mole % to 2 mole % based on the total moles of comonomers used.

In order to further illustrate the preparation and use of the preferred catalysts of the present invention, the following examples are given. The particular components and catalysts utilized in the examples are meant to be illustrative of the present invention and not limiting thereto.

Example 1

Test portions of catalyst of the type described in U.S. Patent No. 3,875,079 to Witt comprised of 2% chromium oxide supported on a silica-titania (2.5% Ti) support purified to reduce occluded alkali metal salt and calcined at 400°C - 500°C were impregnated with various quantities of sodium formate. The catalyst had a pore volume of about 2.5 cc/g and a surface area of about 550 M²/g. The impregnations were carried out by combining methanol solutions of sodium formate with the catalyst portions, stirring the resultant mixtures for about 30 minutes and then removing the methanol by evaporation. The salt impregnated catalyst test portions were reactivated by heating in air at a temperature of 650°C for 5 hours.

Each of the impregnated catalyst test portions were used in ethylene homopolymer polymerization reactions carried out in isobutane solutions at 109°C and 3895 kPa (550 psig). The polymer from each polymerization was recovered and tested for melt index in accordance with ASTM 1238-65T, condition E. The activity of the catalyst in each polymerization was also determined.

The results of these tests are given in Table I below.

TABLE I

	Catalyst ¹	Polymerization Conditions ³			Polymer Melt Index ⁴
	Quantity of Sodium ² , micromoles Na/g	Induction Period, Min.	Run Time, Min.	Activity, g/g - hr.	
10	0	30	72	3620	0.7
15	0	30	64	3950	0.6
	65	20	45	5690	1.4
	87	20	53	5110	2.0
20	109	20	65	4320	2.1
	217	20	54	4980	2.5
	326	45	130	1870	1.6
25	434	30	190	1240	1.4

¹ The catalyst was chromium oxide on a silica-titania support (1% Cr; 2.5% Ti) prepared in accordance with U.S. Patent No. 3,875,079 to Witt.

² Micromoles of sodium impregnated into catalyst prior to activation as sodium formate per gram of catalyst.

³ Polymerization carried out in isobutane at 109°C and 550 psig.

⁴ Determined in accordance with ASTM 1238-65T, condition E.

From Table I it can be seen that the activity and polymer melt index are appreciably increased when a catalyst of the present invention is utilized.

Example 2

The procedure described in Example 1 is repeated except that lithium formate was used for preparing the catalyst in lieu of sodium formate. The results of these tests are given in Table II below.

TABLE II

	Catalyst ¹ Quantity of Lithium ² , micromoles Li/g	Polymerization Conditions ³			Polymer Melt Index ⁴
		Induction Period, Min.	Run Time, Min.	Activity, g/g - hr.	
5					
10	0	30	64	3950	0.6
	65	20	45	5230	2.2
	86	15	52	5000	2.4
15	108	15	55	5080	2.3
	216	15	47	4810	3.5
20	324	15	60	4040	2.6

¹ The catalyst was chromium oxide on a silica-titania support (1% Cr; 2.5% Ti) prepared in accordance with U.S. Patent No. 3,875,079 to Witt.

² Micromoles of lithium impregnated into catalyst prior to activation as lithium formate per gram of catalyst.

³ Polymerization carried out in isobutane at 109°C and 550 psig.

⁴ Determined in accordance with ASTM 1238-65T, condition E.

From Table II it can be seen that the catalysts treated with lithium formate resulted in appreciable increases in activity and polymer melt index as compared to untreated catalyst.

Example 3

The procedure of Example 1 was repeated except that various alkali and alkaline earth metal salts were utilized. The results of these tests are given in Table III below.

