

PROCESS AND PLANT FOR THE PURIFICATION OF TRICHLOROSILANE AND SILICON TETRACHLORIDE

5 The present invention concerns a process and plant for the purification of trichlorosilane and silicon tetrachloride.

More in particular the invention refers to the purification of technical grade trichlorosilane and silicon tetrachloride in order to obtain electronic grade trichlorosilane and silicon tetrachloride.

10 It is known that the raw material for the production of silicon polycrystals for electronic use is constituted by technical grade trichlorosilane (also identified by means of the acronym TCS TG, wherein TCS stands for trichlorosilane and TG stands for technical grade) and/or silicon tetrachloride (identified, with the same above methodology, by means of the acronym TET TG). These products contain different
15 impurities, principally consisting of other silanes, such as silicon tetrachloride and dichlorosilane, but also of metallic chlorides, boron trichloride BCl_3 and other boron compounds (the boron acting in silicon as a doping agent of positive electrical charges) and arsenic and phosphorus
20 trichlorides AsCl_3 e PCl_3 (which act in silicon as doping agents of negative charges). The presence of the said impurities prevents technical grade trichlorosilane and silicon tetrachloride from being used in processes for the production of semiconductors, wherein the electrical resistivity control is managed by a rigorous control of doping impurities.

25 Moreover, the hydrochloric acid used in the synthesis of chlorosilanes, being a recycle product from the production of organosilanes, is generally contaminated by carbon impurities.

The presence of metallic impurities, boron, arsenic and phosphorus chlorides and of carbon-chlorine compounds, does not allow
30 the direct use of TCS TG or TET TG neither for the production of silicon polycrystals for electronic use and for the growing of epitaxial layers in convenient reactors named Epi, nor for the production of electronic semiconductor devices.

35 In order to use TCS TG and TET TG in these processes, i.e. can be classified as having an electronic purity grade, they must be further purified, in order to reduce the concentration of impurities by a factor of at least 10000 or 100000 times.

The purification of TCS TG or TET TG is generally obtained by means of hyper distillation, based on the difference between the impurities boiling temperature and the TCS and TET boiling temperatures. The following Table 1 shows the boiling temperature of the different compounds.

Table 1

Low boiling		High boiling	
Compound	T(°C)	Compound	T(°C)
Trichlorosilane TCS	33,0	Silicon tetrachloride TET	57,6
Boron trichloride BCl ₃	12,5	Phosphorus trichloride PCl ₃	75,5
Dichlorosilane DCS	8,3	Arsenic trichloride AsCl ₃	130,2

Nevertheless, simple distillation requires using columns having a high number of plates and very high reflux ratios, implying very high columns and high stroke diameters, requiring high investment costs. For such boron compounds having a boiling point very close to that of TCS, distillation even is unable to remove the impurity in an efficient way.

An alternative purification process is constituted by the purification process by means of wet nitrogen bubbles. In this process, the reaction of TCS and/or TET with moisture carried by nitrogen leads to the formation of SiO₂ and high boiling point poly-siloxanes (Si-OH bonds), acting also as complexing agents. The purity grade that is obtainable by means of the purification process with "wet N₂" does not exceed a P-type value of 100 ohm·cm. In fact, the complexing effect of the H₂O molecules and of the polysiloxanes is in any case lower than the complexing capacity proper of electron rich big molecules.

This kind of capacity, proper of some compounds, is exploited in the purification processes by means of complexation of the impurities with tin or titanium chlorides or with electron rich big molecules, wherein a first step of complexation is followed by distillation. This class of processes, in spite of the fact that they are improvement with respect to the direct distillation and to the complexation with H₂O, does not grant an optimal level purity of electronic grade TCS and TET, in terms of p-type resistivity (this feature being very important in cases where the obtained purified TCS is subsequently used for the growth of the layers in epitaxial reactors).

Amongst the purification processes by means of complexation of the impurities, a process is known (developed by

Amongst the purification processes by means of complexation of the impurities, a process is known (developed by Pechiney, patent GB975000) making use of tin and titanium chlorides (SnCl_4 and TiCl_4), bromine (Br_2) and chlorine (Cl_2), in order to oxidize phosphorus to P^{5+} and to complex it at ambient temperature in a 2-24 hours batch cycle. The subsequent removal of the introduced metals and other impurities (such as boron, aluminium, antimony, vanadium) is obtained by a precipitation step, by adding triphenylchloromethane or triphenylmethylchloride (TCM). Electronic grade TCS is then obtained by means of a subsequent distillation.

