CLAIMS:

What is claimed is:

1. A process for separating a product from at least one multicomponent feed by simulated countercurrent adsorptive separation in a simulated moving-bed adsorption apparatus comprising at least one rotary valve and plural sieve chambers, characterized by the steps of: (a) introducing a first multicomponent feed, comprising at least one desired product, through at least one fluid communication conduit into said apparatus; (b) withdrawing a first multicomponent extract, comprising at least one desired product, through at least one fluid communication conduit out of said apparatus; (c) flushing said at least one conduit in step (a) with at least one initial flushing medium, whereby residue of said first multicomponent feed is flushed from the at least one conduit in step (a) into said apparatus by the at least one initial flushing medium, so as to produce a first flush output comprising said at least one initial flushing medium and said residue of said first multicomponent feed; (d) flushing at least one conduit in step (b) with at least one initial flushing medium, whereby residue of said first multicomponent extract is flushed ~~form~~ from the at least one conduit in step (b) out of said apparatus by the at least one initial flushing medium, so as to produce a first flush output comprising said at least one initial flush medium and said residue of said first multicomponent extract; (e) after step (c) flushing said at least one fluid communication conduit with a second flushing medium, with the proviso that said second flushing medium comprises said first flush output from step (d).

2. The process of Claim 1, further characterized by not having a step of distillation of said flush output before it is used as said second flushing medium.

3. The process of Claim 1, wherein said final extract comprises at least 99.7 wt% paraxylene, based on the total amount of C8 aromatic hydrocarbons in said final extract.

4. The process of Claim 1, wherein said first multicomponent feed has a concentration of paraxylene of greater than or equal to the thermodynamic equilibrium concentration of paraxylene in a mixture of C8 aromatic hydrocarbons.

5. The process of Claim 1, wherein the initial flushing medium has a concentration of paraxylene greater than the concentration of xylene in said first multicomponent feed.

6. The process of Claim 1, wherein the volume of the second flushing medium is from 110 to 150 vol% of the volume of the bedline flushed.

~~7. An apparatus adapted for a process for separating a product from at least one multicomponent feed by simulated countercurrent adsorptive separation, having plural bedlines, plural adsorption chambers, and plural flushing steps using plural flushing media, the improvement comprising a fluid connection between a first flush output **101** and a second flush input **105**, without any intervening fluid connection to one or more distillation columns.~~