

EVAPORATIVE COOLER WET AND DRY MODE CONTROL

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CLAIM OF PRIORITY

[0001] This patent application claims the benefit of priority, to Abdel-Salam U.S. Patent Application Serial Number 62/782,944, entitled "EVAPORATIVE COOLER WET AND DRY MODE CONTROL," filed on December 20, 2018 (Attorney Docket No. 5991.064PRV), each of which is hereby incorporated by
10 reference herein in its entirety.

BACKGROUND

[0002] Evaporative coolers are systems commonly used in various heating
15 ventilation and air conditioning (HVAC) applications. Evaporative coolers receive a process fluid from a source, such as a building or nearby HVAC equipment, cool the process fluid, and return the process fluid to the source or other equipment. Evaporative coolers use sensible and latent (or evaporative) cooling to cool the process fluid in a normal mode of operation (wet mode).
20 Some evaporative coolers, such as hybrid evaporative coolers, are able to cool the process fluid in a second mode, such as a dry mode. In a dry mode, evaporative coolers can use only sensible cooling through forced conduction to cool the process fluid.

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BRIEF DESCRIPTION OF THE DRAWINGS

[0003] In the drawings, which are not necessarily drawn to scale, like numerals may describe similar components in different views. Like numerals having different letter suffixes may represent different instances of similar components. The drawings illustrate generally, by way of example, but not by
30 way of limitation, various embodiments discussed in the present document.

[0004] FIG. 1 illustrates a schematic view of a system, in accordance with at least one example of this disclosure.

[0005] FIG. 2 illustrates a schematic view of a system, in accordance with at least one example of this disclosure.

[0006] FIG. 3 illustrates a schematic view of a system, in accordance with at least one example of this disclosure.

[0007] FIG. 4 illustrates a schematic view of a system, in accordance with at least one example of this disclosure.

- 5 [0008] FIG. 5 illustrates a schematic view of a method of operating a system, in accordance with at least one example of this disclosure.

DETAILED DESCRIPTION

[0009] Some evaporative coolers, such as hybrid evaporative coolers, are able
10 to cool process fluid in either a dry mode or a wet mode. A controller can be used to determine when to switch modes. Switching from dry mode to wet mode can be relatively simple. During operation of an evaporative cooler in dry mode, the fan speed will eventually reach a maximum speed as outdoor air temperature increases. When the supply process water temperature is not met (when the
15 supply process water temperature is above the set point) and the maximum fan speed is reached, a maximum available sensible cooling is reached and the wet mode can be enabled to further cool the process water or other fluid to meet the set point.

[0010] However, optimally switching from wet mode to dry mode can be
20 relatively more difficult. This is in part because many variables affect the performance of the evaporative cooler such as the ambient dry bulb and wet bulb temperatures, the entering water temperature, the condition of the cooling coil, the flowrate and/or other properties of the working water. Two approaches are discussed below that are used in the HVAC industry to control the switching
25 from wet to dry mode in hybrid evaporative cooling units.

[0011] A first approach uses a fixed outdoor air dry bulb temperature as a set point to switch from wet mode to dry mode. When the outdoor air dry bulb temperature is below the set point, a controller disables the working fluid or recirculation pump to operate the cooler in the dry mode. A second approach
30 uses a fan speed signal to control switching to dry mode. When the fan reaches its minimum speed in wet mode, the controller can change to dry mode. A drawback of these approaches is that in both cases the evaporative cooler may continue operating under wet mode for more time than is actually required, which can cause more water to be used in wet mode than is required.

[0012] This disclosure provides a proposed control strategy and system that can determine when to switch from wet to dry mode. In one example, an evaporative cooler system can include a controller configured to determine a minimum water temperature that can be produced by the evaporative cooler in dry mode while the evaporative cooler is still in wet mode. The controller can determine the minimum process water temperature that can be produced by the cooling coil using a theoretical or empirical model of the coil of the evaporative cooler. In some examples, the controller can use inputs from sensors of the evaporative cooler to determine the minimum water temperature with the model.

5 The inputs can be, for example, process water inlet and outlet temperatures, a process water flow rate, an air inlet temperature, and an air outlet temperature.

[0013] Such a system and control method can increase the water efficiency of evaporative coolers, increase the lifetime of wet media, and other mechanical equipment associated with them (e.g. pumps, filters, strainers),

15 decrease water treatment requirements due to the associated reduction in water usage, increase shutdown time for wet media and all mechanical equipment associated with them, which enables more accessibility to conduct preventative and corrective maintenance, and can reduce the total cost of ownership for hybrid evaporative coolers.

[0014] In some examples, the system control can be adjusted to account for heat exchanger degradation over time, such as due to scaling, to help ensure that the change from wet to dry mode occurs at an optimal outdoor air temperature through a life of the equipment.

[0015] FIG. 1 illustrates a schematic view of an evaporative cooler system, in accordance with at least one example of this disclosure. The system 100 can include an evaporative cooler 102, a controller 104, a cooling coil 106, a fan 108, and a recirculation pump 110, a process fluid pump 112, a process fluid source 114, an inlet air temperature sensor 116, an outlet air temperature sensor 118, a process fluid flow sensor 120, a process fluid inlet temperature sensor

25 122, and a process fluid outlet temperature sensor 124. Also shown in FIG. 1 is process inlet fluid 126, process fluid 127, process outlet fluid 128, inlet air 130, conditioned air 131, outlet air 132, working fluid (recirculated fluid) 134, and an air flow sensor 144.

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[0016] The evaporative cooler 102 can be an evaporative cooler configured to cool process fluid using one or more of working air and working water or fluid. The evaporative cooler 102 can be a hybrid evaporative cooler located upstream of the cooling coil 106, such as in examples that includes a wet media. The wet media of the evaporative cooler 102 can be of any design such as a membrane air-to-liquid exchanger, falling film exchanger, packed media exchanger, or other wet media design that cools the air stream using evaporative cooling. In some examples, the evaporative cooler 102 and the cooling coil 106 can be combined in a single heat exchanger.

10 [0017] In some examples, the evaporative cooler 102 can be a liquid to air membrane energy exchanger (LAMEE) to transfer heat and moisture between a liquid desiccant and an air stream to condition the temperature and humidity of the air flowing through the LAMEE. The membrane in the LAMEE can be a non-porous film having selective permeability for water, but not for other
15 constituents that form the liquid desiccant. Many different types of liquid desiccants can be used in combination with the non-porous membrane, including, for example, glycols. The non-porous membrane can make it feasible to use desiccants, such as glycols, that had been previously determined to be unacceptable or undesirable in these types of applications. In an example, the
20 membrane in the LAMEE can be semi-permeable or vapor permeable, and generally anything in a gas phase can pass through the membrane and generally anything in a liquid phase cannot pass through the membrane. In an example, the membrane in the LAMEE can be micro-porous such that one or more gases can pass through the membrane. In an example, the membrane can be a selectively-
25 permeable membrane such that some constituents, but not others, can pass through the membrane. It is recognized that the LAMEEs included in the conditioning units disclosed herein can use any type of membrane suitable for use with an evaporative cooler LAMEE.

