

CIRCULAR ECONOMY FOR PLASTIC WASTE TO POLYETHYLENE AND BASE OIL
VIA REFINERY CRUDE UNIT

BACKGROUND

[0001] The world has seen extremely rapid growth of plastics production. According to PlasticsEurope Market Research Group, the world plastics production was 335 million tons in 2016, 348 million tons in 2017, 359 million tons in 2018, and 367 million tons in 2020. According to McKinsey & Company, the global plastics-waste volume is estimated to be 460 million tons per year by 2030 if the current trajectory continues.

[0002] Single use plastic waste has become an increasingly important environmental issue. At the moment, there appear to be few options for recycling polyethylene and polypropylene waste plastics to value-added chemical and fuel products. Currently, only a small amount of polyethylene and polypropylene is recycled via chemical recycling, where recycled and cleaned polymer pellets are pyrolyzed in a pyrolysis unit to make fuels (naphtha, diesel), stream cracker feed or slack wax. The majority, greater than 80%, is incinerated, land filled or discarded.

[0003] The current method of chemical recycling via pyrolysis cannot make a big impact for the plastics industry. The current pyrolysis operation produces poor quality fuel components (naphtha and diesel range products), but the quantity is small enough that these products can be blended into fuel supplies. However, this simple blending cannot continue if very large volumes of waste polyethylene and polypropylene is to be recycled to address environmental issues. The products as produced from a pyrolysis unit are of too poor quality to be blended in large amounts in transportation fuels.

[0004] Processes are known which convert waste plastic into hydrocarbon lubricants. For example, U.S. Pat. No. 3,845,157 discloses cracking of waste or virgin polyolefins to form gaseous products such as ethylene/olefin copolymers which are further processed to produce synthetic hydrocarbon lubricants. U.S. Pat. No. 4,642,401 discloses the production of liquid hydrocarbons by heating pulverized polyolefin waste at temperatures of 150-500° C and pressures of 20-300 bars. U.S. Pat. No. 5,849,964 discloses a process in which waste plastic materials are depolymerized into a volatile phase and a liquid phase. The volatile phase is separated into a gaseous phase and a condensate. The liquid phase, the condensate and the gaseous phase are refined into liquid fuel components using standard refining techniques. U.S. Pat. No. 6,143,940 discloses a procedure for converting waste plastics into heavy wax compositions. U.S. Pat. No. 6,150,577 discloses a process of converting waste plastics into lubricating oils. EP0620264 discloses a process for producing lubricating oils from waste or

virgin polyolefins by thermally cracking the waste in a fluidized bed to form a waxy product, optionally using a hydrotreatment, then catalytically isomerizing and fractionating to recover a lubricating oil.

[0005] U.S. Pub. No. 2021/0130699 discloses processes and systems for making recycle content hydrocarbons from recycled waste material. The recycle waste material is pyrolyzed to form a pyrolysis oil composition, at least a portion of which may then be cracked to form a recycle olefin composition.

[0006] Other documents which relate to processes for converting waste plastic into lubricating oils include U.S. Patent Nos. 6,288,296; 6,774,272; 6,822,126; 7,834,226; 8,088,961; 8,404,912 and 8,696,994; and U.S. Patent Application Publication Nos. 2019/0161683; 2016/0362609; and 2016/0264885. The foregoing patent documents are incorporated herein by reference in their entirety.

[0007] Globally, recycling or upcycling of plastic waste has gained great interest to save resources and the environment. Mechanical recycling of plastic waste is rather limited due to different types, properties, additives, and contaminants in the collected plastics. Usually, the recycled plastics are of degraded quality. Chemical recycling to the starting material or value-added chemicals has emerged as a more desirous route.

[0008] However, in order to achieve chemical recycling of single use plastics in an industrially significant quantity to reduce its environmental impact, more robust processes are needed. The improved processes should establish “circular economy” for the waste polyethylene and polypropylene plastics where the spent waste plastics are recycled effectively back as starting materials for the polymers or value-added chemicals or fuels.

SUMMARY

[0009] Provided is a continuous process for converting waste plastic into recycle for polyethylene polymerization. The process comprises selecting waste plastics containing polyethylene and/or polypropylene. These waste plastics are blended with a petroleum feed material. The resulting blend is generally a stable blend and a homogenous mixture, particularly at a temperature below the melting point of the waste plastic. The blend comprises about 20 wt. % or less of the selected waste plastic. The blend is then cofed with conventional refinery feed, such as crude oil, to a crude unit in a refinery.

[0010] The incorporation of the process with an oil refinery is an important aspect of the present process and allows the creation of a circular economy with a single use waste plastic such as polyethylene. Thus, the blend is passed to a refinery crude unit. The blend is passed at

a temperature above its pour point in order to be able to pump the blend to the refinery crude unit. The blend is heated above the melting point of the plastic before injected to the crude distillation unit. A liquid petroleum gas C₃-C₄ mixture is recovered from the crude unit. The C₃-C₄ mixture is passed to a steam cracker to produce ethylene, from which polyethylene and polyethylene products can be prepared.

[0011] In another embodiment, a naphtha (C₅-C₈) can be recovered from the crude unit and passed to a steam cracker to produce ethylene.

[0012] In another embodiment, flow from the refinery crude unit is fed to a refinery hydrocracking unit. The feed to the hydrocracking unit comprises at least any heavy fraction resulting from the crude unit. A LPG stream comprising C₃-C₄ hydrocarbons, and a naphtha stream comprising C₅-C₈ hydrocarbons are recovered from the hydrocracking unit. The C₃-C₄ and naphtha streams can be passed onto a steam cracker to make ethylene. A heavy fraction is also recovered from the hydrocracking unit, which fraction is passed to an isomerization/dewaxing unit. Good base oil can be recovered from the dewaxing unit, which can be sent for further processing to a hydro finishing unit to create a truly premium base oil.

[0013] The refinery will generally have its own hydrocarbon feed flowing through the refinery units. An important aspect of the present process is to not negatively impact the operation of the refinery. The refinery must still produce valued chemicals and fuels. Otherwise, the incorporation of the process with an oil refinery would not be a workable solution. The flow volume must therefore be carefully observed.

