

A MULTICOMPONENT DIESEL COMPOSITION

FIELD OF THE INVENTION

The present invention is related to the field of diesel compositions and to manufacturing diesel composition having improved properties. More specifically, it is related to diesel compositions comprising at least three components, a fossil diesel component, a renewable paraffinic diesel component and an oxygenate, providing benefits with diesel emissions. It is also related to a method for producing said compositions. Further, it is related to use of a combination of renewable paraffinic diesel component and oxygenate as fuel blending components to fossil fuel.

10 BACKGROUND

Oxygenates have been studied as diesel components for fossil fuels, before renewable diesels rose attention. Typically, an improvement achieved with an oxygenate in one of diesel characteristics, for example higher cetane number, better cold properties or reduced emissions, have been compromised by a deficit in another. For example, certain ethers combined with fossil diesel have been shown to reduce particulate matter (PM) emissions, but such an advantage is burdened with an increase in NO_x emissions.

On the other hand, recently the regulations and concern for environment have encouraged the use of renewable fuels. Oxygenates have been studied as components in renewable diesel or biodiesel as well. Publication WO2012074925 envisions a composition comprising renewable diesel, which they call RHE, and oxygenates. Both components are discussed very generally. As possible oxygenates, it discusses esters, ethers and/or hemiacetals comprising alcohols, polyols or combinations thereof. However, in experimental part, no actual tests are conducted. Publication WO2012074925 also lists several references to measuring techniques and possible outcome thereof.

Publication EP1398364 claims a composition comprising 0.1 - 99% paraffinic diesel component, 0 - 20 % compound containing oxygen and the rest can be regular crude oil based diesel. Said component containing oxygen may be selected from aliphatic alcohols, ethers, fatty acid esters, water or mixtures thereof. A blend of fossil diesel fuel 40 % and hydrogenated and isomerized tall oil fatty acids (TOFA) 60 % was characterized. In another example, a 70/30 blend of fossil diesel fuel and an ester was compared to another blend, 70/30, of fossil diesel and TOFA, which showed how ester seemed to affect an increase in both NO_x and PM emissions. The desired result in reduced emissions was obtained only by

the two component blend of fossil diesel and hydrogenated and isomerized TOFA. No results from blends comprising three components were presented.

Thus, there is a need to provide further diesel fuel compositions comprising oxygenates while reducing harmful effects typically related thereto.

5 SUMMARY

According to the first aspect of the invention there is provided a diesel composition comprising:

- a) fossil diesel component
 - b) oxygenate component from 10 vol-% to 40 vol-%, preferably from 10 vol-% to 30 vol-% of the total fuel composition volume, wherein
 - i. said oxygenate is a monoether having molar mass from 128 to 300 g/mol, and
 - ii. said oxygenate is of structure
$$R_1-O-R_2 \quad (\text{formula 1}),$$
in which formula R_1 and R_2 are same or different and selected from C_1 - C_{15} alkyl groups, and
 - c) renewable paraffinic diesel component from 10 vol-% to 30 vol-% of the total fuel composition volume,
- wherein the sum of said oxygenate component and said renewable paraffinic diesel component is from 26 to 70 vol-%, preferably from 30 vol-% to 50 vol-% of the total fuel composition volume.

Against expectations, compositions containing renewable paraffinic diesel fuel from 10 to 30%, an oxygenate component of formula 1 from 10 to 40 % and fossil diesel, have been shown to reduce PM emissions. Without being bound to a theory, the surprising reduction in PM emissions with this specific blend is considered to be due to synergistic effect of the renewable paraffinic diesel component and the oxygenate component present in said composition.

According to a preferred embodiment, composition comprises renewable paraffinic diesel fuel from 10 to 30 vol-%, a monoether oxygenate component 10 - 40 vol-% and regular (fossil)

diesel from 30 to 74 vol-%, wherein the renewable paraffinic diesel component is produced by a hydrogenation process of vegetable oil, animal fat, fish fat, fish oil, algae oil, microbial oil and/or wood and/or other plant based oil as well as recyclable waste and/or residue or a combination thereof, or preferably by a hydrodeoxygenation-isomerization process thereof, 5 which have shown excellent performance in emission experiments. Without binding to any theory, the results indicate that the characteristic paraffin profile of the renewable paraffinic diesel component acts synergistically with the monoether having molar mass from 128 to 300 g/mol providing a beneficial effect on the cetane number in fuel blends.

The oxygenate component is advantageously selected to provide desired characteristics to 10 the blend. Monoethers studied for their properties in blends showed some variability as to cetane number and cold properties. Depending on the desired diesel characteristics, selections among monoethers could be made. Symmetrical and unsymmetrical straight chain monoethers provide increase in cetane number in addition to desired emission effects. According to unexpected results in emission tests, the most preferable oxygenate is di-n- 15 pentyl-ether (DNPE).

