

SPECIFICATION

AK-9604

TITLE OF THE INVENTION

PROCESS FOR INJECTION MOLDING POLYETHYLENE TEREPHTHALATE

BACKGROUND OF THE INVENTION

5 1. Field of the Invention

This invention relates to a process for injection molding a preform which is indispensable for the stretch blow molding of a thin-wall bottle, wide-mouthed vessel and the like by using amorphous polyethylene terephthalate as a
10 molding material.

2. Background Art

Polyethylene terephthalate (PET) which is produced by melt polymerizing ethylene glycol with terephthalic acid
15 or dimethyl terephthalate is amorphous (uncrystallized) and transparent. Since PET which does not reach equilibrium moisture content is moisture absorptive and is hydrolyzed when it is molten while it absorbs moisture, thereby making impossible its molding.

20 A granular material of amorphous PET (to be referred to as "A-PET" hereinafter) is slightly softened to achieve fusion bonding property when heating temperature is higher than its glass transition temperature (T_g). This fusion bonding property makes it difficult for the granular
25 material to go into a screw during the molding of a preform,

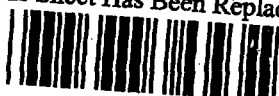


thereby making it impossible to supply the granular material. However, crystallized PET (to be referred to as "C-PET" hereinafter) is not softened at a temperature higher than its Tg, retains its hardness and does not achieve fusion bonding
5 property.

Since the above C-PET is obtained by solid-phase polymerizing A-PET at a high temperature, it is more expensive than A-PET. However, it has a higher IV (intrinsic viscosity) value than that of A-PET, is easily plasticized,
10 and produces less acetaldehyde than A-PET. Therefore, it is widely used as a molding material for producing a vessel and the like by stretch blow molding.

Then the inventors of the present invention have invented an injection molding process (refer to European
15 Patent Publication No.0623466A1 or Japanese Patent Application No.6-99163) which is capable of obtaining at low costs almost the same molded article even when A-PET which is cheaper than C-PET is used as a molding material as one obtained when C-PET is used as a molding material by
20 employing a vent type injection molding machine.

This injection molding process is to limit the amount of a granular molding material to be supplied to a feed zone of a vent type injection machine to ensure that the granular material is not stagnated by compression even if it
25 is softened into an elastic state before it reaches a



compression zone before the feed zone. This process makes possible the injection molding of a preform using A-PET which has been difficult to be molded as a molding material and some effect is obtained.

5 However, the above effect cannot be obtained when the IV value of A-PET used as a molding material is low, which makes difficult kneading during plasticization, affects the density of an injection molded preform, readily produces a molded article having a non-uniform thickness after stretch
10 blow molding and causes a problem with rigidity. These problems are solved by A-PET having a high IV value (e.g., 0.72) which is available on the market as a material for stretch blow molding out of A-PETs. However, such A-PET having a high IV value is expensive and has problems in
15 supply to a screw or plasticization in comparison with C-PET and hence, is hardly used even though it is available on the market as a material for stretch blow molding.

 It is therefore an object of the invention to provide a novel polyethylene terephthalate injection molding
20 process which can increase the IV value of the molding material in the plasticization stage even when A-PET which is inexpensive and has a low IV value is used as a molding material and can thereby overcome the difficulty of molding a preform due to its low IV value and solve a problem with its
25 physical properties.



SUMMARY OF THE INVENTION

To attain the above object, the present invention provides a process for injection molding a preform of a thin-wall vessel such as a bottle using A-PET as a molding material by using a vent type injection machine, the process comprising adding a required amount of C-PET to A-PET, plasticizing the mixture material to increase the IV value of the molding material to a value higher than the IV value of A-PET, and injection molding the preform.

10 The above C-PET can be mixed on the site and its mixing ratio is different according to the IV values of A-PET and C-PET used. When inexpensive A-PET is used as a molding material, it is not preferred that the amount of C-PET is greater than the amount of A-PET. A-PET may be moisture
15 absorptive, C-PET is supplied to a vent type injection machine as a material to be mixed without being dried, and a preform is injection molded.

In the present invention, as the vent type injection machine a vent type injection machine in which an
20 injection screw consisting of a first stage and a second stage is incorporated in a heating cylinder equipped with a vent in such a manner that it can be rotated and moved back and forth is employed, and the amount of a granular material to be supplied to the feed zone of the first stage of the
25 vent type injection machine is limited so that the granular



material is not stagnated by compression even if it is softened into an elastic state before it reaches the compression zone before the feed zone.