The purity level that can be obtained by means of the above said process can be successfully used in cases where a TCS EG having a p-type value of 1000 ohm·cm is considered sufficient. In fact, this kind of process was developed in a period when this level of purity was able to meet the market requirements.

A further process for the purification of chlorosilanes, in particular TCS, belonging to the same category, was developed by Dynamit Nobel (patent GB1241108) and makes use of a process for the complexation of boron and metallic impurities by means of one or more heterocyclic mononuclear or polynuclear solid compounds, containing nitrogen (N) as part of a heterocyclic ring and sulfur (S) as part of another heterocyclic ring, and being able to block the impurities in the form of solid complexes and subsequently allowing the distillation of pure TCS.

As a common feature, these additives (about ten are listed in the patent) have a very high electron number and consequently have a great aptitude to the formation of covalent bonds, N (nitrogen) bonds, S (sulfur) bonds, OH groups (examples: 6-methyl-2-thiouracil, N(phenyl)N- $\text{CH}_3\text{-SH}$, N-methyl-2-thioimidazoline, H-N(phenyl)N- $\text{CH}_3\text{-S}$, phenothiazine, HN-(phenyl-phenyl)S).

This process also was developed in the second half of the sixties, when a TCS EG purity level around p-type levels of about 1000 ohm·cm was considered sufficient in order to meet the market requirements.

The solution according to the present invention is to be considered in this context, with the aim of providing a process and a plant for the purification of technical grade trichlorosilane and silicon tetrachloride in order to obtain electronic grade trichlorosilane and silicon

tetrachloride, by means of a reaction of complexation of the boron impurities (trichloride BCl_3) and other metallic impurities, optionally present, with diphenylthiocarbazone (Ditizone or also DTZ) and triphenylchloromethane (TCM), and subsequent removal of the
5 complexation products and the remaining impurities.

These and other results are obtained according to the present invention by providing a process in three steps: 1) removal of boron trichloride BCl_3 other boron compounds and metallic impurities by means of complexation thereof, 2)
10 PCl_3 and phosphorus containing compounds, arsenic chlorides AsCl_3 and arsenic containing compounds, aluminium compounds, antimony compounds and in general all the metals and metalloids compounds and carbon-silanes compounds by means of distillation (the purity level obtained after the removal of these compounds is sufficient for the
15 production of the electronic grade polycrystal); 3) removal of the possibly present dichlorosilane by means of further distillation (for the production of TCS EG suitable for feeding epitaxial reactors).

It is therefore a first specific object of the present invention a process for the purification of trichlorosilane and/or silicon tetrachloride comprising the following steps of treating technical grade trichlorosilane
20 and/or technical grade silicon tetrachloride:

- complexation of the boron impurities (trichloride BCl_3) and other metallic impurities by addition of diphenylthiocarbazone and/or triphenylchloromethane, with the formation of complex macromolecules
25 having high boiling point,

- first column distillation of the complexation step products, wherein the complexed boron impurities, together with other metallic impurities are removed as bottoms, and

- second column distillation of the tops of the previous
30 distillation, wherein electronic grade trichlorosilane (plus dichlorosilane possibly present) and/or silicon tetrachloride are obtained as tops and phosphorus chlorides PCl_3 and phosphorus containing compounds, arsenic chlorides AsCl_3 and arsenic containing compounds, aluminium compounds, antimony compounds and in general all the present metals
35 and metalloids compounds and carbo-silanes compounds, having a certain residual amount of trichlorosilane and/or silicon tetrachloride, are obtained as bottoms.

The purification process according to the invention can comprise a further distillation step of the bottoms of said second distillation, through which trichlorosilane and/or dichlorosilane free silicon tetrachloride are obtained as tops and phosphorus chlorides PCl_3 and phosphorus containing components, arsenic chlorides AsCl_3 and arsenic containing compounds, aluminium compounds, antimony compounds and in general all the metals and metalloids and carbon-silanes compounds which are present are obtained as bottoms.

In particular, according to the invention, said complexation step takes place by adding an excess amount, with respect to the stoichiometric amount, of one or both diphenylthiocarbazon and/or triphenylchloromethane.

Preferably, according to the invention, said complexation step takes place by adding diphenylthiocarbazon in an amount that is twice the amount of triphenylchloromethane.