[0018] In an example, the LAMEE or exchanger can use a flexible polymer
30 membrane, which is vapor permeable, to separate air and water. The water flow rate through the LAMEE may not be limited by concerns of carryover of water droplets in the air stream, compared to other conditioning systems. The LAMEE can operate with water entering the LAMEE at high temperatures and high flow

rates, and can therefore be used to reject large amounts of heat from the water flow using latent heat release (evaporation).

[0019] The cooling fluid circulating through the LAMEE or exchanger can include water, liquid desiccant, glycol, other hygroscopic fluids, other evaporative liquids, and/or combinations thereof. In an example, the cooling fluid is a liquid desiccant that is a low concentration salt solution. The presence of salt can sanitize the cooling fluid to prevent microbial growth. In addition, the desiccant salt can affect the vapor pressure of the solution and allow the cooling fluid to either release or absorb moisture from the air. The concentration of the liquid desiccant can be adjusted for control purposes to control the amount of cooling of the scavenger air or cooling fluid within the LAMEE or exchanger.

[0020] Membrane exchangers may have some advantages over other types of evaporative coolers. For example, the LAMEE may eliminate or mitigate maintenance requirements and concerns of conventional cooling towers or other systems including direct-contact evaporation devices, where the water is in direct contact with the air stream that is saturated by the evaporated water. For example, the membrane barriers of the LAMEE inhibit or prohibit the transfer of contaminants and micro-organisms between the air and the liquid stream, as well as inhibiting or prohibiting the transfer of solids between the water and air. The use of LAMEEs along with an upstream or downstream cooling coil can result in a lower temperature of the water leaving the LAMEE and a higher cooling potential. Various configurations of cooling systems having a LAMEE can boost performance in many climates. Higher cooling potential and performance can result in lower air flow and fan power consumption in the cooling system, which is the main source of energy consumption in liquid-cooling systems. In an example in which the heat load is from a data center, this can increase the overall data center cooling system efficiency.

[0021] The cooling coil 106 can be a heat exchanger configured to exchange heat between the process fluid (127), the air (130, 131, 132), and the working fluid 134. In some examples, the cooling coil 106 can include tubes and/or fins for transfer of heat between the fluids and can include an evaporative media configured to receive the working fluid 134 thereon and to evaporate the working fluid 134 into the air (130, 132) to transfer heat from the process fluid

(126, 128) to the air (130, 132) through latent heat of vaporization of the working fluid 134.

[0022] The controller 104 can be a programmable controller, such as a single or multi-board computer, a direct digital controller (DDC), or a programmable logic controller (PLC). In other examples the controller 104 can be any computing device, such as a handheld computer, for example, a smart phone, a tablet, a laptop, a desktop computer, or any other computing device including a processor and wireless or wired communication capabilities. Though the connections to the controller are shown as being a single direction, communication can occur in both directions between the controller 104 and components connected thereto. The various components can be connected via wire, optical cable, and/or wirelessly. Though the controller 104 is discussed as being an electronic controller, the controller 104 can be other types of controllers, such as a pneumatic controller.

[0023] The fan 108 can be one or more fans or pumps configured to motivate air to flow. The fan 108 can be an axial, centrifugal (plug), or the like and can be located in or connected to an air tunnel or chamber either upstream or downstream of the cooling coil 106.

[0024] The recirculation pump 110 can be a fluid pump (such as a water or glycol pump) configured to pump fluid to the evaporative cooler 102 for wetting of the evaporative media of the evaporative cooler 102. In some examples, the pump 110 can be connected to a basin, drain pan, tank, or sump where run-off from the coil can be collected. In some examples, the evaporative cooler 106 can receive fluid from a tank in a gravity-fed arrangement. In some examples, the recirculation pump 110 can be a positive displacement or rotary pump, such as a centrifugal pump configured to pump fluid to a top portion of evaporative cooler 102 for distribution across and down the evaporative cooler 102. In other examples, the fluid can be pumped to other portions of the evaporative cooler 102 for distribution. In some examples, the recirculation pump 110 can be electrically connected to the controller 104 such that the controller can control operation of the recirculation pump 110, such as whether the recirculation pump 110 is on or off and at what speed the recirculation pump 110 operates.

[0025] Similarly, the process fluid pump 112 can be a fluid pump (such as a water or glycol pump) configured to pump the process fluid 127 from the source

114 to the cooling coil 106 and back to the source. The circuit including the source 114, the cooling coil 106, and the process fluid pump 112 can include various other components, such as valves, strainers, air separators, expansion tanks, other heat exchanges, or the like. The process fluid pump 112 can be a positive displacement or rotary pump, such as a centrifugal pump configured to pump water through the process fluid circuit. In some examples, the process fluid pump 112 can be electrically connected to the controller 104 such that the controller can control operation of the process fluid pump 112, such as whether the process fluid pump 112 is on or off and at what speed the process fluid pump 112 operates.

[0026] The process fluid source 114 can be a piece of equipment configured to use the process fluid 127. For example, the process fluid source 114 can be a cooling coil of an air tunnel, computer room air conditioning (CRAC) unit, chilled beam, fan coil, or the like. The process fluid source 114 can receive chilled or cooled fluid from the process fluid outlet 128, transfer heat to the process fluid 127 and discharge the process fluid 127 to the process fluid pump 112.

[0027] The inlet air temperature sensor 116 can be located in the inlet air stream 130 and can be configured to produce an inlet temperature signal based on a dry bulb and/or a wet bulb temperature of the inlet air stream 130. In some examples, the air temperature sensor 116 can measure (or can effectively measure) an ambient air temperature. The inlet air temperature sensor 116 can be electrically connected to controller 104 and configured to transmit the inlet temperature signal thereto. Each of the inlet air temperature sensor 116 and the outlet air temperature sensor 118 can be any type of temperature sensor, such as a thermistor, thermocouple, resistance temperature detector, a wetted wick, a chilled mirror sensor, a capacitive humidity sensor, a resistive humidity sensor, or the like.

[0028] Similarly, the outlet air temperature sensor 118 can be located in the outlet air stream 132 and can be configured to produce an outlet temperature signal based on a dry bulb and/or a wet bulb temperature of the outlet air stream 132. The outlet air temperature sensor 118 can be electrically connected to controller 104 and configured to transmit the outlet temperature signal thereto.