[0014] The flow volume of the waste plastic/petroleum blend to the refinery units can comprise any practical or accommodating volume % of the total flow to the refinery units. Generally, the flow of the blend can be up to about 50 vol. % of the total flow. In one embodiment, the flow of the blend is an amount up to about 25 vol. % of the total flow, i.e., the refinery flow and the blend flow.

[0015] Among other factors, it has been found that by adding refinery operations one can efficiently and effectively recycle plastic waste while also complementing the operation of a refinery in the preparation of higher value products such as gasoline, base oil, jet fuel and diesel. But also, by adding refinery operations it has been found that clean ethylene can be efficiently and effectively produced from the waste plastics for ultimate polyethylene polymer production. Positive economics are realized for the overall process from recycled plastics to a polyethylene product with product quality identical to that of virgin polymer. The present process also offers the ability of recycling the waste plastics to prepare good/premium base oil, while also preparing the polyethylene products.

BRIEF DESCRIPTION OF THE DRAWINGS

- [0016] FIG. 1 depicts the current practice of pyrolyzing waste plastics to produce fuel or wax.
- [0017] FIG. 2 depicts a present process of preparing a hot, homogenous liquid blend of plastic and petroleum feedstock, and how the blend can be fed to a refinery conversion unit.
- [0018] FIG. 3 depicts in detail a stable blend preparation process, and how the stable blend can be fed to a refinery conversion unit.
- [0019] FIG. 4 depicts the plastic type classification for waste plastics recycling.
- [0020] FIG. 5 depicts a present process where the prepared blend is passed to a refinery crude unit.
- [0021] FIG. 6 depicts another embodiment of the present process where the prepared blend is passed to a refinery crude unit and a hydrocracking unit.
- [0022] FIG. 7 graphically depicts a thermal gravimetric analysis (TGA) of the thermal stability of polyethylene and polypropylene.

DETAILED DESCRIPTION

[0023] In the present process, provided is a method to recycle waste polyethylene and/or polypropylene back to virgin polyethylene to establish a circular economy by combining distinct industrial processes. And in one embodiment premium base oil can be obtained due to the integration of the process with a refinery. A substantial portion of polyethylene and polypropylene polymers are used in single use plastics and get discarded after its use. The single use plastic waste has become an increasingly important environmental issue. At the moment, there appear to be few options for recycling polyethylene and polypropylene waste plastics to value-added chemicals and fuel products. Currently, only a small amount of polyethylene/polypropylene is recycled via chemical recycling, where recycled and cleaned polymer pellets are pyrolyzed in a pyrolysis unit to make fuels (naphtha, diesel), steam cracker feed or slack wax.

[0024] Ethylene is the most produced petrochemical building block. Ethylene is produced in hundreds of millions tons per year via steam cracking. The steam crackers use either gaseous feedstocks (ethane, propane and/or butane) or liquid feed stocks (naphtha or gas oil). It is a noncatalytic cracking process that operates at very high temperatures, up to 850° C.

[0025] Polyethylene is used widely in various consumer and industrial products. Polyethylene is the most common plastic, over 100 million tons of polyethylene resins are produced

annually. Its primary use is in packaging (plastic bags, plastic films, geomembranes, containers including bottles, etc.). Polyethylene is produced in three main forms: high-density polyethylene (HDPE, $\sim 0.940\text{-}0.965\text{ g/cm}^3$), linear low-density polyethylene (LLDPE, $\sim 0.915\text{-}0.940\text{ g/cm}^3$) and low-density polyethylene (LDPE, $(< 0.930\text{ g/cm}^3)$, with the same chemical formula $(\text{C}_2\text{H}_4)_n$ but different molecular structure. HDPE has a low degree of branching with short side chains while LDPE has a very high degree of branching with long side chains. LLDPE is a substantially linear polymer with significant numbers of short branches, commonly made by copolymerization of ethylene with short-chain alpha-olefins.

[0026] Low density polyethylene (LDPE) is produced via radical polymerization at $150\text{--}300^\circ\text{C}$ and very high pressure of $1,000\text{-}3,000\text{ atm}$. The process uses a small amount of oxygen and/or organic peroxide initiator to produce polymer with about $4,000\text{--}40,000$ carbon atoms per the average polymer molecule, and with many branches. High density polyethylene (HDPE) is manufactured at relatively low pressure ($10\text{-}80\text{ atm}$) and $80\text{-}150^\circ\text{C}$ temperature in the presence of a catalyst. Ziegler-Natta organometallic catalysts (titanium(III) chloride with an aluminum alkyl) and Phillips-type catalysts (chromium(IV) oxide on silica) are typically used, and the manufacturing is done via a slurry process using a loop reactor or via a gas phase process with a fluidized bed reactor. Hydrogen is mixed with ethylene to control the chain length of the polymer. Manufacturing conditions of linear low-density polyethylene (LLDPE) are similar to those of HDPE except copolymerization of ethylene with short-chain alpha-olefins (1-butene or 1-hexene).

[0027] Today, only a small portion of spent polyethylene products is collected for recycling, due to the inefficiencies and ineffectiveness of the recycling efforts discussed above.

[0028] FIG. 1 shows a diagram of the pyrolysis of waste plastics fuel or wax that is generally operated in the industry today. Generally, the waste plastics are sorted together 1. The cleaned plastic waste 2 is converted in a pyrolysis unit 3 to offgas 4 and pyrolysis oil (liquid product). The offgas 4 from the pyrolysis unit 3 is used as fuel to operate the pyrolysis unit. An on-site distillation unit separates the pyrolysis oil to produce naphtha and diesel 5 products which are sold to fuel markets. The heavy pyrolysis oil fraction 6 is recycled back to the pyrolysis unit 3 to maximize the fuel yield. Char 7 is removed from the pyrolysis unit 3. The heavy fraction 6 is rich in long chain, linear hydrocarbons, and is very waxy (i.e., forms paraffinic wax upon cooling to ambient temperature). Wax can be separated from the heavy fraction 6 and sold to the wax markets.

[0029] The present process, however, does not pyrolyze the waste plastic. Rather, a stable blend of petroleum feedstock and the waste plastic is prepared. Thus, the pyrolysis step can be avoided, which is a significant energy savings.

[0030] The present blend can be prepared in a hot blend preparation unit where the operating temperature is above the melting point of the plastic (about 150-250° C), to make a hot, homogeneous liquid blend of plastic and oil. The hot homogeneous liquid blend of plastic and oil can be fed directly to the refinery units.

