Description

The present invention relates to the preparation of titania extrudates, to the preparation of a shapable dough for titania extrudates, to a shapable dough for titania extrudates and to the preparation of calcined titania extrudates and to their use.

Titania is a well-known material, which is often used as catalyst carrier or catalyst in various processes. It should be noted that the titania-containing catalyst systems described in the art are invariably based on titania powder, which does not make such systems directly suitable for industrial applications. In order to bring titania into an industrially more appropriate form it has been recently described in DE-C-3217751 to produce titania pellets by pelletising pyrogenically manufactured titania using a certain class of pelletising agents such as polyvalent alkanols and, in particular, graphite in powder form.

In EP-A-38 741 a process for the preparation of a porous shaped titania carrier has been described. The process comprises mixing powdered titania, water and a shaping additive within certain ranges. The examples disclose that titania extrudates having an average pore diameter of about 30 nm invariably have a low surface area. Fr-A-2 231 423 relates to a method for producing a hard attrition-resistant catalyst carrier, also having good fluidizing properties. The method comprises mixing a titanium chelate with titanium oxide and a gelling agent, allowing the mixture to gel, drying and calcining. The gelling agent may be water, aqueous ammonia or solutions of other suitable bases. The titanium chelate is preferably diethanolamine titanate. De-A-2 426 496 relates to a method for producing a hard attrition-resistant catalyst carrier, also having good fluidizing properties. The method comprises dispersing a titania powder in water, removing any excess water, drying and calcining. In order to facilitate the dispersion of the titania in water, surface-active agents or water-soluble organic compounds or highly polar inorganic compounds may be added.

Thusfar, it has not been possible to extrude titania like other carriers such as alumina in conventional extrusion equipment to give reasonably strong products. Since titania is an interesting carrier material, especially in the absence of binder material, it was considered important to investigate whether this notoriously difficult to shape material could be subjected to an extrusion process to obtain titania extrudates of sufficient strength to be of industrial importance.

It has now been found that titania extrudates can be suitably prepared when use is made of an alkanolamine or ammonia or an ammonia-releasing compound in the preparation of a dough from which titania extrudates can be obtained.

The present invention therefore relates to a process for the preparation of a shapable dough which comprises mixing and kneading a particulate titania with water and with an alkanolamine or ammonia or an ammonia-releasing compound to obtain a mixture having a total solids content of from 50 to 85% by weight, the alkanolamine or ammonia being present in an amount of from 0.5 to 20% by weight on the total solids content of the mixture.

The invention further relates to a process for the preparation of titania extrudates which comprises mixing and kneading a particulate titania with water and with an alkanolamine or ammonia or an ammonia-releasing compound to obtain a mixture having a total solids content of from 50 to 85% by weight, the alkanolamine or ammonia being present in an amount of from 0.5 to 20% by weight on the total solids content of the mixture and extruding the mixture.

The invention further relates to a process for manufacturing calcined titania extrudates which comprises extruding a shapable dough into titania extrudates and drying and calcining the titania extrudates to a final temperature of between 300 °C and 1000 °C, and to calcined titania extrudates obtained by said process.

The titania to be used in the process according to the present invention can be both of rutile and of anatase nature. Also mixtures of both forms of titania can be suitably applied. In the event that it is necessary or advisable to use titania containing both rutile and anatase it will be clear that the preferred rutile:anatase ratio to be applied will be depending to some extent on the particular application concerned. Generally, ratios ranging between 0.66:1 and 100:1 can be suitably applied. When aiming at synthesis gas conversion reactions preference is given to the use of rutile:anatase ratios of at least 2:1. Examples of a suitable titania source comprise commercially available P25 (Degussa), a low surface area titania (a mixture of anatase and rutile) and a high surface area material consisting of anatase. Also various forms of pyrogenically produced titania can be used in the preparation of the shapable doughs and the corresponding extrudates in accordance with the present invention.

