METHODS AND SYSTEMS FOR FORMING VATERITE FROM CALCINED LIMESTONE USING ELECTRIC KILN

CROSS-REFERENCE TO RELATED APPLICATION

[0001] This application claims benefit of US Provisional Application No. 63/046,239, filed June 30, 2020, which is incorporated herein by reference in its entirety in the present disclosure.

BACKGROUND

[0002] Carbon dioxide (CO_2) emissions have been identified as a major contributor to the phenomenon of global warming. CO_2 is a by-product of combustion and it creates operational, economic, and environmental problems. It is known that elevated atmospheric concentrations of CO_2 and other greenhouse gases facilitate greater storage of heat within the atmosphere leading to enhanced surface temperatures and rapid climate change. In addition, elevated levels of CO_2 in the atmosphere may also further acidify the world's oceans due to the dissolution of CO_2 and formation of carbonic acid. The impact of climate change and ocean acidification may likely be economically expensive and environmentally hazardous if not timely handled. Reducing potential risks of climate change requires sequestration and avoidance of CO_2 from various anthropogenic processes.

SUMMARY

[0003] Provided herein are processes and systems that relate to using electric kilns to produce clean CO_2 devoid of pollutants that are emitted from the combustion of fuel, such as e.g. fossil fuel; and the sequestration of the clean CO_2 into commercially useful cementitious products or disposal underground.

[0004] In one aspect, there is provided a process, comprising: a) calcining limestone in an electric kiln to form a mixture comprising calcium oxide and a gaseous stream comprising clean carbon dioxide, wherein the clean carbon dioxide or the first gaseous stream comprises no gaseous or non-gaseous component from combustion of fuel; b) treating the mixture comprising calcium oxide with a N-containing salt solution to produce an aqueous solution comprising calcium salt; and c) contacting the aqueous solution with the first gaseous stream comprising clean carbon dioxide to produce a precipitation material comprising vaterite, aragonite, calcite, or combination thereof.

[0005] In some embodiments of the foregoing aspect, the calcining limestone in the electric kiln produces less than 20% of at least one component selected from the group consisting of SOx; thermal NOx; carbon monoxide; metal; volatile organic matter; particulate matter; and combinations thereof. In some embodiments of the foregoing aspect and embodiments, the first

[0038] In some embodiments of the foregoing aspect and embodiments, the cementitious product is a formed building material selected from masonry unit, construction panel, conduit, basin, beam, column, slab, acoustic barrier, insulation material, and combinations thereof.

[0039] In one embodiment, there are provided product(s) formed by the foregoing process aspect and embodiments.

[0040] In one aspect, there is provided a system, comprising:

(i) a calcining system configured for calcining limestone in an electric kiln to form a mixture comprising calcium oxide and a gaseous stream comprising clean carbon dioxide, wherein the clean carbon dioxide comprises no gaseous or non-gaseous components from combustion of fuel;

(ii) a treatment reactor operably connected to the calcining system configured for receiving the mixture comprising calcium oxide and configured for dissolving the mixture comprising calcium oxide in a N-containing salt solution to produce an aqueous solution comprising calcium salt; and

(iii) a contacting reactor operably connected to the treatment reactor and the calcining system and configured for receiving the aqueous solution comprising calcium salt and the first gaseous stream comprising clean carbon dioxide, and configured for treating the aqueous solution comprising calcium salt with the gaseous stream comprising clean carbon dioxide to form a precipitation material comprising vaterite, aragonite, calcite, or combinations thereof.

[0041] In some embodiments of the foregoing aspect, the treatment reactor further produces a second gaseous stream comprising ammonia and the contacting reactor is further configured for receiving the second gaseous stream comprising ammonia, and configured for treating the first aqueous solution comprising calcium salt with the first gaseous stream comprising clean carbon dioxide and the second gaseous stream comprising ammonia.