[0031] Alternatively, a blend is prepared in a stable blend preparation unit where the hot homogeneous liquid blend is cooled to ambient temperature in a controlled manner to allow for easy storage and transportation. By using this method, a stable blend can be prepared at a facility away from a refinery and can be transported to a refinery unit. Then the stable blend is heated above the melting point of the plastic to feed to the refinery conversion unit. The stable blend is a physical mixture of micron size plastic particles finely suspended in the petroleum-based oil. The mixture is stable, and the plastic particles do not settle or agglomerate upon storage for extended period.

[0032] What is meant by heating the blend to a temperature above the melting point of the plastic is clear when a single plastic is used. However, if the waste plastic comprises more than one waste plastic, then the melting point of the plastic with the highest melting point is exceeded. Thus, the melting points of all plastics must be exceeded. Similarly, if the blend is cooled below the melting point of the plastic, the temperature must be cooled below the melting points of all plastics comprising the blend.

[0033] Compared with the pyrolysis unit, these blend preparation units operate at a much lower temperature (~500-600° C vs. 120-250° C). Thus, the present process is a far more energy efficient process in preparing a refinery feedstock derived from waste plastic than a thermal cracking process such as pyrolysis.

[0034] The use of the present waste plastic/petroleum blend further increases the overall hydrocarbon yield obtained from the waste plastic. This increase in yield is significant. The hydrocarbon yield using the present blend offers a hydrocarbon yield that can be as much as 98%. To the contrary, pyrolysis produces a significant amount of light product from the plastic waste, about 10-30 wt. %, and about 5-10 wt. % of char. These light hydrocarbons are used as fuel to operate the pyrolysis plant, as mentioned above. Thus, the liquid hydrocarbon yield from the pyrolysis plant is at most 70-80%.

[0035] When the present blend is passed into the refinery units, such as a crude unit, only a minor amount of offgas is produced. Refinery units use catalytic cracking processes that are

different from the thermal cracking process used in pyrolysis. With catalytic processes, the production of undesirable light-end byproducts such as methane and ethane is minimized. Refinery units have efficient product fractionation and are able to utilize all hydrocarbon products streams efficiently to produce high value materials. Refinery co-feeding will produce only about 2% of offgas (H₂, methane, ethane, ethylene). The C₃ and C₄ streams are captured to produce useful products such as circular polymer and/or quality fuel products, including premium base oils. Thus, the use of the present petroleum/plastic blend offers increased hydrocarbons from the plastic waste, as well as a more energy efficient recycling process compared to a thermal process such as pyrolysis.

[0036] The present process converts single use waste plastic in large quantities by integrating the waste plastic blended with petroleum product streams into an oil refinery operation. The resulting processes produce the feedstocks for the polymers (naphtha or C₃ and C₄ for ethylene cracker), high quality gasoline, diesel, jet fuel, and/or quality base oil.

[0037] Generally, the present process provides a circular economy for polyethylene plants. Polyethylene is produced via polymerization of pure ethylene. Clean ethylene can be made using a steam cracker. Either naphtha or a C₃ or C₄ stream can be fed to the steam cracker. The ethylene is then polymerized to create polyethylene.

[0038] By adding refinery operations to upgrade the waste plastic to higher value products (gasoline, jet fuel, diesel, and base oil) and to produce clean ethylene for ultimate polyethylene polymer production, positive economics are realized for the overall process of recycled plastics to polyethylene products with product quality identical to that of the virgin polymer. And, by integrating the present recycle process with an oil refinery operation, a more energy efficient and effective process is achieved while avoiding any issues with the refinery operation.

[0039] The integration of a refinery operation becomes quite important in another aspect. Waste plastics contain contaminants, such as calcium, magnesium, chlorides, nitrogen, sulfur, dienes, and heavy components, which products cannot be used in a large quantity for blending in transportation fuels. It has been discovered that by having these products go through the refinery units, the contaminants can be captured in pre-treating units and their negative impacts diminished. The fuel components can be further upgraded with appropriate refinery units using chemical conversion processes, with the final transportation fuels produced in the integrated process being of higher quality and meeting the fuels quality requirements. The integrated process will generate a much cleaner and more pure ethylene stream for polyethylene production. These large on-spec productions allow “cyclical economy” for the recycle plastics to be feasible.

[0040] The carbon in and out of the refinery operations are “transparent,” meaning that all the molecules from the waste plastic do not necessarily end up in the exact olefin product cycled back to the polyolefin plants, but are nevertheless assumed as “credit” as the net “green” carbon in and out of the refinery is positive. With these integrated processes, the amount of virgin feeds needed for polyethylene plants are reduced significantly.

[0041] In some cases, the conversion of waste plastic into clean fuels takes less energy than production of fuels from a virgin petroleum feedstock. As the collection and processing of waste plastic improves the gain in energy efficiencies will further improve. Such fuels and base oil produced from the blend of waste plastic and oil will have recycle contents and lower carbon footprints than corresponding fuels and base oil made from pure petroleum feedstock. The present process can produce clean gasoline, jet fuel, diesel and base oil with recycle contents and a lower CO₂ (lower carbon) footprint from waste plastic.

[0042] FIG. 2 illustrates a method for preparing a hot homogenous blend of plastic and petroleum feedstock for use in the present process for direct injection to a refinery unit where a hot, homogeneous liquid blend of plastic and oil is prepared in a hot blend preparation unit. The preferred range of the plastic composition in the blend is about 1-20 wt. %. If high molecular weight polypropylene (average molecular weight of 250,000 or greater) waste plastic or high-density polyethylene (density above 0.93 g/cc) is used as the predominant waste plastic, e.g., at least 50 wt. %, then the amount of waste plastic used in the blend is more preferably about 10 wt. %. The reason being that the pour point and viscosity of the blend would be high.

[0043] The preferred conditions for the hot homogeneous liquid blend preparation include heating the plastic above the melting point of the plastic while vigorously mixing with a petroleum feedstock. The preferred process conditions include heating to a 250- 500° F temperature, with a residence time of 5- 240 minutes at the final heating temperature, and 0-10 psig atmospheric pressure. This can be done in the open atmosphere as well as preferably under an oxygen-free inert atmosphere.

