

SPECIFICATION

TITLE OF THE INVENTION

CONTINUOUS POLYMERIZATION APPARATUS AND
PROCESS FOR PRODUCING POLYMER COMPOSITION

5

BACKGROUND OF THE INVENTION

Field of the Invention

The present invention relates to a continuous polymerization apparatus, that is, an apparatus for conducting polymerization, continuously. Further, the present invention also relates to a process for producing a polymer composition conducted by using such continuous polymerization apparatus.

15 Description of Related Art

Resin compositions such as methacrylic ester polymers are produced by continuous polymerization in which a raw material polymer, a polymerization initiator and the like are continuously supplied to a reactor to be polymerized. As such continuous polymerization processes, there are known a continuous solution polymerization process using a solvent (or a dispersion medium, which also applies hereinafter) to conduct continuous polymerization, and a continuous bulk polymerization process using no solvent to conduct continuous polymerization.

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In general, a continuous solution polymerization process is not efficient since use of a solvent causes a low productivity. In contrast, a continuous bulk polymerization process has an advantage of being able to produce a polymer composition efficiently since the polymerization is conducted without using a solvent. Practically, the continuous bulk polymerization, however, has various problems compared with the continuous solution polymerization, such as that reaction control is difficult due to high viscosity of a reaction mixture, and when an inner surface of a reactor is cooled to remove heat from a reaction system, this degrades quality of a polymer composition and thus of a resin composition obtained therefrom. Then, a process is proposed which uses a reactor of a complete mixing type, fully fills the reactor with liquid to exclude a gas phase part therefrom, and conducts continuous bulk polymerization under an adiabatic condition with no heat transfer to or from the outside (JP 07-126308 A). Further, in order to assure such adiabatic condition, a continuous bulk polymerization apparatus is proposed which controls a supply amount of a raw material monomer and a supply amount of a polymerization initiator so as to make a temperature in the reactor equal to a setting temperature of an outer surface of the reactor (JP 2006-104282 A).

SUMMARY OF THE INVENTION

Technical Problem

In recent years, applications of resin compositions
5 such as methacrylic ester polymers has been expanded
furthermore, a demand is increasing for more efficiently
producing a polymer composition which has a variety of
properties. However, it has been proved that the
conventional continuous polymerization apparatuses (JP 07-
10 126308 A and JP 2006-104282 A) are not always sufficient to
meet the demand.

The purpose of the present invention is to provide a
novel continuous polymerization apparatus and to provide a
process for producing a polymer composition, which process
15 is able to be conducted by using such continuous
polymerization apparatus and to more efficiently produce a
polymer composition having a variety of properties.

Solution to Problem

20 The inventors considered using at least two reactors
of a complete mixing type in combination to conduct
continuous polymerization. As to a continuous solution
polymerization process, apparatuses having two stages of
reactors are known, such as that the most part of
25 polymerization is conducted in the former reactor and the

polymerization is completed in the latter reactor while removing a polymerization initiator therefrom (JP 01-172401 A); and that polymerization is conducted to some extent in the former reactor and a solvent is added to the latter reactor to conduct polymerization (JP 05-331212 A). In such apparatuses, however, removal of heat from a reaction system is conducted by reflux cooling (a raw material monomer or the like in the reactor is evaporated to be taken out of the reactor, and it is returned to the reactor again after subjected to cold condensation), this brings about local or rapid cooling of the reaction system, which causes gel to adhere to and grow on the inner surface of the reactor. Especially when the polymerization is conducted under conditions of a small amount of a solvent or a high polymerization ratio to attain an increased productivity, a mixture in the reaction system has an increased viscosity, this tends to cause local or rapid cooling of the reaction system, and the adhering and growing of the gel on the inner surface of the reactor proceeds significantly. Thus, there is a problem such as that gelled substance is immixed into a resultant polymer composition as impurities. Further, as methods for obtaining a polymer composition having a bimodal molecular weight distribution, there are known a melt kneading method by melt blending a polymer of a high molecular weight and a

polymer of a low molecular weight which have been produced separately (JP 2008-538794 A), and a two stage polymerization method in which a polymer is preliminary produced and then a polymer having a molecular weight different therefrom is produced (WO 2007/060891). However, all of these methods merely use a conventional and commonly-used polymerization apparatus. The inventors have considered earnestly on a novel continuous polymerization apparatus which is able to more efficiently produce a polymer composition having a variety of properties, and finally completed the present invention.