TABLE III

Catalyst ¹		Polymerization Conditions ³			Polymer Melt Index ⁴
Salt Used	Quantity ² , micromoles/g	Induction Period, Min.	Run Time, Min.	Activity, g/g - hr.	
Li Acetate	216	20	50	4970	2.5
Li NO ₃	216	40	100	2600	2.5
Li OH	217	20	50	5240	3.0
Li OH	109	20	46	4970	3.0
Li OH	360	15	47	4990	3.0
Na ClO ₃	217	15	58	4570	3.2
KOH	109	50	90	3250	1.3
K Formate	217	30	120	2030	1.7
Ca Cl ₂	109	15	58	3730	1.1
Ca NO ₃	109	10	53	5030	0.8
Ca NO ₃	217	14	52	4740	0.7
Mg Acetate	109	20	60	3860	0.7
Mg Formate	217	15	62	4000	0.8
Mg Nitrate	109	11	49	5690	1.6

¹ The catalyst was chromium oxide on a silica-titania support (1% Cr; 2.5% Ti) prepared in accordance with U.S. Patent No. 3,875,079 to Witt.

² Micromoles of salt impregnated into catalyst prior to activation per gram of catalyst.

³ Polymerization carried out in isobutane at 109 °C and 3895 kPa (550 psig).

⁴ Determined in accordance with ASTM 1238-65T, condition E.

The data presented in Table III illustrates that various alkali metal and alkaline earth metal salts can be utilized in accordance with the present invention.

Example 4

The procedure of Example 1 was repeated except that ethylene-hexene copolymerization reactions were carried out. The results of these tests are given in Table IV below.

TABLE IV

Catalyst ¹ Quantity of Sodium ² micromoles Na/g	Copolymerization Conditions ³				Polymer Melt Index ⁴
	Induction Period, Min.	Run Time, Min.	Wt. % Hexene in Feed	Activity, g/g - hr.	
0	-	-	2.9	4710	0.21
26	15	43	3.2	6940	0.43
39	25	33	3.1	5240	0.58
52	10	40	3.0	5920	0.79
65	20	40	2.9	6300	0.90

¹ The catalyst was chromium oxide on a silica support prepared in accordance with U.S. Patent No. 3,875,079 to Witt.

² Micromoles of sodium impregnated into catalyst prior to activation as sodium formate per gram of catalyst.

³ Polymerization carried out in isobutane at 94°C and 3378 kPa (475 psig).

⁴ Determined in accordance with ASTM 1238-65T, condition E.

From Table IV it can be seen that the copolymer melt indexes are increased when catalysts of the present invention are utilized.

Example 5

Test portions of activated catalysts of the type described in U.S. Patent No. 4,364,842 to McDaniel et al. comprised of chromium oxide supported on an aluminophosphate support (the mole ratio of phosphate to alumino in the support = 0.4) were impregnated with various quantities of lithium formate and sodium formate. The impregnations were carried out by combining methanol solutions of the lithium and sodium formate salts with the catalyst portions, stirring the resultant mixtures for 30 minutes and then removing the methanol by evaporation. The salt impregnated catalyst test portions were reactivated by heating in air at a temperature of 600 °C for 3 hours.

Each of the impregnated catalyst test portions along with triethylborane co-catalyst were used in ethylene homopolymer polymerization reactions carried out in isobutane solutions at 95 °C and 3895 kPa (550 psig). The polymer from each polymerization was recovered and tested for high load melt index in accordance with ASTM 1238-65T, condition F. The activity of the catalyst in each polymerization was also determined. The results of these tests are given in Table V below.

TABLE V

Salt Used to Impregnate Catalyst	Catalyst ¹		Cocatalyst ³ Quantity, ppm.	Polymerization Conditions ⁴		Polymer High Load Melt Index ⁵
	Quantity of Salt ² micromoles/g	Quantity of Catalyst Used in Polymerization, g		Run Time, min.	Activity, g/g - hr.	
-	0	0.0474	8	30	4325	4.3
Li Formate	53	0.0745	8	30	6550	8.2
Li Formate	53	0.0533	8	30	4600	5.6
Li Formate	108	0.0523	8	30	5180	8.3
Li Formate	217	0.0363	8	30	2700	19.7
Na Formate	217	0.0379	8	30	4540	17.6

¹ The catalyst was chromium oxide supported on aluminum phosphate (P/Al = 0.4)

² Micromoles of metal salt impregnated into catalyst prior to activation.

