suitable conveyor belts or discontinuous introduction into open block molds for producing slabstock foams are also customary.

Molded foams can also be produced by the two-component process.

Slabstock foams are usually produced by the multicomponent process. The reaction products are, in the case of slabstock foams, combined in a mixing head and applied directly or via a trough to the open foaming strip.

The temperatures here are preferably in the range from 20 to 25°C.

The starting components are mixed at a temperature of from 15 to 90°C, preferably from 20 to 60°C and in particular from 20 to 35°C, and introduced into the open mold or, if appropriate under superatmospheric pressure, into the closed mold or applied in a continuous workstation to a belt which accommodates the reaction composition. Mixing can be carried out mechanically by means of a stirrer, by means of a stirring screw or by means of high-pressure mixing in a nozzle. The mold temperature is advantageously from 20 to 110°C, preferably from 30 to 60°C and in particular from 35 to 55°C.

The polyurethane foams advantageously have a density of from 10 to 150 kg/m^3, preferably from 40 to 60 kg/m^3 in the case of molded foams and preferably from 14 to 100 kg/m^3 and in particular from 20 to 80 kg/m^3 in the case of slabstock foams. The compressive strengths are then in the range from 1 to 20 kPa, preferably from 1.5 to 12 kPa.

The polyol dispersions of the invention display good flow behavior under high shear stress and are therefore particularly suitable for producing polyurethane foams. As a result, the filtration rate in purification of the polyol dispersion after production is increased or a smaller filter area is required for the same throughputs.

Furthermore, they display a good storage stability and very good processing properties in the further processing to polyurethane end products. In the case of foam shapes having complicated geometries (automobile carpet backing, automobile seats~~, etc.~~), the reaction mixture flows well which leads to a reduction in formation of voids.

Owing to the improved cell opening behavior when the polyol dispersions of the invention are used, the use of cell-opening polyols and other processing aids can be restricted, for example in high-resilience foam formulations, which makes the formulation cheaper, eliminates a possible source of metering errors and improves the