The mixture material of A-PET and C-PET which is
5 softened in the feed zone is compressed by a tapered surface of the compression zone, molten stretched, kneaded primarily and supplied to the second stage where a volatile content produced by melting and water content thereof are sucked and removed from a vent opening by a vacuum pump. In this
10 process of kneading, the IV value of the molding material becomes higher than the IV value of A-PET as a whole by mixing C-PET which has a higher IV value than that of A-PET and kneading is thereby carried out fully.

Although the above vent continues vacuum suction
15 without being interrupted even at the time of injection, a reduced pressure is made smaller at the time of injection than at the time of plasticization to prevent the molten molding material from overflowing through the vent opening by the forward movement of the injection screw. The molten
20 material which has been further plasticized in the second stage is metered at the front of the screw as in a normally-structured injection machine and injection filled in a mold by the forward movement of the injection screw to become a preform. The preform is transferred to a blow mold
25 immediately or later to be stretch blow molded into a



thin-wall vessel such as a bottle.

BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 is a schematic vertical side view of an
5 example of a vent type injection machine capable of
practicing the injection molding process of the present
invention.

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

10 In the figure, reference numeral 1 is an injection
screw which is inserted into the inside of a heating cylinder
2 in such a manner that it can be rotated and moved back and
forth. This injection screw 1 is a combination of two
screws, each having deep groove portions and shallow groove
15 portions: a screw 10 located in a rear portion of the heating
cylinder 2 and designed as the first stage and a screw 20
located in a front portion and designated as the second
stage.

The above heating cylinder 2 is provided with a
20 vent opening 3 in a wall portion thereof where the rear
portion of the second stage 20 is located and the opening is
sealed hermetically and connected to a vacuum pump (unshown).
A feed port 4 is provided in a rear wall portion of the
heating cylinder 2 where the rear portion of the first stage
25 10 is located and a hopper 5 is attached to the port 4. Not



shown in the figure, band heaters for heating the molding material supplied from the above feed port 4 by the rotation of the screw are provided at the outer periphery of the heating cylinder 2 and a nozzle 6.

5 To mold the preform using this vent type injection machine, the temperature of a portion of the heating cylinder 2 corresponding to the first stage 10 is set at 280°C and the temperature of a portion of the heating cylinder 2 corresponding to the second stage 20 is set at 270°C. The
10 molding material obtained by mixing undried granular A-PET and a required amount of granular C-PET is placed in the above hopper 5 and the injection screw 1 is rotated at a high speed (100 rpm). The vent opening 3 is depressurized to -730 mmHg by the vacuum pump.

15 The molding material in the above hopper 5 is supplied to the feed zone of the first stage 10 by the rotation of the injection screw 1 while the amount of its supply is limited. The limitation of the amount of supply is carried out by reducing the sectional area of the screw
20 groove in the rear portion of the feed zone to $\frac{2}{3}$ that of the screw groove in the front portion of the feed zone, whereby the overconjection of the granular material in the front portion of the feed zone is prevented to ensure that the granular material is not solidified and stagnated by
25 compression even if it is softened into an elastic state by



heating before it reaches the compression zone.

The granular materials of A-PET and C-PET which are softened in the feed zone are compressed by a tapered surface of the compression zone, molten and drawn to be fused together and the total IV value of the materials is increased to a value higher than that of A-PET due to the IV value of C-PET in comparison with the case where only A-PET is used as a molding material. Thereby, A-PET which is hardly kneaded due to its low IV value is kneaded completely and plasticization proceeds.

This molten material is supplied to the second stage 20 which is set at a temperature lower than that of the first stage 10. Since the screw groove of the feed zone of this stage is formed deep, the pressure of the molten material is lowered, the volatile content and the water content of the resin are vaporized, the volatile content and the water content enclosed by the molten material are further separated by the rotation of the screw, sucked and removed from the vent opening 3 by the vacuum pump. The molten material from which the volatile content and the water content have been removed is supplied to the metering zone of the second stage 20 by the rotation of the screw, further plasticized there and transferred to the front portion of the screw as in the normally-structured injection machine.