The advantage of the novel composition is that the blend can decrease particulate matter (PM) emissions without penalty on NOx emissions. It is generally known that oxygenates, such as ethers can decrease the PM emissions of regular diesel, but simultaneously the NOx emissions increase. Paraffinic diesel is capable of reducing PM emissions significantly 20 without compromising the advantage by heavily increased NOx emissions.

According to the second aspect of the invention there is provided a method for producing a blend fuel, wherein the renewable paraffinic diesel component is produced from a renewable feedstock by a process selected from

- 25 a) hydrogenation or deoxygenation of vegetable oil, animal fat, fish fat, fish oil, algae oil, microbial oil and/or wood and/or other plant based oil as well as recyclable waste and/or residue or combinations thereof to obtain a paraffinic C₉-C₂₄ hydrocarbon fraction, which is optionally subjected to isomerization, or
- b) gasification of biomass to produce syngas and production of paraffins from said syngas by Fischer-Tropsch synthesis to obtain a paraffinic C₉-C₂₄ 30 hydrocarbon fraction, or
- c) a combination thereof,

and blending the renewable paraffinic diesel component thereby obtained, with an monoether oxygenate component having molar mass from 128 to 300 g/mol; and with fossil diesel component to obtain a diesel composition as described above.

According to the third aspect, herein is provided use of a monoether oxygenate having molar
5 mass from 128 to 300 g/mol and renewable diesel as fuel blending components to fossil diesel component to obtain a fuel composition, wherein the total fuel composition comprises from 10 vol-% to 40 vol-% of monoether oxygenate, and from 10 vol-% to 30 vol-% renewable paraffinic diesel and the sum of said oxygenate component and said renewable paraffinic diesel component is from 26 to 70 vol-%, preferably from 30 vol-% to 50 vol-%, wherein vol-
10 % is calculated of the total fuel composition volume.

An advantage achieved by the present fuel composition, method and use is the decrease in PM emissions. As evidenced by the examples, the oxygenate content of fuel compositions could be increased with composition containing said components in said proportions, but PM emissions decreased significantly while NO_x emissions stayed practically the same or were
15 increased considerably less than expected. The advantageous effect was observed in particular in blends comprising fossil fuel.

According to a further aspect, in composition or use the oxygenate component or raw material therefor, is derived from biomass, whereby it can be considered as renewable component. Together with renewable paraffinic diesel component it contributes to the percentage of
20 renewable, non-fossil components in the total fuel composition.

BRIEF DESCRIPTION OF THE FIGURES

Fig 1 shows emission results as compared to reference fuel for blends comprising different proportions of an oxygenate, renewable paraffinic diesel component and fossil diesel component calculated as an average for all measured points. Significant decrease of PM
25 emissions was measured for fuels according to present claims.

DETAILED DESCRIPTION

A fuel composition as used herein refers to diesel fuel complying with standards. The proportions of components are discussed here as percentages of the total fuel composition volume.

30 In the context of fuel composition, the sum amount of the oxygenate component as defined in claim 1, and said renewable paraffinic diesel component is of special interest. In the context of diesel blends, they can be considered as the most relevant blend components to fossil

diesel, the sum amount of which is from 26 to 70 vol-%, preferably from 30 vol-% to 50 vol-% of the total fuel composition volume.

According to a preferable embodiment, in which the oxygenate component consists of ethers derived from renewable sources, i. e. biomass, the sum amount of said oxygenate and said
5 renewable paraffinic diesel sets also the amount of renewable components or biocomponents of the total fuel composition, varying from 26 to 70 vol-%, preferably from 30 vol-% to 50 vol-% of the total fuel composition volume

Parameters measured herein comprise both physical and chemical characteristics of diesel fuel as well as analyses relating to combustion in a diesel engine and emissions therefrom.
10 Common emissions include unburned hydrocarbons (HC), carbon monoxide (CO), nitrogen oxides (NO_x) or particulate matter (PM). Emissions are regulated by variable standards depending on geographics, international agreements, engine types etc. Effects obtained herein are not dependent on a specific standard, but instead evidenced as decrease against a reference fuel for which experiments were conducted exactly the same manner.

15 RENEWABLE PARAFFINIC DIESEL COMPONENT

Renewable paraffinic diesel component refers here to paraffinic hydrocarbons, n-paraffins or a mixture of straight chain and branched paraffins, derived from biomass. Two approaches dominate, hydrotreating oils or fats of bio-origin or fuels made by Fischer-Tropsch synthesis of gasified biomass (BTL).

20 It is noted that paraffins exist also in fossil diesel fuels which additionally contain significant amounts of aromatics and naphthenics. Renewable paraffinic diesel component is practically free of aromatics and has properties quite similar to GTL and BTL diesel fuels made by Fischer Tropsch synthesis from natural gas and gasified biomass.