The total solids content of the mixture of titania, alkanolamine or ammonia or ammonium-releasing component (expressed as ammonia) and water ranges from 50 to 85% by weight, preferably from 55 to 80% by weight and more preferably from 60 to 75% by weight, in order to obtain an extrudable mixture.

The amount of alkanolamine or ammonia or ammonia-releasing component (expressed as ammonia) ranges from 0.5 to 20% by weight, preferably from 2 to 15% by weight, more preferably from 3 to 10% by weight,

calculated on the total solids content.

Suitably, ammonia-releasing compounds other than NH_4OH or alkanolamines can be used in the formation of the shapable doughs and the extrudates produced therefrom. Ammonia-releasing compounds are defined for the purpose of the present invention as compounds capable of releasing NH_3 gas on decomposition, e.g. under the influence of heat.

Suitable alkanolamines to be used in the process according to the present invention comprise the mono-, di- and tri- alkanolamines containing 2 to 10 carbon atoms. Preferred are monoalkanolamines, e.g. ethanolamine, propanolamine, hexanolamine, nonanolamine and decanolamine. Other examples of suitable alkanolamines comprise diethanolamine and triethanolamine. Preference is given to the use of monoethanolamine. If desired, mixtures of alkanolamines or mixtures comprising ammonia and one or more alkanolamines can be suitably applied.

To improve the flux properties in the extruder the dough to be extruded may also comprise a polyelectrolyte, such as Nalco 7879 (obtainable from Nalco). The dough to which a polyelectrolyte may be added can readily be extruded e.g. over the metal die-plate of a Bonnot-extruder. Cylindrical extrudates can be prepared, but other forms may be prepared as well, such as mentioned, for instance, in US patent specification 4,028,227. The surface area of the titania extrudates ranges suitably between 40 and 300 m^2/g depending on the starting titania used in preparing the shapable dough.

It has been found that the surface areas of the titania extrudates produced are dependent to some extent of the surface area of the starting powder material. When using powders with relatively low surface areas, the extrudates produced have typically similar surface areas, whereas the use of powders having relatively large surface areas may well lead to extrudates having considerable lower surface areas, e.g. some 30 to 50% lower, but still sufficiently larger than obtained when starting from a low surface area powder.

It is possible, though not necessarily advantageous, to add other oxides such as silicium dioxide and/or zirconium dioxide to the composition to be extruded. Amounts of up to 50%, but preferably of not more than 20% by weight of other oxides may be present in the composition to be extruded. It has been found that the presence of rather large amounts of other oxides may have a detrimental effect on the strength of the extrudates produced.

It is also possible to incorporate other materials such as crystalline (metallo)silicates, in particular zeolites, such as zeolite Y, into the dough to be extruded so as to arrive at zeolite-containing titania extrudates which have considerable strength.

After extrusion, the titania-containing extrudates are subjected to drying and normally also to calcining. Drying is suitably carried out by subjecting the extrudates to a mild heat treatment, e.g. at a temperature of up to 150 °C to remove water still present in the extrudates. Good results have been obtained using a drying temperature of about 120 °C.

The calcination of the extrudates is normally carried out at a temperature in the range between 300 °C and 1000 °C. Preferably, the calcination is carried out at a temperature in the range of from 450 °C to 750 °C, most preferably in the range of from 475 °C to 725 °C.

The titania extrudates can be suitably used, for example, as carriers for catalysts which are normally used in hydroconversion processes, like the hydrodemetallization and hydrodesulphurization of heavy hydrocarbon oils, in the hydrogenation of hydrogenatable components or hydrocarbon fractions such as kerosene and various types of cycle oils, in hydrocarbon synthesis reactions, in the epoxidation of olefinically unsaturated compounds with organic hydroperoxides, in the hydration of olefinically unsaturated compounds to produce the corresponding alkanols and in the purification of exhaust gases, in particular in the denoxing of nitrogen containing oxygenates.