Further, in the process according to the invention, the bottom temperature in said first distillation step is comprised between 38°C and 48°C (preferably it is 42°C) for the purification of trichlorosilane and between 65°C and 75°C (preferably 69°C) for the purification of silicon tetrachloride.

In particular, according to the invention, said first distillation step is initially operated with a total reflux of the tops, in order to allow the boron and other metals impurities complete complexation, preferably for a time period of at least 3 hours, and, following that period of total reflux, the distillation is conducted with a top reflux flow comprised between 0,3 as a minimum and 2,8 as a maximum, preferably 1,33 as far as TCS is concerned and between 0,17 as a minimum and 5 as a maximum, preferably 2,5 as far as TET is concerned.

Said values represents the reflux ratio, i.e. the ratio between the flow of condensate tops returned to the top of the column and the flow of extracted tops (distillate)).

It is further a second specific object of the present invention a plant for the purification of trichlorosilane and/or silicon tetrachloride comprising the following apparatuses for treating technical grade trichlorosilane and/or technical grade silicon tetrachloride:

- a column for the complexation and distillation of boron (trichloride BCl_3) impurities and other metallic impurities, working in batch,

by adding diphenylthiocarbazone and/or triphenylchloromethane, with the formation of high boiling complex macromolecules, wherein the complexed boron impurities, together with other complexed metallic impurities are removed as bottoms, and

5 - a column for the distillation of the tops of the previous complexation and distillation column, wherein electronic grade trichlorosilane (and possibly present dichlorosilane) and/or silicon tetrachloride are obtained as tops and phosphorus chlorides PCl_3 and phosphorus containing compounds, arsenic chlorides AsCl_3 and arsenic
10 containing compounds, aluminium compounds, antimony compounds and in general all the metals and metalloid and carbon-silanes compounds that are present, together with a certain residual amount of trichlorosilane and/or silicon tetrachloride, are obtained as bottoms, and, possibly ,

 - an intermediate vessel between said complexation and
15 distillation column and said distillation column, wherein the tops of the complexation and distillation column are collected in order to constitute a feed reservoir for the distillation column, during the starting phase of the following operative cycle of the complexation and distillation column, and

 - a further distillation column, for the bottoms of said
20 distillation column, wherein trichlorosilane and/or dichlorosilane free silicon tetrachloride are obtained as tops and phosphorus chlorides PCl_3 , phosphorus containing compounds, arsenic chlorides AsCl_3 and arsenic containing compounds, aluminium compounds, antimony compounds and in general all the metals and metalloid and carbon-silanes compounds that
25 are present, together with a certain residual amount of trichlorosilane and/or silicon tetrachloride, are obtained as bottoms.

In particular, according to the invention, in said purification plant according to any of claims 11-13, characterised in that the bottom temperature in said complexation and distillation column is comprised
30 between 38 and 48°C (preferably is 42°C) for the purification of trichlorosilane and between 65 and 75°C (preferably 69°C) for the purification of silicon tetrachloride, while the thermal fluid temperature of the exchanger at the bottom of the column is comprised between 58 and 73°C (preferably is 60°C) for the purification of trichlorosilane and between
35 75 and 83°C (preferably 79°C).

The purification plant according to the present invention further comprises linking conduits between the different apparatuses,

linking conduits to other plants, inlet conduits for the materials to treat and outlet conduits for the treated materials, pumps, adjustment and control instruments.

5 The effectiveness of the purification process and plant according to the present invention are self-evident. In fact, the use of the two complexing agents TCM e DTZ and the rigorous control of the complexation temperature, have a much higher boron and metallic impurities reducing power than the previously known processes and is able to guarantee a remarkable stability and qualitative repeatability over
10 the time.

In particular, even if TCM and DTZ allow to realise the complexation of TCS and TET impurities also if singularly used (TCM allows the complexation of many metals except boron), the use of these complexing agents together is needed in order to complex all the
15 impurities.

In conclusion, the combined effect of TCM and DTZ shows optimal complexation efficiency, creating a synergy with respect to the separate and/or sequential use of said two complexing agents.

The invention will be described herein below for illustrative,
20 but non limitative, purpose with reference in particular to Figure 1 enclosed, in which it is shown a schematic flow diagram related to the purification of trichlorosilane and/or silicon tetrachloride according to a preferred embodiment of the present invention.

In particular, a complexation and distillation column 1, a
25 distillation column 2 and a further distillation column 3 of the dichlorosilane free trichlorosilane are shown.