[0029] The process fluid flow sensor 120 can be connected to the process fluid circuit, such as upstream of the cooling coil 106 near the process fluid inlet 126. The process fluid flow sensor 120 can be any type of flow or pressure sensor, such as a differential pressure sensor, a Coriolis sensor, a paddle sensor, a paddle wheel sensor, or the like. The process fluid flow sensor 120 can be configured to produce a flow signal based on a flow rate of the process fluid 127 through the cooling coil 106. The process fluid flow sensor 120 can be connected to the controller 104 to transmit the process fluid flow signal thereto.

[0030] The process fluid inlet temperature sensor 122 can be connected to the process fluid circuit, such as upstream of the cooling coil 106 in the process fluid inlet 126. The process fluid inlet temperature sensor 122 can be configured to produce a process fluid inlet temperature signal based on a temperature of the process fluid 127 at the process fluid inlet 126 to the cooling coil 106. The process fluid inlet temperature sensor 122 can be connected to the controller 104 to transmit the process fluid inlet temperature signals thereto. The process fluid inlet temperature sensor 122 and the process fluid outlet temperature sensor 124 can be any type of fluid temperature sensor, either in a thermowell, coupled to a pipe of the process fluid circuit, or in direct contact with the process fluid, such as a thermistor, thermocouple, resistance temperature detector, or the like.

[0031] The process fluid outlet temperature sensor 124 can be connected to the process fluid circuit, such as downstream of the cooling coil 106 in the process fluid outlet 128. The process fluid outlet temperature sensor 124 can be configured to produce a process fluid outlet temperature signal based on a temperature of the process fluid 127 at the process fluid outlet 128 of the cooling coil 106. The process fluid outlet temperature sensor 124 can be connected to the controller 104 to transmit the process fluid outlet temperature signal thereto.

[0032] In operation of the evaporative cooler in a first wet mode, which can be referred to as an adiabatic mode, the process fluid pump 112 can be on and pumping fluid through the cooling coil 106 in a cooling coil closed circuit. The recirculation pump 110 can be on and pumping fluid to evaporative media of the evaporative cooler 102 in an evaporative cooler closed circuit. The fan 108 can be on and delivering an air stream to the evaporative cooler 102, which can follow to the cooling coil 106. The working fluid 134 can be evaporated into the inlet air 130 to condition the inlet air 130 adiabatically to create conditioned air

131. The conditioned air 131 can have a reduced dry-bulb temperature with a higher humidity level, while the overall enthalpy can remain constant where the conditioned air 131 can have a larger sensible cooling capacity than the inlet air 130.

5 **[0033]** The conditioned air 131 can be delivered to the cooling coil 106 where the conditioned air 131 can receive heat from the process fluid 127 to cool the process fluid 127 via the cooling coil 106 to provide the process fluid 127 at the process fluid outlet 128 with a temperature at the process fluid set point or target. When the controller 104 determines that the evaporative cooler 102 can be
10 switched from wet mode to dry mode, the controller can send signals to disable the recirculation pump 110 and can adjust a speed of the fan 108, as necessary, to maintain the process fluid set point or target.

[0034] As shown within the controller 104, the controller 104 can perform a step 136 to determine whether the minimum supply water temperature
15 (SWT_{min}) is less than the process fluid set point (PCW set point), where the SWT_{min} is the lowest temperature of process fluid that the cooling coil 106 can deliver at a given ambient temperature or a given inlet air temperature while operating in the dry mode. Such a calculation can be performed when a maximum air flow rate that can be received by the cooling coil 106 is known.
20 The “process fluid set point” or “Process Conditioned Water (PCW) set point” is also referred to herein as the “leaving process fluid temperature set point.” This temperature set point is the target or desired temperature of the fluid leaving (e.g., at the fluid outlet of) the cooling coil 106. The inlet air temperature can be delivered to the controller via the inlet air temperature sensor 116, as discussed
25 above. In examples, where ambient temperature is used to calculate SWT_{min}, an additional outdoor or ambient temperature sensor can be used.

[0035] When it is true that the SWT_{min} is less than the process fluid temperature set point, the controller can enable dry mode at step 140 (in one example by locking out or disabling the evaporative cooler 102), because the
30 controller 104 has determined that dry mode should provide the required process water temperature at the set point. When it is not true that the SWT_{min} is less than the process fluid set point, the controller 104 can maintain wet mode at step 138. By including an ability to use a dry mode whenever possible, the system 100 can help to minimize the fluid usage, helping to save water. The

determination of when to switch to dry mode by the controller 104 is discussed in further detail below.

[0036] In some examples, the controller 104 can calculate the SWTmin when the system 100 is operating in the dry mode (or when the evaporative cooler 102 is not enabled) and when it is not true that the SWTmin is less than the process fluid set point, the controller 104 can maintain dry mode at step 138 when the process fluid outlet temperature signal from the temperature sensor 124 indicates that the temperature of the process fluid 127 at the process fluid outlet 128 of the cooling coil 106 is actually equal or below the PCW set point. In such a circumstance, the controller 104 can update the theoretical model for determining the SWTmin.

[0037] In some examples, the controller 104 can include a theoretical model to predict the SWTmin that can be achieved by the system 100 in dry mode for an ambient (outdoor) or inlet air temperature under any available operating condition. For example, the controller 104 can predict the SWTmin at a maximum speed of the fan 108 and/or at a minimum or maximum air flow rate. In some examples, the controller 104 can predict the SWTmin at any flow rate measured by the air flow sensor 144. The theoretical model can be a computational model using heat transfer and fluid mechanics equations to determine performance of the cooling coil 106 at certain conditions.

[0038] The controller 104 can additionally or alternatively include an empirical model. Such a model can be a performance model of the cooling coil 106 developed based on measurements taken in a lab and/or during operation of the cooling coil 106 or a similar cooling coil of another system. In some examples, the empirical model can be updated during operation of the cooling coil 106 in dry mode.

[0039] The controller 104 can use the empirical model and/or the theoretical model and one or more inputs to determine the SWTmin. For example, the controller 104 can use data from the process fluid inlet temperature signal, the process water outlet temperature signal, the inlet air temperature signal, the outlet air temperature signal, an air flow rate signal (discussed below) and/or the process water flow signal input the data into the theoretical model and/or the empirical model and output the SWTmin. Once the controller 104 has calculated

the SWT_{min}, the controller 104 can determine whether dry mode operation can provide process water with a leaving temperature that meets the set point or target temperature.

[0040] The process water inlet temperature signal can be received at the controller 104 from the process water inlet temperature sensor 122; the process water outlet temperature signal can be received at the controller 104 from the process water outlet temperature sensor 124; the inlet air temperature signal can be received at the controller 104 from the inlet air temperature sensor 116; the outlet air temperature signal can be received at the controller 104 from the outlet air temperature sensor 118; and, the process water flow signal can be received at the controller 104 from the process water flow sensor 120.

