

Method for processing thin stillage and apparatus for producing a protein-containing product

The invention relates to a method as claimed in the
5 preamble of claim 1 and a device as claimed in the preamble of claim 11.

In the recovery of ethanol in a distillation process, recovered from grains such as corn, wheat and/or
10 triticale, a large amount of stillage is left behind.

This stillage can be used as a feed for livestock farming, among other things.

15 In the conventional process up until now, the stillage is separated into thin stillage and thick stillage in a decanter. The thin stillage is fed to an evaporator for further reduction in water content and for further concentration. This process step leads to what is known
20 as "stillage syrup". Then, the thick stillage is mixed back in with the stillage syrup and fed to a dryer which takes the dry matter content to above 90 wt.-%. However, this recovered feed can only be fed to ruminants since the fraction of fibrous material is
25 very high, the use of this nutritious feed additive therefore being limited to only a few areas of application.

DE 20 2009 013 389.3 discloses a device for recovering
30 a product in which the thin stillage is concentrated by way of ultrafiltration and then is sent to a dryer together with the thick stillage. This device has essentially proven its effectiveness, but in this case as well, the product produced can only be fed to
35 ruminants. In addition, it has been shown that in the processing of the thin stillage, ultrafiltration can only be operated economically up to a certain concentration level.

Hence, the object of the present invention on the one hand is to provide a method that ensures optimum operation of a filtration unit, and on the other hand provides a device for manufacturing a product of value that contains proteins and fats, and is essentially free of fiber.

Summary

In one aspect, there is provided a method for processing thin stillage, characterized by the following steps:

- a) Feeding of thin stillage into a working vessel;
- b) Concentrating thin stillage in a filtration unit; and
- c) Returning a first substream of concentrated thin stillage to the thin stillage contained in the working vessel in order to adjust the amount of dry matter.

In another aspect, there is provided a device for producing a valuable product containing protein from thin stillage, comprising a working vessel, a filtration unit, a centrifuge, preferably a separator, and a dryer, characterized in that the filtration unit is connected to the working vessel by way of a return line for a first substream of the concentrated thin stillage.

Detailed Description

The invention meets these objectives referred to above by way of a method with the features of claim 1 and a device with the features of claim 11.

According to the disclosure, a method for processing thin stillage comprises the following steps:

- a) Feeding of thin stillage into a working vessel;
- b) Filtering and pre-concentrating thin stillage in a filtration unit; and
- c) Returning a first substream of pre-concentrated

thin stillage to the thin stillage contained in the working vessel in order to adjust the amount of dry matter.

By returning the first substream of pre-concentrated thin stillage to the thin stillage located in the working vessel, the dry matter content of the thin stillage can be raised, which facilitates a more optimal process and a higher efficiency of the filtration unit.

Advantageous embodiment variations of the invention are objects of the dependent claims.

After the pre-concentration of the thin stillage by way of the filtration unit, the flow can be split, wherein a first substream is returned to the working vessel and a second substream is further processed.

After the filtration unit, this second substream can be routed to a mechanical solid-liquid separator in which

the thin stillage is further concentrated to advantageously form a thin stillage with a dry matter content of preferably greater than 12 wt.-%. By combining a filtration unit with a centrifuge, the thin stillage can be advantageously concentrated in a particularly temperature-sensitive manner.

After further concentration of the thin stillage by way of clarification and decanting of the clarified aqueous phase, the centrifuged thin stillage is transferred as a separator nozzle phase to a dryer, for example a spray dryer, where a product of value containing protein and that is essentially free of fiber is formed by way of drying the concentrated thin stillage, the product being suitable as a feed additive, for example.

The drying can be done in a product-sensitive manner, in other words with no drying in furnaces, flames or the like such that the valuable contents are not damaged by the effect of heat. However, drying can also be done after processing in the centrifuge.

It is advantageous that the thin stillage fed to the working vessel can be prepared by processing grain stillage in a decanter, for example following a distillation process.

It is further advantageous if in addition to the concentrated thin stillage a permeate stream is discharged from the filtration unit, the permeate stream optionally being routable to an anaerobic wastewater treatment facility, for example, or being reusable as process water. This is advantageous since the wastewater can be easily processed as a result and a separate collection and storage system can be avoided, as is frequently needed in this case for process wastewater.

According to the invention, a device for producing a valuable product containing protein from thin stillage comprises a working vessel, a filtration unit, a centrifuge, preferably a separator and a dryer, wherein
5 the filtration unit is connected to the working vessel by way of a return line for a first substream of the concentrated thin stillage. This operating mode results in a nearly fiber-free valuable product, with the filtration unit operating efficiently.