³ Cocatalyst was triethylborane

⁴ Polymerization carried out in isobutane at 95°C and 3895 kPa (550 psig).

⁵ Determined in accordance with ASTM 1238-G5T, condition F.

From Table V it can be seen that the catalysts of the present invention bring about significant increases in polymer high load melt indexes.

Example 6

Ethylene-hexene copolymers were prepared in a continuous particle form process by contacting the catalyst with the monomers in a liquid full loop reactor having a volume of 23 gallons (87 liters). Isobutane was used as the diluent, and occasionally, hydrogen was introduced into the reactor. The reactor temperature was set at 82 °C and the pressure was 4 Mpa (580 psig). At steady state conditions, the isobutane feed rate was 46 l/hr, the ethylene feed rate was about 13.6 kg/h (30 lbs/hr), and the hexene feed rate was varied to control the density of the product polymer. Polymer was removed from the reactor at the rate of 11.3 kg/h (25 lbs/hr).

The tests were conducted according to the following procedures:

Density (g/ml): ASTM D 1505-68 and ASTM D 1928, Condition C. Determined on a compression molded sample, cooled at about 15 degrees C per minute, and conditioned at room temperature for about 40 minutes.

Melt Index (MI): ASTM 1238-65T, Condition E.

High Load Melt Index (HLMI): ASTM 1238-65T, Condition F.

Three catalysts were prepared from a silica-titania supported chromium catalyst which contained 5 weight % titanium and 1 weight % chromium. The basic catalyst had a pore volume of about 2.5 cc/g and a surface area of about 500 square meters per gram. The catalysts are described hereinbelow. Catalyst A was used as a control catalyst.

Catalyst A: Activated in dry air for 6 hours; cooled to 370 °C in nitrogen; treated with 10% carbon monoxide/90% nitrogen at 370 °C for 2 hours; cooled in nitrogen flush to 150 °C over 6 hours to remove CO.

Catalyst B: 600 g of catalyst was mixed with a methanol solution of sodium formate, then dried in a vacuum oven overnight at 80 °C, leaving 200 micromoles of sodium per gram of catalyst. It was then activated in dry air at 650 °C for six hours.

Catalyst C: After activation, Catalyst B was reduced by exposure to 10% carbon monoxide/90% nitrogen at 370 °C for 2 hours. It was then flushed with nitrogen down to 150 °C over 6 hours to remove excess carbon monoxide.

The above catalysts were utilized in the continuous loop reactor described above to prepare the ethylene-hexene copolymers. The copolymers were then tested to determine density, MI, HLMI and other properties as shown in Table VI below.

TABLE VI

Run No.	Catalyst	Reduced With CO	H ₂ , mole %	TEA, ppm.	TEB, ppm.	C ₆ H ₁₂ , wt. %	MI	HIMI	HIMI/MI	Density	Productivity, g Product/g Catalyst	Description
2	C	Yes	1.0	2.5	0	16.8	.04	9.1	202	.9312	2630	Invention
3	C	Yes	1.8	2.5	0	17.5	.09	13.4	151	.9235	2941	Invention
4	C	Yes	1.8	0	1.0	16.8	.19	27.5	145	.9325	2941	Invention
5	C	Yes	1.0	0	1.0	18.8	.19	27.9	149	.9327	2703	Invention
6	A	Yes	1.0	0	1.0	14.5	.09	10.8	119	.9323	2128	Control
7	A	Yes	1.0	0	1.0	14.7	.11	11.9	110	.9257	2083	Control
8	B	No	1.0	0	1.0	16.7	.13	20.9	166	.9379	3125	Invention
9	B	No	1.0	0	1.0	20.8	.22	30.4	139	.9329	2857	Invention
10	B	No	1.0	0	1.0	23.3	.26	36.0	138	.9312	2439	Invention
11	B	No	1.8	0	1.0	23.9	.40	50.0	124	.9234	2632	Invention
12	B	No	2.0	0	0	20.2	.24	25.2	103	.9239	1980	Invention
13	B	No	1.0	1.7	0	17.1	.12	15.5	129	.9290	2778	Invention
14	B	No	1.0	2.0	0	17.3	.04	8.5	213	.9324	3571	Invention

A comparison of runs 5, 8, 9 and 10 to control runs 6 and 7, which were made under similar conditions (1% hydrogen, 1 ppm triethylboron, TEB), shows that the sodium-treated catalysts have higher MI potential and better activity than the control catalysts. The invention catalysts yield a broader molecular weight distribution as indicated by the higher HIMI/MI ratios.