The present invention provides the following [1] to [5].

[1] A continuous polymerization apparatus used for continuously polymerizing a methacrylic ester monomer, and comprising at least two reactors of a complete mixing type, characterized in that

each of the reactors is provided with a supply port and an effluent port;

the respective supply ports of the two reactors are independently connected to a supply source of a raw material monomer and a polymerization initiator; and

the respective effluent ports of the two reactors are connected to a common effluent line.

[2] The continuous polymerization apparatus according

to the above [1], wherein the effluent port of each of the reactors is located at a reactor's top.

[3] The continuous polymerization apparatus according to the above [1] or [2], wherein the two reactors are both
5 used to conduct continuous bulk polymerization.

[4] The continuous polymerization apparatus according to any of the above [1] to [3], wherein the two reactors have an inner volume which is different from each other.

[5] A process for producing a polymer composition
10 conducted by using the continuous polymerization apparatus according to any of the above [1] to [4], which comprises

a first polymerization step of supplying a raw material monomer and a polymerization initiator to a first reactor of said two reactors through the supply port of the
15 first reactor from the supply source of the raw material monomer and the polymerization initiator to be subjected to continuous polymerization under an adiabatic condition in the first reactor, and taking a resultant first polymer fraction from the effluent port of the first reactor;

20 a second polymerization step of supplying a raw material monomer and a polymerization initiator fraction to a second reactor of said two reactors through the supply port of the second reactor from the supply source of the raw material monomer and the polymerization initiator to be
25 subjected to continuous polymerization under an adiabatic

condition in the second reactor, and taking a resultant second polymer fraction from the effluent port of the second reactor; and

5 a blending step of blending the first polymer fraction and the second polymer fraction to obtain a polymer composition.

Advantageous Effects of Invention

10 According to the present invention, there is provided a novel continuous polymerization apparatus. Further, according to the present invention, there is also provided a process for producing a polymer composition, which process is able to be conducted by using such continuous polymerization apparatus and to more efficiently produce a
15 polymer composition having a variety of properties.

Brief Description of Drawings

Fig. 1 shows a schematic view of a continuous polymerization apparatus in one embodiment of the present
20 invention.

Following reference signs denote the following elements:

1, 1' ... raw material monomer tank (supply source of raw material monomer)

25 3, 3' ... polymerization initiator tank (supply source

of polymerization initiator and, if necessary, of raw material monomer)

- 5, 5' ... pump
- 7, 7' ... pump
- 5 8, 8' ... line
- 9, 9' ... raw material supply line
- 10 ... first reactor
- 11a ... supply port
- 11b ... effluent port
- 10 11c ... another supply port
- 13 ... jacket (temperature regulating means)
- 14 ... stirrer
- 15 ... effluent line
- 20 ... second reactor
- 15 21a ... supply port
- 21b ... effluent port
- 21c ... another supply port
- 23 ... jacket (temperature regulating means)
- 24 ... stirrer
- 20 25 ... effluent line
- 26 ... mixer
- 27 ... common effluent line
- 31 ... preheater
- 33 ... devolatilizing extruder
- 25 35 ... discharge line

37 ... recovery tank

T ... temperature sensor (temperature detecting means)

DETAILED DESCRIPTION OF THE EMBODIMENTS

5 A continuous polymerization apparatus of the present invention is used for continuously polymerizing a methacrylic ester monomer, and comprises at least two reactors, and continuous polymerization such as any of continuous bulk polymerization and continuous solution
10 polymerization is conducted in each of the reactors. A continuous polymerization apparatus of the present invention will be understood as a continuous bulk polymerization apparatus when continuous bulk polymerization is conducted in all of the reactors, and
15 understood as a continuous solution polymerization apparatus when continuous solution polymerization is conducted in all of the reactors. However, a continuous polymerization apparatus of the present invention is not limited thereto, but may be those wherein continuous bulk
20 polymerization is conducted in one reactor (e.g. a reactor for which polymerization ratio as a target or a guide is low) and continuous solution polymerization is conducted in another reactor (e.g. a reactor for which polymerization ratio as a target or a guide is high).