[0041] In some examples, only the air side inputs (air temperatures) can be used to determine the SWT_{min}. In some examples, only the water side inputs (process fluid temperatures and/or flowrate) can be used to determine the SWT_{min}. In some examples, a combination of both air and process fluid signals can be used. In one example, the inlet air temperature signal, the inlet process fluid temperature signal, and/or the outlet process fluid temperature signal can be used with the theoretical model and/or the empirical model to determine the SWT_{min}.

[0042] In some examples where it is desired to use a controller requiring less computing power, a lookup table or a regression correlation can be created based on a theoretical model and/or an empirical model and the table or correlation can be included in the controller 104. The controller 104 can then use one or more inputs to lookup the SWT_{min} for making the determination of when to switch to dry mode.

[0043] Because thermal performance of the cooling coil 106 can change over time due to operational factors (e.g. fouling, corrosion), the actual performance of the cooling coil 106 can deviate from the theoretical and/or empirical model developed for a clean coil. To correct for performance degradation over the lifetime of the cooling coil 106, the thermal performance of the cooling coil 106 can be updated. The updates to the theoretical and/or empirical models can be done based on time and/or based on data saved from each of the signals, where the signals can be stored as data and can be used to measure thermal performance of the cooling coil

106 in various conditions. The data and thermal performance can be used to update lookup tables, and can be updated based on artificial neural networks and deep learning tools that account for the degradation in thermal performance of the cooling coil 106.

5 **[0044]** Further, the data can be collected from one or more of the sensors, such as the inlet air temperature sensor 116, the outlet air temperature sensor 118, the process fluid flow sensor 120, the process fluid inlet temperature sensor 122, and/or the process fluid outlet temperature sensor 124, and/or any other sensors discussed above or below. The data from the sensors can be used
10 by artificial neural networks and/or deep learning tools to update the model used to determine the SWT_{min}.

[0045] FIG. 2 illustrates a schematic view of an evaporative cooler system 100A, in accordance with at least one example of this disclosure. Any of the components of the system 100A can be included in the systems discussed above
15 and below.

[0046] The system 100A can include an evaporative cooler 102, a controller 104, a cooling coil 106, a fan 108, a recirculation pump 110, a process fluid pump 112, a process fluid source 114, an inlet air temperature sensor 116, an outlet air temperature sensor 118, a process fluid flow sensor 120, a process fluid
20 inlet temperature sensor 122, and a process fluid outlet temperature sensor 124. Also shown in FIG. 2 is process inlet fluid 126, process fluid 127, process outlet fluid 128, inlet air 130, conditioned air 131, outlet air 132, working fluid (recirculated fluid) 134, and an air flow sensor 144.

[0047] The system 100A can be similar to the system 100 of FIG. 1, except
25 that circuits of the working fluid 134 and the process fluid 127 can be connected (as opposed to adiabatic mode where the working fluid 134 and the process fluid 127 circuits can be isolated) for serial delivery of fluid from the cooling coils 106 to the evaporative cooler 102. In some examples, the system 100A can be the same as the system 100 where the changes in fluid flow are performed by
30 valves in one or more fluid circuits.

[0048] In operation of the system 100A in a second wet mode, which can be referred to as an evaporative mode, the process fluid pump 112 can be on and pumping fluid through the cooling coil 106. The process fluid 127 can be cooled by the conditioned air 131 to create cooled process fluid 127. The cooled process

fluid 127 can then be delivered to the evaporative cooler 102. The working fluid 134 (which can be the same as the process fluid 127) can be delivered to the evaporative cooler 102 to be passed over the evaporative cooler 102, such as media of the evaporative cooler 102, where a portion of the process fluid 127 can be evaporated into the inlet air 130 to cool the inlet air 130 to create the conditioned air 131 (as described above with respect to system 100) and the process fluid 127 can be cooled by the evaporative cooler. The process fluid 127 leaving the evaporative cooler 102 can be delivered to the process fluid outlet 128 to provide the process fluid 127 at a temperature meeting the process fluid set point or target so that the process fluid 127 can be then delivered to the source 114. In some examples of the evaporation wet mode, depending on operating condition, a portion of the fluid leaving the cooling coil 106 can be mixed with fluid leaving the evaporative cooler 102 for delivery to the source 114 at a temperature at the process fluid set point or target.

[0049] On the air side, the fan 108 can be on and delivering an air stream to the evaporative cooler 102 and the cooling coil 106. The working fluid 134 can cool the inlet air 130 to create the conditioned air 131, which can be delivered to the cooling coil 106 for cooling of the process fluid 127.

[0050] In the evaporative wet mode, when the controller 104 determines that the evaporative cooler 102 can be switched from wet mode to dry mode, the controller can send signals to the process fluid pump 112 and valves of the circuits to direct fluid flow through only the cooling coil 106 and can adjust a speed of the fan 108, as necessary, to maintain the process fluid set point or target. As shown within the controller 104, the controller 104 can perform a step 136 to determine whether the SWT_{min} is less than the PCW set point to determine when the switch to dry mode should be made, as discussed above with respect to FIG. 1.

[0051] FIG. 3 illustrates a schematic view of an evaporative cooler system 100B, in accordance with at least one example of this disclosure. Any of the components of the system 100A can be included in the systems discussed above and below.

[0052] The system 100B can include an evaporative cooler 102, a controller 104, a cooling coil 106, a fan 108, and a recirculation pump 110, a process fluid pump 112, a process fluid source 114, an inlet air temperature sensor 116, an

outlet air temperature sensor 118, a process fluid flow sensor 120, a process fluid inlet temperature sensor 122, and a process fluid outlet temperature sensor 124.

Also shown in FIG. 3 are a process inlet fluid 126, process fluid 127, process outlet fluid 128, an inlet air 130, conditioned air 131, outlet air 132, working fluid (recirculated fluid) 134, a pre-cooling coil 142, and an air flow sensor 144.

[0053] The system 100B can be similar to the system 100 of FIG. 1, except that the system can include the pre-cooling coil 142. The pre-cooling coil 142 can be a heat exchanger configured to exchange heat between the fluid and air.

In some examples, the pre-cooling coil 142 can include tubes and/or fins for transfer of heat between the fluids. The pre-cooling coil 142 can be configured to receive working fluid 134 (and/or process fluid) from the recirculation pump 110 (and/or from the process fluid pump 112) for passing through tubes of the pre-cooling coil 142 such that the working fluid 134 can receive heat sensibly from air delivered from the fan 108. The air can be conditioned (such as cooled) by the pre-cooling coil 142 and can be delivered as pre-cooled air to the evaporative cooler 102 to increase a total cooling capacity of the system 100B. In some examples, fluids other than the working fluid 134 can be delivered to the pre-cooling coil. In some examples, the working fluid 134 leaving the pre-cooling coil can be delivered to the evaporative cooler 102.