Examples of hydrocarbon synthesis reactions comprise Fischer-Tropsch type reactions aimed at producing (long chain) hydrocarbons from carbon monoxide and hydrogen. In particular, the titania extrudates loaded with suitable Fischer-Tropsch metal(s), e.g. Group VIII metals as iron, nickel or cobalt, optionally containing one or more promotors such as zirconia or rhenium, can be suitably applied in the heavy paraffin synthesis step which is one of the process steps in an integrated process for the manufacture of middle distillates starting from methane to produce a syngas mixture which serves as starting material for the heavy paraffin synthesis and wherein the heavy paraffins produced are subjected to a catalytic heavy paraffin conversion process to produce the desired middle distillates.

The invention will now be illustrated by means of the following Examples.

EXAMPLE I

A mixture was prepared having the following composition

titania (ex Degussa)	74.5 g
water (demineralized)	32.5 g
monoethanolamine (MEA)	2.6 g
total	109.6 g

The mixture was prepared by adding the MEA and water to the titania and the mixture was kneaded for 30 minutes. The resulting mix was extruded on a laboratory extruder. The obtained extrudates (1.5 mm) were dried at 120 °C for 2 hours and calcined for 2 hours at 500 °C.

The titania obtained had the following properties:
BET surface area 52 m^2/g
medium pore diameter 32 nm
pore volume 0.29 ml/g

EXAMPLE II

The experiment as described in Example I was repeated using a mixture containing 200 g of titania powder, 80 g of water and 8 g MEA. The mixture was kneaded for 45 minutes and then subjected to extrusion, drying and calcining as described in Example I. The titania obtained had the following properties:
BET surface area 51 m^2/g
medium pore diameter 39 nm
pore volume 0.36 ml/g
bulk crushing strength 0.59 MPa

EXAMPLE III

The experiment as described in Example I was repeated using 150 g titania powder, 30 g water and 30 g ammonia (25%). The mixture was kneaded for 20 minutes. Subsequently, two batches of 10 g water were added and the mixing was continued for another 25 minutes. The mixture was extruded, dried and calcined as described in Example I. The titania obtained had the following properties:
BET surface area 47 m^2/g
medium pore diameter 27 nm
pore volume 0.30 ml/g
bulk crushing strength 0.62 MPa

EXAMPLE IV

A mixture was prepared having the following composition

titania (ex TIL)	228 g
water	110 g
MEA	5 g
total	343 g

The mixture was kneaded for 45 minutes. The mixture was then extruded, dried and calcined as described in Example I. The titania obtained had the following properties:
BET surface area 82 m^2/g
medium pore diameter 37 nm
pore volume 0.36 ml/g
bulk crushing strength 0.25 MPa

EXAMPLE V

A mixture was prepared from 114 g titania (ex TIL) and 107 g silica (ex Crossfield). To this mixture were added 5 g MEA and 150 g water. During the next 45 minutes, another 60 g of water was added in small portions.

The resulting mix was extruded, dried and calcined at 700 °C for 2 hours. The titania-silica obtained had the following properties:
BET surface 192 m^2/g
medium pore diameter 22 nm
pore volume 0.76 ml/g
bulk crushing strength 0.33 MPa

EXAMPLE VI

A mixture was prepared from 150 g titania (ex Degussa), 7.5 g of MEA and 50 g of water. To this mixture was added 111 g of a zeolite Y having a silica/alumina molar ratio of 40, and 50 g of water. After 15 minutes another 15 g of water was added. The resultant mixture was smoothly extruded. It was then dried at 120 °C and calcined at 500 °C for 2 hours. The titania-zeolite Y obtained had the following properties:
BET surface area 246 m^2/g
medium pore diameter 32 nm
pore volume 0.33 ml/g
bulk crushing strength 0.90 MPa

EXAMPLE VII

1.6 mm Extrudates prepared in accordance with the experiment described in Example VI were impregnated with a solution of H_2PtCl_6 made up to allow after reduction with hydrogen at 400 °C a Pt-content of 0.8% by weight on titania.