25 Hereinafter, one embodiment of the present invention

will be described in detail with reference to Fig. 1.

A continuous polymerization apparatus in this embodiment comprises at least the first reactor 10 and the second reactor 20. These reactors 10 and 20 are both a reactor of a complete mixing type, and used to conduct continuous bulk polymerization in this embodiment.

More specifically, the first reactor 10 is provided with a supply port 11a and an effluent port 11b, and preferably further provided with a jacket 13 as a temperature regulating means for regulating a temperature of an outer surface of the reactor and a stirrer 14 for stirring (mixing) a content therein. Similarly, the second reactor 20 is provided with a supply port 21a and an effluent port 21b, and preferably further provided with a jacket 23 surrounding an outer surface of the reactor as a temperature regulating means for regulating a temperature of the outer surface of the reactor and a stirrer 24 for stirring (mixing) a content therein. The effluent ports 11b and 21b are located at a top of each of the reactors in this embodiment, but not limited thereto. On the other hand, the supply ports 11a and 21a may be generally located at an appropriate position of a lower part of each of the reactors, although this embodiment is not limited thereto. Each of these reactors 10 and 20 may be provided with a temperature sensor T as a temperature detecting means for

detecting a temperature in the reactor.

The first reactor 10 and the second reactor 20 may have the same or different inner volume from each other. Making the inner volume of the first reactor and the inner
5 volume of the second reactor different from each other, it is possible to effectively differentiate between the first reactor 10 and the second reactor 20 in an average residence time.

The stirrers 14 and 24 are a member for substantially
10 attaining a complete mixing condition in the reactors. These stirrers may have any appropriate stirring blade(s), for example, may have blades of MIG impeller, MAXBLEND impeller (registered trademark, manufactured by Sumitomo Heavy Industries, Ltd.), paddle impeller, double helical
15 ribbon impeller, FULLZONE impeller (registered trademark, manufactured by Kobelco Eco-Solutions Co., Ltd.) and so on. In order to increase stirring effect in the reactor, it is preferable to provide the reactor with a baffle(s). However, this embodiment is not limited thereto, but may
20 have any appropriate configuration in place of the stirrers 14 and 24 as long as a complete mixing condition can be substantially attained in the reactors.

In general, the reactors 10 and 20 are more preferable when they have a higher stirring efficiency. However, in
25 view of avoiding the reactors from being added with an

unnecessary amount of heat by the stirring operation, it is preferable that a power of stirring is not more than necessary. The power of stirring is not specifically limited, but preferably 0.5 to 20 kW/m³, and more preferably 1 to 15 kW/m³. As a viscosity of the reaction system becomes higher (or a content ratio of a polymer in the reaction system becomes higher), it is preferable to set the power of stirring at a larger level.

As shown in the drawings, the supply port 11a of the first reactor 10 is connected through a raw material supply line 9 to a raw material monomer tank (a supply source of a raw material monomer) 1 and a polymerization initiator tank (a supply source of a polymerization initiator and, if necessary, of a raw material monomer) 3 via pumps 5 and 7, respectively. Similarly, the supply port 21a of the second reactor 20 is connected through a raw material supply line 9' to a raw material monomer tank (a supply source of a raw material monomer) 1' and a polymerization initiator tank (a supply source of a polymerization initiator and, if necessary, of a raw material monomer) 3' via pumps 5' and 7', respectively. In this embodiment, the supply source of the raw material monomer and the polymerization initiator with respect to the first reactor 10 is the raw material monomer tank 1 and the polymerization initiator tank 3, and the supply source of the raw material monomer and the

polymerization initiator with respect to the second reactor 20 is the raw material monomer tank 1' and the polymerization initiator tank 3'. The effluent port 11b of the first reactor 10 and the effluent port 21b of the second reactor 20 are connected to a common effluent line 27 through effluent lines 15 and 25, respectively, and via a mixer 26 in the embodiment shown in the drawings. Thus, the first reactor 10 and the second reactor 20 are connected in parallel. There is preferably no pump on the effluent line 15 lying downstream of the effluent port 11b of the first reactor 10, and the effluent line 25 lying downstream of the effluent port 21b of the second reactor 20, and the common effluent line 27.

