

PROCESS AND SYSTEM FOR PRODUCING SYNTHESIS GAS FROM BIOMASS BY CARBONIZATION

FIELD OF THE INVENTION

[0001] The invention relates to the production of synthetic gas, and more particularly to a method and a system for producing synthetic gas from biomass by carbonization. The method belongs to the technical field of producing synthetic gas or combustible gas by using biomass. The synthetic gas is a mixture gas which contains CO, H₂, and a variety of carbohydrates that contain carbon, hydrogen, and oxygen. The synthetic gas produced by the method according to the invention can be used for gas turbine power generation systems, fuel cells, synthetic oil, metallurgical and other systems.

BACKGROUND OF THE INVENTION

[0002] As dwindling of traditional fossil fuels (coal, oil, and natural gas) reserves and the environmental pollution problems caused by the use of fossil fuels directly threaten human survival and development, attaching importance to development of renewable and environmental friendly energy has become a consensus of governments of all countries. Biomass, an organic matter generated by plants through photosynthesis, has wide sources and large available quantity. It can be transformed into clean gas or liquid fuel for power generation and producing industrial raw materials and chemical products. As energy it is clean and renewable with zero emission of carbon dioxide and with the potential to fully replace fossil fuels as a new energy resource which has become a priority for all countries.

[0003] There are many methods for transforming biomass into clean gas or liquid fuel, among which biomass gasification technology can adapt to a variety of species and has good expansibility. The gasification of biomass is a thermochemical process, i.e., biomass reacts with a gasification agent (such as air, oxygen, vapor, carbon dioxide, etc.) under high temperature to produce a mixed gas consisting of carbohydrate containing carbon, hydrogen, and oxygen. The mixed gas is named synthetic gas. The components of the synthetic gas are decided by the species of used biomass, the type of the gasification agent, the reaction conditions, and the structure of a gasifier used therein. The objectives of gasification is, on the one hand, to minimize the consumption of materials and the gasification agent, as well as the tar content in the synthesis gas, and on the other hand, to maximize the gasification efficiency and the efficiency of carbon conversion, as well as the active ingredient (CO and H_2) content in the synthesis gas. The objectives are decided by the type of the used gasifier, the type of the gasification agent, the particle size of the biomass, the gasification pressure and temperature, and moisture and ash of the biomass, etc.

[0004] The gasification furnace used in the gasification process can be divided into three classes: fixed bed, fluidized bed, and entrained flow bed. The fixed bed has a simple gasification structure, convenience operation, flexible operation mode, a higher rate of carbon conversion, a wide range of running load which can be between 20% and 110%, and the solid fuel stays in the bed for a long period of time. However, the temperature is nonuniform and it has less efficiency of heat exchange, low heating value of the synthesis gas at the outlet, and the synthesis gas contains a large amount of tar. The fluidized bed is convenient for material addition and ash release, and the temperature is uniform and easy for adjustment. However, it is sensitive to the characteristics of raw materials. If the adhesion, thermal stability, moisture content, or ash melting point of raw materials changes, the operation will become abnormal. Furthermore, in order to ensure normal

fluidization of the gasification furnace, it needs to keep lower temperature, and the synthetic gas has a large amount of tar. Since a large amount of tar is produced in the fixed bed and the fluidized bed, a tar cracking unit and purification equipment must be installed, which results in a complicated process. The entrained flow bed has a high and uniform operating temperature, good amplification characteristics, and particularly suitable for large-scale industrialization. Tar is cracked completely. However, the entrained flow bed has a strict requirement on particle size of raw materials. Based on current grinding technology, there is no way to grind biomass having much cellulose to a size suitable for the entrained flow bed. So the entrained flow bed cannot be used for gasification of biomass. Nowadays, tar cracking and pretreatment of biomass prior to gasification are tough problems for the development of biomass gasification.

[0005] Chinese Patent Application No. 200510043836.0 discloses a method and a device for gasifying low tar biomass. The method includes pyrolysis and gasification independently, and biomass is transformed into synthetic gas containing low content of tar. In the method, pyrolysis gas and charcoal experience incomplete combustion in the gasifier, and tar is cracked under high temperature. Although the tar content is decreased greatly, a lot of charcoal is consumed, resulting in a low content of CO produced in the subsequent reduction reaction and a high content of CO₂ in the synthetic gas. Secondly, due to a low temperature in the combustion reaction, the temperature at the subsequent reduction becomes lower, and the average temperature in the reduction zone is less than 700°C, and thereby the yield of effective synthetic gas (CO and H₂) is decreased significantly (about 30%). Thirdly, the ash and unreacted carbon residue from the reduction reaction is directly discharged, resulting in a low carbon conversion rate. Finally, the gasifier used in the method is in the form of a fixed bed, since the reduction reaction absorbs heat, the temperature difference between the top and the bottom (the top is about 1000°C and the bottom is about 500°C) of the bed is huge, which is an inherent

disadvantage of fixed bed.

