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Description

This invention relates to a highly crystalline zeolite material, its preparation and use in catalysis, particularly for aromatization. In particular it relates to zeolite L with cylindrical morphology.

Zeolite L has been known for some time as an adsorbant, and in US 3 216 789 is described as an aluminosilicate of the formula:



(where M is an exchangeable cation of valence n and y is from 0 to 9) having an X-ray diffraction pattern with the following more significant d(Å) values:

	16.1±0.3
	7.52±0.04
15	6.00±0.04
	4.57±0.04
	4.35±0.04
	3.91±0.02
20	3.47±0.02
	3.28±0.02
	3.17±0.01
	3.07±0.01
	2.91±0.01
25	2.65±0.01
	2.46±0.01
	2.42±0.01
	2.19±0.01

The preparation of zeolite L described in US 3 216 789 comprises crystallizing the zeolite from a reaction mixture comprising mole ratios:

	$K_2O/(K_2O+Na_2O)$	0.33—1
35	$(K_2O+Na_2O)/SiO_2$	0.35—0.5
	SiO_2/Al_2O_3	10—28
	$H_2O/(K_2O+Na_2O)$	15—41

The silica to alumina ratio in this reaction mixture is significantly higher than the ratio in the formed zeolite.

British Patent 1 202 511 describes a revised zeolite L preparation using lower proportions of silica in the reaction mixture which comprises mole ratio of reactants as:

45	$K_2O/(K_2O+Na_2O)$	0.7—1
	$(K_2O+Na_2O)/SiO_2$	0.23—0.35
	SiO_2/Al_2O_3	6.7—9.5
50	$H_2O/(K_2O+Na_2O)$	10.5—50

The ratio $H_2O/(K_2O+Na_2O+SiO_2+Al_2O_3)$ is preferably not greater than 6 to give a "dry gel".

US 3 867 512 discloses a preparation of zeolite L from a reaction mixture having a molar composition:

55	$K_2O/(K_2O+Na_2O)$	0.3—1
	$(K_2O+Na_2O)/SiO_2$	0.3—0.6
60	SiO_2/Al_2O_3	10—40
	$H_2O/(K_2O+Na_2O)$	15—140

in which the silica source is a gel having at least 4.5 weight percent water and prepared in a particular manner.

L Wilkosz in *Pr Chem* 409 (1974)—Chemical Abstracts, vol 90 (1979) 573478 describes the preparation of zeolite L from a synthesis sol prepared by treating a solution containing silica, potassium hydroxide and sodium hydroxide with a second solution containing potassium aluminate, potassium hydroxide and sodium hydroxide and crystallizing for 72 hours at 20°C and 122 hours at 100°C. The zeolite L product has a $\text{SiO}_2:\text{Al}_2\text{O}_3$ ratio of 6.4:1.

G V Tsitsishvili *et al* in *Doklady Akademii NaukSSSR*, Vol 243, No. 2, pp 438—440 (1978) describe the synthesis of zeolite L from alumina-silica gels containing tributylamine. The gels used had the following molar ratios:

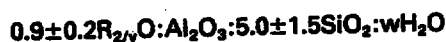
	$\text{SiO}_2:\text{Al}_2\text{O}_3$	25
10	$(\text{K}_2\text{O}+\text{Na}_2\text{O}):\text{Al}_2\text{O}_3$	18
	$(\text{K}_2\text{O}+\text{Na}_2\text{O}):\text{SiO}_2$	0.72
15	$\text{H}_2\text{O}/\text{K}_2\text{O}+\text{Na}_2\text{O}$	20
	$\text{K}_2\text{O}:\text{Na}_2\text{O}$	0.5

Y Nishiimura in *Nippon Kagaku Zasshi* 91, 11, 1970, pp 1046—9 describes in general terms zeolite L preparation from a synthesis mixture containing colloidal silica, potassium aluminate and potassium hydroxide having a $\text{SiO}_2:\text{Al}_2\text{O}_3$ ratio of 15—25, but exemplified only two synthesis mixtures having the following ratios of components.

25	$7\text{K}_2\text{O}:\text{Al}_2\text{O}_3:20\text{SiO}_2:450\text{H}_2\text{O}$ and
	$8\text{K}_2\text{O}:\text{Al}_2\text{O}_3:10\text{SiO}_2:500\text{H}_2\text{O}$.

Frety *et al* in *C R Acad Se Paris*, t275, Serie C-1215 describes the electron microscope examination of zeolite L in which particles were said to be observed in the form of slightly deformed cylinders with very variable dimensions.

US 3 298 780 describes zeolite UJ having a composition, expressed as mole ratios of oxides, corresponding to



wherein R represents at least one cation having a valence of not more than 4, v represents the valence of R and w can be any value up to about 5, said zeolite having an X-ray powder diffraction pattern essentially as shown in the following table:

	Interplanar spacing, d(Å)	Relative intensity
40	16.25 ± 0.25	VS
	7.55 ± 0.15	M
45	6.50 ± 0.10	M
	5.91 ± 0.10	W
	4.61 ± 0.05	S
50	3.93 ± 0.05	S
	3.67 ± 0.05	W
55	3.49 ± 0.05	M
	3.29 ± 0.05	W
	3.19 ± 0.05	M
60	3.07 ± 0.05	M
	2.92 ± 0.05	M
65	2.66 ± 0.05	W

prepared by a process comprising preparing an aqueous reactant solution having a composition, expressed as mole ratios of oxides, corresponding to

$\text{SiO}_2/\text{Al}_2\text{O}_3$ of from 6 to 30,

$\text{R}_{2\nu}\text{O}/\text{SiO}_2$ of from 0.30 to 0.70, and

5 $\text{H}_2\text{O}/\text{R}_{2\nu}\text{O}$ of from 80 to 140;

and maintaining said reactant solution at a temperature between 150°F (65.6°C) and 325°F (162.8°C) until the zeolite crystals are formed. Zeolite UJ is described as having nearly cubic shaped crystals with a crystal size ranging upward from 0.05 micron.

10 water:
GB 1 393 365 describes zeolite AG1, related to zeolite L, having the molar composition other than



15 wherein M is potassium or a mixture of potassium and sodium, and an X-ray powder diffraction pattern substantially as set forth in Columns I and II of the following table, and capable of adsorbing at least 3% w/w perfluorotributylamine.

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	Column I Potassium zeolite AG1		Column II Potassium/sodium zeolite AG1	
	d(A)	Relative intensity	d(A)	Relative intensity
5	15.85	36.9	15.78	37.5
10	—	—	—	—
	7.53	8.5	7.50	10
	6.00	9.5	6.00	10
15	—	—	5.86	7
	5.75	6	—	—
20	4.61	24	4.59	28
	4.40	7	4.40	7
	4.35	5	—	—
25	3.93	31	3.91	35
	—	—	—	—
30	3.66	13	3.65	17
	3.48	17	3.47	23
	3.27	13	3.27	17
35	3.186	29	3.18	31.5
	3.07	20	3.07	24
40	3.01	9.5	—	—
	2.91	21.5	2.91	28
	2.65	15.5	2.65	18.5
45	—	—	—	—
	—	—	2.50	6
50	2.49	5	—	—
	2.46	3	2.46	5
	2.42	3	2.42	4
55	2.19	8	2.19	12

Zeolite AG1 is described as being prepared by reacting at least one aluminium component, at least one silicon component and at least one alkali metal component, in an aqueous medium, the sole or major silicon component being a water glass having a molar ratio $\text{SiO}_2/\text{M}_2\text{O}$ of 3.5 to 4.0 to give a reaction mixture with oxide molar ratios in one of the following ranges:

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5	Range 1	$\text{SiO}_2/\text{Al}_2\text{O}_3$	7—14
		$(\text{K}_2\text{O}+\text{Na}_2\text{O})/\text{SiO}_2$	0.25—0.85
		$\text{K}_2\text{O}/(\text{K}_2\text{O}+\text{Na}_2\text{O})$	0.75—1.0
		$\text{H}_2\text{O}/(\text{K}_2\text{O}+\text{Na}_2\text{O})$	25—160
10	Range 2	$\text{SiO}_2/\text{Al}_2\text{O}_3$	14—20
		$(\text{K}_2\text{O}+\text{Na}_2\text{O})/\text{SiO}_2$	0.25—0.85
		$\text{K}_2\text{O}/(\text{K}_2\text{O}+\text{Na}_2\text{O})$	0.5—1.0
		$\text{H}_2\text{O}/(\text{K}_2\text{O}+\text{Na}_2\text{O})$	25—160
15	Range 3	$\text{SiO}_2/\text{Al}_2\text{O}_3$	20—40
		$(\text{K}_2\text{O}+\text{Na}_2\text{O})/\text{SiO}_2$	0.25—1.0
		$\text{K}_2\text{O}/(\text{K}_2\text{O}+\text{Na}_2\text{O})$	0.4—1.0
		$\text{H}_2\text{O}/(\text{K}_2\text{O}+\text{Na}_2\text{O})$	25—160

It was subsequently found that zeolite L may be used as a catalyst base in aromatization reactions. US 4 104 320 discloses dehydrocyclization of aliphatic compounds in the presence of hydrogen using a catalyst comprising zeolite L and a group VIII metal, in which the zeolite L is of the formula:



(where M is a cation of valence n) but the silica to alumina ratio may vary from 5 to 7. Zeolite L is described as occurring in the form of cylindrical crystals a few hundred Angstroms in diameter.

East German Patent 88789 discloses dehydrocyclization using a catalyst formed from a zeolite precursor with a silica to alumina ratio of 5 or greater which is dealuminised to give a silica to alumina ratio of up to 70. Zeolite L is mentioned as a precursor.

European Patent Application Publication 40119 discloses a dehydrocyclization process operating at low pressure (1 to 7 bars) or low H_2 /hydrocarbon ratio using a catalyst comprising platinum on a potassium zeolite L. BE 888365 describes dehydrocyclization using a catalyst comprising platinum, rhenium (incorporated in the form of its carbonyl) and sulphur to give an atomic ratio of sulphur to platinum of 0.05 to 0.6 on a zeolitic crystalline aluminosilicate base such as zeolite L. BE 792608 discloses the treatment of zeolite L for use as catalyst in isomerization by exchange with ammonium and chromium ions.