GTL

25 Gas to liquid, GTL, is a Fischer-Tropsch derived fuel having a similar cloud point than a fuel derived by hydrotreating triglycerides, fatty acids or fatty acid derivatives. GTL is characterized by broad distribution of paraffinic hydrocarbons in the range C₉-C₂₄. GTL has typically a cetane number in the range 73-81.

BTL

30 When the synthesis gas used in Fischer-Tropsch process originates from gasification of biomass, the process may be referred to as "biomass to liquid", "BTL". Broad distribution of n-paraffinic hydrocarbons in the range C₉-C₂₄ is obtainable, even though selection of a

fraction or fractions could be more specific. In an embodiment, product or a part of it may be subject to isomerization, wherein n-paraffins are at least partly converted to branched chain paraffins, i. e. isomerized.

Hydrotreated renewable paraffinic diesel component

- 5 The hydrotreated renewable paraffinic diesel component is obtainable by hydrotreating vegetable oil, animal fat, fish fat, fish oil, algae oil, microbial oil and/or wood and/or other plant based oil as well as recyclable waste and/or residue or a combination thereof. "Hydrotreated Vegetable Oil" or "Hydrogenated Vegetable Oil" was a common term used during last decade when only vegetable oils were used as feedstocks. Currently more and more of renewable
10 paraffinic diesel is produced by hydrotreatment from waste and residue fat fractions coming from food, fish and slaughterhouse industries, as well as from non-food grade vegetable oil fractions.

In an embodiment the renewable paraffinic diesel component comprises hydrotreated renewable diesel, or consists of hydrotreated renewable diesel. Hydrotreating typically
15 produces bio based middle distillate fuels. The hydrotreated renewable diesels are distinct from "bio-diesel" which is a term reserved for the fatty acid methyl esters (FAME). Chemically hydrotreated vegetable oils are mixtures of paraffinic hydrocarbons and have a very low quantity of sulfur and aromatics. Cold properties of hydrotreated renewable paraffinic diesel can be improved to meet any local requirements, by increasing the amount of i-paraffins by
20 controlling the process parameters or by additional catalytic processing.

In an embodiment the renewable paraffinic diesel component in the fuel composition comprises hydrotreated vegetable oil, hydrotreated animal fat, hydrotreated fish fat, hydrotreated fish oil, hydrotreated algae oil, hydrotreated microbial oil, hydrotreated wood and/or other plant based oil, hydrotreated recyclable waste and /or residue or a combination
25 thereof. In a preferred embodiment said renewable paraffinic diesel component consists of hydrotreated vegetable oil, hydrotreated wood and/or other plant based oil, hydrotreated animal fat, hydrotreated fish fat and oil, hydrotreated algae oil, hydrotreated microbial oil, hydrotreated recyclable waste, hydrotreated recyclable residue, or a combination thereof.

In an embodiment in the hydrotreated renewable paraffinic diesel component the amount of
30 the paraffinic components in the range of carbon number C_{15} - C_{18} is at least 70 vol-%, more preferably more than 80 vol-%, most preferably more than 90 vol-%. When a hydrotreated renewable paraffinic diesel component having said paraffinic component profile is used, a fuel composition of increased cetane number is obtained.

In an embodiment the amount of the paraffinic components in the hydrotreated renewable paraffinic diesel component in the range of carbon number C_3 - C_{14} is less than 25 vol-%, such as less than 20 vol-%, less than 10% vol-%, or less than 7 vol-%. Optionally in the hydrotreated renewable paraffinic diesel component the amount of the paraffinic components

5 in the range of carbon number C_{19} - C_{24} is less than 25 vol-%, such as less than 20 vol-%, less than 10 vol-%, or less than 5 vol-%.

In an embodiment the renewable paraffinic diesel component consists of renewable paraffinic diesel component having a cetane number of at least 70, preferably at least 75. By using a renewable paraffinic diesel component having high cetane number, a smaller addition of

10 renewable paraffinic diesel component and a monoether oxygenate having molar mass from 128 to 300 g/mol provides increased cetane number in a blend comprising a fossil diesel component and PM emission decrease.

In an embodiment the content of the hydrotreated renewable paraffinic diesel component in the total fuel composition is in the range of 10-30 vol-%. In an embodiment the content of the

15 hydrotreated renewable paraffinic diesel component in the fuel composition is 10, 11, 12, 13, 14, 15, 16, 17, 18, 19, 20, 21, 22, 23, 24, 25, 26, 27, 28, 29 or 30 vol-%.

In an embodiment fatty acids or triglycerides are first hydrogenated to n-paraffins and n-paraffins are then at least partly converted to branched chain paraffins, i. e. isomerized.

MONOETHER

20 The ether component contributes to the fuel composition as an oxygenate. Generally oxygenates used in fuels include various alcohols, ethers, esters and carbonates. However, since hydrocarbons comprising oxygen is a very broad and versatile group of chemicals, different oxygenates contribute to different diesel properties and a trade-off to others is often unavoidable.