[0006] U. S. Pat. No. 6,863,878B2 discloses a method and a device of producing synthetic gas with carbon-containing materials. The method includes carbonization (or pyrolysis) and gasification independently. In the method, the carbonization temperature is controlled less than 450°F so as to reduce the tar content resulted from pyrolysis.

However, during carbonization stage, solid products are not ground prior to transporting to the reaction coils of the gasifier, which will affect the speed and degree of gasification reaction. Secondly, since the gasification reaction happens in the reaction coil, a large amount of transport gas is needed, but the transport gas will take away a lot of heat during transporting, and thereby the gasification efficiency is low, the temperature is nonuniform, and the subsequent waste heat recovery system is massive. Thirdly, it is not economic that newly-produced synthetic gas is used to provide heat for gasification and carbonization. Fourthly, combustion products (mainly CO₂ and H₂O) are directly discharged and not fully utilized, resulting in low gasification efficiency. Finally, the ash and unreacted carbon residue in the synthetic gas are also discharged directly, resulting in low carbon conversion rate.

[0007] Chinese Patent Application No. 200810236639.4 discloses a method of producing synthetic gas from biomass by high temperature gasification. The method also adopts combination of carbonization and high temperature gasification. However, the method has following problems: firstly, heat of the carbonization furnace is supplied by direct combustion of external combustible gas and oxygen; the introduced high-quality external fuel gas greatly increases the energy consumption of the system; secondly, the adopted pyrolysis gas powder feeding system is complicated; when the high temperature pyrolysis gas is mixed with the low temperature carbon powder and fed into the gasification furnace, the mixture can easily be condensed to form tar, causing blockage and

influencing the normal operation; finally, the high pressure charcoal produced in the carbonization furnace is fed into the normal pressure milling machine after being decompressed and cooled, so as to be made into powder, and then the carbon powder is pressurized and fed into the gasification furnace by the pyrolysis gas. The whole process is complicated and high in energy consumption so that the feasibility of the project is bad.

[0008] From the above mentioned methods, conventional gasification, whether from biomass or from solid carbon-containing materials, cannot produce synthetic gas with high efficiency and low cost. Although the technology of independent pyrolysis and gasification can adapt to a variety of biomass and reduce the content of tar in synthetic gas, shortcomings such as nonuniform temperature, large investment in equipment for waste heat recovery, high material consumption, low gasification efficiency, and low carbon conversion rate limit the application of biomass gasification in industry. Particularly, there is no effective method for gasifying biomass applied to an entrained flow bed.

SUMMARY OF THE INVENTION

[0009] In view of the above-described problems, it is one objective of the invention to provide a method and a system for producing synthetic gas from biomass by carbonization that have high efficiency and low cost.

[0010] The technical scheme of the invention is described below: a method for producing synthesis gas from biomass by carbonization, the method comprising steps as follows:

[0011] 1) pre-treating a biomass raw material;

[0012] 2) carrying out low-temperature carbonization to obtain products of a pyrolysis gas and a charcoal, cooling the charcoal at an outlet of an carbonization

furnace to a temperature of 60-280°C, and conveying the cooled charcoal to a charcoal storage bin;

[0013] 3) separating the pyrolysis gas from a charcoal powder after allowing a gas output from an upper part of the carbonization furnace to pass through a gas-solid separator;

[0014] 4) delivering part of a separated pyrolysis gas to a combustion bed for combustion, heating the other part of the separated pyrolysis gas with a hot flue gas generated during the combustion of the combustion bed, and then delivering a heated pyrolysis gas to the carbonization furnace as a heat source for the carbonization furnace; delivering a waste hot flue gas after heat exchange to a pretreatment part for the biomass raw material for drying; conveying the separated charcoal powder to the charcoal storage bin;

[0015] 5) milling the charcoal powder to prepare a slurry; and

[0016] 6) introducing the charcoal slurry to a gasification furnace for gasification through a high-pressure charcoal slurry pump.