It is not necessary for this embodiment, but the first reactor 10 may be connected to the polymerization initiator tank 3, separately from the raw material supply line 9. For example, as shown by a dotted line in Fig. 1, an additional line 8 may be located, and the first reactor 10 may be provided with another supply port 11c, so that this supply port 11c is connected to the polymerization initiator tank 3 via the pump 7 through the line 8 as shown in the drawings. Also, the second reactor 20 may be connected to the polymerization initiator tank 3', separately from the raw material supply line 9'. For example, as shown by a dotted line in Fig. 1, an additional

line 8' may be located, and the second reactor 20 may be provided with another supply port 21c, so that this supply port 21c is connected to the polymerization initiator tank 3' via the pump 7' through the line 8' as shown in the drawings. These modifications can be applied alone or in combination to this embodiment.

In this embodiment, the supply source of the raw material monomer and the polymerization initiator connected to the first reactor 10 (the raw material monomer tank 1 and the polymerization initiator tank 3) and the supply source of the raw material monomer and the polymerization initiator connected to the second reactor 20 (the raw material monomer tank 1' and the polymerization initiator tank 3') are shown as different ones in the drawings.

However, the present invention is not limited thereto, a common supply source of the raw material monomer and the polymerization initiator (a raw material monomer tank and a polymerization initiator tank) can be used as long as the first reactor 10 and the second reactor 20 are connected to the supply source of the raw material monomer and the polymerization initiator, independently from each other (in other words, each supply amount is adjustable for each of the reactors, singularly). As to the supply source of the raw material monomer and the polymerization initiator, the number of the supply source of the raw material monomer and

the polymerization initiator, the forms of the raw material monomer and the polymerization initiator (in a case of a mixture, for example, a composition thereof) and so on are not particularly limited as long as the raw material monomer and the polymerization initiator can be separately
5 supplied to the first reactor 10 and the second reactor 20, appropriately.

The pumps 5, 5' and 7, 7' are not particularly limited, but preferably pumps being able to set flow rates from the
10 raw material monomer tanks 1, 1' and the polymerization initiator tanks 3, 3' at constant values. More specifically, multiple reciprocating pumps are preferred, and more preferred are pulsation-free controlled-volume pumps such as a duplicate pulsation-free controlled-volume
15 pump and a triplex pulsation-free controlled-volume pump. By using these, it is possible to control supply amounts (or supply flow rates, which also applies hereinafter) of the raw material monomer and the polymerization initiator to the first reactor 10 and the second reactor 20.

20 It is preferable that each of the members described in the above with reference to Fig. 1 is appropriately connected to a control unit (not shown in the drawings) so as to enable the control unit to control their operations. Thereby, in order to make the temperature of the outer
25 surface of the reactor set for each of the jackets

(temperature regulating means) 13 and 23 correspond to the temperature in the reactor detected by the temperature sensor (temperature detecting means) T with respect to each of the first reactor 10 and the second reactor 20, the apparatus is controllable by adjusting the respective supply amounts of the raw material monomer and the polymerization initiator to the first reactor 10 and the second reactor 20 with the operation of the pumps 5, 5' and 7, 7' or by regulating the temperature of the outer surface of the reactor set for the jackets 13 and 23.

The jackets 13 and 23 surround almost the whole of the reactors 10 and 20, respectively to appropriately heat or retain the heat of the reactors 10 and 20 by introducing steam, hot water, organic heat medium or the like from a heat medium supply route (not shown in the drawings). The temperature of the jackets 13 and 23 is able to be appropriately regulated with a temperature or pressure of the heat medium to be introduced. The heat medium introduced into the jackets 13 and 23 is removed from a heat medium discharge route (not shown in the drawings). The temperature and/or pressure of the jackets 13 and 23 is detected by a sensor such as a temperature sensor (not shown in the drawings) located on the heat medium discharge route. The point of location of a sensor such as the temperature sensor is not particularly limited, but it may

be located, for example, on the heat medium supply route, or in the jackets 13 and 23.

For the polymerization reaction in the reactors 10 and 20, it is required to proceed at a generally constant temperature in each of the reactors 10 and 20 in view of
5 obtaining a polymer with a constant quality. Therefore, the above described temperature regulating means (jackets 13 and 23) is controlled at a constant temperature which has been set beforehand, so that the temperature inside the
10 reactors 10 and 20 can be maintained respectively at a generally constant temperature.