25 To be compatible and soluble to diesel, the oxygenate is selected from monoethers having molar mass from 128 to 300 g/mol, preferably from 150 to 250 g/mol, and more preferably from 150 to 190 g/mol. This molar mass range provides best compatibility to diesels. Monoether refers to a compound comprising only one ether functionality. Said monoethers may be characterized by a formula R_1-O-R_2 , wherein R_1 and R_2 are same or different and

30 selected from straight chain or branched C_1 - C_{15} alkyls, also known as C_1 - C_{15} n-alkyls and i-alkyls respectively.

Ethers suitable for present diesel composition comprise symmetrical or asymmetrical monoethers. In the context of the present fuel composition, the oxygenate component may comprise substantially one monoether or a mixture of monoethers within above definition.

According to one embodiment, R_1 and R_2 are selected from straight chain C_1 - C_{15} alkyls, also known as C_1 - C_{15} n-alkyls. Straight chain ethers have ignition properties better than typical fossil diesel fuel as such. Straight chain ethers having total carbon number of at least 10 are known to have excellent properties as diesel components.

Preferably the oxygenate herein used comprises one of straight chain symmetrical monoethers, wherein formula 1 is of form R_1 -O- R_1 . Such monoethers comprise compounds known to have high cetane number, such as di-n-pentyl-ether (DNPE), di-n-hexyl-ether (DNHE), di-n-heptyl-ether (DNHpE), di-n-octyl-ether (DNOE), di-n-nonyl-ether (DNNE) and di-n-decyl-ether (DNDE). Furthermore, production of symmetrical monoethers from one alcohol only provides advantages both as non-complexity and economics. DNPE was used as oxygenate in present experiments and provided unexpected decrease in NO_x emissions as certain blend with fossil fuel and renewable diesel component. Symmetric monoethers of formula R_1 -O- R_1 can be produced according to known methods. Typically symmetrical ethers may be prepared from their corresponding alcohols over acid catalysts. At high temperatures, reactions catalyzed by aluminium oxide are also known.

Asymmetrical straight chain monoethers, i.e. ethers according to formula R_1 -O- R_2 , wherein R_1 and R_2 are both straight chain C_1 - C_{15} alkyls but different in carbon chain length, may be produced by well-known standard processes. A well-known example is the reaction of an alkyl halide with a sodium alkoxide, by Williamson ether synthesis. Suitable asymmetrical monoethers comprise those of high cetane number within molar mass range specified. Asymmetrical straight chain monoethers may be selected from compounds according to above specifications, such as ethyl-dodecyl ether, ethyl-undecyl ether, ethyl-decyl ether, ethyl-nonyl ether (ENE), ethyl-octyl ether, propyl-dodecyl ether, propyl-undecyl ether, propyl-decyl ether, propyl-nonyl ether, propyl-octyl ether, propyl-heptyl ether, butyl-dodecyl ether, butyl-undecyl ether, butyl-decyl ether (BDE), butyl-nonyl ether, butyl-heptyl ether, butyl-hexyl ether, pentyl-dodecyl ether, pentyl-undecyl ether, pentyl-decyl ether (PDE), pentyl-nonyl ether, pentyl-octyl ether, pentyl-heptyl ether, or pentyl-hexyl ether.

Monoethers comprising straight carbon chain alkyls are preferred, since they provide better cetane number to blends than monoethers comprising a branched carbon chain.

The oxygenate component may be selected from asymmetrical branched monoethers i.e. ethers according to formula R_1-O-R_2 , wherein R_1 and R_2 are different C_1-C_{15} alkyls and at least one of which is branched. Within the molar mass range from 128 to 300 g/mol, such ethers comprise among others, ethers comprising tert-butyl as one of the carbon chains, i.e. as R_1 or R_2 , such as octyl-tert-butyl ether (OTBE), dodecyl-tert-butyl ether (DOTBE) and ethyl-hexyl-tert-butyl ether (EHTBE). Preferably the molar mass range is from 150 to 190 g/mol.

According to another embodiment, the oxygenate component may be selected from symmetrical branched monoethers i.e. ethers according to formula R_1-O-R_2 , wherein R_1 and R_2 are the same C_1-C_{15} alkyls and branched. An example of branched symmetrical monoethers within range comprise i.e. di-ethylhexyl ether (DEHE).

According to one embodiment, the oxygenate component of the composition comprises a renewable oxygenate, preferably the oxygenate component consists of a renewable oxygenate. Oxygenates may be produced by selecting the starting materials, typically alcohols, originating from biomass or biomass waste streams. When the oxygenate component is derived from biomass, it can be classified as renewal and thereby contributes to total share of renewal components in the composition. In such a case, sum of renewable components, i.e. sum of the renewable oxygenate and the renewable diesel is from 26 to 70 vol-% and preferably from 30 vol-% to 50 vol-% of the total fuel composition volume.