[0017] In the method for producing synthesis gas, the low-temperature carbonization is a slow pyrolysis carried out under conditions of an atmospheric pressure and an oxygen insulation in the carbonization furnace, and through adjusting a proportion of the pyrolysis gas and the air, a temperature of the carbonization furnace is controlled at 200-400°C, a rate of temperature rise of the carbonization furnace is controlled at 5-20°C/min, and a retention time of the biomass raw materials in the furnace is controlled in 20-90 min.

[0018] In the process of milling the charcoal powder for preparing the slurry, an atmospheric mill is adopted, and then water and an additive are added for milling for preparing the charcoal slurry.

[0019] In the method for producing synthesis gas, a content of the charcoal powder in the charcoal slurry is 50-70 wt. %, and preferably, 60-65 wt. %.

[0020] In the method for producing synthesis gas, the temperature of the carbonization furnace is preferably controlled at $250^{\circ}\text{C} \pm 10^{\circ}\text{C}$, the rate of temperature rise of the carbonization furnace is preferably controlled at $15^{\circ}\text{C} / \text{min}$, and the retention time of the biomass raw materials in the furnace is preferably controlled in 50 min.

[0021] A gasification system for producing synthetic gas from biomass by pyrolysis comprises: a pre-treatment part for the biomass raw material; a carbonization furnace; a pipeline connector for the carbonization furnace; and a pneumatic conveying system. A top of the carbonization furnace is connected with a cyclone separator; an output end of the cyclone separator is connected with the combustion bed and the charcoal storage bin; an output end of the combustion bed is connected to a heat exchanger for heating recycle pyrolysis gas; and a heated pyrolysis gas outlet is connected with the carbonization furnace, and a heat-exchanged waste heat flue gas outlet is connected with a drying system.

[0022] In the gasification system, a water-cooled screw conveyor is arranged on a pipeline from a charcoal outlet of the carbonization furnace to the charcoal storage bin, and the water-cooled screw conveyor is used for cooling the charcoal at the charcoal outlet of the carbonization furnace to $60\text{-}280^{\circ}\text{C}$ and then conveying the cooled charcoal to the charcoal storage bin.

[0023] In the gasification system, a mill, a charcoal slurry tank, and the high-pressure charcoal slurry pump are arranged on a pipeline from an outlet of the charcoal storage bin to the gasification furnace in sequence.

[0024] In the gasification system, an input gas supply pipe for the combustion bed is connected with an air pipeline, and the air is used as a combustion-supporting gas.

[0025] Advantages of the invention are summarized below:

[0026] First, By adopting the low-temperature slow pyrolysis technology, on one hand, the wood fiber structure of the biomass can be destroyed well, the biomass is milled easily, the energy consumption is reduced, and the volume energy density of biomass is increased; on the other hand, compared with the gasification method in Chinese Patent Application No. 200810236639.4, at the lower temperature, particularly at the temperature of $250^{\circ}\text{C} \pm 10^{\circ}\text{C}$, the higher solid yield and the higher energy yield can be obtained (The mass yield of charcoal is 60-80%, and the energy yield of charcoal is 70-90%), the energy consumption is reduced, and the carbon conversion rate of the whole system is favorably improved.

[0027] Second, the invention adopts the technology of heating the recycle pyrolysis gas as a heat source of the carbonization furnace by using the heat generated by combustion of self-produced pyrolysis gas. The carbonization furnace heating technology of the invention has the following three features: 1) the heat needed by the pyrolysis technique is provided by the inner part of the system so as to realize the thermal equilibrium of the system and not to introduce external energy fundamentally; 2) the heat for heating the recycle pyrolysis gas is provided by direct combustion of the pyrolysis gas and the air. That is to say, the chemical energy of the pyrolysis gas is used, and on the other hand, air, instead of pure oxygen, is used, which greatly reduces the cost of the whole system and increases the use flexibility of the carbonization furnace; 3) the heated recycle pyrolysis gas is directly conveyed to the carbonization furnace to contact the raw material, which not only increases the heating efficiency of the carbonization furnace but also maintains a normal operation for a highest charcoal yield under

conditions of an atmospheric pressure, an oxygen insulation, and a slow pyrolysis.

[0028] Third, the invention uses the waste heat smoke generated by combustion of the pyrolysis gas to dry the raw material, thereby improving the energy efficiency of the whole system.

[0029] Fourth, by adopting the technology of preparing slurry by atmospheric milling, the charcoal at the outlet of the carbonization furnace is introduced to the atmospheric mill and then mixed with a certain amount of water and additives to be prepared into a charcoal slurry. The process is simple and efficient. Compared with the gasification method with Chinese Patent Application No.