It has now been found that a new zeolitic material having some similar characteristics to zeolite L, but having a characteristic morphology and size is particularly valuable for use as a catalyst base in hydrocarbon conversions such as aromatization.

Thus, in one aspect this invention concerns a zeolite having an X-ray diffraction (XRD) pattern obtained with $\text{CuK}\alpha$ radiation having the following significant $d(\text{\AA})$ values:

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TABLE A

	16.1±0.4
5	7.52±0.05
	6.00±0.04
10	4.57±0.04
	4.35±0.04
	3.91±0.02
15	3.47±0.02
	3.28±0.02
20	3.17±0.02
	3.07±0.02
25	2.91±0.02
	2.65±0.02
	2.46±0.02
30	2.42±0.01
	2.19±0.01

and comprising crystallites of which at least 50% are in the form of distinct circular cylinders with a mean diameter of at least 0.5 micron and an aspect ratio of at least 0.5.

The above XRD lines characterize the zeolite of the invention and correspond to those identified as characteristic of zeolite L in US 3 216 789. The spectrum of the zeolite of the invention will also generally show additional lines, and more complete listings of the d(Å) values for specific materials of the invention are given hereinafter. In general the ten most prominent peaks in the XRD pattern of the materials of the invention are given in Table B below:

TABLE B

	16.1±0.4
45	4.57±0.04
	3.91±0.02
50	3.66±0.02
	3.47±0.02
	3.28±0.02
55	3.17±0.02
	3.07±0.02
60	2.91±0.02
	2.65±0.02

The positions and relative intensities of the X-ray lines are found to vary only slightly with changes in the cation form of the materials. However, the intensity of the line at d=16.1±0.4 Å has been observed to be more variable than that of other prominent lines. This is believed to be a result of the sensitivity of this peak

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to the preparation of the XRD sample and not to significant changes in crystal structure of the zeolite. Occasionally, additional lines not belonging to the pattern for zeolite L appear in a pattern along with the X-ray lines characteristic of the zeolite. This is an indication that one or more additional crystalline materials are mixed with zeolite L in the sample being tested. It is a preferred feature of the invention that the amount of such additional crystalline materials is minimised in the zeolite material as synthesized. In particular, as discussed in more detail hereinafter, it is preferred that the synthesis of the zeolite of the invention is conducted so that the amount of zeolite W in the product of the synthesis is minimized. Further, the synthesis of the zeolite of the invention is preferably conducted such that the product of the synthesis is substantially free of any additional crystalline phase giving rise to a line in the X-ray pattern at $d(\text{\AA})$ value of 6.28 ± 0.05 .

The particular X-ray technique and/or apparatus employed, the humidity, the temperature, the orientation of the crystals in the sample and other variables, all of which are well known and understood to those skilled in the art of X-ray crystallography or diffraction, may also cause some variations in the positions and intensities of the X-ray lines. Thus, the X-ray data given herein to identify the zeolites of the invention are not to exclude those materials which, due to some variable mentioned above or otherwise known to those skilled in the art fail to show all of the tabulated X-ray lines, or show a few extra ones that are permissible to the crystal system of the zeolite, or show a shift in position or slight change in intensity of some of the X-ray lines.

The zeolites of the invention are preferably aluminosilicates and will be described hereinafter in terms of aluminosilicates, though other elemental substitutions are possible, for example aluminium may be substituted by gallium, boron, iron and similar trivalent elements, and silicon may be substituted by elements such as germanium or phosphorus. The aluminosilicates preferably have a composition (expressed in terms of molar ratios of the constituent oxides in anhydrous form) of:



wherein M is a cation of valence n, x is from 5 to 7.5, preferably from 5.7 to 7.4. The zeolitic materials of the invention have high crystallinity as shown by a well-defined X-ray diffraction pattern (without binder or other diluents present) with sharp peaks. Crystallinity may be measured relative to a quartz standard by comparing the peak areas for the reflection from the 220 plane ($d=4.57 \pm 0.04 \text{\AA}$) and the 221 plane ($d=3.91 \pm 0.02$) for the zeolitic material of the invention with the peak area for the reflection from the 110 plane ($d=2.46 \pm 0.02$) of the quartz. The ratio of the combined peak areas of the 220 and 221 reflections of the zeolitic material to the peak area of the 110 reflection of quartz is a measure of the crystallinity of the sample. To provide a comparison between different samples and to eliminate cation effects the peak area determination is preferably carried out on the same cation form of the zeolite, and in the Examples given herein the potassium form was chosen.

The exchangeable cation M in general formula I is very preferably potassium, but it is possible for a part of M to be replaced by other cations such as alkali and alkaline earth metals for example sodium, rubidium or caesium. The ratio $M_{2n}O:Al_2O_3$ is preferably from 0.95 to 1.15, and generally above 1.

In the general formula I x (the mole ratio $SiO_2:Al_2O_3$) is more preferably from 6 to 7 and most preferably from 6.0 to 6.5.

The aluminosilicate forms of the invention may be hydrated, typically with from 0 to 9 moles of water per mole of Al_2O_3 . When used as a catalyst base, as described hereinafter, the zeolite of the invention is preferably first calcined to remove water. In normal preparation from aqueous gels a hydrated form is first prepared and this may be dehydrated by heating.

Scanning electron micrographs (SEM) of the materials of the invention show these to have very distinct crystal morphology. As described in more detail hereinafter, preferred materials of the invention appear as distinct circular cylinders in scanning electron micrographs. The terms "cylinder" and "cylindrical" are used herein to describe particles having substantially the shape of a cylinder as defined in solid geometry—that is, a solid bounded by a surface generated by a line moving parallel to a fixed line so as to cut a fixed plane curve and by two parallel planes (bases) which cut the surface. The use of these terms is not intended to exclude particles having generally cylindrical form but having minor surface irregularities or displaying typical crystallographic faults or dislocations. The cylindrical particles of the invention are substantially in the form of circular cylinders (circular cross-section) and preferably substantially in the form of right circular cylinders (wherein the bases are normal to the cylinder axis). The cylindrical particles have an aspect ratio (the length of the cylinder surface to the diameter of the cylinder) of at least 0.5.

Cylindrical particles have been shown to have excellent properties of extending catalyst life when used as catalyst bases for aromatization catalysts. This is in contrast to other morphologies, and in particular particles with cylindrical morphology have been shown better than particles with a clam-like shape. The term "clam" is used to describe particles having two generally convex faces joined to give the appearance of a clam shell. The aluminosilicates of the invention have at least 50%, preferably 70% and more preferably 85%, of the crystalline being cylinders. The aspect ratio of the cylindrical crystallites is preferably from 0.5 to 1.5.

A further particularly surprising feature of the invention is that large crystallites wherein the mean diameter of the cylinders is at least 0.5 micron may be prepared.

The crystallites are more preferably from 0.5 to 4 μ , and most preferably from 1.0 to 3.0 μ . It is a further feature of the invention that there is a relatively narrow particle size distribution, and preferably substantially all the cylindrical particles of zeolite fall within the range of from 0.5 to 4 μ . Transmission electron diffraction indicate these are single crystals rather than agglomerates. It is a further surprising feature of the invention that the zeolite with cylindrical morphology may be prepared by controlling the composition of the reaction mixture within certain limits, depending upon the aspect ratio required, and that by operating within these limits it is possible to obtain relatively large cylindrical particles in a narrow size distribution. Thus, in another aspect the invention also provides a process for the preparation of aluminosilicate zeolites of the invention with at least 50% of the crystallites in the form of distinct circular cylinders with a mean diameter of at least 0.5 micron and an aspect ratio of at least 0.5, in which an alkaline reaction mixture comprising water, a source of silicon and a source of aluminium with a composition falling within the following molar ratios (expressed as oxides):

15	M_2O/SiO_2	0.22—0.36
	H_2O/M_2O	25—90
20	SiO_2/Al_2O_3	6—15

(wherein M is a cation of valence n, and preferably potassium or a mixture of K+M' in which M' is an alkali metal or alkaline earth metal such as sodium, calcium, barium, or rubidium, provided that $K_2O/(M'_2O+K_2O)$ is at least 0.7) is heated to a temperature of from at least 75°C and preferably from 100°C to 250°C, more preferably from 120°C to 225°C, to form the desired cylindrical aluminosilicate.

The ratio of $H_2O/(K_2O+M'_2O+SiO_2+Al_2O_3)$ is preferably greater than 6 and most preferably greater than 8.

There are four principle components to the reaction mixture or synthesis gel and thus generally:

30	aluminium	
	silicon	
	potassium	(optionally with up to 30 mole% replaced by alkali or alkaline earth metal)
35	water	

and the relative proportions of these four components and the chosen reaction conditions are important if the desired cylindrical aluminosilicates of the invention with an aspect ratio of at least 0.5 are to be obtained. The proportions of the four components can be shown graphically in a series of four triangular graphs each showing the percentage composition of three components of the reaction with the content the fourth component being excluded from each graph. As described in more detail hereinafter Figures 1 to 4 shows such plots for preferred reaction mixtures giving aluminosilicates of the invention with an aspect of at least 0.5 and by way of comparison, for reaction mixtures giving conventional zeolite L and other zeolite and non-zeolite products. These graphs show the composition of reaction mixtures in which M is potassium alone, but it is to be understood that as described hereinbefore up to 30 mole% of potassium may be replaced by another alkali or alkaline earth metal and the graphs are to be interpreted with that in mind.

The four graphs together may be considered as the four faces of a three-dimensional graph in the form of a regular tetrahedron, and the points and areas marked thereon represent the projection on those faces of points and volumes within the three-dimensional graph. Thus, while a point may lie within the area designated as constituting the invention in one graph, unless it lies within the area of the invention on all four graphs it does not lie within the volume defined within the three-dimensional graph as being a preferred reaction mixture of the invention.