The complexation and distillation column 1 is the device wherein boron impurities (trichloride BCl₃) and other metallic impurities are removed from trichlorosilane TCS TG and/or from silicon tetrachloride TET
30 TG by means of a batch process constituted by a complexation reaction of said impurities with diphenylthiocarbazone (Ditizone or DTZ) and triphenylchloromethane (TCM).

The complexing additives promote the formation of covalent bonds between the impurities and additives themselves, causing the
35 formation of high boiling complex macromolecules. In particular, the reaction takes place between the big molecules of Ditizone and TCM, rich in available electrons, and the molecules of BCl₃ and other boron

compounds and possibly other metallic chlorides molecules poor in electrons, forming strong complexes having a very high boiling point.

It is a critical feature of this process, in order to obtain an effective removal of the impurities, to control the temperature at which the complexation reaction takes place. In fact, it is required a very rigorous control of the temperature range at which the complexation reaction takes place, otherwise the obtained complexes can decompose. It will be necessary to control that the temperature at the bottom of the column is always comprised between 38 and 48°C (preferably is equal to 42°C) for the purification of trichlorosilane to take place and between 65 and 75°C (preferably 69°C) for the purification of silicon tetrachloride.

The bottom of the complexation and distillation column 1 is heated by means of a heat exchanger 4, inside which a thermal fluid flows, whose temperature is comprised between 58 and 73°C (preferably is equal to 60°C), in the case of trichlorosilane purification and between 75 and 83°C (preferably 79°C) for the purification of silicon tetrachloride.

Heating the bottom of column 1 causes the evaporation of the lowest boiling compounds comprised in the blend to treat. These compounds begins to ascend along column 1, passing through the different stages in which the column is divided up to the top stage. Here, a condenser 5 causes the vapours condensation and their reflux to the column. In stationary conditions, an equilibrium is set between the vapour flow ascending inside column 1 and the liquid flow descending inside the same column 1 and complexed boron impurities separation is obtained, this impurities being removed as bottoms of column 1 together with other complexed metallic impurities. In order to reach the equilibrium conditions, column 1 is initially operated with a 100% reflux at the top. After the equilibrium condition are reached, column 1 is operated according to design specifications untill the complete depletion of the batch.

The tops of column 1 are used to feed an intermediate section of the distillation column 2, in which electronic grade trichlorosilane (and dichlorosilane possibly present) and/or silicon tetrachloride are obtained as tops and phosphorus chlorides PCl_3 and phosphorus containing compounds, arsenic chlorides AsCl_3 and arsenic containing compounds, aluminium compounds, antimony compounds and in general all the present metals and metalloid and carbon-silanes compounds,

together with a certain residual amount of trichlorosilane and/or silicon tetrachloride, are obtained as bottoms.

The distillation column 2 is a common packed column, with a condenser 6 at the top and a reboiler 7 at the bottom.

Between the complexation and distillation column 1 and the distillation column 2 an intermediate vessel 8 is shown, in which the tops of column 1 are accumulated in order to constitute a reserve for the feed of the distillation column 2, during the starting phase of the subsequent operative cycle of the complexation and distillation column 1. Further, inside the intermediate vessel 8 the tops of column 1 can be mixed together with a flow of trichlorosilane, dichlorosilane and various impurities (not comprising boron and/or other metallic impurities), coming from the reactors of a polycrystalline silicon production plant.

The bottoms of distillation column 2 are used to feed the intermediate section of a further distillation column 3, which is present in case the electronic grade trichlorosilane has to be used for the deposition of epitaxial layers. In fact, TCS EG suitable to produce silicon polycrystal contains a certain percentage of dichlorosilane (DCS) that must be removed if the TCS EG is used for the deposition of epitaxial layers.

The distillation column 3 is also a packed column, with a condenser 9 at the top and a reboiler 10 at the bottom, in which trichlorosilane and/or dichlorosilane free silicon tetrachloride are obtained as tops and phosphorus chlorides PCl_3 and phosphorus containing compounds, arsenic chlorides $AsCl_3$ and arsenic containing compounds, aluminium compounds, antimony compounds and in general all the present metals and metalloids and carbon-silanes compounds are obtained as bottoms.

EXAMPLE

In the following the features of the various process parameters of a plant for the purification of trichlorosilane and/or silicon tetrachloride realised according to the present invention are listed.