200810236639.4 for feeding at inlet, the method of the invention greatly reduces the energy consumption of the inlet raw material and increases the stability, reliability, and feasibility of the system.

[0030] Fifth, the invention adopts the technology of charcoal slurry pump pressurizing and transportation. Compared with the gasification method with patent number of 200810236639.4, the method avoids the technical problem about pneumatic conveying of powder and tar blockage when feeding dry carbon powder, and also increases the stability, reliability and feasibility of the system.

[0031] In short, the invention aims to realize simplicity, efficiency, energy conservation, economy and high project feasibility. Meanwhile, the invention enhances the gasification efficiency, decreases the amount of effective synthesis gas and improves the energy conversion rate of the system.

BRIEF DESCRIPTION OF THE DRAWINGS

[0032] FIG. 1 is a schematic diagram of a method and a system for producing synthetic

gas from biomass by carbonization according to one embodiment of the invention.

DETAILED DESCRIPTION OF THE EMBODIMENTS

[0033] The preferred examples, the process and the system layout structure according to the invention, are described with accompanying drawings.

[0034] As shown in FIG. 1, a gasification system of this invention comprises: a biomass raw material delivery port 1, a drying system 2, a biomass storage bin 3, a carbonization furnace 4, a cyclone separator 5, an air pipeline 6 for a combustion bed, a combustion bed 7, a compressor 8, a heat exchanger 9 for heating recycle pyrolysis gas, a waste heat flue gas pipeline 10 for the drying system, a water-cooled screw conveyor 11, a charcoal storage bin 12, a mill 13, a water pipeline 14 for slurry preparation for the mill, an additive pipeline 15 for the mill, a charcoal slurry tank 16, a high-pressure charcoal slurry pump 17, an oxygen pipeline 18 for a burner nozzle of a gasification furnace, the burner nozzle 19 of the gasification furnace, the gasification furnace 20, a water cooled wall 21 of the gasification furnace, a synthesis gas pipeline 22, an ash residue pipeline 23, a desalted and deoxygenated water pipeline 24, a saturated steam pipeline 25, an external fuel pipeline N1, and an emptying pipeline N2.

[0035] In the gasification system, a top of the carbonization furnace 4 is connected with the cyclone separator 5, and an output end of the cyclone separator 5 is connected with the combustion bed 7 and the charcoal storage bin 12 respectively. An output end of the combustion bed 7 is connected to the heat exchanger 9 for heating recycle pyrolysis gas. A heated pyrolysis gas outlet is connected with the carbonization furnace 4, and a heat-exchanged waste heat flue gas outlet is connected with the drying system 2.

[0036] The water-cooled screw conveyor 11 is arranged on a pipeline from a charcoal outlet of the carbonization furnace 4 to the charcoal storage bin 12, and used for cooling

the charcoal at the charcoal outlet of the carbonization furnace to 60-280°C and then conveying the cooled charcoal to the charcoal storage bin **12**.

[0037] The mill **13**, the charcoal slurry tank **16**, and the high-pressure charcoal slurry pump **17** are arranged on a pipeline from an outlet of the charcoal storage bin **12** to the gasification furnace **20** in sequence.

[0038] An input gas supply pipe for the combustion bed **7** is connected with the air pipeline **6**, and the air is used as combustion-supporting gas.

[0039] The method for producing synthesis gas from biomass by carbonization comprises the following steps:

[0040] 1) pre-treating the biomass raw materials;

[0041] 2) carrying out low-temperature carbonization to obtain products of pyrolysis gas and charcoal, cooling the charcoal at the outlet of the carbonization furnace to 60-280°C , and then conveying the cooled charcoal to the charcoal storage bin;

[0042] 3) separating the pyrolysis gas from charcoal powder after allowing the gas removed from the upper part of the carbonization furnace to pass through a gas-solid separator;

[0043] 4) delivering part of the separated pyrolysis gas to the combustion bed for combustion, heating the other part of pyrolysis gas with the hot flue gas generated during the combustion of the combustion bed through the heat exchanger, and then delivering the heated pyrolysis gas to the carbonization furnace as a heat source for the carbonization furnace; delivering the waste hot flue gas after heat exchange to the pretreatment part for biomass raw materials for drying; conveying the separated charcoal powder to the charcoal storage bin;

[0044] 5) milling the charcoal powder to prepare slurry; and

[0045] 6) introducing the charcoal slurry to the gasification furnace for gasification through the high-pressure charcoal slurry pump.