Figure 1 is a triangular graph of the content of the reaction mixture (in weight percentage of oxides excluding alumina) showing the relative properties of water, silicon and potassium. To obtain the preferred aluminosilicates of the invention the reaction mixture should desirably lie within the area marked I_A in the graph, preferably within the area marked II_A in the graph and most preferably within the area marked III_A in the graph.

Figure 2 is a triangular graph of the content of the reaction mixture (in weight percent of oxides excluding water) showing the relative properties of aluminium, silicon and potassium. To obtain the preferred aluminosilicates of the invention the reaction mixture should desirably lie within the area marked I_B in the graph, preferably within the area II_B in the graph and most preferably within the area marked III_B in the graph.

Figure 3 is a triangular graph of the content of the reaction mixture (in weight percent of oxides excluding silica) showing the relative properties of aluminium, water and potassium. To obtain the

preferred aluminosilicates of the invention the reaction mixture should desirably lie within the area marked I_c in the graph, preferably within the area II_c in the graph and most preferably within the area marked III_c in the graph.

Figure 4 is a triangular graph of the content of the reaction mixture (in weight percent of oxides excluding potassium oxide) showing the relative properties of aluminium, silicon and water. To obtain the preferred aluminosilicates of the invention the reaction mixture should desirably lie within the area marked I_o in the graph, preferably within the area II_o in the graph and most preferably within the area marked III_o in the graph.

Very preferably the reaction mixture falls within the areas marked III_A, III_B, III_C and III_o in the graphs of Figures 1, 2, 3 and 4, respectively. Such a reaction mixture results in the highest proportion of well-defined crystals particularly when the reaction mixture is heated to the preferred temperature range of 120°C to 225°C, and most preferably to a temperature of about 150°C.

Zeolite W tends to be formed in some extremes of gel composition. It is advantageous for the zeolite W content of the product to be minimized. The zeolite W content of the product can be monitored by its X-ray diffraction pattern. A characteristic prominent line in the zeolite W XRD pattern is at $2\theta = 12.6^\circ$ ($d = 7.09\text{\AA}$), while a prominent line in the zeolite L XRD pattern is at $2\theta = 22.7^\circ$ ($d = 3.91\text{\AA}$). The relative peak intensities of these peaks can be compared to determine the relative proportions of the two zeolite types, since these peaks are not obscured in mixtures of the two zeolites. It is a preferred feature that zeolite of the invention has an XRD pattern in which the peak height ratio ($d = 7.09\text{\AA}$)/($d = 3.91\text{\AA}$) is not greater than 0.2. Very preferably the product is substantially free of zeolite W as evidenced by an absence of the XRD pattern of a line at a d spacing of $7.09\text{\AA}$. To achieve this low level of zeolite W contamination the reaction mixture preferably comprises the reactants in the following molar ratios:

$$M_{2/n}O/SiO_2 = > 0.25$$

$$H_2O/M_{2/n}O = < 65$$

$$SiO_2/Al_2O_3 = 7.5 - 10.5$$

Products with particularly high peak intensities, measured as defined hereinbefore, have been obtained by employing a reaction mixture comprising the reactants in the following molar ratios:

$$M_{2/n}O/SiO_2 = 0.21 - 0.36$$

$$H_2O/M_{2/n}O = 28 - 80$$

$$SiO_2/Al_2O_3 = 8.5 - 10.7$$

Furthermore, the formation of crystallites with cylindrical morphology with an aspect ratio in excess of 0.5 is found to be favoured by employing a reaction mixture comprising the reactants in the following molar ratios:

$$M_{2/n}O/SiO_2 = > 0.2$$

$$H_2O/M_{2/n}O = > 40$$

$$SiO_2/Al_2O_3 = < 22$$

In particular, an optimum composition for a process in which the reaction mixture is heated to from 120°C to 225°C has been found to be substantially in the following mole ratios:



and particularly good results have been obtained by heating to about 150°C. Investigation of individual variations in the components at a crystallization temperature of 150°C has shown that good yields of cylindrical aluminosilicate are obtained if the water content in the optimum composition is reduced to 120 moles in the above ratio, but that further reduction in the water content still results in the formation of a good yield of Zeolite L but increasingly in the form of clam-shaped particles. In particular, at 80 moles water a high yield of clams is obtained. Thus, at the mole ratio of $H_2O/K_2O + Na_2O + Al_2O_3 + SiO_2$ less than 8 specified in GB 1 202 511 the aluminosilicates of the invention are not obtained. If the water content in the optimum ratio is increased the aluminosilicate of the invention is still obtained at 240 moles water, but at 320 moles water a significant amount of contaminating Zeolite W phase is obtained.

Similarly it is possible to obtain the aluminosilicate of the invention if the silica content in the optimum composition is varied between about 8 and about 12 moles, but at higher levels of silica there is an

increasing proportion of amorphous material and at lower levels of silica Zeolite W again is produced in larger amounts. 24

The reaction mixture is particularly sensitive to the content of K_2O (or of M_2O as defined hereinbefore) and variations in the K_2O content in the optimum composition beyond the range of about 0.24 to about 0.30 moles gave at higher levels of K_2O an increasing proportion of clam-shaped Zeolite L particles and at lower levels of K_2O a less crystalline product.

The variation of alumina content from that specified in the optimum composition set out above shows that variation of alumina from about 0.6 to about 1.3 moles was possible with the aluminosilicate of the invention still being a product. Low levels of alumina of the order of 0.5 moles resulted in an amorphous product.

Thus, the preferred aluminosilicates of the invention may be obtained within the following preferred ranges:

15	K_2O/SiO_2	0.24—0.30
	H_2O/K_2O	35—65
	SiO_2/Al_2O_3	8—12

In addition to varying the proportions of the reactants in the reaction mixture it is possible to vary the reaction conditions and in particular the crystallization temperature. By using different temperatures it is possible to deviate further from the optimum composition defined above for a crystallization temperature of $150^\circ C$ and yet still obtain the desired product. In general, within the broad reactant ratios defined for the process of the invention a higher crystallization temperature enables the silicon content to be lowered and/or the water content to be lowered and/or the potassium content (and thus the alkalinity) to be raised. By contrast operating at lower temperatures tends to decrease the nucleation rate which can be countered by lowering the alkalinity and/or by increasing the water content and/or by introducing seeds of preformed zeolite L. When operating in larger scale syntheses it has been found advantageous to minimise the temperature difference at any time within the crystallization gel, preferably to not more than $15^\circ C$, more preferably not more than $10^\circ C$. This may be done by a slow heating of the crystallization vessel or by limiting the maximum wall temperature of the heat-up.

In the synthesis of all zeolitic materials of the invention, the source of silicon for the reaction mixture is generally silica, and this is usually most conveniently in the form of a colloidal suspension of silica such as Ludox HS 40 available from E. I. DuPont de Nemours and Co. Colloidal silicon sols are preferred since they result in less contaminating phases. However other forms such as silicates may be used.

The source of aluminium may be an alumina introduced into the reaction medium as, for example, $Al_2O_3 \cdot 3H_2O$, previously dissolved in alkali. However, it is also possible to introduce aluminium in the form of the metal, which is dissolved in alkali.

The aluminosilicates of the invention are preferably obtained from reaction mixtures containing potassium. This potassium is preferably introduced as potassium hydroxide. The reaction mixture may contain small quantities of other metal cations and salt forming anions as already described, but it has been found that there is an increasing tendency for other aluminosilicates to be found as the content of other ions is increased, resulting in less pure forms of the aluminosilicate of the invention. For example, sodium and rubidium ions favour erionite formation, caesium ions favour pollucite formation. Thus it is highly preferred for potassium hydroxide to be the source of potassium and the source of alkalinity, and the purest products were obtained when other potassium salts were excluded.

The product of the processes described above is predominantly a potassium form of the aluminosilicate—that is, aluminosilicate where M in general formula I is K. By ion exchange of the product in the manner conventional to zeolite chemistry other cations such as Na or H can be introduced for M.

Within the ranges specified hereinbefore for the composition of the reaction mixture it is possible to choose ratios of oxides and alkalinity to given particular forms of the aluminosilicate product. However, although the SiO_2/Al_2O_3 ratio in the reaction mixture may vary over a wide range the SiO_2/Al_2O_3 ratio in the product preferably lies in a relatively narrow range of 5.7 to 7.4. The higher the SiO_2/Al_2O_3 ratio in the reaction mixture, the higher the ratio in the product. Also, decreasing alkalinity (OH^-/SiO_2) tends to increase the SiO_2/Al_2O_3 ratio in the formed product. Dilution of the reaction mixture with water and thus increasing the H_2O/K_2O ratio also tends to increase the SiO_2/Al_2O_3 ratio in the product. Other cations such as tetramethylammonium and the presence of other potassium salts can be used to raise the SiO_2/Al_2O_3 ratio, but as described hereinbefore this may also result in the formation of other zeolite forms.

Particle size is also affected by the composition of the reaction mixture. Generally the particles formed are in the range of from 0.5 to 4.0μ , but within that range larger particle sizes are favoured by each of lower alkalinity, higher dilution and higher temperatures.

Crystallization is related to the crystallization temperature. The crystallization is preferably carried out in the region of $150^\circ C$ and at this temperature the crystallization time may be from about 24 to 96 hours, typically from 48 to 72 hours. Lower temperatures may require much longer times to achieve good yield of

the desired product, whereas times of less than 24 hours are possible when higher temperatures are used. A time of 8 to 15 hours is typical for a temperature of greater than 200°C.

The crystallization is generally carried out in a sealed autoclave and thus at autogenous pressure. It is generally inconvenient, although possible to employ higher pressures. Lower pressure will require longer crystallization times.

Following the preparation as described above the aluminosilicate may be separated, washed and dried in the normal manner.

The products of the processes of the invention described hereinbefore are preferably substantially free from contaminant crystalline and amorphous materials. However, in employing these products in catalytic applications it may be desired to combine them with additional crystalline or amorphous materials and this invention extends to such combinations.