[0054] The system 100B can also include an air flow sensor 144, which can be a sensor configured to measure a volumetric (or mass) flow rate of air through the pre-cooling coil 142, the evaporative cooler 104, and the cooling coil 106.

The fan flow sensor can be connected to the controller 102 and configured to deliver an air flow rate signal to the controller 102 based on a detected flow rate of the air stream (such as at the inlet air 130, the conditioned air 131, and/or the outlet air 132). In some examples, the air flow rate signal can be used by the controller 102 to determine the SWT_{min}. Though the air flow sensor 144 is shown as between the pre-cooling coil 142 and the evaporative cooler 102, the air flow sensor 144 can be positioned anywhere in the air stream (130, 131, 132).

Though not discussed with respect to the systems 100 and 100A, either system can include the air flow sensor 144, as shown in FIGS. 1 and 2.

[0055] In operation of the evaporative cooler in a third wet mode, which can be referred to as a super-evaporative mode, the process fluid pump 112 can be on and pumping fluid through the cooling coil 106 where the process fluid 127 can

be cooled by the conditioned air 131 to provide the process fluid 127 at the process fluid outlet 128 with a temperature at the process fluid set point or target where the process fluid 127 can be then delivered to the source 114.

[0056] In some examples, a portion of the process fluid from the cooling coil 106 can be delivered to the evaporative cooler 102 and can be evaporated into the inlet air stream 130 to create the conditioned air 131. In some examples, the recirculation pump 110 can provide all or some of the flow to the evaporative cooler 102. Some or all of the fluid leaving the evaporative cooler 102 can provide the process fluid 127 at the process fluid outlet 128 (mixed with fluid leaving the cooling coil 106 in some examples) with a temperature at the process fluid set point or target, where the process fluid 127 can be then delivered to the source 114. In other examples, some or all of the fluid leaving the evaporative cooler 102 can be delivered to the pre-cooling coil 142. The pre-cooling coil can use fluid from the evaporative cooler 102 and/or the recirculation pump 110 to pre-cool the inlet air 130. Fluid leaving the pre-cooling coil 142 can be delivered to the process fluid outlet 128 (and can be mixed with fluid leaving the cooling coil 106 and/or the evaporative cooler 102 in some examples) with a temperature at the process fluid set point or target, where the process fluid 127 can be then delivered to the source 114. On the air side, the fan 108 can be on and delivering an air stream to the pre-cooling coil 142, the evaporative cooler 102, and then to the cooling coil 106.

[0057] When the controller 104 determines that the evaporative cooler 102 can be switched from wet mode to dry mode, the controller can send signals to disable the recirculation pump 110 and can adjust a speed of the fan 108, as necessary, to maintain the process fluid set point or target. During such a switch, bypass dampers can be used to divert the airstream to bypass the pre-cooling coil 142 to reduce unnecessary air-side pressure drop and therefore save fan motor power. As shown within the controller 104, the controller 104 can perform a step 136 to determine whether the SWTmin is less than the PCW set point to determine when the switch to dry mode should be made, as discussed above with respect to FIG. 1.

[0058] FIG. 4 illustrates a schematic view of an evaporative cooler system 400, in accordance with at least one example of this disclosure. In some examples, any of the components of the evaporative cooler system 400 can be

included in any of the systems 100, 100A, and 100B discussed above. In some examples, instead of switching entirely between the distinct modes of operation for the adiabatic mode and evaporation mode, the system 400 can include a blended mode operation. Such a blended mode operation can include blending the adiabatic and evaporative modes together in differing ratios to control the mode transition and maintain optimal water efficiency. The transition between modes can involve significant changes in the operational state of the unit and can be difficult to control or avoid fluctuations in supply water temperature. The transition from the adiabatic mode to the evaporative mode can involve a sudden mixing of water or a sudden increase in cooling power as the evaporative coolers begin to receive warmer water and the evaporation rate increases significantly. This can result in the fan speed modulating from full speed (at the limit of the adiabatic mode) to a low speed in the evaporative mode to prevent over cooling. In examples where multiple cooling units are used, as the cooling load on the system 400 increases (when fewer conditioning units are selected for a given facility heat load), system 400 can spend minimal time in the adiabatic mode and switch to the evaporative mode where it can develop sufficient cooling capacity. The evaporative mode can be less efficient in terms of water usage, relative to the adiabatic mode, and water consumption can increase.

[0059] Operating in the blended mode can include monitoring and varying the ratio of the return process water from the cooling coil (RC) 420 into first and second sections of a water storage tank 428, and the first and second sections can be at least partially separated from one another. The blended mode operation can involve varying distribution of return process water from the cooling coil (RC) 420 into two pump suction bays of the tank 428 and corresponding pump suction inlets (for example of pumps 430 and 432 of FIG. 4) and consequently varying a mix ratio of warm and cold water into the pumped cold water supply (to the heat load 492) via the pump 430 and into the pumped recirculated water (to the evaporative cooler 418) via the pump 432. Valves (such as the 3-way valve 494) can control the proportion of hot return water going into the suction inlets of the pumps 430, 432, respectively (P-1, P-2). Though the system 400 shows a 3-way valve to control proportioning, two 2-way valves can be used in other examples to control the proportioning of hot return water going into the suction inlets of the pumps 430, 432, respectively (P-1, P-2).

[0060] The system 400 can be controlled to maintain a supply water temperature set point under varying ambient air conditions or varying cooling loads. The system 400 accomplishes this by varying the mix ratio of EC discharge water (into a back portion of the tank 428) and RC return water into the pump suction bays. For example, if the system 400 enters the wet mode of operation in the equivalent of the adiabatic mode (100% of RC return water into the first pump suction and 100% evaporative cooler discharge into the second pump suction) and the ambient outdoor air conditions rise (increased temperature or humidity), the supply water temperature delivered by the first pump 430 (P-1) may rise above the set point. In this case, a controller of the system 400 can begin to modulate the RC return valves (such as the 3-way valve 494) to divert a portion of the return water into the second pump suction bay, which can cause an equivalent portion of cold EC discharge water to flow into the first pump suction bay, lowering the supply water temperature to the set point. The mix ratio can be continuously modulated by the controller to maintain supply water temperature set point in response to varying ambient conditions and load. At peak ambient conditions or peak cooling loads the system may operate in the equivalent of the evaporative mode (100% of RC return water into P-2 suction, and P-1 suction being supplied essentially all by EC discharge water).