[0046] The low-temperature carbonization is slow pyrolysis carried out under the conditions of one atmospheric pressure and oxygen insulation in the carbonization furnace, and through adjusting the proportion of the pyrolysis gas and air, the temperature of the carbonization furnace is controlled at 200-400°C the rate of temperature rise of the carbonization furnace is controlled at 5-20°C /min, and the retention time of biomass raw materials in the furnace is controlled in 20-90 min. The temperature of the carbonization furnace is preferably controlled at 250°C ±10°C, the rate of temperature rise of the carbonization furnace is preferably controlled at 15°C /min, and the retention time of biomass raw materials in the furnace is preferably controlled in 50 min.

[0047] In the process of milling the charcoal powder for preparing slurry, an atmospheric mill is adopted, and then water and additives are added for milling for preparing charcoal slurry. The content of charcoal powder in the charcoal slurry is 50-70 wt. %, and preferably, 60-65wt. %.

[0048] Working process:

[0049] 1. System start-up process:

[0050] 1) opening a control valve **V1** on a pipeline from the biomass storage bin **3** to the carbonization furnace **4** and a control valve **V4** on the emptying pipeline **N2**, and keeping a control valve **V2** on the combustion bed **7** and a control valve **V3** on a pipeline from the cyclone separator **5** to the compressor **8** closed;

[0051] 2) opening a control valve **V6** on the external fuel pipeline **N1**, a control valve **V5** on the air pipeline **6** for the combustion bed as well as a control valve **V8** on a pipeline from the combustion bed **7** to the carbonization furnace **4** and a control valve **V9** on a pipeline from the combustion bed **7** to the drying system **2**,

and keeping a control valve **V7** on a pipeline from the combustion bed **7** to the heat exchanger **9** for heating recycle pyrolysis gas closed, so as to enable the hot flue gas generated during the combustion of fuels and air in the combustion bed **7** to be introduced in the drying system **2** and the carbonization furnace **4** for providing energy; and

[0052] 3) after 30-40 minutes' operation according to the process from step 1) to step 2), opening the control valves **V2**, **V3**, and **V7**, and simultaneously closing the control valves **V4**, **V6**, **V8**, and **V9**, so that the system starts to work normally at the time.

[0053] 2. Normal operation process of system:

[0054] The biomass raw material is fed to the drying system **2** via the biomass raw material delivery port **1**. The biomass raw material is dried and dehydrated by the heat smoke in the system and then conveyed to the biomass stock bin **3** for storage, and the biomass raw material is conveyed to the carbonization furnace **4**.

[0055] The product of the carbonization furnace **4** comprises pyrolysis gas and charcoal containing CO , H_2 , CO_2 , H_2O , CH_4 , and tar. The coarse pyrolysis gas is separated by the cyclone separator **5** and then the charcoal particles in the coarse pyrolysis gas are conveyed to charcoal storage bin **12**, and pyrolysis gas after the coarse separation are fed to the combustion bed **7** and the compressor **8**.

[0056] In the combustion bed **7**, the pyrolysis gas for combustion undergoes combustion reaction with the air from the pipeline **6**. The heat smoke generated by combustion heats the recycle pyrolysis gas; by adjusting the ratio of the pyrolysis gas generated by combustion to air the temperature of the carbonization furnace **4** is controlled at $400\text{-}600^\circ\text{C}$, and the rate of temperature rise of the carbonization furnace **4** is controlled at

5-20°C /min.

[0057] After being introduced to the compressor **8** for pressure increase, the recycle pyrolysis gas is heated to a certain temperature through the heat exchange **9** for heating recycle pyrolysis gas, and then the heated recycle pyrolysis gas enters the carbonization furnace **4** for providing energy required for the carbonization furnace; the hot flue gas after heat exchange enters the drying system **2** for drying the biomass raw materials.

[0058] The charcoal generated through the carbonization furnace **4** is conveyed to the charcoal storage bin **12** for storage after being cooled through the water-cooled screw conveyor **11**. The charcoal enters the mill **13** to be milled with water from the water pipeline **14** for slurry preparation for the mill and an additive from the additive pipeline **15** for the mill to obtain charcoal slurry. The prepared charcoal slurry is introduced to the charcoal slurry tank **16** and then introduced to the burner nozzle **19** of the gasification furnace after the pressure of charcoal slurry is increased to the working pressure of the gasification furnace **20** through the high-pressure charcoal slurry pump **17**. The oxygen from the oxygen pipeline **18** is also delivered to the burner nozzle **19** of the gasification furnace to carry out high-temperature gasification reaction in the gasification furnace **20**, and the temperature of synthesis gas at the outlet of the gasification furnace is controlled at 1200-1600°C by adjusting the amount of oxygen and the heat exchange amount of the water-cooled wall **21** (of the gasification furnace) in which desalted and deoxygenated water is introduced. The gasification products are mainly CO and H₂, a small amount of CO₂ and H₂O and a trace amount of CH₄; the desalted and deoxygenated water generates sub-high pressure saturated steam after heat absorption through the water-cooled wall **21** of the gasification furnace, the sub-high pressure saturated steam enters a subsequent system through the saturated steam pipeline **25**, and the ash residues generated during gasification are discharged through the ash residue pipeline **23**.