The setting temperature of the above described temperature regulating means (jackets 13 and 23) is transmitted to a supply flow rate control means, which
15 hereinafter described, to be used as data for determining whether control of the supply flow rate with the monomer supply means (pumps 5, 5') and/or the initiator supply means (pumps 7, 7') is necessary or not. The setting
20 temperature of the above described temperature regulating means (jackets 13 and 23) can be regulated by controlling the temperature or pressure of the above described heat medium.

As to the supply flow rate control means, an example thereof is a control unit (not shown in the drawings)
25 provided with CPU, ROM, RAM and so on.

The ROM of the control unit is a device for storing a program which controls the pumps 5, 5', 7, 7'. The RAM of the control unit is a device for temporary storing data of the temperatures in the reactors 10 and 20 detected by the temperature sensor T, data of the setting temperatures of the jackets 13 and 23 in order to execute the above program.

The CPU of the control unit executes the program stored in the ROM based on data such as the data of the temperatures in the reactors 10 and 20 and the data of the setting temperatures of the jackets 13 and 23 stored in the above RAM so that the supply flow rates of the raw material monomer and/or the polymerization initiator to the reactors 10 and 20 is controlled by the monomer supply means (pumps 5, 5') and/or the initiator supply means (pumps 7, 7').

An example of the control by the supply flow rate control means (control unit) will be described below.

When the temperature in the reactor 10 detected by the temperature sensor T exceeds the setting temperature of the jacket 13 as the temperature regulating means, the CPU executes the program in the ROM to control, for example, the pump 7 so as to decrease the supply flow rate of the polymerization initiator into the reactor 10. When the temperature in the reactor 20 detected by the temperature sensor T exceeds the setting temperature of the jacket 23 as the temperature regulating means, the CPU executes the

program in the ROM to control, for example, the pump 7' so as to decrease the supply flow rate of the polymerization initiator into the reactor 20. By conducting such control, polymerization heat generated in the reactors 10 and/or 20 can be decreased, and thereby the temperatures in the reactors 10 and/or 20 can be lowered.

On the other hand, when the temperature in the reactor 10 is below the setting temperature of the jacket 13, the CPU executes the program in the ROM to control, for example, the pump 7 so as to increase the supply flow rate of the polymerization initiator into the reactor 10. When the temperature in the reactor 20 is below the setting temperature of the jacket 23, the CPU executes the program in the ROM to control, for example, the pump 7' so as to increase the supply flow rate of the polymerization initiator into the reactor 20. By conducting such control, polymerization heat generated in the reactors 10 and/or 20 can be increased, and thereby the temperatures in the reactors 10 and/or 20 can be raised.

For example, when the control over the pumps 7, 7' for the polymerization reaction in the reactors 10 and 20 results in remarkable decrease in the total supply flow rate into the reactors 10 and 20, it is preferable to not only control the pumps 7, 7' so as to decrease the supply flow rate of the polymerization initiator, but also to

control the pumps 5, 5' respectively so as to increase the supply flow rate of the raw material monomer at the same time.

Further, as another example of the control, the following control is noted. That is, when the temperature in the reactor 10 detected by the temperature sensor T exceeds the setting temperature of the jacket 13 as the temperature regulating means, the pump 5 is controlled to increase the supply flow rate of the raw material monomer, so that the relative supply flow rate of the polymerization initiator into the reactor 10 is decreased. When the temperature in the reactor 20 detected by the temperature sensor T exceeds the setting temperature of the jacket 23 as the temperature regulating means, the pump 5' is controlled to increase the flow rate of the raw material monomer, so that the relative flow rate of the polymerization initiator into the reactor 20 is decreased. By conducting such control, the temperature in the reactor 10 and/or 20 can also be lowered.

A ratio of the supply flow rate of the raw material monomer and the supply flow rate of the polymerization initiator can be appropriately set depending on the kind of the polymer generated, the kind of the polymerization initiator used, and so on.