[0061] Such a blended wet mode can be interrupted when the controller (such as the controller 104 of FIGS. 1-3) determines that the SWT_{min} is less than the PCW set point of the system 400 when operating in the blended mode. In some examples, the controller 104 can make this determination by comparing the SWT_{min} to the PCW set point at each possible operating point of the blended mode at any given ambient temperature of the system 400.

[0062] Examples according to the present application can include a method of operating the system 400 in a blended mode at particular operating conditions between the adiabatic mode and the evaporative mode, where operating the conditioning system in the blended mode comprises distributing a first cooling fluid exiting the recovery coil between the first and second portions of the tank in a ratio such that a mix of the first and second cooling fluids in the supply water delivered to the heat load is at a temperature at or near a set point temperature for the conditioning system. Operating in the blended mode can include continuously monitoring and varying a ratio of the first cooling fluid

distributed to the first and second portions of the tank to maintain the temperature of the supply water at or near the set point temperature.

[0063] FIG. 5 illustrates a schematic view of a method 500, in accordance with at least one example of this disclosure. The steps or operations of the method 500 are illustrated in a particular order for convenience and clarity; many of the discussed operations can be performed in a different sequence or in parallel without materially impacting other operations. The method 500 as discussed includes operations performed by multiple different actors, devices, and/or systems. It is understood that subsets of the operations discussed in the method 500 can be attributable to a single actor, device, or system could be considered a separate standalone process or method.

[0064] The method 500 can begin at step 502, where the fan can be operated to deliver an airstream. For example, the fan 108 can be operated by the controller 104 to deliver the inlet air stream 130. At step 504, the recirculation pump can be operated to provide a working fluid. For example, the recirculation pump 110 can be operated by the controller 104 to provide the working fluid 134 to the cooling coil 106.

[0065] At step 506, the cooling coil can be located in the airstream and can receive a process fluid from a source. For example, the cooling coil 106 can be located in the airstream (130, 132) and can receive the process fluid 127 at the process fluid inlet 126 from the source 114. At step 508, the process fluid can be cooled in a wet mode by the evaporative cooler and by the cooling coil using the working fluid from the recirculation pump and the airstream. For example, the airstream 130 can be conditioned by the evaporative cooler 102 and the working fluid 134 from the recirculation pump 110. Then, while the system 100 is in a wet mode, the process fluid 127 can be cooled by the cooling coil 106 using the conditioned air 131.

[0066] At step 510, a leaving process water temperature set point can be received at a controller. For example, a leaving process water temperature set point can be received at the controller 104. At step 512, a minimum supply water temperature deliverable by the cooling coil in the dry mode can be determined based on a coil performance model. For example, a minimum supply water temperature deliverable by the cooling coil 106 in the dry mode (SWT_{min}) can be determined based on a coil performance model by the controller 104. Then, at

step 514, the system can be switched from the wet mode to the dry mode when the leaving process water temperature set point is greater than the minimum supply water temperature. For example, the system 100 can be switched from the wet mode to the dry mode when the leaving process water temperature set point
5 (PCW set point) is greater than the minimum supply water temperature (SWT_{min}).

NOTES AND EXAMPLES

[0067] The following, non-limiting examples, detail certain aspects of the
10 present subject matter to solve the challenges and provide the benefits discussed herein, among others.

[0068] Example 1 is a hybrid evaporative cooler system comprising: an evaporative cooler located in an airstream; a cooling coil located in the airstream downstream of the evaporative cooler and configured to receive a process fluid
15 from a source; and a controller configured to operate the hybrid evaporative cooler system in a wet mode, in which the evaporative cooler is activated to receive a working fluid and to condition at least one of the working fluid and the airstream and in which the cooling coil cools the process fluid using the airstream, and configured to operate the evaporative cooler system in a dry mode
20 in which the evaporative cooler is deactivated and in which the cooling coil cools the process fluid using the airstream, the controller further configured to: receive a leaving process fluid temperature set point; determine a minimum supply fluid temperature deliverable by the cooling coil in the dry mode based on a coil performance model; and operate the hybrid evaporative cooler system
25 in the dry mode on condition that the leaving process fluid temperature set point is greater than the minimum supply fluid temperature.

[0069] In Example 2, the subject matter of Example 1 optionally includes a process fluid inlet temperature sensor configured to transmit an inlet temperature signal to the controller based on a process fluid inlet temperature; wherein the
30 minimum supply fluid temperature is determined based on the inlet temperature sensor signal.

[0070] In Example 3, the subject matter of Example 2 optionally includes a process fluid outlet temperature sensor configured to transmit an outlet temperature signal to the controller based on a process fluid outlet temperature;

wherein the minimum supply fluid temperature is determined based on the inlet temperature signal and the outlet temperature signal.

[0071] In Example 4, the subject matter of Example 3 optionally includes a process fluid flow sensor configured to transmit a flow signal to the controller based on a process fluid flow rate; wherein the minimum supply fluid temperature is determined based on the inlet temperature signal, the outlet temperature signal, and the flow signal.

[0072] In Example 5, the subject matter of Example 4 optionally includes a temperature sensor configured to transmit an air temperature signal to the controller based on an inlet air temperature; wherein the minimum supply fluid temperature is determined based on the inlet temperature signal, the outlet temperature signal, the air temperature signal, and the flow signal.

[0073] In Example 6, the subject matter of any one or more of Examples 2–5 optionally include a process fluid flow sensor configured to transmit a flow signal to the controller based on a process fluid flow rate; wherein the minimum supply fluid temperature is determined based on the inlet temperature signal and the flow signal.

[0074] In Example 7, the subject matter of any one or more of Examples 1–6 optionally include wherein the coil performance model is based on a theoretical performance of the cooling coil.

[0075] In Example 8, the subject matter of Example 7 optionally includes wherein the coil performance model uses one or more of a process fluid inlet temperature signal, a process fluid outlet temperature signal, an air temperature signal, and a process water flow rate signal.

[0076] In Example 9, the subject matter of any one or more of Examples 1–8 optionally include wherein the coil performance model is based on an empirical performance of the cooling coil.

[0077] In Example 10, the subject matter of any one or more of Examples 7–9 optionally include wherein the coil performance model uses one or more of a process fluid inlet temperature signal, a process fluid outlet temperature signal, an air temperature signal, and a process fluid flow rate signal.

[0078] In Example 11, the subject matter of any one or more of Examples 1–10 optionally include wherein the controller is configured to update the coil

performance model based on time to account for degradation in performance of the cooling coil.

[0079] Example 12 is a method of controlling a hybrid evaporative cooler system, the method comprising: cooling a process fluid from a source using a cooling coil located in an airstream downstream of an evaporative cooler, the evaporative cooler operable together with the cooling coil in a wet mode; and receiving a leaving process fluid temperature set point; determining a minimum supply fluid temperature deliverable by the cooling coil in a dry mode where the evaporative cooler is deactivated based on a coil performance model; and operating the hybrid evaporative cooler system in the dry mode when the leaving process fluid temperature set point is greater than the minimum supply fluid temperature.