The catalyst thus prepared was used in a hydrogenation experiment. The hydrogenation experiment was carried out using a hydrotreated light cycle oil containing 273 mmol monoaromatics/100 grammes. Its 90% by weight boiling point amounted to 351 °C and it contained 112 ppmw (parts per million by weight) of sulphur and 7.6 ppmw of nitrogen. The experiment was carried out at a pressure of 50 bar and at a temperature of up to 340 °C. It was found that the monoaromatics content had been reduced to about 70 mmol/100 grammes.

Claims

1. A process for the preparation of a shapable dough which comprises mixing and kneading a particulate titania with water and an alkanolamine or ammonia or an ammonia-releasing compound to obtain a mixture having a total solids content of from 50 to 85% by weight, the alkanolamine or ammonia being present in an amount of from 0.5 to 20% by weight on the total solids content of the mixture.

2. A process according to claim 1 wherein the total solids content is from 55 to 80% by weight, preferably 60 to 75% by weight.

3. A process according to claim 1 or 2 wherein use is made of anatase and/or rutile as titania source.

4. A process according to one or more of claims 1-3 wherein use is made of an alkanolamine or ammonia in an amount between 2 and 15% by weight, preferably between 3 and 10% by weight.

5. A process according to one or more of claims 1-4 wherein use is made of a mono-, di- or trialkanolamine having 2 to 10 carbon atoms.

6. A process according to claim 5 wherein use is made of monoethanolamine.

7. A process according to one or more of claims 1-6 wherein at most 50% by weight of silica and/or zirconium dioxide and/or a zeolite, preferably a zeolite Y, is admixed.

8. A process for the preparation of titania extrudates from a shapable dough according to claim 1, which comprises mixing and kneading a particulate titania with water and an alkanolamine or ammonia or an ammonia-releasing compound to obtain a mixture having a total solids content of from 50 to 85% by weight, the alkanolamine or ammonia being present in an amount of from 0.5 to 20% by weight on the total solids content of the mixture and extruding the mixture.

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Claims

1. A process for the preparation of a shapable dough which comprises mixing and kneading a particulate titania with water and an alkanolamine or ammonia or an ammonia-releasing compound to obtain a mixture having a total solids content of from 50 to 85% by weight, the alkanolamine or ammonia beirg present in an amount of from 0.5 to 20% by weight on the total solids content of the mixture.

2. A process according to claim 1 wherein the total solids content is from 55 to 80% by weight, preferably 60 to 75% by weight.

3. A process according to claim 1 or 2 wherein use is made of anatase and/or rutile as titania source.

4. A process according to one or more of claims 1-3 wherein use is made of an alkanolamine or ammonia in an amount between 2 and 15% by weight, preferably between 3 and 10% by weight.

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7. A process according to one or more of claims 1-6 wherein at most 50% by weight of silica and/or zirconium dioxide and/or a zeolite, preferably a zeolite Y, is admixed.

8. A process for the preparation of titania extrudates from a shapable dough according to claim 1, which comprises mixing and kneading a particulate titania with water and an alkanolamine or ammonia or an ammonia-releasing compound to obtain a mixture having a total solids content of from 50 to 85% by weight, the alkanolamine or ammonia being present in an amount of from 0.5 to 20% by weight on the total solids content of the mixture and extruding the mixture.

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9. A process according to claim 8 which comprises mixing and kneading a particulate titania with water and an alkanolamine having 2 to 10 carbon atoms or ammonia to obtain a mixture having a total solids content of from 60 to 75% by weight, the alkanolamine or ammonium being present in an amount of from 3 to 10% by weight on the total solids content of the mixture and extruding the mixture.

10. A process for manufacturing calcined titania extrudates which comprises drying and calcining the titania extrudates according to claim 8 or 9 to a final temperature of between 300 °C and 1000 °C.

