

PROCESS FOR GENERATING AND SEPARATING A HYDROGEN-CARBON
MONOXIDE MIXTURE BY CRYOGENIC DISTILLATION

The present invention relates to a process and to an
5 apparatus for the generation and separation of a
mixture of hydrogen and carbon monoxide.

The units for the production of carbon monoxide and
hydrogen can be separated into two parts:

- 10 - generation of syngas (mixture comprising H_2 , CO , CH_4 ,
 CO_2 , Ar , H_2O and N_2 essentially). Among the various
industrial routes for the production of syngas, those
based on partial oxidation of natural gas, on
autothermal reforming or on coal gasification can
15 prove to be advantageous when the H_2/CO production
ratio is low (less than approximately 3).
- purification of syngas. The following are found:
 - * a unit for scrubbing with a liquid solvent in order
to remove most of the acid gases present in the
20 syngas,
 - * a unit for purification on a bed of adsorbents,
 - * a unit for separation by the cryogenic route,
referred to as "cold box", for the production of
CO.

25 In the case of a syngas resulting from a partial
oxidation reactor, from an autothermal reactor or from
a reactor for the gasification of coal or of heavy
hydrocarbon feedstocks, the residual methane content in
30 the syngas at the inlet of the cold box is too low for
a process of the scrubbing with methane type; the CH_4
contents can be of the order of 0.1% in the case of a
coal gasification or else of the order of 0.9% in the
case of a partial oxidation or autothermal reactor,
35 whereas the minimum content at the inlet of the cold
box is generally in the vicinity of 2%. In this case,
the conventional cryogenic process for the purification
of a syngas (CO cold box) is a partial condensation.

All the percentages in this document are molar percentages.

- 5 In the context of a combined production of pure hydrogen and CO under pressure, the partial condensation process has disadvantages in comparison with the scrubbing with methane:
- 10 - the partial condensation does not make it possible to produce pure hydrogen with a low CO content without PSA (for example, the hydrogen comprises approximately 10 ppm of CO when produced by scrubbing with methane, whereas it comprises from 2 to 15% of CO when produced by partial condensation);
 - 15 - the CO yield of the partial condensation is lower; in order to increase the yield of the partial condensation, it is necessary to invest in a compressor for recycling the waste gases from the partial condensation;
 - 20 - the methane present in the syngas is only in part found in the methane bleed at the bottom of the tank of the CO/CH₄ column. A large amount of methane exits from the cold box with the hydrogen-rich gas at the top of the scrubbing column by thermodynamic equilibrium at the temperature level of the top of the scrubbing column, another amount exiting with the flash gas withdrawn at the stripping column top by thermodynamic equilibrium at the temperature level of the top of the stripping column. In order to ensure a positive material balance of the system for CH₄, it is necessary for the amount of CH₄ which enters the cold box with the syngas to be greater than the sum of the amounts of CH₄ which leave with the hydrogen-rich gas and the flash gas in order to ensure a CH₄ bleed which makes it possible to control the system.
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The slight traces of CO₂ at the outlet of the purification (0.3 ppm) are found dissolved in the tank

liquid of the CO/CH₄ column. In order to avoid any accumulation of CO₂ in the system (in the scrubbing loop), it is necessary for all the CO₂ which enters the cold box to leave via the CH₄ bleed.

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Generally, the CH₄ bleed and the scrubbing circuit are withdrawn together at the bottom of the tank of the CO/CH₄ column. The CO₂ content in the bleed is thus the same as in the scrubbing circuit. As the scrubbing circuit is supercooled to -180°C in order to optimize the scrubbing, the CO₂ content in the scrubbing circuit and thus in the bleed has to be lower than the value of the solubility of CO₂ in CH₄ at -180°C in order to avoid solidification of the CO₂ in this circuit in the passageways of the exchanger.

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Taking into consideration a CO₂ content at the outlet of the purification of 0.3 ppm and a value for solubility of CO₂ in CH₄ at -180°C of 42 ppm, this defines a maximum level of concentration of CO₂, expressed by the ratio of the flow rate of syngas entering the cold box to the CH₄ bleed, of 140.