[0080] In Example 13, the subject matter of Example 12 optionally includes receiving an inlet temperature signal produced by a fluid inlet temperature sensor based on a process fluid inlet temperature; wherein determining the minimum supply fluid temperature deliverable by the cooling coil in the dry mode is based on the inlet temperature signal.

[0081] In Example 14, the subject matter of Example 13 optionally includes receiving an outlet temperature signal produced by a fluid outlet temperature sensor based on a process fluid outlet temperature; wherein determining the minimum supply fluid temperature deliverable by the cooling coil in the dry mode is based on the inlet temperature signal and the outlet temperature signal.

[0082] In Example 15, the subject matter of Example 14 optionally includes receiving a flow signal produced by a process fluid flow sensor based on a process fluid flow rate; wherein determining the minimum supply fluid temperature deliverable by the cooling coil in the dry mode is based on the inlet temperature signal, the outlet temperature signal, and the flow signal.

[0083] In Example 16, the subject matter of Example 15 optionally includes receiving an air temperature signal produced by a temperature sensor based on an inlet air temperature; wherein determining the minimum supply fluid temperature deliverable by the cooling coil in the dry mode is based on the inlet temperature signal, the outlet temperature signal, the air temperature signal, and the flow signal.

[0084] In Example 17, the subject matter of any one or more of Examples 12–16 optionally include receiving a flow signal produced by a process fluid flow sensor based on a process fluid flow rate; wherein determining the minimum supply fluid temperature deliverable by the cooling coil in the dry mode is based on the inlet temperature signal and the flow signal.

[0085] In Example 18, the subject matter of any one or more of Examples 12–17 optionally include wherein the coil performance model is based on a theoretical performance of the cooling coil.

[0086] In Example 19, the subject matter of any one or more of Examples 12–18 optionally include wherein the coil performance model is based on an empirical performance of the cooling coil.

[0087] Example 20 is a hybrid evaporative cooler system comprising: an evaporative cooler located in an airstream; a cooling coil located in the airstream downstream of the evaporative cooler and configured to receive a process fluid from a source; and a controller configured to enable and disable the evaporative cooler and the cooling coil, the controller further configured to: receive a leaving process fluid temperature set point; determine a minimum supply fluid temperature deliverable by the cooling coil on condition that when the evaporative cooler is off based on a coil performance model; and disable the evaporative cooler on condition that the leaving process fluid temperature set point is greater than the minimum supply fluid temperature.

[0088] In Example 21, the subject matter of Example 20 optionally includes a process fluid inlet temperature sensor configured to transmit an inlet temperature signal to the controller based on a process fluid inlet temperature; wherein the minimum supply fluid temperature is determined based on the inlet temperature sensor.

[0089] In Example 22, the subject matter of Example 21 optionally includes a process fluid outlet temperature sensor configured to transmit an outlet temperature signal to the controller based on a process fluid outlet temperature; wherein the minimum supply fluid temperature is determined based on the inlet temperature signal and the outlet temperature signal.

[0090] In Example 23, the subject matter of any one or more of Examples 20–22 optionally include an air flow sensor configured to transmit an air flow signal to the controller based on a flow rate of air through the hybrid evaporative cooler

system; wherein the minimum supply fluid temperature is determined based on the air flow signal.

[0091] In Example 24, the subject matter of any one or more of Examples 1–23 optionally include wherein the controller is configured to update the coil performance model based on a machine learning model using performance data collected over time to account for degradation in performance of the cooling coil.

[0092] In Example 25, the apparatuses or method of any one or any combination of Examples 1 – 24 can optionally be configured such that all elements or options recited are available to use or select from.

[0093] The above detailed description includes references to the accompanying drawings, which form a part of the detailed description. The drawings show, by way of illustration, specific embodiments in which the invention can be practiced. These embodiments are also referred to herein as “examples.” Such examples can include elements in addition to those shown or described. However, the present inventors also contemplate examples in which only those elements shown or described are provided. Moreover, the present inventors also contemplate examples using any combination or permutation of those elements shown or described (or one or more aspects thereof), either with respect to a particular example (or one or more aspects thereof), or with respect to other examples (or one or more aspects thereof) shown or described herein.

[0094] In the event of inconsistent usages between this document and any documents so incorporated by reference, the usage in this document controls.

[0095] In this document, the terms “a” or “an” are used, as is common in patent documents, to include one or more than one, independent of any other instances or usages of “at least one” or “one or more.” In this document, the term “or” is used to refer to a nonexclusive or, such that “A or B” includes “A but not B,” “B but not A,” and “A and B,” unless otherwise indicated. In this document, the terms “including” and “in which” are used as the plain-English equivalents of the respective terms “comprising” and “wherein.” Also, in the following claims, the terms “including” and “comprising” are open-ended, that is, a system, device, article, composition, formulation, or process that includes elements in addition to those listed after such a term in a claim are still deemed to fall within the scope of that claim. Moreover, in the following claims, the

terms “first,” “second,” and “third,” etc. are used merely as labels, and are not intended to impose numerical requirements on their objects.

[0096] The above description is intended to be illustrative, and not restrictive. For example, the above-described examples (or one or more aspects thereof)
5 may be used in combination with each other. Other embodiments can be used, such as by one of ordinary skill in the art upon reviewing the above description. The Abstract is provided to comply with 37 C.F.R. §1.72(b), to allow the reader to quickly ascertain the nature of the technical disclosure. It is submitted with the understanding that it will not be used to interpret or limit the scope or
10 meaning of the claims. Also, in the above Detailed Description, various features may be grouped together to streamline the disclosure. This should not be interpreted as intending that an unclaimed disclosed feature is essential to any claim. Rather, inventive subject matter may lie in less than all features of a particular disclosed embodiment. Thus, the following claims are hereby
15 incorporated into the Detailed Description as examples or embodiments, with each claim standing on its own as a separate embodiment, and it is contemplated that such embodiments can be combined with each other in various combinations or permutations. The scope of the invention should be determined with reference to the appended claims, along with the full scope of equivalents to which such
20 claims are entitled.