Table 1 shows the features of TCS TG fed to the complexation and distillation column 1.

Table 1

Parameter	Range	Notes
TCS (% by weight)	> 99,7	
DCS (% by weight)	< 0,1	

TET (% by weight) < 0,2
 C-H, Transmittance (Cell path = 10 mm) 3,37 - 3,42 > 75%
 Methylsilanes (total) < 6 ppm By weight
 Boron < 300 ppb By weight
 5 Phosphorus < 5 ppb By weight
 Arsenic < 5 ppb By weight

Table 2 shows the features of TET TG fed to the complexation and distillation column 1.

Table 2

10	Parameter	Range	Notes
	TCS (mg/kg)	≤ 500	
	SiOH (RC)	≤ 0,30	
	-CH (RC)	≤ 0,30	
	Fe, Co, Ni (mg/kg)	≤ 0,10	
15	Cr, Mn, Cu (mg/kg)	≤ 0,10	
	Titanium (mg/kg)	≤ 0,01	
	Metals total (mg/kg)	≤ 0,30	
	Aluminium (mg/kg)	≤ 0,10	
	Boron (mg/kg)	≤ 0,50	
20	Sodium (mg/kg)	≤ 0,50	
	Calcium (mg/kg)	≤ 0,20	
	Methyltrichlorosilane (mg/kg)	≤ 0,50	

In the following the standard and preferred values are reported for a series of operative parameters (with reference to the case of trichlorosilane (TCS) and silicon tetrachloride (TET) purification):

Complexation and distillation column 1 level: above 2500 kg (preferably 6900 kg) for TCS; above 3500 kg (preferably 11500 kg) for TET.

Complexing agent amount: preferably 50 g of TCM and 25 g of DTZ for TCS; 100 g of TCM and 50 g of DTZ for TET.

Column 1 total top reflux functioning phase time: above 3 hours (preferably 3 hours) both for TCS and TET.

Top reflux flow at Total Reflux conditions (during the starting and complexation phase): between 3100 and 3800 kg/h (preferably 3500 kg/h) for TCS; between 3500 and 6000 kg/h (preferably 5000 kg/h) for TET.

Top extraction flow (distillate after complexation time): between 1000 and 2400 kg/h (preferably 1500 kg/h) for TCS; between 1000 and 3000 kg/h (preferably 2000 kg/h) for TET.

5 Column bottom temperature: between 38 and 48°C (preferably 42°C) for TCS; between 65 and 75°C (preferably 69°C) for TET.

Column bottom reboiler thermal fluid temperature: between 58 and 73°C (preferably 60°C) for TCS; between 75 and 83°C (preferably 79°C) for TET.

10 The present invention was described for illustrative, but not limitative purposes, according to its preferred embodiments, but it is to be understood that changes and/or modifications can be made by those skilled in the art without for this departing from the related scope of protection, as defined by the enclosed claims.

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CLAIMS

5 1. A process for the purification of trichlorosilane and/or silicon tetrachloride comprising the following steps of treating technical grade trichlorosilane and/or technical grade silicon tetrachloride:

- complexation of the boron impurities (trichloride BCl_3) and other metallic impurities by addition of diphenylthiocarbazone and/or triphenylchloromethane, with the formation of complex macromolecules
10 having high boiling point,

- first column distillation of the complexation step products, wherein the complexed boron impurities, together with other metallic impurities are removed as bottoms, and

- second column distillation of the tops of the previous
15 distillation, wherein electronic grade trichlorosilane (plus dichlorosilane possibly present) and/or silicon tetrachloride are obtained as tops and phosphorus chlorides PCl_3 and phosphorus containing compounds, arsenic chlorides AsCl_3 and arsenic containing compounds, aluminium compounds, antimony compounds and in general all the present metals
20 and metalloids compounds and carbo-silanes compounds, having a certain residual amount of trichlorosilane and/or silicon tetrachloride, are obtained as bottoms.

2. Purification process according to claim 1, characterised in that it comprises a further distillation step of the bottoms of said second
25 distillation, through which trichlorosilane and/or dichlorosilane free silicon tetrachloride are obtained as tops and phosphorus chlorides PCl_3 and phosphorus containing components, arsenic chlorides AsCl_3 and arsenic containing compounds, aluminium compounds, antimony compounds and in general all the metals and metalloids and carbo-silanes compounds
30 which are present are obtained as bottoms.