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This defines, for a given flow rate of syngas, a minimal value of CH₄ content at the inlet of the cold box in order to ensure, simultaneously, an excess CH₄ balance and a CH₄ bleed for controlling the system and limiting the level of concentration of CO₂ in order to prevent solidification of the CO₂ in the scrubbing CH₄ circuit and thus to prevent blocking of the cryogenic exchanger.

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In order to benefit, for a process for the generation of syngas by a partial oxidation or autothermal reactor or else by a reactor for gasification of coal or heavy feedstocks, from the advantages of the process of scrubbing with methane type, the idea is to increase the CH₄ content in the syngas at the inlet of the cold

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box, for example in order to obtain a methane content of at least 1.8% and preferably at least 2% and more advantageously still of 2.3%, and the like.

5 It is sometimes possible to carry out a methane scrubbing process with a feed gas comprising at least 1.8% of methane, generally possible with a feed gas comprising at least 2% of methane and in any case possible with a feed gas comprising at least 2.3% of
10 methane.

It is very obviously possible to enrich a syngas comprising at most 1.8% of methane in order to obtain a gas comprising at least 2% of methane, indeed even 2.3%
15 of methane, as it is possible a syngas comprising at most 2% of methane in order to obtain a gas comprising at least 2.3% of methane, according to the invention.

It is also a question of introducing solutions for
20 treating the C₂+ components which might be present in the syngas.

According to one subject matter of the present disclosure, provision is made for a process for the generation and
25 separation of syngas in which a syngas is generated from a methane-rich feedstock gas, for example natural gas, the syngas, comprising hydrogen and carbon monoxide, is purified by at least one treatment process to produce a purified syngas and the syngas is
30 separated by cryogenic distillation in a plant comprising at least one column for scrubbing with methane to produce a gas enriched in hydrogen and/or a gas enriched in carbon monoxide, the syngas generated comprising less than 2.3% of methane, preferably less
35 than 2% of methane, indeed even less than 1.8% of methane, and the syngas is enriched upstream of the separation by cryogenic distillation by sending a portion of the feedstock gas to a treatment process

downstream of the stage of generation of syngas, without passing through the stage of generation of syngas, to obtain a syngas comprising more than 2.3% of methane if the syngas generated comprises less than 2.3% of methane, or more than 2% of methane if the syngas generated comprises less than 2% of methane, or more than 1.8% of methane if the syngas generated comprises less than 1.8% of methane.

- 10 In one aspect, there is provided a process for the generation and separation of syngas in which a syngas is generated from a feedstock gas, and the syngas is separated by cryogenic distillation in a plant comprising at least one column for scrubbing with methane to produce a gas enriched in hydrogen and/or a gas enriched in carbon monoxide, the syngas generated comprising less than 2.3% of methane, preferably less than 2% of methane, indeed even less than 1.8% of methane, characterized in that the syngas is enriched upstream of the separation by cryogenic distillation by sending a portion of the feedstock gas to a treatment process downstream of the stage of generation of syngas, without passing through the stage of generation of syngas, to obtain a syngas comprising more than 2.3% of methane if the syngas generated comprises less than 2.3% of methane, or more than 2% of methane if the syngas generated comprises less than 2% of methane, or more than 1.8% of methane if the syngas generated comprises less than 1.8% of methane, the feedstock gas is rich in methane and the syngas, comprising hydrogen and carbon monoxide, is purified by the treatment process to produce a purified syngas.

According to other optional embodiments:

- the feedstock gas sent to the treatment process downstream of the stage of generation can originate from a prereformer upstream of the stage of generation and/or from a hydrodesulfurization unit upstream of the stage of generation;
- a methane-rich gas, optionally originating from an external source, is sent downstream of the stage of generation of syngas and upstream of the stage of separation by cryogenic distillation;
- the methane-rich gas is sent to a treatment process upstream of the stage of separation by cryogenic distillation;
- a flow enriched in methane originating from the cryogenic distillation process is sent, optionally after pressurization, downstream of the stage of generation of syngas;
- a flow enriched in methane originating from the cryogenic distillation process is sent to a process for treatment of the syngas;
- the processes for treatment of the syngas comprise at least one of the following processes: removal of acid gases, drying, adsorption of carbon dioxide;
- a methane-rich fluid is withdrawn a few theoretical plates above the tank of a CO/CH₄ column, optionally in order to act as methane-rich gas to be sent, optionally after pressurization, downstream of the stage of generation of syngas, and a tank liquid is withdrawn from the CO/CH₄ column in order to act as

bleed;

- a methane-rich fluid is withdrawn a few theoretical plates above the tank of a CO/CH₄ column, optionally in order to be used for scrubbing at the top of the column for scrubbing with methane, and a tank liquid is withdrawn from the CO/CH₄ column in order to act as bleed;
- the bleed liquid is mixed with a liquid rich in heavy hydrocarbons which is obtained by separation from the syngas in the cryogenic distillation plant.

