

WET GAS COMPRESSION

CROSS REFERENCE TO RELATED APPLICATIONS

[0001] This application claims the priority benefit of United States Patent Application
5 62/138,753 filed March 26, 2015 entitled WET GAS COMPRESSION, the entirety of which
is incorporated by reference herein.

BACKGROUND

[0002] This section is intended to introduce various aspects of the art, which may be
associated with exemplary embodiments of the present invention. This discussion is believed
10 to assist in providing a framework to facilitate a better understanding of particular aspects of
the present invention. Accordingly, it should be understood that this section should be read in
this light, and not necessarily as admissions of prior art.

[0003] Traditionally, it is understood that centrifugal compressors or gas expanders do not
handle liquid slugs and thus it is assumed that they can only handle a fraction of one percent
15 liquid by volume. Thus in many applications expensive liquid separators, dehydration
processes and/or unit scrubbers are utilized to try and remove or separate the liquids prior to
using centrifugal compressors or expanders. These devices are often designed for specific
operating conditions and are then limited in the range of Gas Volume Fraction (GVF) that can
be handled with a given process flow rate. Even with this expensive and complex processing
20 equipment, if there is a sudden high level of liquids they can quickly saturate, fill and overflow
the liquid separators once their capacity for liquid is exceeded resulting in slugging the
compressor or expander equipment.

[0004] In general, multiphase pumps can be used if it is known that the fluid will generally
be below 90% GVF. Centrifugal compressors are often restricted to applications with GVFs
25 of 99.7 or higher and even this can cause problems within the machine for stability and
affecting the reliability of the seals and bearings. Therefore, for processes outside this small
range, the current practice is to separate the fluids prior to utilizing a centrifugal compressor
even with the design limitation with the associated process and equipment. The same is true
for gas expanders, which are functionally a centrifugal compressor running in reverse to extract
30 energy in one form or another through a process pressure drop across the expander. The
separators, scrubbers and dehydration units are not only expensive and limited in liquid
capacity and volume flow range but they also tend to be very bulky, taking up expensive real

estate in locations such as offshore platforms, subsea processing or onshore facilities. This coupled with complex control systems and additional auxiliary equipment like pumps, regulators, level controllers, transmitters and filters adds to the complexity and likelihood of failure of these systems. An example of a typical oil or gas well stream service process may
5 use a separator to separate liquids from the gas in order to prevent or mitigate damage caused by slugs. A centrifugal compressor and pump may subsequently be used to boost the gas and liquid separately, with downstream recombination of the gas and liquid in order to transport both through a pipeline to a processing facility.

[0005] Problems with compressing liquids include reduced machine stability, erosion of
10 impellers and diffusers, and fouling and resulting in imbalance if the liquids flash or vaporize while being compressed in the machine.

[0006] The foregoing discussion of need in the art is intended to be representative rather than exhaustive. Technology that would improve the ability of compressors or expanders to handle the multiphase flow of fluid with a higher liquid content compared to the current state
15 of the art would be of great value.

SUMMARY OF THE INVENTION

[0007] The disclosure includes a centrifugal compressor, comprising an inlet configured to receive a gas stream, an outlet, and a liquid injection port configured to introduce a liquid into the gas stream and create a multiphase fluid, wherein the centrifugal compressor is configured
20 to compress the multiphase fluid.

[0008] The disclosure includes a method of operating a centrifugal compressor, comprising passing a gas stream to a centrifugal compressor inlet, introducing a quantity of liquid into the gas stream to create a multiphase stream, and compressing the multiphase stream.

DESCRIPTION OF THE DRAWINGS

25 [0009] So that the manner in which the present invention can be better understood, certain illustrations, charts and/or flow charts are appended hereto. It is to be noted, however, that the drawings illustrate only selected embodiments of the inventions and are therefore not to be considered limiting of scope, for the inventions may admit to other equally effective embodiments and applications.

30 [0010] FIG. 1 is an illustrative compressor performance map showing a traditional sequence of operating points moving into a region of higher pressure ratio / head.

[0011] FIG. 2 is a compressor performance map plotting compressor operation for one percent (1%) Nominal Liquid Volume Fraction (LVF) at various flow and pressure ratio conditions.

5 [0012] FIG. 3 is another compressor performance map plotting compressor operation for increasing LVFs at a given speed which show how the pressure ratio varies with the quantity of liquid.

[0013] FIG. 4 is a schematic diagram of one embodiment of a multiphase fluid handling system according to the disclosure for compressing a multiphase fluid.