[0044] Referring to FIG. 2 of the Drawings, a stepwise preparation process of preparing the hot homogeneous liquid blend is shown. Mixed waste plastic is sorted to create post-consumer waste plastic 21 comprising polyethylene and/or polypropylene. The waste plastic is cleaned 22 and then mixed with an oil 24 in a hot blend preparation unit 23. After the mixing in 23, the homogeneous blend of the plastic and oil is recovered 25. Optionally a filtration device may be added (not shown) to remove any undissolved plastic particles or any solid impurities present in the hot liquid blend. The hot blend of the plastic and oil can then be combined with a refinery feedstock, such as crude oil 50, and become a mixture of the plastic/oil blend and crude oil, 26,

which can then be passed to a refinery unit. In the present process, the refinery unit in one embodiment is a crude unit.

[0045] FIG. 3 illustrates a method for preparing a stable blend of plastic and oil for use in the present process. The stable blend is made in a stable blend preparation unit by a two-step process. The first step produces a hot, homogeneous liquid blend of plastic melt and petroleum feedstock, the step identical to the hot blend preparation described in Figure 2. The preferred range of the plastic composition in the blend is about 1-20 wt. %. If high molecular weight polypropylene (average molecular weight of 250,000 or greater) waste plastic or high-density polyethylene (density above 0.93 g/cc) is used as the predominant waste plastic, e.g., at least 50 wt. %, then the amount of waste plastic used in the blend is more preferably about 10 wt. %. The reason being that the pour point and viscosity of the blend would be high.

[0046] The preferred conditions for the hot homogeneous liquid blend preparation include heating the plastic above the melting point of the plastic while vigorously mixing with a petroleum feedstock. The preferred process conditions include heating to a 250- 500° F temperature, with a residence time of 5- 240 minutes at the final heating temperature, and 0-10 psig atmospheric pressure. This can be done in the open atmosphere as well as preferably under an oxygen-free inert atmosphere.

[0047] In the second step, the hot blend is cooled down below the melting point of the plastic while continuously vigorously mixing with petroleum feedstock, and then further cooling to a lower temperature, preferably ambient temperature, to produce a stable blend of plastic and oil.

[0048] It has been found that the stable blend is an intimate physical mixture of plastic and petroleum feedstock. The plastic is in a “de-agglomerated” state. The plastic maintains a finely dispersed state of solid particles in petroleum feedstock at temperatures below the melting point of the plastic, and particularly at ambient temperatures. The blend is stable and allows easy storage and transportation. At a refinery, the stable blend is heated in a preheater above the melting point of the plastic to produce a hot, homogenous liquid blend of the plastic and petroleum. The hot liquid blend can then be fed to a refinery unit as a cofeed with conventional refinery feed.

[0049] In FIG. 3, further details of the stable blend preparation are shown. The stable blend is made in a stable blend preparation unit 100 by a two-step process. As shown, clean waste 22 is passed to the stable blend preparation unit 100. The selected plastic waste 22 is heated and mixed with a refinery feedstock oil 24. The plastic waste is heated above the melting point of the plastic to melt the plastic. The petroleum feedstock is mixed with the heated plastic at 23. The mixing is often quite vigorous. The mixing and heating conditions can generally comprise

heating at a temperature in the range of about 250-500° F, with a residence time of 5-240 minutes at the final heating temperature. The heating and mixing can be done in the open atmosphere or under an oxygen-free inert atmosphere. The result is a hot, homogenous liquid blend of plastic and oil 25. Optionally a filtration device may be added (not shown) to remove any undissolved plastic particles or any solid impurities present in the hot homogeneous liquid blend.

[0050] The hot blend 25 is then cooled below the melting point of the plastic while continuing the mixing of the plastic with the petroleum oil feedstock 101. Cooling generally continues, usually to an ambient temperature, to produce a stable blend of the plastic and oil 102. At a refinery, the stable blend can be fed to a preheater, 29, which heats the blend above the melting point of the plastic to produce a mixture of plastic/oil blend and crude oil, 26, which is then fed to a refinery conversion unit. In the present process, the refinery unit in one embodiment is a crude unit.

[0051] The preferred plastic starting material for the present process is sorted waste plastics containing predominantly polyethylene and polypropylene (plastics recycle classification types 2, 4, and 5). The pre-sorted waste plastics are washed and shredded or pelleted to feed to a blend preparation unit. FIG. 4 depicts the plastic type classification for waste plastics recycling. Classification types 2, 4, and 5 are high density polyethylene, low density polyethylene and polypropylene, respectively. Any combination of the polyethylene and polypropylene waste plastics can be used. For the present process, at least some polyethylene waste plastic is preferred. Polystyrene, classification 6, can also be present in a limited amount.

[0052] Proper sorting of waste plastics is very important in order to minimize contaminants such as N, Cl, and S. Plastics waste containing polyethylene terephthalate (plastics recycle classification type 1), polyvinyl chloride (plastics recycle classification type 3) and other polymers (plastics recycle classification type 7) need to be sorted out to less than 5%, preferably less than 1% and most preferably less than 0.1%. The present process can tolerate a moderate amount of polystyrene (plastics recycle classification type 6). Waste polystyrene needs to be sorted out to less than 20%, preferably less than 10% and most preferably less than 5%.

[0053] Washing of waste plastics can remove metal contaminants such as sodium, calcium, magnesium, aluminum, and non-metal contaminants coming from other waste sources. Non-metal contaminants include contaminants coming from the Periodic Table Group IV, such as silica, contaminants from Group V, such as phosphorus and nitrogen compounds, contaminants from Group VI, such as sulfur compounds, and halide contaminants from Group VII, such as

fluoride, chloride, and iodide. The residual metals, non-metal contaminants, and halides need to be removed to less than 50 ppm, preferentially less than 30ppm and most preferentially to less than 5ppm.

[0054] If the washing does not remove the metals, non-metal contaminants, and halide impurities adequately, then a separate guard bed can be used to remove the metals and non-metal contaminants.

[0055] The petroleum with which the waste plastic is blended is generally a petroleum feedstock for the refinery. It is preferred that the petroleum blending oil is the same as the petroleum feedstock for the refinery. The petroleum can also comprise any petroleum derived oil or petroleum based material. In one embodiment, the petroleum feedstock oil can comprise atmospheric gas oil, vacuum gas oil (VGO), atmospheric residue, or heavy stocks recovered from other refinery operations. In one embodiment, the petroleum feedstock oil with which the waste plastic is blended comprises VGO. In one embodiment, the petroleum feedstock oil with which the waste plastic is blended comprises light cycle oil (LCO), heavy cycle oil (HCO), FCC naphtha, gasoline, diesel, toluene, aromatic solvent derived from petroleum.