Along with the transfer of the molten material, the



injection screw 1 moves backward, its rotation stops at a predetermined position, and the metering of the material is thus completed. The metered molten material is injection filled in a mold for molding a preform by the forward movement of the injection screw. At this time, the suction of the vent opening 3 by the vacuum pump is changed to -650 mmHg to continue suction during injection. This suction can be easily controlled by taking in the outside air into a suction line by valve operation.

10 The mixing ratio of A-PET and C-PET and a simple average IV value are shown below.

MATERIALS USED

A-PET	IV value: 0.63	J005 of Mitsui PET Resin Co.
15 C-PET	IV value: 0.79	J125 of Mitsui PET Resin Co.
C-PET	IV value: 0.85	J135 of Mitsui PET Resin Co.

MIXING RATIO (1)

	A-PET	C-PET	simple average IV value
20	J005	J125	
	5	5	0.710
	6	4	0.694
	7	3	0.678
	8	2	0.662

25 MIXING RATIO (2)

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	A-PET	C-PET	simple average IV value
	J005	J135	
	5	5	0.740
	6	4	0.718
5	7	3	0.696
	8	2	0.674

Example

Material Resin: A-PET J005/C-PET J125

Mixing Ratio: 7:3, IV value: 0.678

10 Molded Article: flat bottle

Dimension: total height: 250 mm, diameter of mouth
portion: 23.5 mm, length below neck: 230
mm, outer diameter of barrel portion: 90
x 50 mm, thickness of barrel portion: 0.4
mm, weight: 36 g

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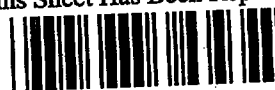
Preform

Dimension: total height: 142 mm, inner diameter of
mouth portion: 23.5 mm, length below
neck: 122 mm, thickness of barrel
portion: 2.9 mm, outer diameter of upper
barrel portion: 28 mm, outer diameter of
lower end barrel portion: 24 mm, draft:
2/122

20

Preform Molding Conditions

25 Heating Cylinder Setting Temperature



first stage: front portion: 285°C, intermediate
portion: 285°C, rear end portion:
280°C

second stage: front portion: 270°C, rear portion:
270°C

5

Nozzle Temperature: 270°C

Injection Mold Temperature (set temperature)

cavity mold: 15°C

core mold: 15°C

10

Injection Pressure (dwell): 75 kg/cm²

Fill Dwell Time: 6.0 seconds

Cooling Time: 2.8 seconds

Release Temperature: 60 to 70°C (preform surface
temperature)

15 Stretch Blow Molding Conditions

Mold Temperature (set temperature): 20°C

Stretch Blow Temperature: 86°C (preform surface
temperature)

Blow Pressure (stretch): 20 kg/cm²

20

Blow Time: 2.0 seconds

Stretch Ratios

longitudinal (axial direction): 1.9 times

transverse (radial direction): 3.6 x 2 times

Results

25

The preform taken out from the injection mold after



being cooled completely was transparent and free from distortion and had uniform density. . When a plurality of preforms were molded simultaneously, there was no difference among them and good products were obtained. Molded articles
5 obtained by stretch blow molding were transparent, had no unevenness in thickness and were comparable to C-PET products.

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* C L M S *

WHAT IS CLAIMED IS:

1. A process for injection molding a preform using amorphous polyethylene terephthalate as a molding material by using a vent type injection machine, comprising the steps of adding a
5 required amount of crystallized polyethylene terephthalate to amorphous polyethylene terephthalate, plasticizing the resulting mixture material to increase the intrinsic viscosity value of the molding material to a value higher than the intrinsic viscosity value of the amorphous
10 polyethylene terephthalate, and injection molding the preform.

2. A process for injection molding a preform using amorphous polyethylene terephthalate as a molding material according to
15 claim 1, wherein said vent type injection machine comprises a heating cylinder, a vent opening provided on said heating cylinder, an injection screw consisting of a first stage and a second stage and provided within said heating cylinder rotatably and movably, and the amount of a granular material
20 to be supplied to a feed zone of the first stage of the vent type injection machine is limited so that the granular material is not stagnated by compression even if it is softened into an elastic state before it reaches the compression zone of the first stage before the feed zone of
25 the first stage.

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3. A process for injection molding a preform using amorphous polyethylene terephthalate as a molding material according to claim 2, wherein the amount of supply is limited by reducing the sectional area of the screw groove in the rear portion of
5 the feed zone to $2/3$ that of the screw groove in the front portion of the feed zone.

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