Example 1

[0059] Take wood as a raw material of biomass. The elemental composition and characteristic data of the dried wood are listed in Table 1.

Table 1 Elemental composition and characteristic data of the dried wood

Items	Symbol	Unit	Value
Carbon	C_{ar}	%(Kg/Kg)	39.43
Hydrogen	H_{ar}	%(Kg/Kg)	5.21
Oxygen	O_{ar}	%(Kg/Kg)	38.36
Nitrogen	N_{ar}	%(Kg/Kg)	0.15
Sulfur	S_{ar}	%(Kg/Kg)	0.21
Chlorine	Cl_{ar}	%(Kg/Kg)	0.00
Ash	A_{ar}	%(Kg/Kg)	5.00
Moisture	M_{ar}	%(Kg/Kg)	11.64
Ash fusion point	FT	°C	1436
Low heat value	LHV	MJ/Kg	14.75

[0060] The main operating conditions are set as follows:

[0061] 1) The water content of materials at the outlet of the drying system 2 is 15 wt. %;

[0062] 2) The pressure of the carbonization furnace 4 is atmospheric pressure, and the temperature of the carbonization furnace 4 is controlled at 200°C;

[0063] 3) The rate of temperature rise of the carbonization furnace 4 is controlled at 20°C/min;

[0064] 4) The retention time of biomass raw materials in the furnace is controlled in 90 min;

[0065] 5) The high-temperature charcoal is cooled to 60°C through the water-cooled screw conveyor 11; and

- [0066] 6) The pressure of the gasification furnace **20** is controlled at 4.0 MPa (A), and the temperature of the gasification furnace **20** is controlled at 1400°C.
- [0067] According to the set conditions, in the implementation process for illustrating the system with accompanying drawings, the main data and performance parameters of the system are as follows:
- [0068] 1) The mass yield of charcoal in the biomass raw materials introduced into the carbonization furnace **4** is 75%;
- [0069] 2) In the synthesis gas output through the synthesis gas pipeline **22**, the content of CO and H₂ is 78%;
- [0070] 3) The carbon conversion rate of the gasification system is 99.9%, and the oxygen consumption of available synthesis gas is 0.33 mol/mol.

Example 2

- [0071] Take wood in Example **1** as a raw material of biomass (Table 1).
- [0072] The main operating conditions are set as follows:
- [0073] 1) The water content of materials at the outlet of the drying system **2** is 10 wt. %;
- [0074] 2) The pressure of the carbonization furnace **4** is atmospheric pressure, and the temperature of the carbonization furnace **4** is controlled at 300°C;
- [0075] 3) The rate of temperature rise of the carbonization furnace **4** is controlled at 10°C/min;
- [0076] 4) The retention time of biomass raw materials in the furnace is controlled in 80 min;
- [0077] 5) The high-temperature charcoal is cooled to 60°C through the

water-cooled screw conveyor **11**; and

[0078] 6) The pressure of the gasification furnace **20** is controlled at 4.0 MPa (A), and the temperature of the gasification furnace **20** is controlled at 1400°C.

[0079] According to the set conditions, in the implementation process for illustrating the system with accompanying drawings, the main data and performance parameters of the system are as follows:

[0080] 1) The mass yield of charcoal in the biomass raw materials introduced into the carbonization furnace **4** is 80%;

[0081] 2) In the synthesis gas output through the synthesis gas pipeline **22**, the content of CO and H₂ is 82%;

[0082] 3) The carbon conversion rate of the gasification system is 99.9%, and the oxygen consumption of available synthesis gas is 0.32 mol/mol.

Example 3

[0083] Take wood in Example **1** as a raw material of biomass (Table **1**).