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The invention is explained in more detail through the following exemplary embodiment and with the aid of the drawings in Fig. 1 and 2. Shown are:

15 Fig. 1 A schematic representation of a known process for preparing thin stillage and

Fig.2 A schematic representation of a device for manufacturing a valuable product from thin
20 stillage.

Fig. 1 shows a known processing step for a grain stillage (whole stillage) WS, for example following an ethanol distillation process. This stillage WS has a
25 dry matter content of about 10 wt.-%, with about 7 wt.-% being suspended solids and 3 wt.-% being dissolved solids, and is routed through a pump 1a to a decanter 1 where the stillage is processed into thick stillage (wet grains) WG and thin stillage TS.

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The fraction of dry matter in the thin stillage TS is about 4.15 wt.-% relative to the total mass of thin stillage TS, with about 1.15 wt.-% being suspended solids and about 3 wt.-% being dissolved solids. The
35 fraction of dry matter in the wet grains WG is greater than 30 wt.-% relative to the total mass of the wet grains WG.

The wet grains are routed from the decanter 1 to a dryer, such as a drum dryer 2, where the carrier fluid of the wet grains, usually water, is evaporated as much as possible resulting in a nutritious solid, called dry stillage (dried distillers grains with solubles) DDGS, which is used as a feed for livestock farming, among other things.

The thin stillage has a volumetric flow of 6-7 m³/h and is then forwarded to a working vessel 3.

The recovery of proteins and fats from thin stillage TS is described in more detail using a concrete exemplary embodiment in the system of Fig.2.

The working vessel 3 holds 20m³ in this concrete exemplary embodiment, and has a total of three inputs 4, 5 and 6. Input 4 of the working vessel 3 is an input for feeding thin stillage (TS) to the system, the input fed from the decanter 1 in Fig. 1, for example. The other inputs 5 and 6 to the working vessel 3 are provided for recycled thin stillage from the process and for the supernatant liquid phase.

The working vessel 3 also comprises an outlet 7 that connects the working vessel 3 to an ultrafiltration unit 9 and allows the transfer of thin stillage from the working vessel 3 to the ultrafiltration unit 9. The thin stillage is transported from the working vessel 3 to the ultrafiltration unit 9 by way of a feed pump 8 at a pressure of 3-4 bar, wherein the feed pump power output is preferably 15 KW.

The ultrafiltration unit 9 is only shown schematically in Fig. 2 and comprises at least one loop pump 10, a cooler 11 and one or more ultrafiltration modules 12.

During the filtration, liquid is drawn out of the thin

stillage and is discharged from the ultrafiltration unit 9 as permeate P at a volumetric flow of about 6 m³/h.

5 A plurality of ceramic membrane filter rods (not shown), preferably alpha-aluminum oxide and zirconium oxide filter rods, are disposed in the ultrafiltration modules 12. These membrane filter rods are penetrated by parallel channels running in the longitudinal
10 direction thereof, wherein the channels comprise a filter membrane, consisting of zirconium oxide deposited on an alpha-aluminum oxide carrier substance, along the channel wall and the entire perimeter thereof. In the process, the zirconium oxide layer
15 comprises finely distributed pores, whereas the support material is constructed of aluminum oxide with coarse pores. The filter membrane has an average pore size of 50nm.

20 A total of 168 membrane filter rods are disposed in the six ultrafiltration modules shown in Fig. 2. These filter rods provide a filtering surface area of 72 m² for separating liquid from the thin stillage. In the process, the permeate is forced through the ceramic
25 filter membrane by the 3-4 bar of pressure produced by the feed pump. The retentate and the pre-concentrated thin stillage are discharged from the ultrafiltration unit by way of a control valve 13.

30 Solids that are not able to pass through the 50 nm pores of the filter membrane build up on the surface of the membrane during filtration. In order to prevent plugging of the filter membrane, a turbulent flow of 5m/s can be generated by the loop pump 10 with the
35 valve 13 closed, at a volumetric flow of 810 m³/h. Such a flow can loosen or remove the accumulated solid particles from the filter membrane.

After filtration, a concentrated thin stillage leaves the ultrafiltration unit as a retentate and is divided into two substreams TS1 and TS2.

5 A second retentate substream or concentrated thin stillage substream TS2, which is preferably about 4-5 m³/h, is sent to a centrifuge, preferably a two-phase separator 16. The extent of the substream can be controlled by means for splitting flow, in this case a
10 valve 15, for example as a function of the flow rate. This flow rate can be determined through a sensor 14 which then adjusts the flow to a pre-determined setpoint by way of the valve 15.

15 In the centrifuge, the retentate produced in the ultrafiltration process is concentrated to a dry matter content of preferably greater than 12 wt.-%, wherein a clarified liquid is discharged at the overflow of the centrifuge as a supernatant liquid Z.