According to another subject matter of the present disclosure, provision is made for an apparatus for the generation and separation of syngas, comprising a unit for generation of a syngas from a feedstock gas, a unit for purification of syngas comprising hydrogen and carbon monoxide by at least one treatment process to produce a purified syngas and a unit for separation of the syngas by cryogenic distillation comprising at least one column for scrubbing with methane to produce a gas enriched in hydrogen and/or a gas enriched in carbon monoxide, the unit for generation of syngas being adjusted in order to generate a syngas comprising less than 2.3% of methane, preferably less than 2% of

methane, indeed even less than 1.8% of methane, and in that it comprises means for enriching the syngas upstream of the unit for separation by cryogenic distillation in order to obtain a syngas comprising
5 more than 2.3% of methane if the syngas generated comprises less than 2.3% of methane, or more than 2% of methane if the syngas generated comprises less than 2% of methane, or more than 1.8% of methane if the syngas generated comprises less than 1.8% of methane, the
10 enriching means comprising means for sending a portion of the feedstock gas to a treatment process downstream of the stage of generation of syngas, without passing through the stage of generation of syngas.

15 In another aspect, there is provided an apparatus for the generation and separation of syngas, comprising a unit for generation of a syngas from a feedstock gas, for example natural gas, a unit for separation of the syngas by cryogenic distillation comprising at least
20 one column for scrubbing with methane to produce a gas enriched in hydrogen and/or a gas enriched in carbon monoxide, the unit for generation of syngas being adjusted in order to generate a syngas comprising less than 2.3% of methane, preferably less than 2% of
25 methane, indeed even less than 1.8% of methane, and in that it comprises means for enriching the syngas upstream of the unit for separation by cryogenic distillation capable of producing a syngas comprising more than 2.3% of methane if the syngas generated
30 comprises less than 2.3% of methane, or more than 2% of methane if the syngas generated comprises less than 2% of methane, or more than 1.8% of methane if the syngas generated comprises less than 1.8% of methane, characterized in that these enriching means are
35 composed of means for sending a portion of the

feedstock gas which is rich in methane to a treatment process downstream of the unit for generation of syngas, without passing through the unit for generation of syngas and in that it comprises a unit for purification of syngas comprising hydrogen and carbon monoxide for carrying out the treatment process to produce a purified syngas.

According to other optional embodiments, the apparatus comprises:

- means for sending the portion of the feedstock gas taken downstream of a prereformer upstream of the stage of generation;
- means for sending the portion of the feedstock gas taken downstream of a hydrodesulfurization unit upstream of the stage of generation;
- means for sending a methane-rich gas, optionally originating from an external source, downstream of the stage of generation of syngas and upstream of the stage of separation by cryogenic distillation;
- means for sending a flow enriched in methane originating from the process of cryogenic distillation to a process of treatment of the syngas;
- means for sending the methane-rich gas to a treatment process upstream of the stage of separation by cryogenic distillation;
- means for sending a flow enriched in methane originating from the cryogenic distillation process, optionally after pressurization, downstream of the stage of generation of syngas;
- units for treatment of the syngas comprising at least one of the following units: unit for removal of acid

gases, drying unit, unit for adsorption of carbon dioxide;

- means for withdrawing a methane-rich fluid a few theoretical plates above the tank of a CO/CH₄ column, optionally in order to act as methane-rich gas to be sent, optionally after pressurization, downstream of the stage of generation of syngas, and means for withdrawing a tank liquid from the CO/CH₄ column in order to act as bleed;
- means for withdrawing a methane-rich fluid a few theoretical plates above the tank of a CO/CH₄ column, optionally in order to be used for scrubbing at the top of the column for scrubbing with methane, and means for withdrawing a tank liquid from the CO/CH₄ column in order to act as bleed;
- means for mixing the bleed liquid with a liquid rich in heavy hydrocarbons which is obtained by separation from the syngas in the cryogenic distillation plant;
- means for sending a portion of the feedstock gas sent to a unit for removal of acids downstream of the stage of generation, without passing through the unit for generation of syngas;
- means for sending a portion of the feedstock gas sent to an adsorption unit downstream of the stage of generation, without passing through the unit for generation of syngas.