10 [0014] FIG. 5 is a schematic diagram of another embodiment of a multiphase fluid handling system according to the disclosure for compressing a multiphase fluid.

[0015] FIG. 6 is a schematic diagram of still another embodiment of a multiphase fluid handling system according to the disclosure for compressing a multiphase fluid.

15 [0016] It should be noted that the figures are merely exemplary of several embodiments of the present invention and no limitations on the scope of the present invention are intended thereby. Further, the figures are generally not drawn to scale, but are drafted for purposes of convenience and clarity in illustrating various aspects of the invention.

DETAILED DESCRIPTION

20 [0017] Reference will now be made to exemplary embodiments and specific language will be used to describe the same. It will nevertheless be understood that no limitation of the scope of the invention is thereby intended. Alterations of further modifications of the inventive features described herein, and additional applications of the principles of the invention as described herein, which would occur to one skilled in the relevant art and having possession of this disclosure, are to be considered within the scope of the invention. Further, before particular embodiments of the present invention are disclosed and described, it is to be understood that
25 this invention is not limited to the particular process and materials disclosed herein as such may vary to some degree. It is also to be understood that the terminology used herein is used for the purpose of describing particular embodiments only and is not intended to be limiting, as the scope of the present invention will be defined only by the appended claims and equivalents thereof.

30 [0018] Testing has shown that erosion can be reduced or prevented by slowing down the liquid velocity at impact points and by reducing the droplet size. Fouling has also been reduced

or even removed by increasing the liquid levels above the flash point in effect washing the internals of the machine. Disclosed techniques include using the thermodynamic and aerodynamic effects of liquid injection as a control method for a centrifugal compressor system. Whereas current technology focuses on conditioning, restricting, and/or minimizing the amount of liquid, the disclosed techniques include intentionally adding liquid and/or changing the liquid fraction to obtain a change in the operating condition(s) of the compressor system. Suitable liquids and/or injectants include one of or a combination of water, produced water, liquid hydrocarbons, corrosion inhibitor (e.g., water soluble or oil soluble chemicals (often amine based) used to inhibit aqueous corrosion), process liquid(s), diluents (e.g., xylene, etc.), liquid chemicals (e.g., glycols, amines, etc.), drilling fluids, fracking fluids, etc. The liquids and/or injectants may be byproducts of an existing process in a facility or a liquid from an external source. Suitable compressor systems include those found in surface facilities, subsea applications, pipeline applications, gas gathering, refrigeration, etc., as well as future possible configurations of centrifugal compressor systems such as in-pipe compressors and/or down-hole compressors.

[0019] As described above, adding liquid may increase the pressure ratio of a centrifugal compressor. In other words, the non-compressibility of the liquid may be utilized to increase pressure producing capability of the compressor. For example, as reservoirs deplete and enhanced oil recovery (EOR) with water is undertaken, a higher compression ratio with lower volumes of gas and additional liquid may be required. Using the liquid may replace a problem with a benefit that may eliminate the need to re-wheel, re-stage, and/or re-bundle a compressor.

[0020] FIG. 1 is an illustrative compressor performance map plotting pressure ratio (PR) (the pressure at the compressor exducer versus the pressure at the compressor inducer) or head on the Y-axis against flow (e.g., in actual cubic feet per minute (ACFM)) on the X-axis. In Fig. 1, points 1 and 2 depict exemplary operating points of a conventional centrifugal compressor for a given speed range over a range of flows.

[0021] Surge line 4 separates a region of unstable flow above the surge line 4 from a region of stable flow below the surge line 4. If a compressor operates above and/or on the left side of the surge line 4, the compressor may surge or pulsate backflow of gas through the device. In general, the surge line 4 may signify the minimum flow rate limit for a given compressor.

[0022] Injecting liquid at operating point 2 allows the compressor to increase the PR and/or produce more head than the original design, depicted by the operating condition moving