[0056] FIG. 5 shows one embodiment of a present integrated process, where the blend is sent to a crude unit. The same numbers in FIG. 5 that correspond to FIGS. 2 and 3 refer to the same items/units. As shown, selected waste 21 is cleaned 22 and then passed to a blend preparation unit 23, where the plastic and refinery feedstock 24, are blended to create a hot blend of the plastic and oil 25. To this blend, when desired, a crude oil 50, preferentially desalted crude oil, is added. If the blend of plastic/oil is still hot, (25 in FIG. 2) then it can be mixed with the co-feed oil 50 immediately. However, if the stable blend of plastic/oil needs heating due to storage or transportation (102 in FIG. 3) the blend is generally heated, for example, with a preheater (preheater 29 in FIG. 3) to a temperature above the melting point of the plastic before mixing with the co-feed crude oil. This homogeneous plastic/oil blend and crude oil 26 is then sent to a crude unit 27 in a refinery. In another embodiment, the heated blend and the crude oil co-feed are each passed directly, but separately, to the crude unit.

[0057] The refinery crude unit separates crude oil into multiple fractions such as liquefied petroleum gas (LPG), naphtha, kerosene, diesel and gas oil which will be further treated into useful petroleum products. The refinery crude unit consists of a crude treating section, commonly known as a desalter, a preheater section and a crude oil distillation or fractionation section. The distillation section typically includes an atmospheric distillation unit and/or vacuum distillation unit.

[0058] The blend and any co-feed are fed to the preheater unit or downstream of the preheater unit. The blend and co-feed should not be fed to the desalter unit, which removes the salts and solids contained in the oil to protect downstream equipment from the harmful effects of the contaminants. The desalter unit typically operates at temperatures between about 215° F to about 280° F, which are too low and may cause some loss of plastic particles in the blend.

[0059] The refinery will generally have its own hydrocarbon feed flowing through the refinery units. In this case, as shown in FIG. 5, the hydrocarbon feed is a crude oil 50. The flow volume of the blend to the refinery units, here a crude unit, can comprise any practical or accommodating volume % of the total flow to the refinery units. Generally, the flow of the blend, for practical reasons, can be up to about 50 vol. % of the total flow, i.e., the refinery flow and the blend flow. In another embodiment, the volume flow of the blend is an amount up to about 25 vol. % of the total flow. About 50 vol. % has been found to be an amount that is quite practical in its impact on the refinery while also providing excellent results and being an amount that can be accommodated. Avoiding any negative impact on the refinery and its products is important. If the amount of the plastic in the final blend (comprising the plastic/oil blend and co-feed petroleum) is greater than 20 wt. % of the final blend, difficulties in crude unit operation might ensue. By the final blend is meant the present plastic/oil blend and any co-feed petroleum.

[0060] The atmospheric distillation unit of the crude unit is heated to about 340-372° C (644-700° F) at the bottom of the distillation column, and liquid is removed at various points of the fractional distillation column to produce various fuels. The fuels from the crude units can be sent to various upgrading units in the refinery to remove impurities (nitrogen, sulfur) and to catalytically transform the fractions to improve the product properties, such as octane and cetane numbers.

[0061] In FIG. 5, the bottom residue or heavy fraction 30 from the atmospheric distillation column in the refinery crude unit 27 is recovered. A heavy naphtha fraction and a diesel fraction 33 can also be recovered. These fractions can be sent to various upgrading processes 34. The overall process can produce LPG (<80° F), gasoline (80-400° F), jet fuel (360-500° F), and diesel fuel (300-700° F). The boiling points for these fractions are adjusted depending on the season and local specifications.

[0062] From the refinery crude unit, a C₃-C₄ LPG (liquid petroleum gas) stream 31 and a straight run, a C₅-C₈ naphtha stream 32 are collected. The C₃-C₄ stream 31 can be passed to a steam cracker 36 to make ethylene 37. The naphtha stream 32 can also contribute in whole or in part to the feed to the steam cracker 36. Part of the naphtha stream can also be passed to a

clean gasoline pool. Product streams from the various conversion processes can be passed to the gasoline, jet fuel and diesel fuel pools 35. LPG and naphtha 45 from the various upgrading processes 34 can also contribute to the feed to the steam cracker 36.

[0063] The ethylene 37 is passed on to a polymerization unit 40 to produce polyethylene. The polyethylene is processed further to produce various polyethylene products 41 to fit the needs of consumer products.

[0064] Referring to FIG. 6, as in FIG. 5, the same numerals as in FIGS. 2 and 3 refer to the same streams, blends or units. Selected waste 21 is cleaned 22 and then passed to a blend preparation unit 23, where the plastic and refinery feedstock 24, are blended to create a hot blend of the plastic and oil 25. To this blend, when desired, a crude oil 50 is added. If the blend of plastic/oil is still hot, (25 in FIG. 2) then it can be mixed with the co-feed oil 50 immediately. However, if the stable blend of plastic/oil needs heating due to storage or transportation (102 in FIG. 3) the blend is generally heated, for example, with a preheater (preheater 29 in FIG. 3) to a temperature above the melting point of the plastic before mixing with the co-feed crude oil. This homogeneous plastic/oil blend and crude oil 26 is then sent to a crude unit 27 in a refinery.

[0065] The bottom residue from the atmospheric distillation column in the crude unit 27 is also known as atmospheric residue, is typically sent to a vacuum distillation column in the crude unit to produce vacuum gas oil (650 – 1050° F) and vacuum residue. The vacuum gas oil may be used to produce lube oil or further cracked to produce gasoline, jet fuel and diesel fuel. The overall process can produce LPG (<80° F), gasoline (80-400° F), jet fuel (360-500° F), and diesel fuel (300-700° F). The boiling points for these fractions are adjusted depending on the season and local specifications.