20 FOSSIL DIESEL COMPONENT

The fossil diesel component means a component or composition, which is naturally occurring and derived from non-renewable sources. Examples of such non-renewable resources include petroleum oil/gas, shale oil/gas, natural gas or coal deposits, and the like, and combinations thereof, including any hydrocarbon-rich deposits that can be utilized from ground/underground sources. The term fossil also refers to recycling material of non-renewable sources.

In an embodiment the fossil diesel component is fossil middle distillate, preferably fossil diesel. Diesel fuel in general is any liquid fuel suitable for use in diesel engines, where fuel ignition takes place without spark, as a result of compression of the inlet air mixture and then injection of fuel. The most common type of diesel fuel is a specific fractional distillate of fossil fuel, preferably petroleum fuel oil. Distillation characteristics define how fuel is evaporated when it is sprayed into the combustion chamber of a diesel engine. Standards (e.g. EN590) include information about typical distillation characteristics.

To distinguish from alternative diesel fuels not derived from petroleum, petroleum-derived diesel is called herein as fossil diesel. It may also be called as e.g. petrodiesel, mineral diesel or petroleum distillate. Fossil diesel can comprise atmospheric or vacuum distillates. The distillate can comprise cracked gas oil or a blend of any proportion of straight run or thermally
5 or catalytically cracked distillates. The distillate fuel can be subjected to further processing such as hydrogen-treatment or other processes to improve fuel properties. Typically fossil diesel comprise naphthenics about 10-50 weight %, monoaromatics about 5-30 weight %, other polyaromatics 0-8 weight % and paraffins about 10-50 weight %.

The present diesel fuel composition comprises fossil diesel component from 30 vol-% to 74
10 vol-%. Use of a high fossil diesel component content is beneficial, because fossil diesels are well known and compatible with diesel engines. According to an embodiment the diesel fuel composition comprises fossil diesel component from 50 vol-% to 70 vol-% of the total fuel volume.

Final fuel composition may contain refinery and performance additives such as lubricity, cold
15 flow, antistatic and detergent additives.

EXAMPLES

The following examples are provided to illustrate various aspects of the present invention. They are not intended to limit the invention, which is defined by the accompanying claims.

Example 1. Combustion experiments

20 Method / Measurements

Engine tests were performed with a single cylinder test engine. Four test fuels having the same components as different blend proportions were analyzed. Fossil EN 590 summer grade was used as reference fuel and represented the fossil diesel component in blends. The renewable paraffinic diesel and a monoether as oxygenate were further components. In the
25 test procedure the test matrix was designed to combine two speeds and three loads per speed.

For exhaust measurements, a single cylinder test engine with free valve lift and timing and fully adjustable injection parameters was used. Charge and exhaust pressure were also adjustable. Cylinder pressure, fuel consumption and four different emissions, CO, HC, NOx,
30 and particulates were measured.

Particulate mass (PM) emission measurements were performed according to ISO8178-1:2006.

AVL SPC472 Smart Sampler was used for the measurements. Sample was taken from raw exhaust gas and diluted with a dilution factor of 6. Sampling time varied from 90 to 600 seconds depending on particulate concentration and pressure drop of the sample filter. Samples were collected on 47 mm TX40HI20-WW Pallflex filters. The filter flow was set to 5 1.3 g/s (60 nl/min) and the filter temperature was kept in between 42-50 °C. Sample filters were weighed before and after the measurements in a climatic room in which the temperature and humidity were controlled. Minimum of 2 hours stabilisation time were used for the filters before weighing.

The flow calibration of Smart Sampler was checked on daily basis and adjusted when 10 needed. During the measurements campaign the need for adjustments was negligible. On each measurement point 2-3 samples were collected. The reference fuel was measured in the beginning and after the measurement period. Test matrix is given in table 1.

Table 1. Parameters for test points studied.

Test point	Charge air mass flow	Charge air temperature	Charge air back pressure	Injection timing	Injection pressure
	[kg/h]	[Deg C]	[bar]	[DBTDC]	[bar]
1700 rpm 70% load	163	28	1,81	12	1400
1700 rpm 50% load	104	28	0,69	9	1399
1300 rpm 100% load	138	28	1,78	10	1200
1300 rpm 80% load	115	28	0,95	8	1200
1300 rpm 65% load	80	28	0,53	7	1200

15 Results

The PM results measured with reference fuel are not presented alone, but used as reference level in figure 1 presenting overall performance of different blend compositions. The exact compositions shown in Figure 1 are compiled in table 2. All compositions are not according to present claims but shown as reference. The final results have been calculated according 20 to ISO8178-1:2006. Individual load/rpm points are not presented here. Instead, averages for each mixture are shown in figure 1.

Table 2. Compositions of blends tested and shown in figure 1.