The CO reduction treatment usually improves the incorporation efficiency of Cr/silica catalysts. That is, less hexene is needed to suppress the density of the resin product. This can be seen by comparing runs 5 vs. 8-10 and 2 vs. 14, made under the same reactor conditions.

In the presence of triethylboron (TEB), CO-reduced catalysts usually display decreased resin density. Triethyl-aluminum (TEA) usually has little or no effect. However, it is seen in Table VI that the sodium-treated catalysts behave altogether differently. By comparing run 12 (no cocatalyst) with run 11 (TEB added) it can be seen that in the presence of TEB, it actually takes more hexene to suppress the density to a similar level. Comparing run 3 (TEA) to run 4 (TEB), both made at 1.8 mole % hydrogen, or run 2 (TEA) to run 5 (TEB), both made at 1 mole % hydrogen, we see that TEA is more effective than TEB at density suppression for the invention catalysts.

The most surprising benefit seen in the pilot plant experiments is the sensitivity of the invention catalysts to hydrogen. The main influence of hydrogen on the sodium-treated catalysts is not on the melt index, as is usually found, but on the resin density and hexene incorporation efficiency. In the presence of TEA the density drops from .9312 to a low .9235 as the hydrogen was raised from 1% to 1.8% in runs 2 and 3. In runs 4 and 5, the same experiment was run except that the cocatalyst was TEB rather than TEA. Here there was no change in density as hydrogen was raised. In fact it took slightly more hexene to make the same density. Comparing runs 2 to 14 shows that the CO reduction step also contributes slightly to the sensitivity. Thus, the combination of TEA, hydrogen, and the invention catalyst, preferably CO reduced, results in special benefits. Run 3 can be considered the optimum, combining the catalyst of the invention, CO reduction, TEA cocatalyst, and high levels of hydrogen in the reactor. Little hexene is needed compared to other runs to make the low .9235 density resin. Also the productivity is about 50% better than the untreated catalyst.

Another series of runs were made with catalyst C as shown in Table VII.

TABLE VII

Run No.	H ₂ , Mole %	TEA, ppm.	HLMI	Density	Wt. % C ₆ H ₁₂
15	0	0	3	.940	14
16	0	2	3.5	.933	15
17	1.0	2	11	.931	18
18	1.5	2	13	.924	17
19	2.0	2	14	.923	17
20	2.0	TEB 1	30	.933	17

The presence of TEA greatly lowers the density compared to no co-catalyst (run 15 vs. 16) or to TEB (run 19 vs. 20).

In the presence of TEA (runs 16-19) the density drops precipitously as hydrogen is added to the reactor. Thus, run 19 can be considered as the optimum, including sodium salt treatment, CO reduction, TEA cocatalyst, and high levels of hydrogen in the reactor. Little hexene is needed in the reactor to suppress the density to the low value of 0.9235.

Claims

1. A process for preparing an activated polymerization catalyst comprised of a supported chromium oxide catalyst, the support containing one or more of silica, titania, thoria, alumina, zirconia and aluminophosphates, characterized by impregnating said supported chromium oxide catalyst with a metal salt selected from formates, acetates, hydroxides, nitrates, chlorates and chlorides of an alkali metal, an



