CLAIMS:

1. A hydrocracking catalyst for improved diesel production, wherein the catalyst comprises:

a) an aggregated form of zeolite Y comprising small size primary crystallites of zeolite Y, wherein at least a portion of the primary crystallites are aggregated to form larger secondary particles, wherein the aggregated zeolite Y has a silica-to-alumina ratio of at least 4:1, and an alkali metal content of less than 4 wt% based on the zeolite; and

b) a binder;

wherein the hydrocracking catalyst has an Alpha value of less than 15, and an External Surface Area-to-Total Surface Area ratio of at least 0.35:1.

2. The hydrocracking catalyst of claim 1, wherein the aggregated zeolite Y has been stabilized by steaming at a temperature of at least 700°C.

3. The hydrocracking catalyst of claim 2, wherein the average pore diameter of the catalyst is at least 7.0 nm.

4. The hydrocracking catalyst of claim 3, wherein the steam-stabilized aggregated zeolite Y has been further acid washed.

5. The hydrocracking catalyst of claim 3, wherein the aggregated zeolite Y has been calcined prior to steaming.

6. The hydrocracking catalyst of claim 3, wherein the binder comprises a material selected from metal oxides, zeolites, aluminum phosphates, polymers, carbons, and clays.

7. The hydrocracking catalyst of claim 6, wherein the binder is comprised of at least one metal oxide, preferably selected from silica, alumina, silica-alumina, amorphous aluminosilicates, boron, titania, and zirconia.

c) separating a diesel range boiling point product from the liquid hydrocracked effluent fraction;

wherein the hydrocracking catalyst comprises:

- an aggregated form of zeolite Y comprising small size primary crystallites of zeolite Y, wherein at least a portion of the primary crystallites are aggregated to form larger secondary particles, wherein the aggregated zeolite Y has a silica-to-alumina ratio of at least 4:1, and an alkali metal content of less than 4 wt% based on the zeolite; and
- a binder;

wherein the hydrocracking catalyst has an Alpha value of less than 15, and an External Surface Area-to-Total Surface Area ratio of at least 0.35:1.

24. The process of claim 23, wherein the hydrocracking conditions include a reaction temperature from about 550°F (288°C) to about 800°F (427°C), a total pressure from about 300 psig (2.1 MPag) to about 3000 psig (20.7 MPag), an LHSV from about 0.1 hr^{-1} to about 20 hr^{-1}, and a hydrogen treat gas rate from about 500 scf/bbl (85 Nm^3/m^3) to about 10000 scf/bbl (1700 Nm^3/m^3).

25. The process of claim 24, wherein hydrocarbon feedstock is comprised of a gasoil having an initial boiling point above about 400°F (204°C), a T50 boiling point of at least about 500°F (260°C) and an end boiling point of at least about 600°F (315°C).

26. The process of claim 25, wherein the hydrocarbon feedstock contains at least 25 wt% hydrocarbons with boiling points above 700°F (371°C).

27. The process of claim 26, wherein the portion of the hydrocarbon feedstock boiling above 700°F (371°C) has a T50 boiling point above 800°F (427°C).

28. The process of claim 26, wherein the aggregated zeolite Y has been stabilized by steaming at a temperature of at least 700°C.

29. The process of claim 28, wherein the average pore diameter of the catalyst is at least 7.0 nm.