The solution according to the invention is the injection of a CH_4 -rich stream, constituted by part of the feedstock gas which has not been sent to the reactor, into the syngas after the reactor for generation of the syngas and before the column for scrubbing with methane of the cold box.

Examples

1. Recycling of the CH_4 before the cold box (figures 1 and 2):

This is applicable in the case where the CH_4 content in the syngas (before this CH_4 recycling) makes possible a positive CH_4 balance in the cold box but exhibits an excessively high level of CO_2 . In order to lower the level of concentration of CO_2 , the following are provided:

1. The increase in the discharge pressure of the pumps for CH_4 and for CH_4 recycle between the cold box and the upstream of the drying in order to limit the level of concentration of CO_2 in the material withdrawn from the tank of the CO/CH_4 column.
2. The cooling of the top of the scrubbing column in order to reduce the CH_4 content for the hydrogen-rich gas.

2. Prereformer with POX, ATR, SMR (figure 1):

Bypassing the reactor between the outlet of the prereformer and the outlet of the reactor (in order to reduce the content of C_2+ components in the syngas at

the inlet of the cold box, (all the C2+ components of the natural gas feeding the prereformer being converted to CH₄ in the prereformer) provides a positive material balance in the process for scrubbing with methane, a portion of the feedstock at the prereformer outlet being directly injected downstream of the reactor.

1. The increase in the discharge pressure of the pumps for CH₄ and for CH₄ recycle between the cold box and the upstream of the drying makes it possible to limit the level of concentration of CO₂ in the material withdrawn from the tank of the CO/CH₄ column.

2. The cooling at the top of the scrubbing column makes it possible to reduce the CH₄ content in the hydrogen-rich gas.

3. Reactor without prereformer (POX, ATR, SMR) and with HDS (figure 3):

By bypassing the reactor between the outlet of the hydrodesulfurization (HDS) unit and the outlet of the reactor, in order to provide a positive material balance in the process of scrubbing with methane, a portion of the feedstock at the outlet of the HDS is directly injected downstream of the reactor.

Injection of the bypass fluid takes place after the reactor and before the scrubbing column:

- a) if the bypassed fluid comprises CO₂, provision is made for the injection of this fluid between the outlet of the reactor and before the removal of acid gases,
- b) if the bypassed fluid comprises a very small amount of CO₂ (< 50 vpm), provision is made for the injection of this fluid between the outlet of the reactor and before the adsorbers of the drying,

c) if the bypassed fluid does not comprise any CO_2 or H_2O at all, provision is made for the injection of this fluid between the outlet of the reactor and before the column for scrubbing with methane.

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The increase in the discharge pressure of the pumps for CH_4 and for CH_4 recycle between the cold box and the upstream of the drying makes it possible to limit the level of concentration of CO_2 in the CH_4 bleed.

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A vessel for two-phase separation in the cold box at a temperature level of approximately -145°C removes the C_3+ components and prevents them from solidifying when the syngas is cooled to colder temperature levels in the exchange line.

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The addition of a supplementary section in the tank of the CO/CH_4 distillation column is sometimes necessary. The CH_4 bleed is withdrawn at the column tank and comprises the C_2 component.

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The withdrawal at the top of this tank section of the flow for scrubbing with CH_4 and of the CH_4 recycle is used (comprising little C_2 component, it being possible for a high content of C_2 component in the scrubbing circuit to bring about phenomena of foaming or other phenomena and to result in poor operation of the scrubbing column).

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The cooling of the top of the scrubbing column makes it possible to reduce the CH_4 content in the hydrogen-rich gas.

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The processes and apparatuses according to the invention will be described in more detail with reference to the figures, in which figures 1 and 3 represent a process for the generation and separation of a mixture of carbon monoxide and hydrogen according to the invention and figures 2 and 4 show the breakdown of the process for separation of a mixture of carbon monoxide and hydrogen suitable for incorporation therein.