We have found that the aluminosilicates of the invention are excellent catalyst bases and may be used in a wide variety of catalytic reaction. The particular morphology of the crystals appears to result in a particular stable base for catalytically active metals with a surprising resistance to metal catalyst deactivation. In addition, the aluminosilicates of the invention have displayed low acidity which makes them especially suited to catalytic applications where a low acid site strength is advantageous such as aromatization.

The catalytically-active metal(s) may be, for example, a Group VIII metal such as platinum, tin, or germanium as described in US 4 104 320, or a combination of platinum and rhenium as described in GB 2 004 764 or BE 888365. In the latter case the catalyst may for appropriate circumstances also incorporate halogen as described in US 4 165 276, silver as described in US 4 295 959 and US 4 206 040, cadmium as described in US 4 295 960 and US 4 231 897 or sulphur as described in GB 1 600 927.

We have found a particularly advantageous catalyst composition to incorporate from 0.1 to 6.0 weight%, preferably from 0.1 to 1.5 weight% platinum or palladium, since this gives excellent results in aromatization. From 0.4 to 1.2 wt% platinum is particularly preferred, especially in conjunction with the potassium form of the aluminosilicate. The invention extends to catalysts comprising the zeolitic material and a catalytically-active metal.

It may also be useful to incorporate into the catalyst of the invention one or more materials substantially inert under the conditions in which the catalyst is to be employed to act as a binder. Such binders may also act to improve the resistance of the catalyst to temperature, pressure and attrition.

The aluminosilicates of the invention may be used in a process for the conversion of a hydrocarbon feed in which the feed is contacted with a catalyst as described above under appropriate conditions to bring about the desired conversion. They may for example be useful in reactions involving aromatization and/or dehydrocyclization and/or isomerization and/or dehydrogenation reaction. They are particularly useful in a process for the dehydrocyclization and/or isomerization of acyclic hydrocarbons in which the hydrocarbons are contacted at a temperature of from 430°C to 550°C with a catalyst comprising an aluminosilicate of the invention having at least 90% of the exchangeable cations M as alkali metal ions and incorporating at least one Group VIII metal having dehydrogenating activity, so as to convert at least part of the acyclic hydrocarbons into aromatic hydrocarbons.

The process is preferably otherwise carried out in the manner described in US 4 104 320, BE 888365 or EP 40119.

It has been found that use of the aluminosilicates of the invention in this way enables greatly improved catalyst lifetimes to be achieved as compared to the lifetime obtained with a conventionally prepared zeolite.

The invention will now be described in more detail, though only by way of illustration, in the following Examples and Evaluations, with reference to the accompanying drawings, in which:

Figures 1 to 4 are, as described hereinbefore, triangular graphs showing the preferred proportions of components of the synthesis gel. On these graphs the reaction mixtures used in the Examples in the production of aluminosilicates of the invention are shown as crosses identified by the number of Example, and those reaction mixtures used in the Comparative Examples are shown as solid circles identified by the letter of the Comparative Example; and

Figure 5 is a graph showing the performance of catalysts of the invention in aromatization against catalysts based on conventional zeolites.

Example 1: Preparation of zeolite L

A synthesis gel was prepared having the following composition expressed in moles of pure oxide:



This gel was prepared as follows:

23.40 g of aluminium hydroxide was dissolved by boiling in an aqueous solution of 51.23 g of potassium hydroxide pellets (86% pure KOH) in 100.2 g to form solution A. After dissolution any water loss was corrected. A separate solution, solution B, was prepared by diluting a 225 g of colloidal silica (Ludox HS40) with 195.0 g of water.

Solutions A and B were mixed for two minutes to form 224 g of gel, and just before the gel became fully

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stiff it was transferred to Teflon-lined autoclaves, preheated to 150°C and held at that temperature for 72 hours to bring about crystallization.

The formed zeolite was highly crystalline with a typical zeolite L X-ray diffraction (XRD) pattern. Scanning electron micrographs (SEM) show the product to be formed solely of well-defined cylindrical crystals having a particle size of 2 to 2.5 microns. The $\text{SiO}_2:\text{Al}_2\text{O}_3$ ratio in the product was 6.3. $\text{K}_2\text{O}:\text{Al}_2\text{O}_3$ was measured as 0.99.

Comparative Example A

Repetition of US 3 867 512, Example 9

A synthesis gel was prepared using the procedure of Example 9 of US 3 867 512 which is judged to be the disclosure in that prior art document which provides the most relevant comparison with the invention, although presented in US 3 867 512 as a comparative example. 2.92 g of aluminium hydroxide were dissolved in a solution of 19.52 g potassium hydroxide in 25.0 g water to form solution A. 56.5 g Ludox HS40 were dissolved in 101.0 g water to form solution B. Solutions A and B were mixed for two minutes to form synthesis gel.

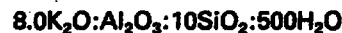
Crystallization was carried out at 116°C for 68 hours, and the product was separated as in Example 1. The gel combination was:



and thus very dilute, and more alkaline than required by the present invention. The product was Zeolite L but contained no cylindrical crystallites which are the characteristic product of the present invention.

Comparative Example B—Repetition of Nishimura

The synthesis procedure described in Y Nishimura, Nippon Kagaku Zasshi 91, 11, 1970, pp 1046—9 was repeated to prepare a gel composition:



This was crystallized in an autoclave at 100°C for 65 hours.

The Japan disclosure is of gels which are more dilute and of high alkalinity than required for the present invention. The product of this Comparative Example was essentially Zeolite W, not Zeolite L and there was no trace of Zeolite L of this invention.

Comparative Example C

Repetition of DT 1813099 Example 6

A synthesis gel was prepared having substantially the composition described in Example 6 of DT 1813099 (equivalent to GB 1 202 511):



7.37 g of aluminium hydroxide were dissolved in an aqueous solution of 16.98 gms of potassium hydroxide (86% pure KOH) in 30.9 gms water to Solution A. 25.04 g of silica as Aerosil 200 were mixed with 55.4 g water for 5 minutes to form Solution B. Solutions A and B were mixed for 1 minute and the formed putty-like gel was heated in an autoclave at 140°C for 46.5 hours.

The product was separated and dried as in Example 1. XRD and SEM showed the product to be a mixture of Zeolite W with Zeolite L. No cylindrical crystallites characteristic of the invention were observed. The procedure of DT 1813099 used drier gels than the present invention and somewhat higher alkalinity, so that effectively the gel alkalinity was significantly higher.

Examples 2 and 3 and Comparative Example H

Variation of aluminium content

The general procedure of Example 1 was repeated with different amounts of aluminium present in the gel. The gels employed are detailed in Table 1 below, together with an indication of the products obtained.

Example 3 ($2.58\text{K}_2\text{O}:0.67\text{Al}_2\text{O}_3:10\text{SiO}_2:160\text{H}_2\text{O}$) and Example 2 ($2.62\text{K}_2\text{O}:1.25\text{Al}_2\text{O}_3:10\text{SiO}_2:160\text{H}_2\text{O}$) yielded Zeolite EL of the invention and Example 3 gave a particularly high yield (20%—measured as zeolite product as a percentage of the initial gel weight). Comparative Example H ($2.58\text{K}_2\text{O}:0.5\text{Al}_2\text{O}_3:10\text{SiO}_2:160\text{H}_2\text{O}$) gave a largely amorphous product.

Examples 4 and 5 and Comparative Examples D and E

Variation of water content

The procedure of Example 1 was repeated for further syntheses using various amounts of water. The gel composition and results are given in Table 1 below.

Example 4 ($2.62\text{K}_2\text{O}:\text{Al}_2\text{O}_3:10\text{SiO}_2:120\text{H}_2\text{O}$) gave good yields of cylindrical Zeolite EL, but as the water content is further reduced there is a tendency to form clam-shaped particles. Comparative Example D ($2.62\text{K}_2\text{O}:\text{Al}_2\text{O}_3:10\text{SiO}_2:80\text{H}_2\text{O}$) resulted in a high proportion of clam Zeolite L.

Example 5 shows that increasing the water content to 240 moles H_2O still resulted in Zeolite EL, but as water is increased there is an increasing product of Zeolite W. At 320 moles H_2O in Comparative Example E Zeolite W predominates.

5 Examples 6—8 and Comparative Examples F and G
Variation in silicon content

A similar investigation of the variation of silicon content of the synthesis gel of Example 1 was carried out as shown in Table 1. Increasing silicon content resulted in an increasing amount of contaminating phases of Zeolite W and amorphous material, but Example 6 with 12 moles SiO_2 gave a satisfactory Zeolite EL product. Comparative Example F using 15 moles SiO_2 gave a largely amorphous product.

10 EL product. Comparative Example F using 15 moles SiO_2 gave a largely amorphous product.
The silicon content was reduced in Example 8 to 8 moles SiO_2 with satisfactory Zeolite L product, but further reduction to 7 moles SiO_2 in Comparative Example G gave a product containing Zeolite W and Zeolite L.

15 Examples 9, 10 and 11 and Comparative Examples J and K
Variation of potassium content

As shown in Table 1, the variation of the amount of potassium in the case where $M=K$ was also investigated. Variation of potassium content from 2.41 moles K_2O (Example 10) to 2.75 moles K_2O (Example 9) gave Zeolite L. Example 11 gave Zeolite L with a morphology intermediate the clam shape and the cylinder shape.

20 A low potassium content of 2.15 moles K_2O (Comp. Ex. K) gave a product with low crystallinity. A high potassium content of 3.4 moles K_2O (Comp. Ex. J) gave a clam-shaped product.