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The most surprising benefit seen in the pilot plant experiments is the sensitivity of the invention catalysts to hydrogen. The main influence of hydrogen on the sodium-treated catalysts is not on the melt index, as is usually found, but on the resin density and hexene incorporation efficiency. In the presence of TEA the density drops from .9312 to a low .9235 as the hydrogen was raised from 1% to 1.8% in runs 2 and 3. In runs 4 and 5, the same experiment was run except that the cocatalyst was TEB rather than TEA. Here there was no change in density as hydrogen was raised. In fact it took slightly more hexene to make the same density. Comparing runs 2 to 14 shows that the CO reduction step also contributes slightly to the sensitivity. Thus, the combination of TEA, hydrogen, and the invention catalyst, preferably CO reduced, results in special benefits. Run 3 can be considered the optimum, combining the catalyst of the invention, CO reduction, TEA cocatalyst, and high levels of hydrogen in the reactor. Little hexene is needed compared to other runs to make the low .9235 density resin. Also the productivity is about 50% better than the untreated catalyst.

Another series of runs were made with catalyst C as shown in Table VII.

TABLE VII

Run No.	H ₂ , Mole %	TEA, ppm.	HLMI	Density	Wt. % C ₆ H ₁₂
15	0	0	3	.940	14
16	0	2	3.5	.933	15
17	1.0	2	11	.931	18
18	1.5	2	13	.924	17
19	2.0	2	14	.923	17
TEB					
20	2.0	1	30	.933	17

The presence of TEA greatly lowers the density compared to no co-catalyst (run 15 vs. 16) or to TEB (run 19 vs. 20).

In the presence of TEA (runs 16-19) the density drops precipitously as hydrogen is added to the reactor. Thus, run 19 can be considered as the optimum, including sodium salt treatment, CO reduction, TEA cocatalyst, and high levels of hydrogen in the reactor. Little hexene is needed in the reactor to suppress the density to the low value of 0.9235.

Claims

1. A process for preparing an activated polymerization catalyst comprised of a supported chromium oxide catalyst, the support containing one or more of silica, titania, thoria, alumina, zirconia and aluminophosphates, characterized by impregnating said supported chromium oxide catalyst with a metal salt selected from formates, acetates, hydroxides, nitrates, chlorates and chlorides of an alkali metal, an



alkaline earth metal and mixtures thereof, and activating said salt-impregnated catalyst.

2. The process of claim 1 wherein said impregnation step comprises mixing said supported chromium oxide catalyst with a non-aqueous solution of said metal salt and then removing the non-aqueous solvent from said mixture.
3. The process of claim 2 wherein said supported chromium oxide catalyst is calcinated at a temperature in the range of 400 to 600 °C prior to being impregnated with said salt.
4. The process of claim 3 wherein said supported chromium oxide catalyst is comprised of chromium oxide and a predominately silica support.
5. The process of claim 3 or 4 wherein said supported chromium oxide catalyst is combined with an alcohol solution, preferably a methanol solution, of said salt and said alcohol is removed therefrom by evaporation.
6. The process of any of the preceding claims wherein said salt is an alkali metal salt.
7. The process of claim 6 wherein said salt is a lithium or sodium salt, preferably a formate, acetate or hydroxide.
8. The process of claim 7 wherein said non-aqueous solution contains said metal salt in an amount to provide from 50 to 500 micromoles of said salt per gram of catalyst.
9. The process of any of the preceding claims wherein activating said salt-impregnated catalyst comprises heating the catalyst in air at a temperature in the range of 400 to 900 °C for a time period of 1 to 10 hours.
10. The process of claim 9 wherein the activated catalyst is contacted with a reducing agent to at least partially reduce the chromium in said catalyst to a lower valance state.
11. The process of claim 10 wherein said reducing agent is carbon monoxide and said contact is carried out at a temperature in the range of 300 to 500 °C.
12. The use of the activated polymerization catalyst as obtained in any of the preceding claims for polymerizing olefins.
13. The use of claim 12 wherein said polymerization catalyst is used in combination with a cocatalyst.
14. The use of claim 13 wherein said cocatalyst is a trialkyl aluminum compound, the alkyl groups having from 1 to 10 carbon atoms, preferably wherein said cocatalyst is triethyl aluminum.
15. The use of any of claims 12 to 14 wherein said polymerization is carried out in the presence of hydrogen, preferably wherein said hydrogen is present in the range of 1 to 2 mole % based on the total moles of olefin monomer reacted.