Also, degree of increase or decrease in the supply

flow rate of the raw material monomer and/or the supply
flow rate of the polymerization initiator can be
appropriately set depending on the kind of the polymer
generated, the kind of the polymerization initiator used,
5 and so on. However, in a case what is supplied to the
reactors 10 and 20 by the initiator supply means is not the
polymerization initiator only, but the raw material monomer
comprising the polymerization initiator, it is necessary to
consider a content ratio of the polymerization initiator in
10 the raw material monomer comprising polymerization
initiator to control the supply flow rate of the
polymerization initiator.

The mixer 26 is to evenly mix polymer fractions taken
out through the respective effluent lines 15 and 25, and
15 may be located at a confluent part of the effluent lines 15
and 25 as shown in the drawings or on the common effluent
line 27. Additionally, it is not necessary for this
embodiment, but a preheater 31 and a devolatilizing
extruder 33 may be located downstream of the common
20 effluent line 27. In a case where the preheater 31
presents, in place of the mixer 26 and the preheater 31
shown as a separate apparatuses in the drawings, a combined
apparatus of the mixer 26 and the preheater 31 such as a
static mixer or the like may be used and located at a
25 position of the shown preheater 31 in the drawings. There

may be a pressure adjusting valve (not shown in the drawings) provided between the preheater 31 and the devolatilizing extruder 33. An extruded object after devolatilization is discharged from a discharge line 35.

5 As the preheater 31, any appropriate heater can be used as long as it is able to heat a viscous fluid. As the devolatilizing extruder 33, a single or multi screw devolatilizing extruder can be used.

10 Further, there may be a recovery tank 37 for storing the raw material monomer which is separated and recovered from a volatile component (comprising unreacted raw material, mainly) having separated with the devolatilizing extruder 33.

15 Next, a process for producing a polymer composition conducted by using such apparatus will be described. In this embodiment, a case of conducting continuous polymerization of a methacrylic ester monomer, in the other words, a case of producing a methacrylic ester polymer will
20 be described, although the present invention is not limited thereto.

• Preparation

25 At first, the raw material monomer, the polymerization initiator and so on are prepared.

As the raw material monomer, a methacrylic ester monomer is used in this embodiment.

Examples of the methacrylic ester monomer are

- alkyl methacrylate (of which alkyl group has 1 to 4
5 carbons) alone, or

- a mixture of not less than 80% by weight of alkyl methacrylate (of which alkyl group has 1 to 4 carbons) and not more than 20% by weight of other vinyl monomer copolymerizable therewith.

10 Examples of alkyl methacrylate (of which alkyl group has 1 to 4 carbons) include methyl methacrylate, ethyl methacrylate, n-propyl methacrylate, isopropyl methacrylate, n-butyl methacrylate, t-butyl methacrylate, sec-butyl methacrylate, isobutyl methacrylate, and so on. Among them,
15 methyl methacrylate is preferred. The above described examples of alkyl methacrylate may be used alone or in combination of at least two of them.

 Examples of copolymerizable vinyl monomer include methacrylic esters such as benzyl methacrylate and 2-
20 ethylhexyl methacrylate (except for the above described alkyl methacrylate (of which alkyl group has 1 to 4 carbons)); acrylic esters such as methyl acrylate, ethyl acrylate, propyl acrylate, butyl acrylate, and 2-ethylhexyl acrylate; unsaturated carboxylic acids or acid anhydrides
25 thereof such as acrylic acid, methacrylic acid, maleic acid,

itaconic acid, maleic acid anhydride, and itaconic acid anhydride; hydroxy group-containing monomers such as 2-hydroxyethyl acrylate, 2-hydroxypropyl acrylate, monoglycerol acrylate, 2-hydroxyethyl methacrylate, 2-hydroxypropyl methacrylate, and monoglycerol methacrylate; nitrogen-containing monomers such as acrylamide, methacrylamide, acrylonitrile, methacrylonitrile, diacetoneacrylamide, and dimethylaminoethyl methacrylate; epoxy group-containing monomers such as allyl glycidyl ether, glycidyl acrylate, and glycidyl methacrylate; styrene based monomers such as styrene and α -methylstyrene.

As the polymerization initiator, for example, a radical initiator is used in this embodiment.