[0084] The main operating conditions are set as follows:

[0085] 1) The water content of materials at the outlet of the drying system **2** is 20 wt. %;

[0086] 2) The pressure of the carbonization furnace **4** is atmospheric pressure, and the temperature of the carbonization furnace **4** is controlled at 400°C;

[0087] 3) The rate of temperature rise of the carbonization furnace **4** is controlled at 5°C/min;

[0088] 4) The retention time of biomass raw materials in the furnace is controlled in 30 min;

[0089] 5) The high-temperature charcoal is cooled to 60°C through the water-cooled screw conveyor **11**; and

[0090] 6) The pressure of the gasification furnace **20** is controlled at 4.0 MPa (A), and the temperature of the gasification furnace **20** is controlled at 1400°C.

[0091] According to the set conditions, in the implementation process for illustrating the system with accompanying drawings, the main data and performance parameters of the system are as follows:

[0092] 1) The mass yield of charcoal in the biomass raw materials introduced into the carbonization furnace **4** is 70%;

[0093] 2) In the synthesis gas output through the synthesis gas pipeline **22**, the content of CO and H₂ is 75%;

[0094] 3) The carbon conversion rate of the gasification system is 99.9%, and the oxygen consumption of available synthesis gas is 0.34 mol/mol.

Example 4

[0095] Take wood in Example **1** as a raw material of biomass (Table **1**).

[0096] The main operating conditions are set as follows:

[0097] 1) The water content of materials at the outlet of the drying system **2** is 12 wt. %;

[0098] 2) The pressure of the carbonization furnace **4** is atmospheric pressure, and the temperature of the carbonization furnace **4** is controlled at 250°C;

[0099] 3) The rate of temperature rise of the carbonization furnace **4** is controlled at 15°C/min;

[0100] 4) The retention time of biomass raw materials in the furnace is controlled

in 40 min;

[0101] 5) The high-temperature charcoal is cooled to 60°C through the water-cooled screw conveyor **11**; and

[0102] 6) The pressure of the gasification furnace **20** is controlled at 4.0 MPa (A), and the temperature of the gasification furnace **20** is controlled at 1400°C.

[0103] According to the set conditions, in the implementation process for illustrating the system with accompanying drawings, the main data and performance parameters of the system are as follows:

[0104] 1) The mass yield of charcoal in the biomass raw materials introduced into the carbonization furnace **4** is 82%;

[0105] 2) In the synthesis gas output through the synthesis gas pipeline **22**, the content of CO and H₂ is 84%;

[0106] 3) The carbon conversion rate of the gasification system is 99.9%, and the oxygen consumption of available synthesis gas is 0.31 mol/mol.

Example 5

[0107] Take wood in Example **1** as a raw material of biomass (Table 1).

[0108] The main operating conditions are set as follows:

[0109] 1) The water content of materials at the outlet of the drying system **2** is 16 wt. %;

[0110] 2) The pressure of the carbonization furnace **4** is atmospheric pressure, and the temperature of the carbonization furnace **4** is controlled at 220°C;

[0111] 3) The rate of temperature rise of the carbonization furnace **4** is controlled at 12°C/min;

[0112] 4) The retention time of biomass raw materials in the furnace is controlled in 50 min;

[0113] 5) The high-temperature charcoal is cooled to 60°C through the water-cooled screw conveyor **11**; and

[0114] 6) The pressure of the gasification furnace **20** is controlled at 4.0 MPa (A), and the temperature of the gasification furnace **20** is controlled at 1400°C.

[0115] According to the set conditions, in the implementation process for illustrating the system with accompanying drawings, the main data and performance parameters of the system are as follows:

[0116] 1) The mass yield of charcoal in the biomass raw materials introduced into the carbonization furnace **4** is 85%;

[0117] 2) In the synthesis gas output through the synthesis gas pipeline **22**, the content of CO and H₂ is 86%;

[0118] 3) The carbon conversion rate of the gasification system is 99.9%, and the oxygen consumption of available synthesis gas is 0.3 mol/mol.

Example 6

[0119] Take wood in Example **1** as a raw material of biomass (Table **1**).

[0120] The main operating conditions are set as follows:

[0121] 1) The water content of materials at the outlet of the drying system **2** is 18 wt. %;

[0122] 2) The pressure of the carbonization furnace **4** is atmospheric pressure, and the temperature of the carbonization furnace **4** is controlled at 320°C;

[0123] 3) The rate of temperature rise of the carbonization furnace **4** is controlled

at 18°C/min;

[0124] 4) The retention time of biomass raw materials in the furnace is controlled in 70 min;

[0125] 5) The high-temperature charcoal is cooled to 60°C through the water-cooled screw conveyor **11**; and

[0126] 6) The pressure of the gasification furnace **20** is controlled at 4.0 MPa (A), and the temperature of the gasification furnace **20** is controlled at 1400°C.