Sample	Oxygenate	Renewable diesel	Fossil diesel 1	Density (15°C)	Viscosity (40°C)	Cetane number	Distillation IBP	Distillation FBP	Lower heating value
unit	vol-%	vol-%	vol-%	kg/m ³	mm ² /s		°C	°C	MJ/kg
standard				EN ISO 12185	EN ISO 3104	ASTM D6890	EN ISO 3405	EN ISO 3405	ASTMD 4809
1	10	10	80	824,5	3,04	63,4	179,8	359,5	42,8
2	10	30	60	813,6	2,907	67,7	184,9	356,1	42,9
3	20	10	70	820,3	2,662	68,5	178,2	347,1	42,4
4	20	30	50	808,5	2,517	74,5	179,6	353,2	42,4
5	-	100	-	779,8	2,919	78,9	209,9	301,9	43,8

Figure 1 shows that unexpectedly heavy reductions in PM emissions were observed with mixtures comprising 20 vol-% of DNPE and 10 and 30 vol-% of renewable paraffinic diesel component in 70 and 50 vol-% of fossil diesel component respectively. Compared to fossil fuel, the most significant PM emission decrease was more than 20 % for sample 3 comprising 20 % of DNPE, 10 % of renewable paraffinic diesel component and the rest fossil diesel component. Mixture of 10 vol-% DNPE, 10 vol-% renewable paraffinic diesel component and 80 vol-% of fossil diesel component (sample 1, not according to the present invention) showed increase in PM emissions, but surprisingly low NO_x emissions.

- 10 It is acknowledged also, that potential for further emission reductions by engine calibration may exist.

Conclusions

The results showed DNPE as a straight chain, symmetrical monoether oxygenate lowering the particulate matter (PM) emissions. The renewable diesel component lowered both PM and NO_x emissions. The surprising synergistic effect with blends comprising both oxygenate component and renewable diesel component lowering PM emissions considerably and at the same time, the NO_x emissions were not increased, but remained almost at the same level as for the reference fossil diesel fuel.

The blends (fuels 3 and 4) gave the best PM results with very low NO_x-penalty. According to these tests higher renewable diesel component content would probably bring the NO_x emission down to the reference level.

Example 2: Ether testing

Several monoethers, both symmetrical and asymmetrical were tested for their characteristics as mixtures containing oxygen from about 1 to 2 wt-% in fossil diesel. The fossil diesel used as both reference diesel and blend base varied slightly for different experiment series (fossil diesel 2 and 3). Both straight and branched chain ethers were studied. Depending on the carbon chain length, the desired oxygen content was achieved with different ether concentrations in diesel. Standard methods were applied and the results are compiled in tables 3 and 4 (symmetrical straight chain), table 5 (asymmetrical straight chain) and table 6 (asymmetrical branched).

- 10 Table 3. Characteristics measured for ether-diesel mixtures for straight chain symmetrical monoethers according to the present invention.

		Fossil diesel 2	89,3% Fossil diesel 2	84,7% Fossil diesel 2	69,3% Fossil diesel 2	81,3% Fossil diesel 2
	ASTM		10,7 % DNPE	15,3% DNOE	30,7 % DNOE	18,7% DNDE
Density (15°C) kg/m ³	D4052	816.1	812.6	815.2	814.4	816.9
kV (15°C) mm ² /s	D445	2,62	2,35	2,79	3,06	3,26
Cloud point °C	D2500	-48	<-46	-41	-30	-9
Flash point °C	D93	75				76
Distillation IBP °C	D86	174	189	195	199	181
Distillation FBP °C		291	283	286	286	335
Cetane number	D613	48	53.9	59.9	70	57.8
Oxyg. blend cetane number bCN			104.7	125.8	119.7	100.4
Oxygen (calc) %-wt		0	1	1	2	1
Carbon (calc) %-wt		85.9	84.8	84.8	83.8	84.8
Hydrogen (calc) %-wt		14,1	14	14	14	14

Table 4. Further straight chain symmetrical monoether characteristics and some values concerning ether-diesel mixture.

	Method	Fossil diesel 3	90% Fossil diesel 3 10% DNHE
Density (15°C) kg/m ³	EN ISO12185	818,4	816,3
Cloud point °C	ASTM D7689	-28,6	-29,5
Cetane number	ASTM D6890	47,5	57
Oxyg. blend cetane number bCN			142
Oxygen (calc) %-wt		0	0,8

Table 5. Characteristics measured for ether-diesel mixtures for straight chain asymmetrical monoethers according to the present invention.