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TABLE 1

Example	Gel composition				(wt%)				Product*
	K ₂ O	Al ₂ O ₃	SiO ₂	H ₂ O	K ₂ O	Al ₂ O ₃	SiO ₂	H ₂ O	
1	2.62	1	10	160	6.4	2.7	15.7	74.6	cylindrical zeolite L
2	2.62	1.25	10	160	6.4	3.4	15.6	74.6	zeolite L
3	2.58	0.67	10	160	6.4	1.8	15.8	76.0	cylindrical zeolite L+
H	2.58	0.50	10	160	6.4	1.4	15.9	76.3	amorphous
4	2.62	1	10	120	7.9	3.3	19.3	69.5	cylindrical zeolite L
5	2.62	1	10	240	4.7	1.9	11.4	82.0	cylindrical zeolite L+(W)
D	2.62	1	10	80	10.3	4.3	25.1	60.3	clam-shaped zeolite L
E	2.62	1	10	360	3.7	1.5	8.9	85.9	zeolite W+(zeolite L)
6	2.62	1	12	160	6.2	2.6	18.2	72.9	zeolite L+(W+amorphous)
7	2.62	1	9	160	6.5	2.7	14.3	76.4	cylindrical zeolite L
8	2.58	1	8	160	6.5	2.8	13.0	77.7	cylindrical zeolite L(+W)
F	2.62	1	15	160	6.0	2.5	21.8	69.8	amorphous
G	2.62	1	7	160	6.8	2.8	11.5	78.9	zeolite W+(zeolite L)
9	2.75	1	10	160	6.7	2.7	15.6	75.0	cylindrical zeolite L
10	2.41	1	10	160	5.9	2.7	15.8	75.6	cylindrical zeolite L
11	3.01	1	10	160	7.3	2.6	15.5	74.5	clam/cylinder zeolite L
K	2.15	1	10	160	5.3	2.7	15.9	76.1	low crystallinity product
J	3.4	1	10	160	8.2	2.6	15.4	73.8	clam-shaped zeolite L

*"L" indicates that small amounts of other phases were present. Where other phases were identified these are shown in parenthesis.

Figures 1 to 4 plot the relative proportions of the components of the gel composition and the preferred proportions for these components in the process of the invention. The Examples of the invention are marked as numbered crosses and the Comparative Examples are shown as lettered dots. This clearly demonstrates that the areas of preferred gel composition marked on the Figures correspond to gels yielding zeolite L.

Various additional tests have been carried out on substitution of potassium by other metals such as sodium. Since this introduces a further variable it is not possible to show these results in Figures 1 to 4.

Examples 12—14 Replacement of potassium

Example 1 was repeated in a generally similar manner but a part of the potassium hydroxide used in preparing Solution A was replaced by sodium hydroxide. Replacement of 10, 20 and 30 mole% was effected and product were obtained and analysed by XRD and SEM. The results are set out in Table 2 below:

Example	Gel composition (moles)					Product
	K ₂ O	Na ₂ O	Al ₂ O ₃	SiO ₂	H ₂ O	
12	2.36	0.26	1	10	160	cylindrical zeolite L
13	2.10	0.52	1	10	160	"
14	1.83	0.78	1	10	160	"

Comparative Example L

Repetition of US 3 216 789 Example 4

The procedure of Example 4 of US 3 216 789 was repeated to prepare a synthesis gel of molar composition (based on actual purities of reactants):



This was then crystallized at 150°C for 45 hours and worked up as described in US 3 216 789. The product was a crystalline zeolite L but the crystallites were clam-shaped and there was no trace of cylindrical Zeolite L of the invention. This result is consistent with the trend noted in increasing alkalinity from Example 9 to Comparative Example J.

Comparative Example M

Repetition of Tsitsishvili

The synthesis procedure described in Tsitsishvili *et al.*, Doklady Akademii Nauk SSSR, Vol 243, No. 2, pp 438—440 (1973) was repeated to prepare a gel with a molar composition:



and containing tributylamine at a rate of 37 ml of tributylamine in 132 g of gel. This was crystallized at 100°C for 45 hours.

This synthesis, which differs from the invention in using high alkalinity, high sodium content and an organic component, gave a product that was largely Zeolite W with a second unidentified phase. No Zeolite L was identified in the product.

Example 15: Zeolite L preparation using aluminium as metal

A synthesis gel of 133 g was prepared having a composition (measured as moles of pure oxide per mole of aluminium measured as Al₂O₃) 2.60 moles K₂O, 10 moles SiO₂ and 160 moles water. The following method was employed:

Aluminium pellets were dissolved in an aqueous solution of potassium hydroxide (86% pure) by heating. After complete dissolution extra water was added to correct for weight losses. Finally the silica source, a diluted Ludox HS 40 solution, was added. The mixture containing all components was mixed for 4 minutes in a high shear mixer. The resulting aluminosilicate gel was charged to a clean Teflon-lined autoclave (within a few minutes a very viscous gel is obtained). The filled autoclave was put in an already heated oven (150°C) and maintained at that temperature for 48 hours to allow zeolite crystallization.

The solid product was separated by centrifuging, washed with cold water (4 times) and dried at 150°C for 4 hours.

The formed zeolite L was in the form of large (1.5—2.5 μ) crystals with a cylindrical shape. The SiO₂/Al₂O₃ ratio in the product was 6.3.

**Example 15 and Comparative Examples O to W**

The procedure of Example 15 was repeated with different synthesis gels. The synthesis gels and the products obtained are summarized in Table 3 below.

The Zeolite L product of the invention was not obtained.

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TABLE 3

Example	Gel wt(g)	K ₂ O	Gel composition (moles) SiO ₂	Al ₂ O ₃	H ₂ O	Zeolite	Product Shape	Size (μ)	SiO ₂ /Al ₂ O ₃
O	270	3.5	10	1	160	L	Clam	1.5—2.6	5.6
P	230	3.5	20	1	640	Amorphous	—	—	—
Q	140	3.5	20	1	160	Amorphous	—	—	—
R	114 ^(a)	3.5	10	1	160	L	Sphere	0.3—0.5	5.6
S	134 ^(b)	3.5	10	1	160	L	Clam	1.5—2.5	6.1
T	134 ^(c)	3.5	10	1	160	L	Clam	1.5—2.5	5.8
U	138	4.4	10	1	160	L	Sphere	0.3—0.5	5.0
V	135	3.5	10	1	160	L	Clam	1—2.5	5.4
W	83	3.5	10	1	84	L	Sphere	0.1—0.2	5.4

(a) silicon source=hydrated silicic acid SiO₂ · nH₂O(b) aluminium source=50% Al 50% Al₂O₃ · 3H₂O(c) aluminium source=25% Al 75% Al₂O₃ · 3H₂O

Comparative Examples X: Effect of anions

Example 15 was repeated except that an additional mole of potassium (measured as moles K_2O /mole Al_2O_3) was introduced as a potassium salt. This gave the gel the following composition (in terms of moles of oxides):



The products of the crystallization showed mixed crystallite types which indicated that mixtures of zeolite types were formed. Zeolite W was identified by its X-ray diffraction pattern. The additives also increased the SiO_2/Al_2O_3 ratio in the product. The results are given in Table 4 which follows:

TABLE 4

TABLE 4						
	Comp Ex	Additive	Product			
15			Zeolite type	Shape	Size (μ)	SiO ₂ /Al ₂ O ₃
	Xa	KBr	L	clam & disc	2.5—3	6.8
	Xb	KCL	L and W	clam	3—4	7.2
20	Xc	K ₂ CO ₃	L and W	clam & irregular	2—3	6.5
	Xd	K ₂ SO ₄	L and W	disc & cylinder	2—2.5	6.8
25	Xe	K toluene sulphonate	L and W	irregular	0.5	6.9

30 Comparative Examples Y: Repeat of GB 1 393 365

Example 10 of GB 1 393 365 describes a synthesis mixture with the composition:



35 wherein K_2O/M_2O (i.e. K_2O+Na_2O)=0.8 for the preparation of zeolite AG-1. GB 1 393 365 specifies a water glass starting material for this synthesis with the composition:



40 However, the use of such a silicon source makes it impossible to comply with the other requirement of GB 1 393 365 that the water glass should be the only or major source of silicon.

A synthesis mixture of the specified composition was prepared using potassium aluminate and Ludox Hs-40 as the raw materials. A similar synthesis (not described in GB 1 393 365) was also performed using a mixture containing no sodium. The results are given in Table 5 below. The products had poor crystallinity, and showed clam morphology.

TABLE 5

Gel composition				Crystallization		Product characteristics		
Na ₂ O	mole/mole Al ₂ O ₃ K ₂ O	SiO ₂	H ₂ O	Temp°C	time hrs	Zeolite	Shape	Size (μ m)
—	2.70	8.75	83.7	135	25	L	clam	0.5—1
0.54	2.16	8.75	83.7	135	25	L	clam	0.5—1

Example 16: Scaled-up synthesis

The synthesis of Example 1 was repeated in a 2 litre autoclave with a diameter of 10.2 cms using amounts of reactants increased to give a total synthesis gel weight of 1709 grams. A heating-up period of 9 hours was employed to bring the gel to the crystallization temperature of 150°C so that a maximum temperature difference of 10°C was obtained in the gel. 260 grams of a highly crystalline zeolite L product was obtained, with the crystals having a particle size of 1 to 1.5 μ and substantially all of the particles having a cylindrical morphology.

X-ray diffraction

X-ray diffraction patterns were obtained for the product of Example 16 and Comparative Example O, and these were compared with the patterns for EC-19, a zeolite L sample obtained from Union Carbide Corporation and for quartz. The samples for the X-ray diffraction measurements were prepared by two techniques, to give a hydrated and a dried sample.

Hydrated sample preparation

The sample as synthesized was loaded into a diffractometer cell without first washing. It was then hydrated by being placed for at least 16 hours in a closed vessel over saturated calcium chloride. The cell was taken from the vessel and immediately placed in the diffractometer.

Dry sample preparation

The sample after synthesis was washed 5—6 times with cold demineralized water and the washings decanted by centrifuging. The sample was dried for 16 hours at 150°C in air, and then homogenized by hand using a mortar and pestle, and loaded into the diffractometer cell.

