

PCTWORLD INTELLECTUAL PROPERTY ORGANIZATION
International Bureau01002660-1
1902

INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁶ : C07C 7/04, 11/04	A1	(11) International Publication Number: WO 98/29366 (43) International Publication Date: 9 July 1998 (09.07.98)
(21) International Application Number: PCT/US97/23878 (22) International Filing Date: 31 December 1997 (31.12.97) (30) Priority Data: 60/034,240 31 December 1996 (31.12.96) US 60/033,948 31 December 1996 (31.12.96) US (71) Applicant: EXXON CHEMICAL PATENTS INC. [US/US]; 5200 Bayway Drive, Baytown, TX 77520-5200 (US). (72) Inventors: KUECHLER, Keith, H.; 4500 Bayway Drive, Baytown, TX 77522 (US). LUMGAIR, David, R., Jr.; 5111 Middle Falls Drive, Kingwood, TX 77345 (US). (74) Agents: RUSSELL, Linda, K. et al.; Exxon Chemical Com- pany, P.O. Box 2149, Baytown, TX 77522-2149 (US).		(81) Designated States: AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GE, GH, HU, ID, IL, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, TJ, TM, TR, TT, UA, UG, UZ, VN, YU, ARIPO patent (GH, GM, KE, LS, MW, SD, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG). Published <i>With international search report.</i> <i>Before the expiration of the time limit for amending the</i> <i>claims and to be republished in the event of the receipt of</i> <i>amendments.</i>
(54) Title: RECOVERY OF A SECONDARY ETHYLENE STREAM FROM AN ETHYLENE PURIFICATION PROCESS		
(57) Abstract		
<p>The invention relates to a process for the production of a secondary ethylene stream (10) from a pressurised mixed olefin bearing charge gas (4) as the overhead of one fractional distillation tower (2) contained in an overall olefin recovery and separation facility, wherein said tower is operated under conditions to produce a bottom stream (15) from which a primary ethylene rich product stream (20) can be recovered. This may eliminate the need for cryogenic fractional distillation and/or the need for a circulating lean oil absorbant material.</p>		