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The supernatant liquid Z has a solids fraction of less than one vol.-% and is returned from the centrifuge 16 to the working vessel through the return line 18 and the input 5 at a volumetric flow rate of 2.2-3.2 m³/h.

25 The nozzle phase DP or centrifuged phase has a dry matter content of more than 12 wt.-%, preferably up to 18 wt.-% and an FC factor of 7-8, and is then processed into a transportable and storable product using a dryer, not shown here. This product can be converted to
30 a more compact form, such as pellets, for example using a pelleting press 19. The pellets thus produced can be used as valuable feed additives, and have a fraction of dry matter of over 90 wt.-%, of which 40% is protein, 55% is fat and the rest is fiber and ash.

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A fractional second flow substream TS2 of 30m³/h is returned to the working vessel 3 through a return line 17 and the input 6 by way of flow control and mixed

with the thin stillage from the decanter of the input 4
so that a dry matter content of about 7 wt.-% is
adjusted for the thin stillage in the working vessel 3
and the FC factor, a concentration factor, is raised by
5 a factor of 3 to 4 compared to the thin stillage from
the decanter 1.

The thin stillage TS leaving the decanter 1 is
concentrated by the return line 17 for returning or
10 recycling a second retentate substream TS2 to the
working vessel 3. It was surprising to find that the
optimum operating point for an ultrafiltration unit 9
in the processing of thin stillage is reached at a
concentration of thin stillage TS to a dry matter
15 content of about 7%.

Solid particles in the size range of 5-100 nm were
removed from the permeate P separated from the
ultrafiltration unit 9, the permeate volume being
20 preferably 6 m³/h and primarily water, so that this
permeate can be fed to the community wastewater
treatment facility or can be subjected to an anaerobic
wastewater treatment. Moreover, the aqueous phase could
be further used as process water, for example for
25 creating a mash.

Claims

1. A method for processing thin stillage, characterized by the following steps:
 - 5 a) Feeding of thin stillage into a working vessel;
 - b) Concentrating thin stillage in a filtration unit; and
 - 10 c) Returning a first substream of concentrated thin stillage to the thin stillage contained in the working vessel in order to adjust the amount of dry matter.
- 15 2. The method as claimed in claim 1, characterized in that after the concentration of the thin stillage in a filtration unit a flow splitting is done of the concentrated thin stillage into at least the first substream and a second substream.
- 20 3. The method as claimed in claim 2, characterized in that after the flow splitting, at least the second substream of the concentrated thin stillage is clarified by a centrifuge, preferably by a separator, wherein the thin stillage is further
25 concentrated.
4. The method as claimed in claim 3, characterized in that a concentrated thin stillage with a dry matter amount of more than 12 wt.-%, preferably 18
30 wt.-% or higher is formed by further concentrating.
5. The method as claimed in claim 3 or 4, characterized in that after clarification, the
35 concentrated thin stillage is dried, forming a product of value containing protein.

6. The method as claimed in one of the previous claims, characterized in that the first substream following the flow splitting is at least three times, preferably at least six times greater than the second substream.
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7. The method as claimed in one of the previous claims, characterized in that the thin stillage fed to the working vessel is prepared by processing grain stillage in a decanter.
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8. The method as claimed in one of the previous claims, characterized in that in addition to the concentrated thin stillage a permeate stream is discharged from the filtration unit, the permeate stream being routable to an anaerobic wastewater treatment facility or being reusable as process water.
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9. The method as claimed in one of the previous claims, characterized in that the flow splitting is done after the concentrating of thin stillage in a filtration unit as a function of the dry matter content of the thin stillage located in the working vessel.
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10. The method as claimed in one of the previous claims, characterized in that flow control is regulated by way of the flow rate after concentration of thin stillage in a filtration unit.
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11. A device for producing a valuable product containing protein from thin stillage, comprising a working vessel, a filtration unit, a centrifuge, preferably a separator, and a dryer, characterized in that
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the filtration unit is connected to the

working vessel by way of a return line for a first substream of the concentrated thin stillage.

12. The device as claimed in claim 11, characterized
5 in that the filtration unit is an ultrafiltration unit.
13. The device as claimed in claim 11 or 12,
characterized in that the filtration unit
10 comprises means for flow splitting the concentrated stillage into a first substream and a second substream.
14. The device as claimed in one of the previous
15 claims, characterized in that the means for flow splitting is regulated as a function of the flow rate.
15. The device as claimed in one of the previous
20 claims, characterized in that the centrifuge is connected to the working vessel by way of a return line for returning the clarified centrifugate phase to the working vessel.