[0066] In FIG. 6, flow from the refinery crude unit 27, which includes the vacuum gas oil 20, is passed to a refinery hydrocracking unit 28. Any suitable hydrocracking operation can be run. The catalyst in the hydrocracker can be selected from any known hydrocracking catalysts. The hydrocracking conditions generally include a temperature in the range of from 175° C to 485° C, molar ratios of hydrogen to hydrocarbon charge from 1 to 100, a pressure in the range of from 0.5 to 350 bar, and a liquid hourly space velocity (LHSV) in the range of from 0.1 to 30. Larger molecules are cracked into smaller molecules in the hydrocracking reactor. A hydrocracking catalyst normally comprises a large pore zeolite such as USY, and various combinations of Group VI and VIII base metals such as nickel, cobalt, molybdenum and tungsten, which are finely dispersed on an alumina or oxide support.

[0067] From the hydrocracking unit is recovered an LPG C₃-C₄ stream 51, a clean naphtha stream 52, and a heavy fraction 54. The heavy fraction 54 is passed to an

isomerization/dewaxing unit 55. Within the dewaxing reactor, the feed may first be contacted with a hydrotreating catalyst under hydrotreating conditions in a hydrotreating zone or guard layer to provide a hydrotreated feedstock. A hydrotreating catalyst normally contains various combinations of Group VI and VIII base metals such as nickel, cobalt, molybdenum and tungsten, which are finely dispersed on an alumina or oxide support. Contacting the feedstock with the hydrotreating catalyst in a guard layer may serve to effectively hydrogenate aromatics in the feedstock, and to remove N- and S-containing compounds from the feed, thereby protecting the hydroisomerization catalysts of the catalyst system. By “effectively hydrogenate aromatics” is meant that the hydrotreating catalyst is able to decrease the aromatic content of the feedstock by at least about 20%. The hydrotreated feedstock may generally comprise C₁₀+ n-paraffins and slightly branched isoparaffins, with a wax content of typically at least about 20%.

[0068] Hydroisomerization catalysts useful in the present processes typically will contain a catalytically active hydrogenation metal. The presence of a catalytically active hydrogenation metal leads to product improvement, especially viscosity index (VI) and stability. Typical catalytically active hydrogenation metals include chromium, molybdenum, nickel, vanadium, cobalt, tungsten, zinc, platinum, and palladium. The metals platinum and palladium are especially preferred, with platinum most especially preferred. If platinum and/or palladium is used, the total amount of active hydrogenation metal is typically in the range of 0.1 wt. % to 5 wt. % of the total catalyst, usually from 0.1 wt. % to 2 wt. %. In addition, a hydroisomerization catalyst normally contains a medium pore size zeolite such as ZSM-23, ZSM-48, ZSM-35, SSZ-32, SSZ-91 dispersed on an oxide support.

[0069] The refractory oxide support may be selected from those oxide supports, which are conventionally used for catalysts, including silica, alumina, silica-alumina, magnesia, titania and combinations thereof.

[0070] The conditions in the isomerization/dewaxing reactor unit 55 will generally include a temperature within a range from about 390° F to about 800° F (199° C to 427° C). In an embodiment, the hydroisomerization dewaxing conditions includes a temperature in the range from about 550° F to about 700° F (288° C to 371° C). In a further embodiment, the temperature may be in the range from about 590° F to about 675° F (310° C to 357° C). The total pressure may be in the range from about 500 to about 3000 psig (0.10 to 20.68 MPa), and typically in the range from about 750 to about 2500 psig (0.69 to 17.24 MPa).

[0071] From the isomerization/dewaxing unit 55 a dewaxed oil 56 can be recovered, which oil can be used as a base oil. The oil can also be passed to a hydrofinishing unit 57 to prepare a

premium base oil 58. In the hydrofinishing unit 57, the hydrofinishing may be performed in the presence of a hydrogenation catalyst, as is known in the art. The hydrogenation catalyst used for hydrofinishing may comprise, for example, platinum, palladium, or a combination thereof on an alumina support. The hydrofinishing may be performed at a temperature in the range from about 350° F to about 650° F (176° C to 343° C), and a pressure in the range from about 400 psig to about 4000 psig (2.76 to 27.58 MPa). Hydrofinishing for the production of lubricating oils is described, for example, in U.S. Pat. No. 3,852,207, the disclosure of which is incorporated by reference herein.

[0072] The LPG stream 51, and the clean naphtha stream 52 can be passed to a steam cracker 36 to make ethylene 37. The stream 52 can be passed in whole or in part to the steam cracker 36, as it also contains clean gasoline, jet fuel and diesel fuel fractions. At least some of the stream 52 can also be passed to gasoline pools or upgrading processes in order to upgrade the fuel fractions. LPG and naphtha 53 can also be recovered from the dewaxing unit 55 and passed to the steam cracker 36 as feed to make ethylene 37. The ethylene is passed on to an ethylene polymerization unit 40 to produce polyethylene, which is processed further to produce various polyethylene products 41 to fit the needs of consumers.

[0073] The steam cracker and ethylene polymerization unit is preferably located near the refinery so that the feedstocks (propane, butane, naphtha, or propane/propylene mix) can be transferred via pipeline. For a petrochemical plant located away from the refinery, the feedstock can be delivered via truck, barge, rail car, or pipeline.

[0074] The benefits of a circular economy and an effective and efficient recycling campaign are realized by the present integrated process.

[0075] The following examples are provided to further illustrate the present process and its benefits. The examples are meant to be illustrative and not limiting.

[0076] Example 1: Properties of Plastic Samples, and Feedstocks Used for Blend Preparations

[0077] Four plastic samples, low density polyethylene (LDPE, Plastic A), high density polyethylene (HDPE, Plastic B), two polypropylene samples with average molecular weight of ~12,000 (PP, Plastic C) and ~250,000 (PP, Plastic D) were purchased, and their properties are summarized in Table 1.

Table 1
Properties of Plastics Used

	LDPE (Plastic A)	HDPE (Plastic B)	PP (Plastic C)	PP (Plastic D)
Form	Pellets	Pellets	Pellets	Pellets
Melt Index	25 g/ 10 min (190 °C/2.16 kg)	12 g/ 10 min (190 °C/2.16 kg)	-	12 g/ 10 min (230 °C/2.16 kg)
Melting Point, °C	116	125 – 140	157	160 – 165
Transition Temp, °C	93, softening	125, softening	163, softening	-
Density, g/mL at 25 °C	0.925	0.952	0.9	0.9
Hardness	-	66	-	100
Average molecular weight, M_w	-	-	~12,000	~250,000
Average molecular weight, M_n	-	-	~5,000	~67,000

[0078] Petroleum feedstocks used to prepare the stable blends with plastic includes hydrotreated vacuum gas oil (VGO), Aromatic 100 solvent, light cycle oil (LCO), and diesel. Their properties are shown in Table 2 below. Aromatic 100 is a commercially available aromatic solvent manufactured from petroleum-based material, and mainly contains C9-C10 dialkyl and trialkyl benzenes.