Examples of a radical initiator include azo compounds such as azobisisobutyronitrile, azobisdimethylvaleronitrile, azobiscyclohexanenitrile, 1,1'-azobis(1-acetoxy-1-phenylethane), dimethyl 2,2'-azobisisobutylate, and 4,4'-azobis-4-cyanovaleric acid; organic peroxides such as benzoyl peroxide, lauroyl peroxide, acetyl peroxide, caprylyl peroxide, 2,4-dichlorobenzoyl peroxide, isobutyl peroxide, acetyl cyclohexylsulfonyl peroxide, t-butyl peroxy-pivalate, t-butyl peroxyneodecanoate, t-butyl peroxyneohexanoate, t-butyl peroxy-2-ethylhexanoate, 1,1-di(t-butylperoxy)cyclohexane, 1,1-di(t-butylperoxy)-3,3,5-trimethylcyclohexane, 1,1-di(t-hexylperoxy)-3,3,5-

trimethylcyclohexane, isopropyl peroxydicarbonate, isobutyl
 peroxydicarbonate, s-butyl peroxydicarbonate, n-butyl
 peroxydicarbonate, 2-ethylhexyl peroxydicarbonate, bis(4-t-
 butylcyclohexyl) peroxydicarbonate, t-amyl peroxy-2-
 5 ethylhexanoate, 1,1,3,3-tetramethyl butyl peroxy-
 ethylhexanoate, 1,1,2-trimethyl propyl peroxy-2-
 ethylhexanoate, t-butyl peroxy isopropyl monocarbonate, t-
 amyl peroxy isopropyl monocarbonate, t-butyl peroxy-2-
 ethylhexyl carbonate, t-butyl peroxy allyl carbonate, t-
 10 butyl peroxy isopropyl carbonate, 1,1,3,3-tetramethyl butyl
 peroxy isopropyl monocarbonate, 1,1,2-trimethyl propyl
 peroxy isopropyl monocarbonate, 1,1,3,3-tetramethyl butyl
 peroxy isononate, 1,1,2-trimethyl propyl peroxy-isononate,
 and t-butyl peroxybenzoate.

15 These polymerization initiators may be used alone or
 in combination of at least two of them.

The polymerization initiator is selected according to
 the kinds of the polymer generated and the raw material
 monomer used. For example, while the present invention is
 20 not particularly limited, those of radical polymerization
 initiator having a half-life not more than one minute at
 the polymerization temperature are preferable. When the
 half-life at the polymerization temperature is at most one
 minute, the reaction rate is suitable, thus the initiator
 25 is suitable for the polymerization reaction in the

continuous polymerization apparatus.

The supply amount of the polymerization initiator (radical initiator) is not particularly limited, but generally 0.001 to 1% by weight with respect to the raw material monomer (the raw material monomer eventually supplied to each of the reactors 10 and 20). The ratio of the polymerization initiator to the raw material monomer may be different between the first reactor 10 and the second reactor 20.

In addition to the raw material monomer and the polymerization initiator described above, any appropriate other component(s), for example, a chain transfer agent, a rubbery polymer such as butadiene and styrene-butadiene rubber (SBR), and so on may be used. The chain transfer agent is used for adjusting a molecular weight of the polymer generated.

As to the chain transfer agent, either monofunctional or polyfunctional chain transfer agent can be used. More specifically, examples thereof include alkyl mercaptans such as n-propyl mercaptan, isopropyl mercaptan, n-butyl mercaptan, t-butyl mercaptan, n-hexyl mercaptan, n-octyl mercaptan, 2-ethylhexyl mercaptan, n-dodecyl mercaptan, and t-dodecyl mercaptan; aromatic mercaptans such as phenyl mercaptan and thiocresol; mercaptans having 18 or less carbons such as ethylene thioglycol; polyalcohols such as

ethylene glycol, neopentyl glycol, trimethylolpropane, pentaerythritol, dipentaerythritol, tripentaerythritol, and sorbitol; those of which hydroxyl group is esterified with thioglycolic acid or 3-mercaptopropionic acid, 1,4-dihydronaphthalene, 1,4,5,8-tetrahydronaphthalene, β -terpinene, terpinolene, 1,4-cyclohexadiene, hydrogen sulfide and so on. These may be used alone or in combination of at least two of them.