Diffractometer

The XRD measurements were taken on a Phillips APD 3600 diffractometer using CuK α radiation operating as follows:

X-ray tube energy:	40 mA, 45 kV
Measuring time:	0.6 sec
Scan speed:	1° 20/min
Scanning range:	4°—100°
Step width:	0.01°

The diffractometer incorporates a theta compensating slit and is integral with a Data General Nova 4X computer using Phillips Software to process the data.

Procedure

The XRD patterns were measured in the following sequence:

Quartz
Hydrated samples
Quartz
Dry samples
Quartz

The peak heights and peak areas for quartz used in the following calculations were the average of the 3 quartz samples. The XRD patterns for d values above 2Å are given in Tables 6 and 7.

In addition, the peak heights of the eight peaks identified in the table were summed and divided by the sum of the peak height for the peaks in the quartz pattern at d values of:

4.26±0.04

3.35±0.04

2.46±0.02

The ratio gives a measure of the relative peak height of the samples. It will be noted that the peak heights of the Example 16 product are greater than the peak heights of EC-19 or the Comparative Example O product.

Crystallinity

The XRD data was analysed to determine the ratio of the peak areas for the reflection from the plane 220 ($d=4.57\pm0.04\text{\AA}$) and 221 plane ($d=3.91\pm0.02\text{\AA}$) of the zeolite to the peak area for the reflection from the 110 plane ($d=2.46\pm0.02\text{\AA}$) of the quartz. The peaks were chosen as being in areas where there was no overlap with other peaks and being relatively insensitive to hydration effects.

For each peak the integrated area was determined and expressed as a percentage of the quartz peak. The sum of these percentages for the two peaks are given in Tables 6 and 7. A straight line background was calculated in determining these peak areas by a least-squares fit of linear equation through portions of the scan on either side of the peak in question. The area A then calculated as:

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$$A = \sum_{i=T_1}^{T_2} (I_i - B_i)$$

- 5 where I_i the measured intensity and B_i the calculated background for each point i between T_1 and T_2 which are the initial and final 20 integration values.

The results show the product of Example 16 to have good crystallinity.

XRD patterns

- 10 It is noted that the dry and hydrated samples of the product of Example 16 showed an absence of reflections at d spacings of $6.28 \pm 0.05 \text{ \AA}$.

Evaluation: Aromatization

- 15 The performance of certain of the Zeolite L samples of the Examples as a catalyst base in aromatization was compared to products of the Comparative Examples, and a zeolite L, designated EC19, obtained from Union Carbide Corporation, referred to a "Control". In each case a catalyst was prepared by impregnating the base with 0.6 wt% platinum.

- 20 The zeolite sample under test (typically about 25 g) was slurried in 700 ml of distilled water in a 5 litre flask. The appropriate amount of tetraamino-platinum dichloride to give impregnation at a rate of 0.6 wt% platinum was dissolved in 300 ml of distilled water. The platinum salt solution was then added to the sample slurry over a 6 hour period. The mixture was stirred for 24 hours after platinum salt addition, then the impregnated sample was dried at 110°C .

- 25 The sample was then pelletized, crushed to 14—20 mesh (US sieve size) and loaded into a vertical tubular reactor and air (substantially water-free) was passed over the catalyst at a rate of 25 ml/min of air per gram of sample. The catalyst was heated to 480°C in four hours and held at 480°C for three hours. The sample was then reduced by passing hydrogen over it at 207 kPa and a rate of 75 ml/min per gram of sample, while the catalyst was heated to 527°C in 3 hours, held at 527°C for ten minutes and then cooled to the desired reaction temperature.

- 30 The aromatization test was carried out at a temperature of 510°C and 690 KPa (100 psig) pressure with a C_6 mixed feed comprising:

	Component	Wt%
35	iso- C_6 (3-methyl-pentane)	30
	n- C_6	60
	methyl cyclopentane	10

- 40 at a space velocity of 2.5 w/w hr^{-1} and in the presence of hydrogen, the H_2 : hydrocarbon ratio being 6.

- The results are shown graphically in Figure 5, which shows the benzene yield (weight%) as a function of time. The catalyst using the cylindrical aluminosilicate of Example 15 as its catalyst base show a remarkable improved activity life time over extended periods of time, much greater than that achieved with catalysts using the clam-shaped zeolite L of Comparative Examples Xb and O or using the conventional zeolite L of the Control.

- 45 It is a further feature of the aluminosilicate of the invention that in the aromatization evaluation described herein, a catalyst comprising 0.6 wt% platinum of the aluminosilicate has a benzene yield of 45 wt% after at least 150 hours, and preferably after 200 hours.

- 50 In a repeat of this test the product of Example 16 gave benzene yields in excess of 40% for a period of 430 hours.

TABLE 6
XRD patterns of hydrated samples

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	EC-19		Comparative Example O		Example 16	
	d(Å)	Relative intensity	d(Å)	Relative intensity	d(Å)	Relative intensity
5	16.0	65	15.9	58	15.7	61
10	7.95	4	7.93	4	7.96	4
	7.52	21	7.52	21	7.51	18
15	6.02	33	6.01	28	6.01	29
	5.82	15	5.82	12	5.81	13
	*4.59	61	*4.60	52	*4.59	53
20	4.42	22	4.42	18	4.41	19
	4.34	20	4.34	13	4.33	18
25	*3.92	87	*3.92	91	*3.92	75
	3.81	7	3.81	9	3.81	8
	*3.66	44	*3.66	47	*3.66	44
30	*3.48	63	*3.48	71	*3.48	66
	3.40	4	3.40	5	3.40	6
35	*3.29	44	*3.29	41	*3.28	43
	*3.19	100	*3.19	97	*3.18	100
	*3.07	74	*3.07	78	*3.07	73
40	3.01	12	3.01	12	3.01	11
	*2.91	89	*2.91	100	*2.91	85
45	2.84	4	2.86	7	2.86	6
	2.80	12	2.84	8	2.84	8
	2.73	2	2.79	11	2.79	13
50	2.68	24	2.68	23	2.72	3
	2.66	60	2.66	57	2.67	20
55	2.62	5	2.62	31	2.65	47
	2.51	16	2.55	3	2.62	29
	2.48	20	2.51	19	2.55	5
60	2.43	20	2.47	19	2.50	14
	2.38	3	2.43	19	2.47	21
65	2.35	3	2.42	14	2.43	16

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TABLE 6 (contd.)
XRD patterns of hydrated samples

	EC-19		Comparative Example O		Example 16	
	d(Å)	Relative intensity	d(Å)	Relative intensity	d(Å)	Relative intensity
5	2.30	10	2.38	4	2.41	12
10	2.28	12	2.30	10	2.37	2
	2.20	38	2.28	12	2.35	2
15	2.12	2	2.20	43	2.30	9
	2.04	10	2.15	3	2.27	11
20	2.01	4	2.12	2	2.20	32
			2.04	8	2.18	3
					2.12	3
25					2.04	8
					2.01	4
30	Sum peak heights					
	Quartz peak heights					
	0.35		0.32		0.47	
35	Zeolite 220+221 peak areas					
	100x					
	Quartz 110 peak area					
40	157		146		163	
45						
50						
55						
60						
65						

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TABLE 7
XRD patterns of dried samples

(37)

EC-19		Comparative Example O		Example 16		
	d(Å)	Relative intensity	d(Å)	Relative intensity	d(Å)	Relative intensity
5	15.7	63	15.9	66	15.8	81
10	7.90	4	9.21	2	9.15	2
	7.49	19	8.00	4	7.93	6
15	5.99	34	7.54	24	7.51	21
	5.80	16	6.02	28	6.00	31
	*4.58	59	5.84	13	5.81	13
20	4.41	22	*4.60	63	*4.59	56
	4.33	18	4.42	19	4.41	19
25	*3.91	86	4.34	13	4.33	18
	3.80	8	*3.93	95	*3.92	83
	*3.65	43	3.81	9	3.81	7
30	*3.47	59	*3.66	46	*3.66	48
	3.39	5	*3.49	72	*3.48	64
35	*3.28	41	3.41	5	3.40	6
	*3.18	100	*3.29	40	*3.28	40
	*3.07	70	*3.19	100	*3.18	100
40	3.00	12	*3.07	78	*3.07	70
	*2.91	87	3.01	10	3.01	11
45	2.86	6	*2.92	96	*2.91	71
	2.83	6	2.84	8	2.86	7
	2.79	11	2.62	30	2.84	7
50	2.73	2	2.55	3	2.79	11
	2.67	23	2.51	20	2.67	20
55	2.65	56	2.48	23	2.65	48
	2.62	31	2.43	20	2.62	33
	2.55	6	2.42	15	2.55	4
60	2.50	17	2.38	3	2.50	16
	2.47	22	2.30	10	2.47	21
65	2.43	20	2.28	15	2.43	18

TABLE 7 (contd.)
XRD patterns of dried samples

	EC-19		Comparative Example O		Example 16	
	d(Å)	Relative intensity	d(Å)	Relative intensity	d(Å)	Relative intensity
5						
10	2.41	13	2.20	44	2.41	12
	2.37	3	2.15	3	2.30	10
	2.35	3	2.12	2	2.27	12
15	2.30	12	2.04	9	2.20	36
	2.27	13	2.01	3	2.15	3
20	2.20	37			2.12	3
	21.12	4			2.04	8
	2.04	10			2.01	4
25	2.00	5				
	Sum peak heights					
	Quartz peak heights					
30	0.33		0.31		0.44	
	(Zeolite 220+221) peak areas					
35	100 × $\frac{\text{Quartz 220+221 peak areas}}{\text{Quartz 110 peak area}}$					
	153		146		164	

Claims

1. A zeolite having an X-ray diffraction pattern obtained from CuK α radiation with the significant d values set out in Table A:

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TABLE 7 (contd.)
XRD patterns of dried samples

Example 16

EC-19

Comparative Example O

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100

Claims

1. A zeolite having an X-ray diffraction pattern obtained from CuK α radiation with the significant d values set out in Table A:

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100

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TABLE A

	16.1±0.4
5	7.52±0.05
	6.00±0.04
10	4.57±0.04
	4.35±0.04
	3.91±0.02
15	3.47±0.02
	3.28±0.02
20	3.17±0.02
	3.07±0.02
	2.91±0.02
25	2.65±0.02
	2.46±0.02
30	2.42±0.01
	2.19±0.01

and comprising crystallites in the form of distinct circular cylinders characterised in that at least 50% of the crystallites are in the form of distinct circular cylinders having a mean diameter of at least 0.5 micron and an aspect ratio of at least 0.5.