vertically along the performance map to point 3. As described above, the ability to increase the PR may be advantageously exploited in a variety of contexts, e.g., EOR operations, to accommodate lower wellhead pressure, to compensate for changing gas composition, to counter increased resistance in an associated discharge system, etc. In some embodiments, liquid ingestion increases the pressure ratio above pre-established surge limits but does not cause the surge phenomenon to occur. Additionally, injecting liquid may extend the surge range of a given compressor, thereby permitting compressors to operate in low flow regions without exhibiting excessive pressure reversals or oscillating axial shaft movement. This technique may be more efficient than opening a recycle line (current technology) or venting gas at an inlet of the compressor. Further, injecting liquid may mitigate possible slugging and liquid carry-over damage to brownfield compressors. For example, a static mixer at a compressor inlet nozzle may atomize a liquid into droplets to reduce possible slugging on the compressor when existing (brownfield) suction scrubbers have liquid carry-over (e.g., due to instrument failure, system upsets, operator error, change in scrubber/separator performance as inlet pressures decrease, gas compositions change which may increase liquid loading, etc.). As used herein, the term “atomize” means to divide, reduce, or otherwise convert a liquid into minute particles, a mist, or a fine spray of droplets having an average droplet size within a predetermined range. In some embodiments, a flow mixer in the suction line may provide an order of magnitude reduction in droplet size, effectively atomizing the liquid. Atomized liquid may represent a lower risk to rotating parts than large droplets or slugs of liquid, thereby substantially reducing the business risk of liquid carry-over events (e.g., damaged compression components). However, it is contemplated that these benefits may be outweighed and non-atomized liquid may be suitable in other contexts.

[0023] FIG. 2 is a compressor performance map 200 plotting compressor operation for an injection of one percent (1%) Nominal Liquid Volume Fraction (LVF) for an embodiment of the disclosed technique. The Y-axis is the PR and the X-axis is the air flow in ACFM. Initially, a compressor was measured at three different operating conditions using a compressor speed of 8,000 revolutions per minute (RPM) and 9,000 RPM on dry gas. Move 1 shows the data associated with adding an injectant, e.g., water, to obtain a 1% LVF input stream. Move 2 shows the adjustment to flow made to obtain substantially the same PR for the compressor at the given speed and with a 1% LVF input stream. As depicted, increasing the LVF (Move 1) increased the PR for a given flow at a given compressor speed at lower flow rates and had a negligible or lessening effect at higher flow rates. In other words, injecting liquid translated

the operating curve in a clockwise orientation about a known point. In Move 2, the air flow was increased while the liquid flow rate was held constant to reduce the PR back to substantially the same as the dry value. As depicted, Move 2 translated the curve to the right along the X-axis, compressed the curve, and further translated the curve clockwise about a known point.

[0024] FIG. 3 is a compressor performance map 300 plotting compressor operation for an injection of various LVFs, i.e., 1% LVF, 2.8% LVF, and 3.8% LVF, at a given speed (8,000 RPM). The Y-axis is the PR and the X-axis is the air flow in ACFM. As depicted, for a given compressor operating speed, e.g., 8,000 RPM, increasing the LVF tends to raise the PR at lower flows and has a negligible or lessening effect on the PR at higher flow rates. In other words, raising the LVF by injecting liquid translates the operating curves in a clockwise orientation about a known point.

[0025] FIG. 4 is a schematic diagram of a compression system 400. Fluid, for example fluid from a well head or separator, is directed to the apparatus by a conduit 450, check valve 451, and conduit 452. The mixture of liquid and gas enters a fluid treatment device 455. The fluid treatment device 455 may be a slug suppressor or a known atomizing device, such as one or more atomizing nozzles or flow mixers, to include a static flow mixer, a dynamic flow mixer, or a combination thereof. The fluid treatment device 455 may also be a combination of these elements. Suitable atomizers may generate droplets having an average droplet size on the order of about 1,000 μm to about 1,500 μm , about 1,000 μm to about 2,000 μm , about 2,000 μm to about 3,000 μm , or larger, while other suitable atomizers, e.g., gas-assisted atomizers, may generate droplets having an average droplet size at least an order of magnitude less than the large droplets (e.g., from about 50 μm to about 100 μm , about 100 μm to about 200 μm , about 50 μm to about 200 μm etc.). The mixture leaving the fluid treatment device 455 flows through conduit 456 to compressor 458 driven by a driver 457, e.g., a motor, a turbine, a variable frequency drive (VFD), etc. In some embodiments, a multi-phase flow meter (MPFM) device (not pictured) is disposed in the conduit 456 to accomplish liquid injection. In some embodiments, this MPFM is disposed close to the compressor suction nozzle to minimize the likelihood of atomized droplets coalescing in the inlet nozzle and/or compressor volute. Such embodiments may utilize the MPFM output to control the ratio of the various streams to obtain the required amount of liquid to obtain the desired operating characteristic, e.g., power, temperature, pressure, erosion characteristics, etc. Additionally, for embodiments having a

plurality of inlet sources, the MPFM may be configured to receive a plurality of inlet sources or a plurality of MPFMs may be individually employed for each of the inlet sources. Compressed fluid leaves compressor **458** through conduit **460** and **461** to check valve **462** and to a distribution conduit **463** which delivers the compressed fluid to a desired location. A
5 recycle line for the mixture from compressor **458** is provided at **466** that includes a recycle valve **467**, and check valve **469**. In some embodiments, the distribution conduit **463** may include additional branches, after coolers, moisture separators or other devices for separating/treating the liquid from the gas and passing a single phase stream downstream out of the compression system **400**. Those of skill in the art will appreciate that the compressor
10 **458** may be any suitable centrifugal compressor, e.g., a multi-stage centrifugal compressor, within the scope of this disclosure.

