Claims

1. A method for producing liquid fuel components from renewable oil **characterized** in that a fresh feedstock comprising saturated fatty acids is subjected to dilution by an organic lipophilic solvent containing less than 5 ppm phosphorus impurities and less than 10 ppm metal impurities before and/or during purification by at least one pretreatment process for removal of phosphorus and metal impurities, and subsequently feeding the resulting purified feedstock into at least one post-treatment process suitable for producing liquid fuel components.

2. The method according to claim 1 **characterized** in that said pretreatment process comprises degumming.

3. The method according to claim 2 **characterized** in that the degumming step is performed to said fresh feedstock prior to said dilution and subsequently the degummed and diluted fresh feed is centrifuged to remove the formed gums.

4. The method according to any one of the claims 1-3 **characterized** in that said post-treatment process comprises a hydrotreating step and an isomerisation step.

5. The method according to claim 4 **characterized** in that said post treatment process comprises first a hydrotreating step including hydrogenation and deoxygenation, and subsequently an isomerisation step.

6. The method according to any one of the claims 1-5 **characterized** in that said renewable oil is selected from the group of animal, plant, microscopic plant and microbe oils and fats.

7. The method according to any one of the claims 1-6 **characterized** in that said fresh feedstock comprising saturated fatty acids has an iodine value of less than 100, preferably less than 75, more preferably less than 60.

8. The method according to any one of the claims 1-7 **characterized** in that said organic lipophilic solvent comprises an additional fresh feed, a recycle stream from said pretreatment process or a recycle stream from said post-treatment process, preferably a recycle stream from said post-treatment.

9. The method according to any one of the claims 1-8 **characterized** in that the volume ratio of said organic lipophilic solvent to said fresh feedstock is within the range from 0.05-5:1, preferably 0.1-2:1 more preferably 0.2-1:1.

10. The method according to any one of the claims 1-9 **characterized** in that said organic lipophilic solvent is removed before said post-treatment process.

11. The method according to claim 10 **characterized** in that a vapour phase formed is removed in said hydrotreating process before entering the feed into said isomerisation step.

What is claimed is:

1. An invention not claimed in any divisional application.