Figure 1 shows a process in which a feedstock gas 1, which can be a methane-rich gas, such as natural gas, is sent to a hydrodesulfurization (HDS) unit 3, as described in "Desulphurization" by Kyte, IChemE, 1995.

The gas produced 5 is sent to a prereformer 7. At the outlet of the prereformer, the gas is composed essentially of CH_4 , the C_2+ components are converted to CH_4 and the CH_4 is only very slightly converted to syngas.

The gas exiting from the prereformer is separated in order to form a bypassing flow 11 and a flow 9. The flow 9 is sent to the reactor 13 of the SMR or ATR type, and the like, in order to produce a syngas 15 comprising less than 2.3% of methane, preferably less than 2% of methane, indeed even less than 1.8% of methane, with which the bypassing flow 11 is mixed. The mixture is sent to the unit for removal of acid gases 17, in order to produce a purified gas 19. The purified gas 19 is sent to an adsorption unit 21 in order to be dried and purified from CO_2 , in order to form a gas 23. The gas 23 is cooled and sent to a cryogenic distillation unit 35 operating by scrubbing with methane. This unit is illustrated in more detail in figure 2. It comprises a column for scrubbing with methane 29, a stripping column 31 and a CO/CH_4 separation column 33 inside a cold box 35. Liquid

methane is withdrawn at the tank of the CO/CH₄ column 33, evaporated, optionally after pumping by the pump 27, and taken out of the cold box as flow 43 and/or 45. The pump 27 can also be used to send methane 37 to the column for scrubbing with methane 29.

A portion 47 of the methane can act as bleed and the remainder 49 can be recycled, optionally after compression, upstream or downstream of the unit for removal of acid gases as flow 51 or 53.

In this way, the methane content of the flow 15 on arriving in the removal unit 17 rises to at least 1.8% of methane, preferably at least 2% of methane, indeed even 2.3% of methane.

Hydrogen-rich gases 39, 41 are produced by the scrubbing column 29 and the stripping column 31.

In figure 2, the purified gas 19 is sent to the adsorption unit 21 of figure 1 in order to be dried and purified from CO₂, in order form a gas 23. The gas 23 is cooled and sent to a cryogenic distillation unit 35 operating by scrubbing with methane. It comprises a column for scrubbing with methane 29, a stripping column 31 and a CO/CH₄ separation column 33 inside a cold box. The gas 23 is cooled in the exchanger 48 and is sent to the tank of the column for scrubbing with methane 29. The tank liquid 61 from this column 29 is sent to the stripping column 31 and the tank liquid 63 from the stripping column is sent to an intermediate point of the CO/CH₄ column 33. Liquid methane is withdrawn at the tank of the CO/CH₄ column 33, evaporated in the exchanger 48, optionally after pumping by the pump 27, and taken out of the cold box as flow 49. The pump 27 can also be used to send methane 37 to the column for scrubbing with methane 29 and methane 65 to the top of the stripping column 31.

The flow 49 is recycled, optionally after compression, upstream or downstream of the unit for removal of acid gases as flow 51 or 53.

- 5 Hydrogen-rich gases 39, 41 are produced by the scrubbing column 29 and the stripping column 31.

10 A gas or a liquid 55 rich in carbon monoxide is withdrawn at the top of the CO/CH₄ column, heated (and optionally evaporated) in the exchanger 48 and optionally compressed in a compressor 57 in order to form the product.

15 Figure 3 shows a process in which the syngas is produced by a reactor 13 of POX, ATR or SMR type without prereformer and with HDS in which a methane-rich feedstock gas 1, which can be natural gas, is sent to a hydrodesulfurization unit 3. The gas produced is divided into two, one portion 5 being sent to a reactor 20 13. The remainder of the gas forms a bypassing flow. The reactor 13 produces a syngas 15 comprising less than 2.3% of methane, preferably less than 2% of methane, indeed even less than 1.8% of methane, with which the bypassing flow 11 is mixed if this flow 25 comprises CO₂. The mixture is sent to the unit for removal of acid gases 17 in order to produce a purified gas 19. The bypassing flow 11A can be mixed therewith if it comprises less than 50 vpm of CO₂. The purified gas 19 is sent to an adsorption unit 21 in order to be 30 dried and purified from CO₂, in order to form a gas 23. The bypassing flow 11B can be mixed therewith if it does not comprise any CO₂ at all. The gas 23 is cooled and sent to a cryogenic distillation unit 35 operating by scrubbing with methane. This unit is illustrated in more detail in figure 2. It comprises a separation 35 vessel 28 in order to remove the C3+ components, a column for scrubbing with methane 29, a stripping