3. Purification process according to any of the previous claims, characterised in that said complexation step takes place by adding an excess amount, with respect to the stoichiometric amount, of one or both diphenylthiocarbazone and/or triphenylchloromethane.

35 4. Purification process according to any of the previous claims, characterised in that said complexation step takes place by adding

diphenylthiocarbazone in an amount that is twice the amount of triphenylchloromethane.

5 5. Purification process according to any of the previous claims, characterised in that the bottom temperature in said first distillation step is comprised between 38 and 48°C for the purification of trichlorosilane and between 65 and 75°C for the purification of silicon tetrachloride.

10 6. Purification process according to claim 5, characterised in that the bottom temperature in said first distillation step is 42°C for the purification of trichlorosilane and 69°C for the purification of silicon tetrachloride.

15 7. Purification process according to any of the previous claims, characterised in that said first distillation step is initially operated with a total reflux of the tops, in order to allow the boron and other metals impurities complete complexation.

 8. Purification process according to claim 7, characterised in that said first distillation step is initially operated with a total reflux of the tops for a time period of at least 3 hours.

20 9. Purification process according to any of the previous claims 7-8, characterised in that, after said period of total reflux, the top reflux flow is comprised between 0,3 as a minimum and 2,8 as a maximum as far as TCS is concerned and between 0,17 as a minimum and 5 as a maximum as far as TET is concerned (said values representing the ratio between the flow of condensate tops returned to the top of the column and the flow of extracted tops (distillate)).

25 10. Purification process according to claim 9, characterised in that the top reflux flow in said first distillation step is 1,33 as far as TCS is concerned and 2,5 as far as TET is concerned.

30 11. A plant for the purification of trichlorosilane and/or silicon tetrachloride comprising the following apparatuses for treating technical grade trichlorosilane and/or technical grade silicon tetrachloride:

35 - a column for the complexation and distillation of boron (trichloride BCl₃) impurities and other metallic impurities, working in batch, by adding diphenylthiocarbazone and/or triphenylchloromethane, with the formation of high boiling complex macromolecules, wherein the complexed boron impurities, together with other complexed metallic impurities are removed as bottoms, and

- a column for the distillation of the tops of the previous complexation and distillation column, wherein electronic grade trichlorosilane (and possibly present dichlorosilane) and/or silicon tetrachloride are obtained as tops and phosphorus chlorides PCl_3 and phosphorus containing compounds, arsenic chlorides AsCl_3 and arsenic containing compounds, aluminium compounds, antimony compounds and in general all the metals and metalloid and carbo-silanes compounds that are present, together with a certain residual amount of trichlorosilane and/or silicon tetrachloride, are obtained as bottoms.

12. Purification plant according to claim 11, characterised in that it comprises an intermediate vessel between said complexation and distillation column and said distillation column, wherein the tops of the complexation and distillation column are collected in order to constitute a feed reservoir for the distillation column, during the starting phase of the following operative cycle of the complexation and distillation column.

13. Purification plant according to any of claims 11 and 12, characterised in that it comprises a further distillation column, for the bottoms of said distillation column, wherein trichlorosilane and/or dichlorosilane free silicon tetrachloride are obtained as tops and phosphorus chlorides PCl_3 , phosphorus containing compounds, arsenic chlorides AsCl_3 and arsenic containing compounds, aluminium compounds, antimony compounds and in general all the metals and metalloid and carbo-silanes compounds that are present, together with a certain residual amount of trichlorosilane and/or silicon tetrachloride, are obtained as bottoms.

14. Purification plant according to any of claims 11-13, characterised in that the bottom temperature in said complexation and distillation column is comprised between 38 and 48°C for the purification of trichlorosilane and between 65 and 75°C for the purification of silicon tetrachloride.

15. Purification plant according to claim 14, characterised in that the bottom temperature in said complexation and distillation column is 42°C for the purification of trichlorosilane and 69°C for the purification of silicon tetrachloride.

16. Purification plant according to any of claims 14-15, characterised in that the temperature of the thermal fluid of the column bottom exchanger in said complexation and distillation column is

comprised between 58 and 73°C for the purification of trichlorosilane and between 75 and 83°C for the purification of silicon tetrachloride.

- 5 17. Purification plant according to claim 16, characterised in that in the temperature of the thermal fluid of the column bottom exchanger in said complexation and distillation column is 60°C for the purification of trichlorosilane and 79°C for the purification of silicon tetrachloride.