Patentansprüche

1. Verfahren zur Herstellung eines aktivierten Polymerisationskatalysators, umfassend einen trägerunterstützten Chromoxid-Katalysator, wobei der Träger eines oder mehrere von Siliciumdioxid, Titandioxid, Thorium(IV)-oxid, Aluminiumoxid, Zirkoniumoxid und Aluminophosphaten enthält, **dadurch gekennzeichnet**, daß der trägerunterstützte Chromoxid-Katalysator mit einem aus Formiaten, Acetaten, Hydroxiden, Nitraten, Chloraten und Chloriden eines Alkalimetalls, eines Erdalkalimetalls und Mischungen davon gewählten Metallsalz imprägniert wird und der mit Salz imprägnierte Katalysator aktiviert wird.
2. Verfahren gemäß Anspruch 1, worin die Imprägnierungsstufe das Mischen des trägerunterstützten Chromoxid-Katalysators mit einer nichtwäßrigen Lösung des Metallsalzes und die anschließende Entfernung des nichtwäßrigen Lösungsmittels aus der Mischung umfaßt.



3. Verfahren gemäß Anspruch 2, worin der trägerunterstützte Chromoxid-Katalysator bei einer Temperatur im Bereich von 400 bis 600 °C calciniert wird, bevor er mit dem Salz imprägniert wird.
4. Verfahren gemäß Anspruch 3, worin der trägerunterstützte Chromoxid-Katalysator aus Chromoxid und einem hauptsächlich aus Siliciumdioxid bestehenden Träger besteht.
5. Verfahren gemäß Anspruch 3 oder 4, worin der trägerunterstützte Chromoxid-Katalysator mit einer Alkohollösung, vorzugsweise einer Methanollösung, des Salzes zusammengebracht wird und der Alkohol daraus durch Verdampfung entfernt wird.
6. Verfahren gemäß mindestens einem der vorhergehenden Ansprüche, worin das Salz ein Alkalimetallsalz ist.
7. Verfahren gemäß Anspruch 6, worin das Salz ein Lithium- oder Natriumsalz, vorzugsweise ein Formiat, Acetat oder Hydroxid, ist.
8. Verfahren gemäß Anspruch 7, worin die nichtwässrige Lösung das Metallsalz in einer Menge enthält, um 50 bis 500 µMol des Salzes pro Gramm Katalysator bereitzustellen.
9. Verfahren gemäß mindestens einem der vorhergehenden Ansprüche, worin die Aktivierung des mit Salz imprägnierten Katalysators das Erhitzen des Katalysators in Luft bei einer Temperatur im Bereich von 400 bis 900 °C während einer Zeitdauer von 1 bis 10 Stunden umfaßt.
10. Verfahren gemäß Anspruch 9, worin der aktivierte Katalysator mit einem Reduktionsmittel kontaktiert wird, um das Chrom in dem Katalysator zumindest teilweise zu einer geringeren Wertigkeitsstufe zu reduzieren.
11. Verfahren gemäß Anspruch 10, worin das Reduktionsmittel Kohlenmonoxid ist und der Kontakt bei einer Temperatur im Bereich von 300 bis 500 °C erfolgt.
12. Verwendung des aktivierten Polymerisationskatalysators, wie er nach mindestens einem der vorhergehenden Ansprüche erhalten wird, zur Polymerisation von Olefinen.
13. Verwendung gemäß Anspruch 12, worin der Polymerisationskatalysator in Kombination mit einem Cokatalysator eingesetzt wird.
14. Verwendung gemäß Anspruch 13, worin der Cokatalysator eine Trialkylaluminiumverbindung ist, wobei die Alkylgruppen 1 bis 10 Kohlenstoffatome besitzen, worin der Cokatalysator vorzugsweise Triethylaluminium ist.
15. Verwendung gemäß mindestens einem der Ansprüche 12 bis 14, worin die Polymerisation in Gegenwart von Wasserstoff durchgeführt wird, worin der Wasserstoff vorzugsweise im Bereich von 1 bis 2 Mol-%, bezogen auf die Gesamtmolanzahl der umgesetzten Olefinmonomere, vorliegt.