[0026] FIG. 5 is a schematic diagram of an exemplary compression system **500** in accordance with this disclosure. The components of FIG. 5 are substantially the same as the corresponding components of FIG. 4 except as otherwise noted. The compression system **500**
15 includes an optional suction scrubber **502**. In the compression system **500**, the fluid treatment device **455** is a flow mixer and/or atomizer, e.g., an atomizer comprising one or more atomizing nozzles or a flow mixer device comprising two or more counter swirling vanes or counter rotating vortices. The compression system **500** depicts a feedback loop **504** having a controller **506**. The controller **506** may monitor discharge pressure and control the injectant fed back to
20 the compression system **500** via the feedback loop **504**. The feedback loop **504** is depicted in dashed lines to illustrate the optional configurations alternately or cumulatively available in some combinations and permutations contemplated herein. For example, if injection location **508** is selected, injectant may be metered and/or injected internally to the compressor **458** at any one or more of the illustrated locations, e.g., the compressor inlet and/or a compressor
25 interstage passage. Alternately or additionally, if injection location **510** is selected, injectant may be metered and/or injected upstream of the fluid treatment device **455**. The injection location **508** and injection location **510** may have the same or different liquid supply, and in various embodiments may each have one or more different liquid supplies. The injection location **508** and the injection location **510** may utilize one or a plurality of liquid injection
30 ports to pass liquid to the compression system **500**. In some embodiments, one or more liquid injection ports may be disposed upstream of a fluid treatment device **455**. In some embodiments, one or more liquid injection ports may be disposed on the compressor **458**, e.g., at the compressor inlet and/or a compressor interstage passage. In embodiments having a

plurality of liquid injection ports, each port may be separately controlled or controlled as part of a bank of liquid injection ports with respect to the quantity of liquid passed therethrough. Alternatively or additionally, in embodiments having a plurality of liquid injection ports, one or more liquid injection ports may be configured to pass a different liquid than another liquid injection port.

[0027] FIG. 6 is a schematic diagram of another embodiment of a compression system 600 in accordance with this disclosure. The components of FIG. 6 are substantially the same as the corresponding components of FIG. 5 except as otherwise noted. The compression system 600 further comprises a process inlet 602 for admitting process fluid, e.g., a process gas, and a multiphase flow meter 606. Other embodiments may utilize multiple process inlets 602, e.g., to accommodate multiple process gases, but only one is shown in FIG. 6. Similarly, other embodiments may utilize multiple conduits 450 (and/or associated control and/or feedback loops) within the scope of this disclosure, e.g., to accommodate multiple kinds of liquids, but only one is shown in FIG. 6. The multiphase flow meter 606 may generate the set point to control the amount of wet gas entering the compressor 458 via the fluid treatment device 455. Those of skill in the art will appreciate that other embodiments may alternately or additionally control the amount of dry gas entering the compressor to similar effect. A feedback loop 604 is provided for aiding in the control of the amount of wet gas entering the compressor 458, e.g., using the control valve 605. A second feedback loop 504 is provided for substantially the same purpose as the feedback loop 504 of FIG. 5. The feedback loop 604 and the feedback loop 504 are depicted in dashed lines to illustrate other optional configurations alternately or cumulatively available in some combinations and permutations contemplated herein. As shown, the feedback loop 504 couples the conduit 461 to the multiphase flow meter 606 for wet gas recycling. Those of skill in the art will appreciate that alternate embodiments may include one or more additional feedback loops for speed control, discharge throttling, suction throttling, recycle control, inlet guide vane control, etc.