[0127] According to the set conditions, in the implementation process for illustrating the system with accompanying drawings, the main data and performance parameters of the system are as follows:

[0128] 1) The mass yield of charcoal in the biomass raw materials introduced into the carbonization furnace **4** is 78%;

[0129] 2) In the synthesis gas output through the synthesis gas pipeline **22**, the content of CO and H₂ is 81%;

[0130] 3) The carbon conversion rate of the gasification system is 99.9%, and the oxygen consumption of available synthesis gas is 0.32 mol/mol.

CLAIMS

1. A method for producing synthesis gas from biomass by carbonization, comprising the following steps:
 - 1) pre-treating a biomass raw material;
 - 2) carrying out low-temperature carbonization to obtain products of a pyrolysis gas and a charcoal, cooling the charcoal at an outlet of an carbonization furnace to a temperature of 60-280°C, and conveying the cooled charcoal to a charcoal storage bin;
 - 3) separating the pyrolysis gas from a charcoal powder after allowing a gas output from an upper part of the carbonization furnace to pass through a gas-solid separator;
 - 4) delivering part of a separated pyrolysis gas to a combustion bed for combustion, heating the other part of the separated pyrolysis gas with a hot flue gas generated during the combustion of the combustion bed, and then delivering a heated pyrolysis gas to the carbonization furnace as a heat source for the carbonization furnace; delivering a waste hot flue gas after heat exchange to a pretreatment part for the biomass raw material for drying; conveying the separated charcoal powder to the charcoal storage bin;
 - 5) milling the charcoal powder to prepare a slurry; and
 - 6) introducing the charcoal slurry to a gasification furnace for gasification through a charcoal slurry pump.
2. The method of claim 1, wherein the low-temperature carbonization is a slow

pyrolysis carried out under conditions of an atmospheric pressure and an oxygen insulation in the carbonization furnace, and through adjusting a proportion of the pyrolysis gas and the air, a temperature of the carbonization furnace is controlled at 200-400°C, a rate of temperature rise of the carbonization furnace is controlled at 5-20°C /min, and a retention time of the biomass raw materials in the carbonization furnace is controlled in 20-90 min.

3. The method of claim 1 or 2, wherein in the process of milling the charcoal powder for preparing the slurry, an atmospheric mill is adopted, and water and an additive are added for milling.
4. The method of claim 1 or 2, wherein a content of the charcoal powder in the charcoal slurry is 50-70 wt. %.
5. The method of claim 1 or 2, wherein the temperature of the carbonization furnace is controlled at 250°C $\pm$ 10°C, the rate of temperature rise of the carbonization furnace is controlled at 15°C /min, and the retention time of the biomass raw materials in the furnace is controlled in 50 min.
6. The method of claim 1 or 2, wherein a content of the charcoal powder in the charcoal slurry is 60-65 wt. %.
7. A gasification system for producing synthetic gas from biomass by pyrolysis using the method of any of claims 1-6, comprising:
 - a) the pre-treatment part for the biomass raw material;

- b) the carbonization furnace;
- c) the gasification furnace;
- d) a pipeline connector for the carbonization furnace and the gasification furnace; and
- e) a pneumatic conveying system;

wherein

a top of the carbonization furnace (4) is connected with a cyclone separator (5);

an output end of the cyclone separator (5) is connected with a combustion bed (7) and the charcoal storage bin (12);

an output end of the combustion bed (7) is connected to a heat exchanger (9) for heating recycle pyrolysis gas;

a heated pyrolysis gas outlet is connected with the carbonization furnace (4); and

a heat-exchanged waste heat flue gas outlet is connected with a drying system (2).

8. The gasification system of claim 7, wherein a water-cooled screw conveyor (11) is arranged on a pipeline from a charcoal outlet of the carbonization furnace (4) to the charcoal storage bin (12), and the water-cooled screw conveyor (11) is used for cooling the charcoal at the charcoal outlet of the carbonization furnace to 60-280°C and then conveying the cooled charcoal to the charcoal storage bin (12).
9. The gasification system of claim 7 or 8, wherein a mill (13), a charcoal slurry tank

(16), and the high-pressure charcoal slurry pump (17) are arranged on a pipeline from an outlet of the charcoal storage bin (12) to the gasification furnace (20) in sequence.

10. The gasification system of claim 7 or 8, wherein an input gas supply pipe for the combustion bed (7) is connected with an air pipeline (6), and the air is used as a combustion-supporting gas.