CLAIMS:

1. A hybrid evaporative cooler system comprising:
an evaporative cooler located in an airstream;
a cooling coil located in the airstream downstream of the evaporative cooler and
5 configured to receive a process fluid from a source; and
a controller configured to operate the hybrid evaporative cooler system in a wet
mode, in which the evaporative cooler is activated to receive a working
fluid and to condition at least one of the working fluid and the airstream
and in which the cooling coil cools the process fluid using the airstream,
10 and configured to operate the evaporative cooler system in a dry mode in
which the evaporative cooler is deactivated and in which the cooling coil
cools the process fluid using the airstream, the controller further
configured to:
receive a leaving process fluid temperature set point;
15 determine a minimum supply fluid temperature deliverable by the
cooling coil in the dry mode based on a coil performance model;
and
operate the hybrid evaporative cooler system in the dry mode on
condition that the leaving process fluid temperature set point is
20 greater than the minimum supply fluid temperature.
2. The hybrid evaporative cooler system of claim 1, further comprising:
a process fluid inlet temperature sensor configured to transmit an inlet
temperature signal to the controller based on a process fluid inlet
25 temperature;
wherein the minimum supply fluid temperature is determined based on the inlet
temperature sensor signal.
3. The hybrid evaporative cooler system of claim 2, further comprising:
30 a process fluid outlet temperature sensor configured to transmit an outlet
temperature signal to the controller based on a process fluid outlet
temperature;
wherein the minimum supply fluid temperature is determined based on the inlet
temperature signal and the outlet temperature signal.

4. The hybrid evaporative cooler system of claim 3, further comprising:
a process fluid flow sensor configured to transmit a flow signal to the controller
based on a process fluid flow rate;
- 5 wherein the minimum supply fluid temperature is determined based on the inlet
temperature signal, the outlet temperature signal, and the flow signal.
5. The hybrid evaporative cooler system of claim 4, further comprising:
a temperature sensor configured to transmit an air temperature signal to the
10 controller based on an inlet air temperature;
wherein the minimum supply fluid temperature is determined based on the inlet
temperature signal, the outlet temperature signal, the air temperature
signal, and the flow signal.
- 15 6. The hybrid evaporative cooler system of claim 2, further comprising:
a process fluid flow sensor configured to transmit a flow signal to the controller
based on a process fluid flow rate;
wherein the minimum supply fluid temperature is determined based on the inlet
temperature signal and the flow signal.
- 20 7. The hybrid evaporative cooler system of claim 1, wherein the coil
performance model is based on a theoretical performance of the cooling coil.
8. The hybrid evaporative cooler system of claim 7, wherein the coil
25 performance model uses one or more of a process fluid inlet temperature signal,
a process fluid outlet temperature signal, an air temperature signal, and a process
fluid flow rate signal.
9. The hybrid evaporative cooler system of claim 1, wherein the coil
30 performance model is based on an empirical performance of the cooling coil.

10. The hybrid evaporative cooler system of claim 7, wherein the coil performance model uses one or more of a process fluid inlet temperature signal, a process fluid outlet temperature signal, an air temperature signal, and a process fluid flow rate signal.

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11. The hybrid evaporative cooler system of claim 1, wherein the controller is configured to update the coil performance model based on performance data collected over time to account for degradation in performance of the cooling coil.

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12. A method of controlling a hybrid evaporative cooler system, the method comprising:

cooling a process fluid from a source using a cooling coil located in an airstream

15 downstream of an evaporative cooler, the evaporative cooler operable

together with the cooling coil in a wet mode; and

receiving a leaving process fluid temperature set point;

determining a minimum supply fluid temperature deliverable by the cooling coil

in a dry mode where the evaporative cooler is deactivated based on a coil

20 performance model; and

operating the hybrid evaporative cooler system in the dry mode when the leaving

process fluid temperature set point is greater than the minimum supply

fluid temperature.

25 13. The method of claim 12, further comprising:

receiving an inlet temperature signal produced by a fluid inlet temperature sensor

based on a process fluid inlet temperature;

wherein determining the minimum supply fluid temperature deliverable by the

cooling coil in the dry mode is based on the inlet temperature signal.

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14. The method of claim 13, further comprising:
receiving an outlet temperature signal produced by a fluid outlet temperature
sensor based on a process fluid outlet temperature;
wherein determining the minimum supply fluid temperature deliverable by the
5 cooling coil in the dry mode is based on the inlet temperature signal and
the outlet temperature signal.
15. The method of claim 14, further comprising:
receiving a flow signal produced by a process fluid flow sensor based on a
10 process fluid flow rate;
wherein determining the minimum supply fluid temperature deliverable by the
cooling coil in the dry mode is based on the inlet temperature signal, the
outlet temperature signal, and the flow signal.
16. The method of claim 15, further comprising:
receiving an air temperature signal produced by a temperature sensor based on
an inlet air temperature;
wherein determining the minimum supply fluid temperature deliverable by the
cooling coil in the dry mode is based on the inlet temperature signal, the
20 outlet temperature signal, the air temperature signal, and the flow signal.
17. The method of claim 12, further comprising:
receiving a flow signal produced by a process fluid flow sensor based on a
process fluid flow rate;
25 wherein determining the minimum supply fluid temperature deliverable by the
cooling coil in the dry mode is based on the inlet temperature signal and
the flow signal.
18. The method of claim 12, wherein the coil performance model is based on
30 a theoretical performance of the cooling coil.
19. The method of claim 12, wherein the coil performance model is based on
an empirical performance of the cooling coil.

20. A hybrid evaporative cooler system comprising:
an evaporative cooler located in an airstream;
a cooling coil located in the airstream downstream of the evaporative cooler and
configured to receive a process fluid from a source; and
5 a controller configured to enable and disable the evaporative cooler and the
cooling coil, the controller further configured to:
receive a leaving process fluid temperature set point;
determine a minimum supply fluid temperature deliverable by the
cooling coil on condition that the evaporative cooler is off based
10 on a coil performance model; and
disable the evaporative cooler on condition that the leaving process fluid
temperature set point is greater than the minimum supply fluid
temperature.
- 15 21. The hybrid evaporative cooler system of claim 20, further comprising:
a process fluid inlet temperature sensor configured to transmit an inlet
temperature signal to the controller based on a process fluid inlet
temperature;
wherein the minimum supply fluid temperature is determined based on the inlet
20 temperature sensor.
22. The hybrid evaporative cooler system of claim 21, further comprising:
a process fluid outlet temperature sensor configured to transmit an outlet
temperature signal to the controller based on a process fluid outlet
25 temperature;
wherein the minimum supply fluid temperature is determined based on the inlet
temperature signal and the outlet temperature signal.
23. The hybrid evaporative cooler system of claim 20, further comprising:
30 an air flow sensor configured to transmit an air flow signal to the controller
based on a flow rate of air through the hybrid evaporative cooler system;
wherein the minimum supply fluid temperature is determined based on the air
flow signal.

24. The hybrid evaporative cooler system of claim 1, wherein the controller is configured to update the coil performance model based on a machine learning model using performance data collected over time to account for degradation in performance of the cooling coil.

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