2. A zeolite as claimed in claim 1, having at least 70% of its crystallites as cylinders.

3. A zeolite as claimed in claim 1 or claim 2, wherein the cylindrical crystallites have a mean diameter of from 0.5 to 4 micron.

4. A zeolite as claimed in any of claims 1 to 3, wherein the aspect ratio of the cylinders is from 0.5 to 1.5.

5. A zeolite as claimed in any of claims 1 to 4, having a composition expressed in terms of the molar ratio of oxides assuming an anhydrous state of:



wherein M is a cation of valence n and x is from 5 to 7.5.

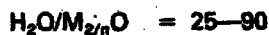
6. A zeolite as claimed in claim 5, wherein x is from 5.7 to 7.4.

7. A zeolite as claimed in claim 6, wherein x is from 6 to 6.5.

8. A zeolite as claimed in any of claims 5 to 7, wherein M is potassium.

9. A zeolite as claimed in any of claims 5 to 8, wherein the mole ratio $M_{2/n}O:Al_2O_3$ is from 0.95 to 1.15.

10. A process for the preparation of a zeolite having an X-ray diffraction pattern obtained from CuK α radiation with the significant d values of Table A as set out in claim 1, in which process an alkaline reaction mixture comprising water, a source of silicon and a source of aluminium is heated characterised in that to form an aluminosilicate zeolite with at least 50% of crystallites in the form of distinct circular cylinders with a mean diameter of at least 0.5 micron and an aspect ratio of at least 0.5, the reaction mixture has a composition (expressed in the mole ratio of oxides) of:



(wherein M is a cation of valence n) and is heated to a temperature of from at least 75°C.

11. A process as claimed in claim 10, in which M is potassium (K) or a mixture of K+M' in which M' is an alkali metal other than potassium, provided that the molar ratio $K_2O/M'_{2/n}O+K_2O$ is at least 0.7.



12. A process as claimed in claim 10 or claim 11, in which the reaction mixture is heated to a temperature of at least 100°C.

13. A process as claimed in claim 12, in which the temperature is from 100 to 250°C.

14. A process as claimed in any of claims 10 to 13, in which the temperature difference with the reaction mixture is not more than 15°C at any time.

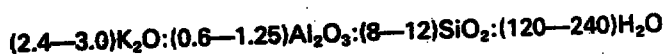
15. A process as claimed in any of claims 10 to 14, in which the reaction mixture has the composition:

$$M_{2/n}O/SiO_2 = 0.24-0.30$$

$$H_2O/M_{2/n}O = 35-65$$

$$SiO_2/Al_2O_3 = 8-12$$

16. A process as claimed in claim 15, in which the reaction mixture has the molar composition:



17. A process as claimed in claim 10, in which the relative proportions of aluminium, water, silicon and potassium in the reaction mixture (measured as wt% of the oxides) are such that the reaction mixture falls within area I_A in Figure 1, area I_B in Figure 2, area I_C in Figure 3 and area I_D in Figure 4, and the reaction mixture is heated to from 120 to 225°C.

18. A process as claimed in claim 17, in which the reaction mixture falls within area II_A in Figure 1, area II_B in Figure 2, area II_C in Figure 3 and area II_D in Figure 4.

19. A process as claimed in claim 18, in which the reaction mixture falls within area III_A in Figure 1, area III_B in Figure 2, area III_C in Figure 3 and area III_D in Figure 4.

20. A process as claimed in any of claims 10 to 19, in which the mole ratio of $H_2O/(M_{2/n}O + Al_2O_3 + SiO_2)$ is greater than 8.

21. A process as claimed in claim 10, in which to form a zeolite which is not an aluminosilicate the source of aluminium is replaced by a source of gallium, boron or iron and/or the source of silicon is replaced by a source of germanium or phosphorus.

22. A catalyst comprising a zeolite as claimed in claim 1, and a catalytically-active metal.

23. A catalyst as claimed in claim 22, in which the catalytically active metal is or includes platinum.

24. A catalyst as claimed in claim 23, comprising 0.4 to 1.2 wt% platinum.

25. A catalyst as claimed in any of claims 22 to 24, in which the zeolite is in the potassium form.

26. Use of the catalyst according to claim 22 in an aromatization process.

27. A process for the dehydrocyclization and/or isomerization of hydrocarbons, in which the hydrocarbons are contacted at a temperature of from 430°C to 550°C with a catalyst according to claim 22 having at least 90% of the exchangeable cations M as alkali metal ions and incorporating at least one Group VIII metal having dehydrogenating activity, so as to convert at least part of the acyclic hydrocarbons into aromatic hydrocarbons.

28. A process for the conversion of hydrocarbons, in which the hydrocarbons are contacted at an appropriate temperature of from 430°C to 550°C with a catalyst comprising a zeolite according to claim 1.

Patentansprüche

1. Zeolith mit einem Röntgenbeugungsspektrum erhalten mit CuKα-Strahlung mit den signifikanten d-Werten gemäß Tabelle A:



TABELLE A
16.1±0.4

5	7.52±0.05
	6.00±0.04
	4.57±0.04
10	4.35±0.04
	3.91±0.02
	3.47±0.02
15	3.28±0.02
	3.17±0.02
20	3.07±0.02
	2.91±0.02
	2.65±0.02
25	2.46±0.02
	2.42±0.01
30	2.19±0.01

und enthaltend Kristallite in Form von ausgeprägten kreisförmigen Zylindern, dadurch gekennzeichnet, daß mindestens 50% der Kristallite in Form von ausgeprägten kreisförmigen Zylindern mit einem durchschnittlichen Durchmesser von mindestens 0,5 µm und einem Aspektverhältnis von mindestens 0,5 vorliegen.

2. Zeolith nach Anspruch 1, dadurch gekennzeichnet, daß mindestens 70% seiner Kristallite als Zylinder vorliegen.

3. Zeolith nach Anspruch 1 oder 2, dadurch gekennzeichnet, daß die zylindrischen Kristallite einen durchschnittlichen Durchmesser von 0,5 bis 4 µm besitzen.

4. Zeolith nach einem der Ansprüche 1 bis 3, dadurch gekennzeichnet, daß das Aspektverhältnis der Zylinder 0,5 bis 1,5 beträgt.

5. Zeolith nach einem der Ansprüche 1 bis 4, dadurch gekennzeichnet, daß er eine Zusammensetzung ausgedrückt als molares Verhältnis der Oxide im angenommenen wasserfreien Zustand von:



besitzt, wobei M ein Kation mit der Wertigkeit n ist und x einen Wert von 5 bis 7,5 besitzt.

6. Zeolith nach Anspruch 5, dadurch gekennzeichnet, daß x einen Wert von 5,7 bis 7,4 besitzt.

7. Zeolith nach Anspruch 6, dadurch gekennzeichnet, daß x einen Wert von 6 bis 6,5 besitzt.

8. Zeolith nach einem der Ansprüche 5 bis 7, dadurch gekennzeichnet, daß M Kalium ist.

9. Zeolith nach einem der Ansprüche 5 bis 8, dadurch gekennzeichnet, daß das molare Verhältnis $M_{2/n}O:Al_2O_3$ 0,95 bis 1,15 beträgt.

10. Verfahren zur Herstellung eines Zeolithen mit einem Röntgenbeugungsspektrum erhalten mit CuKα-Strahlung mit den signifikanten d-Werten gemäß Tabelle A in Anspruch 1, bei dem eine alkalische Reaktionsmischung erhitzt wird, die Wasser, eine Quelle für Silicium und eine Quelle für Aluminium enthält, dadurch gekennzeichnet, daß die Reaktionsmischung zur Bildung eines Aluminosilikat-Zeolithen mit mindestens 50% Kristalliten in Form von ausgeprägten kreisförmigen Zylindern mit einem durchschnittlichen Durchmesser von mindestens 0,5 µm und einem Aspektverhältnis von mindestens 0,5 eine Zusammensetzung (ausgedrückt als das molare Verhältnis der Oxide) von:

$$M_{2/n}O/SiO_2 = 0,22-0,36$$

$$H_2O/M_{2/n}O = 25-90$$

$$SiO_2/Al_2O_3 = 6-15$$



besitzt (wobei M ein Kation mit der Wertigkeit n ist) und auf eine Temperatur von mindestens 75°C erwärmt wird.

11. Verfahren nach Anspruch 10, dadurch gekennzeichnet, daß M Kalium (K) oder eine Mischung von K+M' ist, in der M' ein anderes Alkalimetall als Kalium ist, mit der Maßgabe, daß das molare Verhältnis K_2O/M'_2O+K_2O mindestens 0,7 ist.

12. Verfahren nach Anspruch 10 oder 11, dadurch gekennzeichnet, daß die Reaktionsmischung auf eine Temperatur von mindestens 100°C erwärmt wird.

13. Verfahren nach Anspruch 12, dadurch gekennzeichnet, daß die Temperatur 100 bis 250°C beträgt.

14. Verfahren nach einem der Ansprüche 10 bis 13, dadurch gekennzeichnet, daß die Temperaturdifferenz innerhalb der Reaktionsmischung zu keinem Zeitpunkt mehr als 15°C beträgt.