11. A process according to claim 10 wherein the calcination is carried out at a temperature in the range between 450 °C and 750 °C, preferably in the range between 475 °C and 725 °C.

12. Use of titania extrudates prepared by a process according to any one of claim 10 or 11 as catalyst carriers in hydrocarbon conversion processes, in hydrogenation processes, in hydrocarbon synthesis reactions or in the purification of exhaust gases.

Patentansprüche

1. Verfahren zur Herstellung eines formbaren Teiges, welches Verfahren ein Mischen und Kneten eines teilchenförmigen Titandioxids mit Wasser und einem Alkanolamin oder Ammoniak oder einer Ammoniak-freisetzenden Verbindung zur Ausbildung eines Gemisches mit einem Gesamtfeststoffgehalt von 50 bis 85 Gew.-% umfaßt, wobei das Alkanolamin oder das Ammoniak in einer Menge von 0,5 bis 20 Gew.-%, bezogen auf den Gesamtfeststoffgehalt des Gemisches, vorliegt.

2. Verfahren nach Anspruch 1, worin der Gesamtfeststoffgehalt von 55 bis 80 Gew.-%, vorzugsweise von 60 bis 75 Gew.-% beträgt.

3. Verfahren nach Anspruch 1 oder 2, worin als Titandioxidquelle Anatas und/oder Rutil eingesetzt wird.

4. Verfahren nach einem oder mehreren der Ansprüche 1 bis 3, worin ein Alkanolamin oder Ammoniak in einer Menge von 2 bis 15 Gew.-%, vorzugsweise von 3 bis 10 Gew.-% eingesetzt wird.

5. Verfahren nach einem oder mehreren der Ansprüche 1 bis 4, worin ein Mono-, Di- oder Trialkanolamin mit 2 bis 10 Kohlenstoffatomen eingesetzt wird.

6. Verfahren nach Anspruch 5, worin Monoethanolamin eingesetzt wird.

7. Verfahren nach einem oder mehreren der Ansprüche 1 bis 6, worin bis zu höchstens 50 Gew.-% an Siliciumdioxid und/oder Zirkoniumdioxid und/oder an einem Zeolith, vorzugsweise Zeolith Y, zugemischt werden.

8. Verfahren zur Herstellung von Titandioxid-Extrudaten aus einem formbaren Teig nach Anspruch 1, welches ein Mischen und Kneten eines teilchenförmigen Titandioxids mit Wasser und einem Alkanolamin oder Ammoniak oder einer Ammoniak-freisetzenden Verbindung zur Ausbildung eines Gemisches mit einem Gesamtfeststoffgehalt von 50 bis 85 Gew.-%, wobei das Alkanolamin oder das Ammoniak in einer Menge von 0,5 bis 20 Gew.-%, bezogen auf den Gesamtfeststoffgehalt des Gemisches, vorliegt, und ein Extrudieren des Gemisches umfaßt.

9. Verfahren nach Anspruch 8, welches ein Mischen und Kneten eines teilchenförmigen Titandioxids mit Wasser und einem Alkanolamin mit 2 bis 10 Kohlenstoffatomen oder mit Ammoniak zur Ausbildung eines Gemisches mit einem Gesamtfeststoffgehalt von 60 bis 75 Gew.-%, wobei Alkanolamin oder Ammonium in einer Menge von 3 bis 10 Gew.-%, bezogen auf den Gesamtfeststoffgehalt des Gemisches, zugegen ist, und ein Extrudieren des Gemisches umfaßt.

10. Verfahren zur Herstellung calcinierter Titandioxid-Extrudate, welches ein Trocknen und Calcinieren der Titandioxid-Extrudate nach Anspruch 8 oder 9 auf eine Endtemperatur von 300°C bis 1000°C umfaßt.