column 31 and a CO/CH₄ separation column 33 inside a cold box 35. Liquid methane is withdrawn a few stages above the tank of the CO/CH₄ column 33, evaporated, optionally after pumping by the pump 27, and taken out of the cold box as flow 45. The pump 27 can also be used to send methane 37 to the column for scrubbing with methane 29.

A portion 47 of the methane can be used as bleed and the remainder 49 can be recycled, optionally after compression, upstream or downstream of the unit for removal of acid gases as flow 51 or 53. In this way, the methane content of the flow 15 on arriving in the removal unit 17 rises to at least 1.8% of methane, preferably at least 2% of methane, indeed even 2.3% of methane.

Hydrogen-rich gases 39, 41 are produced by the scrubbing column 29 and the stripping column 31. A methane-rich fluid comprising C₂ components is withdrawn from the tank of the CO/CH₄ column 33 and mixed with the fluid rich in C₃+ components 30 originating from the vessel 28, and the mixture 43 is taken out of the cold box.

In figure 4, the purified gas 19 is sent to the adsorption unit 21 of figure 3 in order to be dried and purified from CO₂, in order to form a gas 23. The gas 23 is cooled and sent to a cryogenic distillation unit 25 operating by scrubbing with methane. It comprises a column for scrubbing with methane 29, a stripping column 31 and a CO/CH₄ separation column 33 inside a cold box. The gas 23 is partially cooled in the exchanger 48 and is sent to a separation vessel 28. The gas produced 34 is sent to the tank of the column for scrubbing with methane 29. The tank liquid 61 from this column 29 is sent to the stripping column 31 and the tank liquid 63 from the stripping column is sent to an

intermediate point of the CO/CH₄ column 33. Liquid methane is withdrawn a few stages above the tank of the CO/CH₄ column 33, evaporated in the exchanger 48, optionally after pumping by the pump 27, and taken out
5 of the cold box as flow 49. The pump 27 can also be used to send methane 37 to the column for scrubbing with methane 29 and methane 65 to the top of the stripping column 31.

10 The fluid 34, which is the tank methane from the column 33, can be pumped by the pump 27 before being mixed with the liquid 30 originating from the vessel 28 and the mixture 43 is sent to the exchanger 48 and can be used subsequently as fuel.

15 A portion of the flow 49 is recycled, optionally after compression, upstream or downstream of the unit for removal of acid gases as flow 51 or 53. Optionally, a portion of the methane composed of the fluid 47 can be
20 used as fuel.

A gas or a liquid 55 rich in carbon monoxide is withdrawn at the top of the CO/CH₄ column, heated (and optionally evaporated) in the exchanger 48 and
25 optionally compressed in a compressor 57 in order to form the product.

Hydrogen-rich gases 39, 41 are produced by the scrubbing column 29 and the stripping column 31.

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WHAT IS CLAIMED IS:

1. A process for the generation and separation of syngas in which a syngas (15) is generated from a feedstock gas, and the syngas is separated by cryogenic distillation in a plant (25) comprising at least one column for scrubbing with methane (29) to produce a gas enriched in hydrogen and/or a gas enriched in carbon monoxide, the syngas generated (15) comprising less than 2.3% of methane, preferably less than 2% of methane, indeed even less than 1.8% of methane, characterized in that the syngas is enriched upstream of the separation by cryogenic distillation by sending a portion (11, 11A, 11B) of the feedstock gas to a treatment process downstream of the stage of generation of syngas, without passing through the stage of generation of syngas, to obtain a syngas comprising more than 2.3% of methane if the syngas generated comprises less than 2.3% of methane, or more than 2% of methane if the syngas generated comprises less than 2% of methane, or more than 1.8% of methane if the syngas generated comprises less than 1.8% of methane, the feedstock gas is rich in methane and the syngas, comprising hydrogen and carbon monoxide, is purified by the treatment process to produce a purified syngas.
2. The process as claimed in claim 1, in which a methane-rich gas (51, 53, 71, 71A, 71B, 71C), optionally originating from an external source, is sent downstream of the stage of generation of syngas and upstream of the stage of separation by cryogenic distillation.
3. The process as claimed in claim 2, in which the methane-rich gas (51, 53, 71, 71A, 71B, 71C) is sent to a treatment process upstream of the stage

of separation by cryogenic distillation.