[0042] In one aspect, there is provided a zero carbon dioxide (CO_2) emission system, comprising:

(i) a calcining system in a cement plant configured for calcining limestone in an electric kiln to form a mixture comprising calcium oxide and a first gaseous stream comprising clean carbon dioxide, wherein the clean carbon dioxide comprises no gaseous or non-gaseous components from combustion of fuel;

(ii) a treatment reactor operably connected to the calcining system configured for receiving the mixture comprising calcium oxide and configured for dissolving the mixture comprising calcium oxide in a N-containing salt solution under one or more dissolution

WHAT IS CLAIMED IS:

1. A process, comprising:

a) calcining limestone in an electric kiln to form a mixture comprising calcium oxide and a gaseous stream comprising clean carbon dioxide, wherein the clean carbon dioxide comprises no gaseous or non-gaseous component from combustion of fuel;

b) treating the mixture comprising calcium oxide with a N-containing salt solution to produce an aqueous solution comprising calcium salt; and

c) contacting the aqueous solution with the gaseous stream comprising clean carbon dioxide to produce a precipitation material comprising vaterite, aragonite, calcite, or combination thereof.

2. The process of claim 1, wherein the fuel is fossil fuel.

3. The process of claim 1 or 2, wherein the gaseous stream comprises, at less than 20% of the gaseous stream, at least one component selected from the group consisting of SOx; carbon monoxide; metal; volatile organic matter; particulate matter; and combination thereof, thereby comprising clean carbon dioxide.

4. The process of any one of the preceding claims, wherein the gaseous stream comprises between 80-95 vol% clean carbon dioxide.

5. The process of any one of the preceding claims, wherein the mixture comprising calcium oxide and/or the first aqueous solution comprising calcium salt further comprises between 1-40 wt% of solid selected from the group consisting of silicate, iron oxide, aluminum oxide, other particulate matter, and combination thereof.

6. The process of any one of the preceding claims, wherein the calcium oxide is an underburnt lime, dead burnt lime, soft burnt lime, or combination thereof.

7. The process of any one of the preceding claims, wherein the N-containing salt is N-containing inorganic salt, N-containing organic salt, or combination thereof.

8. The process of claim 7, wherein the N-containing inorganic salt is selected from the group consisting of ammonium halide, ammonium acetate, ammonium sulfate, ammonium sulfite, ammonium nitrate, ammonium nitrite, and combination thereof; optionally wherein the ammonium halide is ammonium chloride.

9. The process of claim 7, wherein the N-containing salt is N-containing organic salt that has N-containing organic compound selected from the group consisting of aliphatic amine, alicyclic amine, heterocyclic amine, and combination thereof.

10. The process of any one of the preceding claims, wherein the treating step further comprises adding anhydrous ammonia or an aqueous solution of ammonia.

11. The process of any one of the preceding claims, wherein the treating step further produces a second gaseous stream comprising ammonia and the process further comprises removing and optionally recovering the second gaseous stream comprising ammonia; subjecting the gaseous stream comprising clean carbon dioxide and the second gaseous stream comprising ammonia to a cooling process to condense a second aqueous solution comprising ammonium bicarbonate, ammonium carbonate, ammonia, or combination thereof; and treating the aqueous solution comprising calcium salt with the second aqueous solution to form the precipitation material.

12. The process of any one of the preceding claims, wherein the gaseous stream comprising clean carbon dioxide has kinetics in the contacting step of more than 5 times faster to produce the precipitation material compared to a process using regular kiln; optionally wherein the faster kinetics of the contacting step results in high yield of more than 80% vaterite of the gaseous stream; optionally wherein the faster kinetics of the contacting step results in the vaterite with a particle size of between 0.05-20 micron.

13. The process of any one of the preceding claims, further comprising dewatering the precipitation material to separate the precipitation material from supernatant solution, wherein the precipitation material and/or the supernatant solution comprise residual N-containing inorganic salt.

14. The process of claim 13, further comprising removing and optionally recovering the residual N-containing inorganic salt from the supernatant aqueous solution and/or removing and optionally recovering the residual N-containing inorganic salt from the precipitation material; optionally wherein recovering the residual N-containing inorganic salt from the supernatant aqueous solution comprises recovery process selected from the group consisting of thermal decomposition, pH adjustment, reverse osmosis, multi-stage flash, multi-effect distillation, vapor recompression, distillation, and combination thereof.; optionally wherein the step of removing and optionally recovering the residual N-containing inorganic salt from the precipitation material comprises heating the precipitation material between 100-360^{o}C to evaporate the N-containing inorganic salt from the precipitation material with optional recovery by condensation of the N-containing inorganic salt.