11. Verfahren nach Anspruch 10, worin das Calcinieren bei einer Temperatur im Bereich von 450°C bis 750°C, vorzugsweise im Bereich von 475°C bis 725°C ausgeführt wird.

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12. Verwendung von nach einem Verfahren gemäß einem der Ansprüche 10 oder 11 hergestellten Titandioxid-Extrudaten als Katalysatorträger in Kohlenwasserstoffumwandlungsprozessen, in Hydrierverfahren, in Kohlenwasserstoffsynthesereaktionen oder in der Reinigung von Abgasen.

Revendications

1. Procédé de préparation d'une pâte moulable qui comprend de mélanger et de malaxer de l'oxyde de titane sous forme particulaire avec de l'eau et avec une alcanolamine ou de l'ammoniaque ou un composé dégageant de l'ammoniac pour obtenir un mélange qui a une teneur totale en solides comprise entre 50 et 85 % en poids, l'alcanolamine ou l'ammoniac étant présent à une concentration comprise entre 0,5 et 20 % en poids de la teneur totale en solides du mélange.

2. Procédé selon la revendication 1 dans lequel la teneur totale en solide est comprise entre 55 et 80 % en poids, de préférence 60 à 75 % en poids.

3. Procédé selon la revendication 1 ou 2 dans lequel on utilise de l'anatase et/ou du rutile comme source d'oxyde de titane.

4. Procédé selon l'une ou plusieurs des revendications 1-3 dans lequel on utilise de l'alcanolamine ou de l'ammoniaque à raison de 2 à 15 % en poids, de préférence entre 3 et 10 % en poids.

5. Procédé selon l'une ou plusieurs des revendications 1-4 dans lequel on utilise une mono-, di- ou trialcanolamine ayant entre 2 et 10 atomes de carbone.

6. Procédé selon la revendication 5 dans lequel on utilise de la monoéthanolamine.

7. Procédé selon l'une ou plusieurs des revendications 1-6 dans lequel on mélange au plus 50 % en poids de silice et/ou de dioxyde de zirconium et/ou d'une zéolithe, de préférence une zéolithe Y.

8. Procédé de préparation d'extrudats d'oxyde de titane à partir d'une pâte moulable selon la revendication 1, qui comprend de mélanger et de malaxer de l'oxyde de titane sous forme particulaire avec de l'eau et avec une alcanolamine ou de l'ammoniaque ou un composé dégageant de l'ammoniac pour obtenir un mélange qui a une teneur totale en solides comprise entre 50 et 85 % en poids, l'alcanolamine ou l'ammoniac étant présent à une concentration comprise entre 0,5 et 20 % en poids de la teneur totale en solides du mélange.

9. Procédé selon la revendication 8 qui comprend de mélanger et de malaxer de l'oxyde de titane sous forme particulaire avec de l'eau et avec une alcanolamine ayant entre 2 et 10 atomes de carbone ou de l'ammoniaque pour obtenir un mélange qui a une teneur totale en solides comprise entre 60 et 75 % en poids, l'alcanolamine ou l'ammoniac étant présent à une concentration comprise entre 3 et 10 % en poids de la teneur totale en solides du mélange et on extrude le mélange.

10. Procédé de fabrication d'extrudats d'oxyde de titane calciné qui comprend de sécher et de calciner des extrudats d'oxyde de titane selon la revendication 8 ou 9 jusqu'à une température finale comprise entre 300°C et 1000°C.

11. Procédé selon la revendication 10 dans lequel on réalise la calcination à une température comprise dans l'intervalle de 450°C à 750°C, de préférence dans l'intervalle compris entre 475°C et 725°C.

12. Utilisation d'extrudats d'oxyde de titane préparés par un procédé selon l'une quelconque des revendications 10 ou 11 comme supports de catalyseur dans les procédés de conversion d'hydrocarbures, dans les procédés d'hydrogénation, dans les réactions de synthèse d'hydrocarbures ou en purification de gaz d'échappement.