		Fossil diesel 2	88,3% Fossil diesel 2	86,0% Fossil diesel 2	86,0% Fossil diesel 2
	ASTM		11,7% ENE	14,0% BDE	14,0% PDE
Density (15°C) kg/m ³	D4052	816.1	813.3	814.7	814.6
kV (15°C) mm ² /s	D445	2,62	2,44	2,73	2,83
Cloud point °C	D2500	-48	<-46	<-45	-47
Flash point °C	D93	75		76	
Distillation IBP °C	D86	174	194	205	197
Distillation FBP °C		291	285	286	284
Cetane number	D613	48	53.4	56	56.3
Oxyg. blend cetane number bCN			94.1	105.1	107.3
Oxygen (calc) %-wt		0	1,1	1	2
Carbon (calc) %-wt		85.9	84.8	84.8	84.8
Hydrogen (calc) %-wt		14,1	14	14	14

All compounds mentioned here were soluble in diesel fuel. During cold storage, (about -18 °C), no crystallization or phase separation was observed with any of said ethers studied. These results together with parameters in tables 2 and 3, indicate that with these ethers, similar emission results may be achieved as achieved in example 1 for compositions comprising fossil diesel, renewable diesel and a symmetrical, straight chain monoether, DNPE. It can be deduced that monoethers having molar mass within range from 128 to 300 g/mol such as symmetrical DNOE, DNDE, unsymmetrical ENE, BDE, and PDE, perform similarly to DNPE in diesel blends.

Table 6. Characteristics measured for ether-diesel mixtures for branched chain asymmetrical monoethers according to the present invention.

		Fossil diesel 2	88,0% Fossil diesel 2 12,0% EHTBE	76,0% Fossil diesel 2 24,0% EHTBE	76,0% Fossil diesel 2 24,0% OTBE	84,7% Fossil diesel 2 15,3% DOTBE
	ASTM					
Density (15°C) kg/m ³	D4052	816.1	813.6	810.9	810.4	814.9
kV (15°C) mm ² /s	D445	2,62	2,55	2,43	2,56	2,96
Cloud point °C	D2500	-48	<-45	<-45	<-45	<-45
Flash point °C	D93	75	71	72	74	74
Distillation IBP °C	D86	174	178	170	186	182
Distillation FBP °C		291	286	285	286	287
Cetane number	D613	48	45.3	44.3	48.3	52.1
Oxyg. blend cetane number bCN			25.5	32.6	49.3	74.8
Oxygen (calc) %-wt		0	1	2	2	1
Carbon (calc) %-wt		85.9	84.8	83.8	83.8	84.8
Hydrogen (calc) %-wt		14,1	14	14	14	14

Since several ethers listed in the above tables have cetane number greater than that of 5 diesel, they contribute to increase in cetane number of claimed compositions. As another advantage, it can be concluded that with such ethers lower blend ratio of components contributing to cetane number are required in compositions according to present compositions in order to meet cetane number target. In addition to meeting cetane number requirements in EN590 and ASTM D975, it is especially beneficial in producing premium 10 diesel grades with higher cetane number. Based on this reasoning, the oxygenate component is preferable selected from the group of DNPE, DNOE, DNDE, BDE, DNHE, and PDE.

As summary, ethers tested for their desirable blend characteristics comprised di-n-dekyl ether, di-n-octyl ether, di-n-pentyl ether, di-n-hexyl ether, ethyl-nonyl ether, butyl-dekyl ether, pentyl-dekyl ether, octyl-tert-butyl ether, dodecyl-tert-butyl ether, ethyl-hexyl-tert-butyl ether.

15 The foregoing description has provided by way of non-limiting examples of particular implementations and embodiments of the invention a full and informative description of the best mode presently contemplated by the inventors for carrying out the invention. It is however clear to a person skilled in the art that the invention is not restricted to details of the embodiments presented above, but that it can be implemented in other embodiments using 20 equivalent means without deviating from the characteristics of the invention.

Furthermore, some of the features of the above-disclosed embodiments of this invention may be used to advantage without the corresponding use of other features. As such, the foregoing description should be considered as merely illustrative of the principles of the present invention, and not in limitation thereof. Hence, the scope of the invention is only restricted by
5 the appended patent claims.

Claims

1. A fuel composition comprising

a. fossil diesel component

b. oxygenate component in an amount from 10 vol-% to 40 vol-%, preferably
5 from 10 vol-% to 30 vol-% of the total fuel composition volume, wherein

i. said oxygenate has molar mass from 128 to 300 g/mol, and

ii. said oxygenate is of structure

in which formula R_1 and R_2 are same or different and selected from
10 C_1 - C_{15} alkyl groups,

c. renewable paraffinic diesel component in an amount from 10 vol-% to 30 vol-%, preferably from 15 to 20 vol-% of the total fuel composition volume,

wherein the sum amount of said oxygenate component and said renewable paraffinic
15 diesel component is from 26 to 70 vol-%, preferably from 30 vol-% to 50 vol-% of the total fuel composition volume.

2. The composition according to claim 1 wherein said oxygenate component is selected from symmetrical or asymmetrical straight chain monoethers, having molar mass from 150 to 300 g/mol, preferably from 150 to 250 g/mol.