45 Revendications

1. Un procédé pour préparer un catalyseur de polymérisation activé constitué d'un catalyseur d'oxyde de chrome fixé sur un support, le support renfermant un ou plusieurs des composés de silice, oxyde de titane, oxyde de thorium, alumine, oxyde de zirconium et aluminophosphates, caractérisé par l'imprégnation dudit catalyseur d'oxyde de chrome fixé sur un support avec un sel de métal choisi parmi les formiates, les acétates, les hydroxydes, les nitrates, les chlorates et les chlorures d'un métal alcalin, d'un métal alcalinoterreux et leurs mélanges et l'activation dudit catalyseur imprégné de sel.
2. Le procédé selon la revendication 1, dans lequel ladite étape d'imprégnation comprend le mélange dudit catalyseur d'oxyde de chrome fixé sur un support avec une solution non aqueuse dudit sel de métal et ensuite l'élimination du solvant non aqueux dudit mélange.



3. Le procédé selon la revendication 2, dans lequel ledit catalyseur d'oxyde de chrome fixé sur un support est calciné à une température comprise dans la gamme de 400 à 600 °C avant d'être imprégné avec ledit sel.
- 5 4. Le procédé selon la revendication 3, dans lequel ledit catalyseur d'oxyde de chrome fixé sur un support est constitué d'oxyde de chrome et, de façon prédominante, d'un support de silice.
5. Le procédé selon la revendication 3 ou 4, dans lequel ledit catalyseur d'oxyde de chrome fixé sur un support est combiné avec une solution d'alcool, de préférence une solution de méthanol dudit sel et
10 ledit alcool en est retiré par évaporation.
6. Le procédé selon l'une quelconque des revendications précédentes, dans lequel ledit sel est un sel de métal alcalin.
- 15 7. Le procédé selon la revendication 6, dans lequel ledit sel est un sel de lithium ou un sel de sodium, de préférence un formiate, un acétate ou un hydroxyde.
8. Le procédé selon la revendication 7, dans lequel ladite solution non aqueuse renferme ledit sel de métal selon une quantité pour fournir de 50 à 500 micromoles dudit sel par gramme de catalyseur.
- 20 9. Le procédé selon l'une quelconque des revendications précédentes, dans lequel l'activation dudit catalyseur imprégné de sel comprend le chauffage du catalyseur dans l'air à une température comprise dans la gamme de 400 à 900 °C pendant une période de temps de 1 à 10 heures.
- 25 10. Le procédé selon la revendication 9, dans lequel le catalyseur activé est mis en contact avec un agent réducteur pour réduire au moins partiellement le chrome dans ledit catalyseur à un état de valence inférieur.
- 30 11. Le procédé selon la revendication 10, dans lequel ledit agent réducteur est du mono-oxyde de carbone et ledit contact est mis en oeuvre à une température comprise dans la gamme de 300 à 500 °C.
12. L'utilisation du catalyseur de polymérisation activé obtenu selon l'une quelconque des revendications précédentes pour la polymérisation d'oléfines.
- 35 13. L'utilisation selon la revendications 12, dans laquelle ledit catalyseur de polymérisation est utilisé en combinaison avec un co-catalyseur.
14. L'utilisation selon la revendication 13, dans laquelle ledit co-catalyseur est un composé de trialkyl-aluminium, les groupes alkyles ayant de 1 à 10 atomes de carbone, de préférence, dans laquelle ledit
40 co-catalyseur est du triéthyl-aluminium.
15. L'utilisation selon l'une quelconque des revendications 12 à 14, dans laquelle ladite polymérisation est mise en oeuvre en présence d'hydrogène, de préférence, dans laquelle ledit hydrogène est présent dans la gamme de 1 à 2 moles % calculé sur les moles totales du monomère d'oléfine ayant réagi.
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