4. The process as claimed in one of the preceding claims, in which the processes for treatment of the syngas comprise at least one of the following processes: removal of acid gases, drying, adsorption of carbon dioxide.
5. The process as claimed in one of the preceding claims, in which a methane-rich fluid (43, 51) is withdrawn a few theoretical plates above the tank of a CO/CH₄ column (33), in order to act as methane-rich gas to be sent, optionally after pressurization, downstream of the stage of generation of syngas, and a tank liquid (34) is withdrawn from the CO/CH₄ column in order to act as bleed.
6. The process as claimed in one of the preceding claims, in which a methane-rich fluid (37) is withdrawn a few theoretical plates above the tank of a CO/CH₄ column, in order to be used for scrubbing at the top of the column for scrubbing with methane, and a tank liquid is withdrawn from the CO/CH₄ column in order to act as bleed.
7. The process as claimed in claim 6, in which the bleed liquid (34) is mixed with a liquid (30) rich in heavy hydrocarbons which is obtained by separation from the syngas in the cryogenic distillation plant.
8. The process as claimed in one of the preceding claims, in which the portion (11, 11A, 11B) of the feedstock gas sent to the treatment process downstream of the stage of generation, without passing through the stage of generation of syngas,

originates from a prereformer (7) upstream of the stage of generation.

5 9. The process as claimed in one of the preceding
 claims, in which the portion (11, 11A, 11B) of the
 feedstock gas sent to the treatment process
 downstream of the stage of generation, without
 passing through the stage of generation of syngas,
 originates from a hydrodesulfurization unit (3)
10 upstream of the stage of generation.

 10. An apparatus for the generation and separation of
 syngas, comprising a unit for generation of a
15 syngas from a feedstock gas, for example natural
 gas, , a unit for separation of the syngas by
 cryogenic distillation comprising at least one
 column for scrubbing with methane to produce a gas
 enriched in hydrogen and/or a gas enriched in
20 carbon monoxide, the unit for generation of syngas
 being adjusted in order to

generate a syngas comprising less than 2.3% of methane, preferably less than 2% of methane, indeed even less than 1.8% of methane, and in that it comprises means for enriching the syngas upstream of the unit for separation by cryogenic distillation capable of producing a syngas comprising more than 2.3% of methane if the syngas generated comprises less than 2.3% of methane, or more than 2% of methane if the syngas generated comprises less than 2% of methane, or more than 1.8% of methane if the syngas generated comprises less than 1.8% of methane, characterized in that these enriching means are composed of means for sending a portion (11, 11A, 11B) of the feedstock gas which is rich in methane to a treatment process downstream of the unit for generation of syngas, without passing through the unit for generation of syngas and in that it comprises a unit for purification of syngas comprising hydrogen and carbon monoxide for carrying out the treatment process to produce a purified syngas.

11. The apparatus as claimed in claim 10, in which the means for sending the portion (11, 11A, 11B) of the feedstock gas to the treatment process downstream of the stage of generation, without passing through the unit for generation of syngas, are connected to a prereformer (7) upstream of the generation unit (13).

12. The apparatus as claimed in claim 10 or 11, in which the means for sending a portion (11, 11A, 11B) of the feedstock gas to the treatment process downstream of the stage of generation, without passing through the unit for generation of syngas, are connected to a hydrodesulfurization unit (3) upstream of the generation unit (13).

13. The apparatus as claimed in one of claims 10 to 12, comprising means for sending the portion of the feedstock gas to a unit for removal of acids (17) downstream of the generation unit (13),

without passing through the unit for generation of syngas.

14. The apparatus as claimed in one of claims 11 to 13, comprising means for sending the portion of the feedstock gas to an adsorption unit (21) downstream of the generation unit (13) or directly to the separation unit (35), without passing through the unit for generation of syngas.