3. The composition according to claim 1 wherein the amount of the oxygenate component
20 is about 20 vol-% of the total fuel composition volume.4. The composition according to claim 1 wherein said oxygenate component is selected from group of di-n-nonyl ether, di-n-decyl ether, di-n-octyl ether, di-n-heptyl ether, di-n-pentyl ether, di-n-hexyl ether, ethyl-dodecyl ether, ethyl-undecyl ether, ethyl-decyl ether, ethyl-octyl ether, propyl-dodecyl ether, propyl-undecyl ether, propyl-decyl ether, propyl-nonyl ether, propyl-octyl ether, propyl-heptyl ether, butyl-dodecyl ether, butyl-undecyl ether, butyl-nonyl ether, butyl-heptyl ether, butyl-hexyl ether, pentyl-dodecyl ether, pentyl-undecyl ether, pentyl-nonyl ether, pentyl-octyl ether, pentyl-heptyl ether, or pentyl-hexyl ether, ethyl-nonyl ether, butyl-decyl ether, pentyl-decyl ether, octyl-tert-
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butyl ether, dodecyl-tert-butyl ether, ethyl-hexyl-tert-butyl ether, di-ethylhexyl ether, and mixtures thereof.

- 5 5. The composition according to claim 1 wherein said oxygenate component is selected from symmetrical or asymmetrical straight chain monoethers, preferably said oxygenate component comprises di-n-pentyl ether.
- 10 6. The composition according to any one of the preceding claims wherein said renewable paraffinic diesel component comprises hydrocarbons produced from biomass with a process selected from gasification of biomass to produce syngas and production of paraffins from said syngas by Fischer-Tropsch synthesis to obtain a paraffinic C₉-C₂₄ hydrocarbon fraction, hydrotreatment of vegetable oil, animal fat, fish fat, fish oil, algae oil, microbial oil and/or wood and/or other plant based oil as well as recyclable waste and/or residue or a combination thereof to obtain a paraffinic C₉-C₂₄ hydrocarbon fraction, optionally followed by isomerization, or a combination thereof.
- 15 7. The composition according to any one of the preceding claims, wherein said renewable paraffinic diesel component comprises hydrotreated vegetable oil, hydrotreated wood and/or other plant based oil, hydrotreated animal fat, hydrotreated fish fat and oil, hydrotreated algae oil, hydrotreated microbial oil, hydrotreated recyclable waste, hydrotreated recyclable residue, or a combination thereof.
- 20 8. The composition according to any one of the preceding claims, wherein in said renewable paraffinic diesel component the amount of the paraffinic C₁₅-C₁₈ hydrocarbons is at least 70 vol-%, more preferably at least 80 vol-%, most preferably at least 90 vol-%.
- 25 9. The composition according to any one of the preceding claims, wherein in said renewable paraffinic diesel component the amount of the paraffinic components in the range of carbon number C₃-C₁₄ is less than 25 vol-%, such as less than 20 vol-%, less than 10% vol-%, or less than 7 vol-%.
- 30 10. The composition according to any one of the preceding claims, wherein in said renewable paraffinic diesel component the amount of the paraffinic components in the range of carbon number C₁₉-C₂₄ is less than 25 vol-%, such as less than 20 vol-%, less than 10 vol-%, or less than 5 vol-%.

11. A method for producing a fuel composition according to any one of claims 1-10, wherein the renewable paraffinic diesel component is produced from a renewable feedstock by a process selected from
- 5 a. hydrogenation or deoxygenation of vegetable oil, animal fat, fish fat, fish oil, algae oil, microbial oil and/or wood and/or other plant based oil as well as recyclable waste and/or residue or a combination thereof to obtain a paraffinic C₉-C₂₄ hydrocarbon fraction, which is optionally subjected to isomerization, or
 - 10 b. gasification of biomass to produce syngas and production of paraffins from said syngas by Fischer-Tropsch synthesis to obtain a paraffinic C₉-C₂₄ hydrocarbon fraction, or
 - c. a combination thereof,
- and blending the renewable paraffinic diesel component thereby obtained, a monoether oxygenate component having molar mass from 128 to 300 g/mol, and fossil
- 15 diesel component.
12. A method according to claim 11, wherein the feedstock for renewable paraffinic diesel component comprises vegetable oil, wood and/or other plant based oil, animal fat, fish fat and oil, algae oil, microbial oil, recyclable waste, recyclable residue, or a combination thereof.
- 20 13. Use of an oxygenate component and a renewable paraffinic diesel component as fuel blending components to fossil fuel for reducing particulate matter emissions, wherein the total fuel composition comprises a monoether oxygenate component having molar mass from 128 to 300 g/mol in an amount from 10 vol-% to 40 vol-%, preferably from 10 vol-% to 30 vol-% and renewable diesel component in an amount
- 25 from 10 vol-% to 30 vol-%, preferably from 15 to 20 vol-%, and the sum amount of said oxygenate component and said renewable paraffinic diesel component is from 26 to 70 vol-%, preferably from 30 vol-% to 50 vol-% of the total fuel composition weight.