15. Verfahren nach einem der Ansprüche 10 bis 14, dadurch gekennzeichnet, daß die Reaktionsmischung folgende Zusammensetzung besitzt:

$$M_{2/n}O/SiO_2 = 0.24-0.30$$

$$H_2O/M_{2/n}O = 35-65$$

$$SiO_2/Al_2O_3 = 8-12$$

16. Verfahren nach Anspruch 15, dadurch gekennzeichnet, daß die Reaktionsmischung folgende molare Zusammensetzung besitzt:



17. Verfahren nach Anspruch 10, dadurch gekennzeichnet, daß die relativen Anteile von Aluminium, Wasser, Silicium und Kalium in der Reaktionsmischung (gemessen als Gew.% der Oxide) so sind, daß die Reaktionsmischung in die Fläche I_A in Figur 1, Fläche I_B in Figur 2, Fläche I_C in Figur 3 und Fläche I_D in Figur 4 fällt und die Reaktionsmischung auf 120 bis 225°C erhitzt wird.

18. Verfahren nach Anspruch 17, dadurch gekennzeichnet, daß die Reaktionsmischung in die Fläche II_A in Figur 1, Fläche II_B in Figur 2, Fläche II_C in Figur 3 und Fläche II_D in Figur 4 fällt.

19. Verfahren nach Anspruch 18, dadurch gekennzeichnet, daß die Reaktionsmischung in die Fläche III_A in Figur 1, Fläche III_B in Figur 2, Fläche III_C in Figur 3 und Fläche III_D in Figur 4 fällt.

20. Verfahren nach einem der Ansprüche 10 bis 19, dadurch gekennzeichnet, daß das molare Verhältnis von $H_2O/(M_{2/n}O+Al_2O_3+SiO_2)$ größer als 8 ist.

21. Verfahren nach Anspruch 10, dadurch gekennzeichnet, daß die Aluminiumquelle zwecks Bildung eines Zeolithen, der kein Aluminosilikat ist, durch eine Gallium-, Bor- oder Eisenquelle und/oder die Siliciumquelle durch eine Germanium- oder Phosphorquelle ersetzt wird.

22. Katalysator, dadurch gekennzeichnet, daß er einen Zeolithen gemäß Anspruch 1 enthält.

23. Katalysator nach Anspruch 22, dadurch gekennzeichnet, daß das katalytisch aktive Metall Platin ist oder Platin umfaßt.

24. Katalysator nach Anspruch 23, dadurch gekennzeichnet, daß er 0,4 bis 1,2 Gew.% Platin enthält.

25. Katalysator nach einem der Ansprüche 22 bis 24, dadurch gekennzeichnet, daß der Zeolith in der Kaliumform vorliegt.

26. Verwendung des Katalysators nach Anspruch 22 in einem Aromatisierungsverfahren.

27. Verfahren für die Dehydrocyclisierung und/oder Isomerisierung von Kohlenwasserstoffen, dadurch gekennzeichnet, daß Kohlenwasserstoffe bei einer Temperatur von 430 bis 550°C mit einem Katalysator gemäß Anspruch 22 kontaktiert werden, der mindestens 90% austauschbare Kationen M als Alkalimetallionen und mindestens ein Gruppe VIII Metall mit Dehydrierungsaktivität enthält, so daß mindestens ein Teil der acyclischen Kohlenwasserstoffe in aromatische Kohlenwasserstoffe umgewandelt wird.

28. Verfahren zur Umwandlung von Kohlenwasserstoffen, dadurch gekennzeichnet, daß die Kohlenwasserstoffe bei einer geeigneten Temperatur von 430 bis 550°C mit einem Katalysator kontaktiert werden, der einen Zeolithen gemäß Anspruch 1 umfaßt.

Revendications

1. Zéolithe ayant un diagramme de diffraction des rayons X obtenu à partir de la radiation CuKα, avec les valeurs de d significatives énumérées dans le tableau A:



TABLEAU A

(43)

	16,1±0,4
5	7,52±0,05
	6,00±0,04
	4,57±0,04
10	4,35±0,04
	3,91±0,02
15	3,47±0,02
	3,28±0,02
	3,17±0,02
20	3,07±0,02
	2,91±0,02
25	2,65±0,02
	2,46±0,02
	2,42±0,01
30	2,19±0,01

et comprenant des cristallites ayant la forme de cylindres circulaires distincts, caractérisée en ce qu'au moins 50% des cristallites sont sous forme de cylindres circulaires distincts ayant un diamètre moyen d'au moins 0,5 micron et un rapport d'aspect d'au moins 0,5.

35 2. Zéolithe suivant la revendication 1, ayant au moins 70% de ses cristallites sous forme de cylindres.

3. Zéolithe suivant la revendication 1 ou 2, dans laquelle les cristallites cylindriques ont un diamètre moyen de 0,5 à 4 microns.

40 4. Zéolithe suivant l'une quelconque des revendications 1 à 3, dans laquelle le rapport d'aspect des cylindres va de 0,5 à 1,5.

5. Zéolithe suivant l'une quelconque des revendications 1 à 4, ayant la composition suivante exprimée en rapport molaire des oxydes, supposant un état anhydre:



45 dans laquelle M est un cation de valence n et x a une valeur de 5 à 7,5.

6. Zéolithe suivant la revendication 5, dans laquelle x a une valeur de 5,7 à 7,4.

7. Zéolithe suivant la revendication 6, dans laquelle x a une valeur de 6 à 6,5.

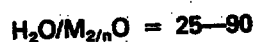
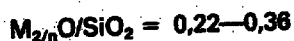
8. Zéolithe suivant l'une quelconque des revendications 5 à 7, dans laquelle M représente le potassium.

9. Zéolithe suivant l'une quelconque des revendications 5 à 8, dans laquelle le rapport molaire

50 $M_{2/n}O:Al_2O_3$ a une valeur de 0,95 à 1,15.

10. Procédé de préparation d'une zéolithe ayant un diagramme de diffraction des rayons X obtenu à partir de la radiation CuK α avec les valeurs de d significatives du tableau A, telles qu'énumérées dans la revendication 1, procédé dans lequel un mélange réactionnel alcalin comprenant de l'eau, une source de silicium et une source d'aluminium est chauffé, procédé caractérisé par la formation d'une zéolithe du type

55 aluminosilicate ayant au moins 50% des cristallites sous forme de cylindres circulaires distincts ayant un diamètre moyen d'au moins 0,5 microns et un rapport d'aspect d'au moins 0,5, le mélange réactionnel ayant la composition suivante (exprimée en rapport molaire des oxydes):



60 (dans laquelle M est un cation de valence n) et étant chauffé à une température d'au moins 75°C.



11. Procédé suivant la revendication 10, dans lequel M représente le potassium (K) ou un mélange de K+M' dans lequel M' est un métal alcalin autre que le potassium, sous réserve que le rapport molaire K_2O/M'_2O+K_2O soit au moins égal à 0,7.

12. Procédé suivant la revendication 10 ou la revendication 11, dans lequel le mélange réactionnel est chauffé à une température d'au moins 100°C.

13. Procédé suivant la revendication 12, dans lequel la température est comprise entre 100 et 250°C.

14. Procédé suivant l'une quelconque des revendications 10 à 13, dans lequel la différence de température avec le mélange réactionnel n'est à aucun moment supérieure à 15°C.

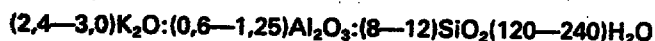
15. Procédé suivant l'une quelconque des revendications 10 à 14, dans lequel le mélange réactionnel possède la composition suivante:

$$M_{2/n}O/SiO_2 = 0,24-0,30$$

$$H_2O/M_{2/n}O = 35-65$$

$$SiO_2/Al_2O_3 = 8-12$$

16. Procédé suivant la revendication 15, dans lequel le mélange réactionnel a la composition molaire suivante:



17. Procédé suivant la revendication 10, dans lequel les proportions relatives d'aluminium, d'eau, de silicium et de potassium dans le mélange réactionnel (mesurées en % en poids des oxydes) sont telles que le mélange réactionnel est situé dans la surface I_A de la figure 1, la surface I_B de la figure 2, la surface I_C de la figure 3 et la surface I_D de la figure 4, et le mélange réactionnel est chauffé à une température de 120 à 225°C.

18. Procédé suivant la revendication 17, dans lequel le mélange réactionnel est situé dans la surface II_A de la figure 1, la surface II_B de la figure 2, la surface II_C de la figure 3 et la surface II_D de la figure 4.

19. Procédé suivant la revendication 18, dans lequel le mélange réactionnel est situé dans la surface III_A de la figure 1, la surface III_B de la figure 2, la surface III_C de la figure 3 et la surface III_D de la figure 4.

20. Procédé suivant l'une quelconque des revendications 10 à 19, dans lequel le rapport molaire $H_2O/(M_{2/n}O+Al_2O_3+SiO_2)$ est supérieur à 8.

21. Procédé suivant la revendication 10, dans lequel, afin de former une zéolithe qui ne soit pas un aluminosilicate, la source d'aluminium est remplacée par une source de gallium, de bore ou de fer et/ou la source de silicium est remplacée par une source de germanium ou de phosphore.

22. Catalyseur comprenant une zéolithe suivant la revendication 1.

23. Catalyseur suivant la revendication 22, dans lequel le métal catalytiquement actif est le platine ou comprend du platine.

24. Catalyseur suivant la revendication 23, comprenant 0,4 à 1,2% en poids de platine.

25. Catalyseur suivant l'une quelconque des revendications 22 à 24, dans lequel la zéolithe est sous la forme potassium.

26. Utilisation du catalyseur suivant la revendication 22 dans un procédé d'aromatisation.

27. Procédé de déshydrocyclisation et/ou d'isomérisation d'hydrocarbures, dans lequel les hydrocarbures sont mis en contact à une température de 430°C à 550°C avec un catalyseur suivant la revendication 22, ayant au moins 90% des cations échangeables M constitués d'ions de métaux alcalins et comprenant au moins un métal du Groupe VIII ayant une activité de déshydrogénation, de manière à transformer au moins une partie des hydrocarbures acycliques en hydrocarbures aromatiques.

28. Procédé de transformation d'hydrocarbures, dans lequel les hydrocarbures sont mis en contact à une température appropriée de 430°C à 550°C avec un catalyseur comprenant une zéolithe suivant la revendication 1.