Table 2
Properties of Petroleum Feedstocks for Blend Preparation

	Hydrotreated VGO Petroleum Feed #1	Aromatic 100 Petroleum Feed #2	LCO Petroleum Feed #3	Diesel Petroleum Feed #4
Specific Gravity	0.897	0.872	0.956	0.811
Carbon, wt%	87.84	89.90	90.50	86.4
Hydrogen, wt%	12.69	10.10	9.50	14.6
H/C Molar Ratio	1.73	1.33	1.26	2.0
Bromine Number	2	-	-	0.1
Total S, ppm	150	0	900	<2
Total N, ppm	273	0	N/A	<0.1
Ni, ppm	<0.6	0	<0.2	<0.2
V, ppm	<0.6	0	<0.2	<0.2
Simdist, °F				
IBP (0.5%)	462	297	235	536
5 wt%	573	325	405	553
10 wt%	616	327	441	563

30 wt%	706	330	490	601
50 wt%	775	336	541	638
70 wt%	854	344	607	673
90 wt%	962	355	689	702
95 wt%	1008	362	718	709
FBP (99.5%)	1107	376	786	717

[0079] Thermal Gravimetric Analysis (TGA) was conducted with Plastic A (LDPE) and Plastic C (Polypropylene) to verify the plastic materials are thermally stable well above the melt preparation temperature. TGA results shown in Figure 7 indicate the LDPE sample is stable up to 800° F and the polypropylene sample up to 700° F.

[0080] Example 2: Feedstocks of C₃-C₄ and/or Naphtha Generation from Waste Plastics/Oil Blend Cofeeding to Refinery Crude Unit

[0081] By feeding the present plastic/oil blend, with or without a cofeed, to a crude unit the blend will be fractionated into multiple components. The refinery crude unit produces substantial amounts of clean propane, butane, and naphtha streams, as well as other streams for refinery conversion units. The conversion units downstream of the crude unit, such as the FCC and Hydrocracking Unit, further produce substantial amounts of clean propane, butane, and naphtha streams, as well as other streams (Figures 5 and 6).

[0082] Example 3: Processing of Plastic and Petroleum Oil Blend in Crude Unit Followed by Conversion Units for Production of Fuels and Base Oil with Recycle Contents and Low CO₂ Footprint

[0083] From the crude unit, the heavy fraction is sent to conversion units such as a FCC unit or Hydrocracking unit where the heavy hydrocarbon molecules are cracked and converted to gasoline, jet fuel, diesel, and heavy fractions. These blending components can be each sent to the corresponding blending pool to be blended to a finished gasoline, jet fuel, diesel or marine oil with recycle contents and a lower CO₂ footprint (Figure 5). Portions of the heavy fraction can be further processed in an isomerization/ dewaxing unit to prepare base oil or white oil with a recycle content and a lower CO₂ footprint (Figure 6).

[0084] Example 4: Feeding of Recycle C₃-C₄ and/or Naphtha to Steam Cracker for Ethylene Production, Followed by Productions of Polyethylene Resin and Polyethylene Consumer Products

[0085] The propane, butane and naphtha streams, produced via cofeeding of a plastic/oil blend to a crude unit per Example 2, are good feedstocks to cofeed to a steam cracker for production of ethylene with a recycle content. At least a portion of the streams, if not all, are fed to the steam cracker. The ethylene can be processed in a polymerization unit to produce polyethylene

resin containing some recycled-polyethylene/ polypropylene derived materials while the quality of the newly produced polyethylene is indistinguishable to virgin polyethylene made entirely from virgin petroleum resources. The polyethylene resin with the recycled material can then be further processed to produce various polyethylene products to fit the needs of consumer products. These polyethylene consumer products would now contain chemically recycled, circular polymer while quality of the polyethylene consumer products are indistinguishable from those made entirely from virgin polyethylene polymer. These chemically recycled polymer products are different from mechanically recycled polymer products whose qualities are inferior to the polymer products made from virgin polymers.

[0086] Example 5: Hydrocracking of VGO derived from plastic and petroleum oil blend

[0087] Hydrocracking a heavy fraction containing plastic and VGO produces C3-C4 streams and naphtha that can be fed to the steam cracker for ethylene generation (Figure 6). Gasoline, jet fuel and diesel boiling range materials are each sent to the corresponding blending pool to be blended to a finished gasoline, jet fuel and diesel. The bottoms product in the boiling range of 650-1000F is a waxy oil.

[0088] Example 6: Dewaxing of hydrocracker bottoms derived from plastic and petroleum oil blend

[0089] The bottoms fraction from Example 5 can be dewaxed for base oil production (Figure 6). The heavy fraction from the hydrocracking unit can be passed to an isomerization/dewaxing unit. Dewaxed oil, or base oil, is recovered from the unit. Then, the base oil can be further passed to a hydrofinishing unit to prepare premium base oil or white oil.

[0090] As used in this disclosure the word “comprises” or “comprising” is intended as an open-ended transition meaning the inclusion of the named elements, but not necessarily excluding other unnamed elements. The phrase “consists essentially of” or “consisting essentially of” is intended to mean the exclusion of other elements of any essential significance to the composition. The phrase “consisting of” or “consists of” is intended as a transition meaning the exclusion of all but the recited elements with the exception of only minor traces of impurities.

[0091] All patents and publications referenced herein are hereby incorporated by reference to the extent not inconsistent herewith. It will be understood that certain of the above-described structures, functions, and operations of the above-described embodiments are not necessary to practice the present invention and are included in the description simply for completeness of an exemplary embodiment or embodiments. In addition, it will be understood that specific structures, functions, and operations set forth in the above-described referenced patents and

publications can be practiced in conjunction with the present invention, but they are not essential to its practice. It is therefore to be understood that the invention may be practiced otherwise than as specifically described without actually departing from the spirit and scope of the present invention as defined by the appended claims.