15. The process of any one of the preceding claims, wherein the N-containing salt is ammonium chloride which evaporates from the precipitation material in a form comprising ammonia gas, hydrogen chloride gas, chlorine gas, or combination thereof; optionally further comprising recycling the recovered residual ammonia and/or N-containing inorganic salt back to the treating and/or contacting step of the process.

16. The process of any one of the preceding claims, wherein the vaterite is stable vaterite or reactive vaterite.

17. The process of claim 16, further comprising adding water to the precipitation material comprising reactive vaterite and transforming the reactive vaterite to aragonite and/or calcite wherein the aragonite and/or the calcite sets and hardens to form cement or cementitious product.

18. The process of claim 17, wherein the cementitious product is a building material, formed building material, and/or artificial marine structure.

19. The process of claim 16, further comprising forming a non-cementitious product from the precipitation material comprising vaterite wherein the non-cementitious product is selected from the group consisting of paper, polymer product, lubricant, adhesive, rubber product, chalk, asphalt product, paint, abrasive for paint removal, personal care product, cosmetic, cleaning product, personal hygiene product, ingestible product, agricultural product, soil amendment product, pesticide, environmental remediation product, and combination thereof.

20. The process of any one of the preceding claims, further comprising adding an additive to the aqueous solution or to the precipitation material, wherein the additive is selected from the group consisting of fatty acid ester, sodium decyl sulfate, lauric acid, sodium salt of lauric acid, urea, citric acid, sodium salt of citric acid, phthalic acid, sodium salt of phthalic acid, taurine, creatine, dextrose, poly(n-vinyl-1-pyrrolidone), aspartic acid, sodium salt of aspartic acid, magnesium chloride, acetic acid, sodium salt of acetic acid, glutamic acid, sodium salt of glutamic acid, strontium chloride, gypsum, lithium chloride, sodium chloride, glycine, sodium citrate dehydrate, sodium bicarbonate, magnesium sulfate, magnesium acetate, sodium polystyrene, sodium dodecylsulfonate, poly-vinyl alcohol, and combination thereof.

21. The process of any one of the preceding claims, wherein the vaterite is unimodal, bimodal, or multimodal distribution of a particulate composition with an average particle size of between 0.1-100 micron.

22. The process of any one of the preceding claims, further comprising blending the precipitation material with Portland Cement, aggregate, or combination thereof.

23. The process of any one of the preceding claims, further comprising mixing the precipitation material with one or more admixture selected from the group consisting of set accelerator, set retarder, air-entraining agent, foaming agent, defoamer, alkali-reactivity reducer, bonding admixture, dispersant, coloring admixture, corrosion inhibitor, damp-proofing admixture, gas former, permeability reducer, pumping aid, shrinkage compensation admixture, fungicidal admixture, germicidal admixture, insecticidal admixture, rheology modifying agent, finely divided mineral admixture, pozzolan, aggregate, wetting agent, strength enhancing agent, water repellent, reinforced material, and combination thereof.

24. The process of claim 23, wherein the reinforced material is a fiber made of zirconia, aluminum, glass, steel, carbon, ceramic, grass, bamboo, wood, fiberglass, synthetic material, or combination thereof.

25. A system, comprising:

(i) a calcining system configured for calcining limestone in an electric kiln to form a mixture comprising calcium oxide and a gaseous stream comprising clean carbon dioxide, wherein the clean carbon dioxide comprises no gaseous or non-gaseous component from combustion of fuel;

(ii) a treatment reactor operably connected to the calcining system configured for receiving the mixture comprising calcium oxide and configured for dissolving the mixture comprising calcium oxide in a N-containing salt solution to produce an aqueous solution comprising calcium salt; and

(iii) a contacting reactor operably connected to the treatment reactor and the calcining system and configured for receiving the aqueous solution comprising calcium salt and the gaseous stream comprising clean carbon dioxide, and configured for treating the aqueous solution comprising calcium salt with the gaseous stream comprising clean carbon dioxide to form a precipitation material comprising vaterite, aragonite, calcite, or combination thereof.

26. The system of claim 25, wherein the treatment reactor further produces a second gaseous stream comprising ammonia and the contacting reactor is further configured for receiving the second gaseous stream comprising ammonia, and configured for treating the aqueous solution comprising calcium salt with the gaseous stream comprising clean carbon dioxide and the second gaseous stream comprising ammonia.