[0028] In operation, the PR for the compression systems 400, 500, and 600 may be controlled by introducing a liquid injectant into an input stream (e.g., passed via conduit 450) to create a multiphase input stream. The compression systems 400, 500, and 600 may compress the multiphase input stream with a centrifugal compressor (e.g., the compressor 458) to create a multiphase discharge stream (e.g., passed via conduit 461). The compression systems 400, 500, and 600 may measure (e.g., using the multiphase flow meter 606) a parameter of the streams (e.g., suction pressure, discharge pressure, suction flow, discharge flow, and/or

- 5 multiphase composition), wherein the discharge parameter corresponds to a PR for the centrifugal compressor. When the measured parameter exceeds a first predetermined point (e.g., when the measured PR drops below a minimum PR set point, when the compressor starts to surge, when the moisture composition of the measured stream passes an impeller erosion limit, etc.), a control system (e.g., the controller **506**) may increase or decrease the pressure ratio by increasing or decreasing (e.g., by manipulating the recycle valve **467**, the control valve **605**, etc.) the quantity of liquid introduced into the compression systems **400**, **500**, and **600**. Again, the liquid may be atomized for purposes of minimizing erosion, but for purposes of controlling the operating point it may be non-atomized.
- 10 **[0029]** While it will be apparent that the invention herein described is well calculated to achieve the benefits and advantages set forth above, it will be appreciated that the invention is susceptible to modification, variation and change without departing from the spirit thereof.

CLAIMS

1. A centrifugal compression system, comprising:
an inlet configured to receive a fluid stream from a well head or separator;
an outlet; and
a liquid injection port configured to introduce a liquid into the fluid stream and create a multiphase fluid;
a fluid treatment device, the fluid treatment device being a slug suppressor, an atomizing device, or a combination thereof;
a centrifugal compressor configured to compress the multiphase fluid;
a feedback loop including a controller to control the liquid introduced into the liquid injection port such that when a discharge parameter corresponding to a pressure ratio of the centrifugal compressor exceeds a first predetermined point, the controller increases the pressure ratio by increasing the quantity of liquid introduced into the compression system corresponding to an increase of the pressure ratio above and/or on a left side of a surge line without causing surge or pulsate backflow through the centrifugal compressor;
and
a recycle line to recycle a portion of the compressed multiphase fluid to the centrifugal compressor.
2. The centrifugal compression system of claim 1, wherein the centrifugal compressor is a multistage compressor.
3. The centrifugal compression system of claim 2, wherein the liquid injection port is also coupled to an interstage passage of the centrifugal compressor.
4. The centrifugal compression system of claim 3, further comprising a plurality of liquid injection ports, wherein at least one liquid injection port is also coupled to a separate interstage passage of the centrifugal compressor.
5. The centrifugal compression system of claim 3, further comprising a plurality of liquid injection ports, wherein at least one liquid injection port is configured to pass a different liquid than is passed by another liquid injection port.
6. The centrifugal compression system of claim 3, further comprising a plurality of liquid injection ports, wherein the quantity of liquid injected to each liquid injection port is individually controlled.
7. A method of operating a centrifugal compression system, comprising:
passing a fluid stream to an inlet of a centrifugal compressor inlet;
in a liquid injection port, injecting a quantity of liquid into the fluid stream to create a multiphase fluid;

passing the multiphase fluid through a fluid treatment device, wherein the fluid treatment device is a slug suppressor, an atomizing device, or a combination thereof;
compressing the multiphase stream in a centrifugal compressor;
using a feedback loop including a controller, controlling the quantity of liquid introduced into the liquid injection port such that when a measured discharge parameter corresponding to a pressure ratio of the centrifugal compressor exceeds a first predetermined point, the controller increases the pressure ratio by increasing the quantity of liquid introduced into the compression system corresponding to an increase of the pressure ratio above and/or on a left side of a surge line without causing surge or pulsate backflow through the centrifugal compressor; and
recycling a portion of the compressed multiphase fluid to the centrifugal compressor.

8. The method of claim 7, wherein introducing the quantity of liquid comprises atomizing the quantity of liquid.

9. The method of claim 7, wherein introducing the quantity of liquid further comprises injecting liquid into the centrifugal compressor inlet.

10. The method of claim 7, wherein introducing the quantity of liquid further comprises injecting liquid into an interstage passage of the centrifugal compressor.

11. The method of claim 10, wherein introducing the quantity of liquid comprises injecting liquid into a plurality of interstage passages of the centrifugal compressor.

12. The method of claim 10, wherein introducing the quantity of liquid comprises injecting liquid into the centrifugal compressor through a plurality of liquid injection ports.

13. The method of claim 12, wherein at least one liquid injection port is configured to pass a different liquid than is passed by another liquid injection port.

14. The method of claim 12, wherein the quantity of liquid passed by at least one liquid injection port is individually controlled.

15. The centrifugal compression system of claim 1, wherein the liquid injection port is coupled to the inlet.