What is claimed is:

1. A continuous process for converting waste plastic into recycle for polyethylene polymerization comprising:
 - (a) selecting waste plastics comprising polyethylene and/or polypropylene;
 - (b) preparing a blend of petroleum and the selected waste plastic with the blend comprising about 20 wt. % or less of the selected waste plastic;
 - (c) passing the blend at a temperature above the melting point of the waste plastic in the blend to a refinery crude unit;
 - (d) recovering a liquid petroleum gas C₃-C₄ mixture from the crude unit; and
 - (e) passing the C₃-C₄ mixture to a steam cracker to make ethylene.
2. The process of claim 1, wherein a gasoline and heavy fraction is recovered from the refinery crude unit.
3. The process of claim 1, wherein the blend of (b) is a hot homogeneous blend of waste plastic and petroleum oil.
4. The process of claim 1, wherein the blend of (b) is a stable blend of waste plastic and petroleum oil.
5. The process of claim 1, wherein the waste plastics selected in (a) comprise plastics from classification group 2, 4, and/or 5.
6. The process of claim 1, wherein a naphtha stream and a heavy fraction are recovered from the crude unit and further processed in the refinery to clean gasoline, diesel, or jet fuel.
7. The process of claim 1, wherein the volume flow of the blend to the refinery crude unit in (c) comprises up to 50 vol. % of the total hydrocarbon flow to the crude unit.
8. The process of claim 7, wherein the blend flow comprises up to 25 vol. % of the total flow to the crude unit.
9. The process of claim 1, wherein the blend of petroleum and selected waste plastic in (b) is prepared by heating the waste plastic above the melting point of the plastic and mixing with the petroleum, and then cooling the blend to a temperature below the melting point of the waste plastic.
10. The process of claim 1, wherein the petroleum in the blend comprises atmospheric gas oil, vacuum gas oil (VGO), atmospheric residue, a petroleum derived oil, a petroleum based material, and/or heavy stock recovered from refinery operations.

11. The process of claim 1, wherein the petroleum in the blend comprises light cycle oil (LCO), heavy cycle oil (HCO), FCC naphtha, gasoline, diesel, toluene, and/or aromatic solvent derived from petroleum.
12. A continuous process for converting waste plastic into recycle for polyethylene polymerization comprising:
- (a) selecting waste plastics containing polyethylene and/or polypropylene;
 - (b) preparing a blend of petroleum and the selected plastic, with the blend comprising about 20 wt. % or less of the selected plastic;
 - (c) passing the blend to a refinery crude unit;
 - (d) recovering a liquid petroleum gas C₃-C₄ olefin/paraffin mixture from the crude unit;
 - (e) passing the C₃-C₄ mixture to a steam cracker to make ethylene;
 - (f) recovering a naphtha stream from the crude unit; and
 - (g) passing the naphtha stream recovered from the crude unit to the steam cracker to make ethylene.
13. The process of claim 12, wherein a gasoline and heavy fraction is recovered from the refinery crude unit.
14. The process of claim 12, wherein the blend of (b) is a hot homogeneous blend of waste plastic and petroleum oil.
15. The process of claim 12, wherein the blend of (b) is a stable blend of waste plastic and petroleum oil.
16. The process of claim 12, wherein the waste plastics selected in (a) comprise plastics from classification group 2, 4, and/or 5.
17. The process of claim 12, wherein a naphtha and a heavy fraction are recovered from the refinery crude unit and further processed in the refinery to clean gasoline, diesel, or jet fuel.
18. The process of claim 12, wherein the volume flow of the blend to the refinery crude unit in (c) comprises up to 50 vol. % of the total hydrocarbon flow to the crude unit.
19. The process of claim 18, wherein the blend flow comprises up to 25 vol. % of the total flow to the crude unit.
20. The process of claim 12, wherein the blend of petroleum and selected waste plastic in (b) is prepared by heating the waste plastic above the melting point of the plastic and mixing with the petroleum, and then cooling the blend to a temperature below the melting point of the waste plastic.

21. The process of claim 12, wherein the petroleum in the blend comprises atmospheric gas oil, vacuum gas oil (VGO), atmospheric residue, a petroleum derived oil, a petroleum based material, and/or heavy stock recovered from refinery operations.

22. The process of claim 12, wherein the petroleum in the blend comprises light cycle oil (LCO), heavy cycle oil (HCO), FCC naphtha, gasoline, diesel, toluene, and/or aromatic solvent derived from petroleum.

23. A process for converting waste plastic into chemicals useful in preparing polyethylene, comprising:

(a) selecting waste plastics containing polyethylene and/or polypropylene;

(b) preparing a blend of petroleum and the selected plastic, with the blend comprising about 20 wt. % or less of the selected plastic; and

(c) passing the blend to a refinery crude unit.

24. A continuous process for converting waste plastic into recycle for polyethylene polymerization comprising:

(a) selecting waste plastics comprising polyethylene and/or polypropylene;

(b) preparing a blend of petroleum and the selected waste plastic with the blend comprising about 20 wt. % or less of the selected waste plastic;

(c) passing the blend at a temperature above the melting point of the plastic in the blend to a refinery crude unit;

(d) recovering a heavy fraction from the crude unit and passing the heavy fraction to a refinery hydrocracking unit;

(e) recovering a heavy fraction from the hydrocracking unit and passing the heavy fraction to an isomerization dewaxing unit; and

(f) recovering base oil from the isomerization dewaxing unit.

25. The process of claim 24, wherein the base oil recovered in (f) is passed to a hydrofinishing unit, from which is recovered a hydrofinished base oil.

26. A continuous process for converting waste plastic into recycle for preparation of lower carbon footprint fuels and base oil comprising:

(a) selecting waste plastics comprising polyethylene and/or polypropylene;

(b) preparing a blend of petroleum and the selected waste plastic with the blend comprising about 20 wt. % or less of the selected waste plastic;

(c) passing the blend at a temperature above the melting point of the plastic in the blend to a refinery crude unit;

- (d) recovering a heavy fraction from the crude unit and passing the heavy fraction to hydrocracking unit;
 - (e) recovering a heavy fraction from the hydrocracking unit and passing the heavy fraction to a refinery isomerization/dewaxing unit; and
 - (f) recovering base oil from the isomerization dewaxing unit.
27. The process of claim 26, wherein the lower carbon footprint fuels includes gasoline, jet fuel, diesel, and/or marine oil.