The supply amount of the chain transfer agent is not particularly limited since it varies depending on the kind of the chain transfer agent used and so on. For example, in a case of using mercaptans, it is preferably 0.01 to 3% by weight, and more preferably 0.05 to 1% by weight with respect to the raw material monomer (the raw material monomer eventually supplied to each of the reactors 10 and 20). The ratio of the chain transfer agent to the raw material monomer may be different between the first reactor 10 and the second reactor 20.

In the raw material monomer tanks 1, 1', the raw material monomer (one kind or a mixture of two or more kinds) as described above is appropriately prepared (together with other component(s) such as the chain transfer agent as the case may be). In the polymerization initiator tanks 3, 3', the polymerization initiator as described above is appropriately prepared with the raw

material monomer if necessary (together with other component(s) such as the chain transfer agent as the case may be). The polymerization initiator tanks 3, 3' may store the polymerization initiator alone or in the form of the mixture of the raw material monomer and the polymerization initiator (may further comprising other component(s) such as the chain transfer agent as the case may be).

The composition of the raw material monomer in the raw material monomer tank 1 and the composition of the raw material monomer in the raw material monomer tank 1' may be the same or different from each other. The composition of the polymerization initiator in the polymerization initiator tank 3 and the composition of the polymerization initiator in the polymerization initiator tank 3' may be the same or different from each other. In an example shown in the drawings, the raw material monomer tank 1 and the polymerization initiator tank 3 are used for the first reactor 10, and the raw material monomer tank 1' and the polymerization initiator tank 3' which are different from them are used for the second reactor 20. However, when the composition of the raw material monomer in the raw material monomer tank 1 is the same as the composition of the raw material monomer in the raw material monomer tank 1', the raw monomer tanks 1 and 1' may be a common raw material

monomer tank. When the composition of the polymerization initiator in the polymerization initiator tank 3 is the same as the composition of the polymerization initiator in the polymerization initiator tank 3', the polymerization initiator tanks 3 and 3' may be a common polymerization initiator.

- First polymerization Step

The raw material monomer and the polymerization initiator are supplied to the first reactor 10 through the supply port 11a from the raw material monomer tank 1 and the polymerization initiator tank 3 as the supply source of the raw material monomer and the polymerization initiator. More specifically, the raw material monomer is supplied from the raw material monomer tank 1 by the pump 5, and the polymerization initiator (preferably, the mixture of the raw material monomer and the polymerization initiator, which is also simply referred to as the polymerization initiator herein) is supplied from the polymerization initiator tank 3 by the pump 7, and they merge together through the raw material supply line 9 into the first reactor 10 via the supply port 11a.

For supplying the polymerization initiator to the first reactor 10, when the mixture of the raw material monomer and the polymerization initiator is prepared in the

polymerization initiator tank 3 and supplied therefrom, it is preferable to adjust a ratio A : B in a range from 80:20 to 98:2 wherein A represents the supply flow rate (kg/h) of the raw material monomer from the raw material monomer tank 1, and B represents the supply flow rate (kg/h) of the mixture of the raw material monomer and the polymerization initiator (of which content ratio of the polymerization initiator is 0.002 to 10% by weight) from the polymerization initiator tank 3.

The temperature of the raw material monomer and the polymerization initiator supplied to the first reactor 10 is not particularly limited. However, this is one of factors which may change the polymerization temperature by losing a heat balance in the reactor, and therefore it is preferable to adjust that temperature appropriately by a heater/cooler (not shown in the drawings) before the supply to the first reactor 10.

The raw material monomer and the polymerization initiator supplied to the first reactor 10 as described in the above are subjected to continuous polymerization, continuous bulk polymerization in this embodiment (in other words, polymerization with no solvent), under an adiabatic condition (condition with substantially no heat transfer to or from outside of the reactor) in the first reactor 10.

This first polymerization step is to subject the raw

material monomer and the polymerization initiator to continuous polymerization and let the polymerization reaction proceed to the desired polymerization rate, and a first polymer fraction (or polymerization syrup) is taken
5 from the effluent port 11b of the first reactor 10.

In the first polymerization step, the continuous polymerization is preferably conducted under a condition in which the reactor is filled with the reaction mixture while substantially no gas phase presents (hereinafter referred
10 to as a fully filled condition). This is especially suitable to the continuous bulk polymerization. The fully filled condition can prevent beforehand the problems such as that gel adheres to and grows on the inner surface of the reactor, and that this gel is immixed into the reaction
15 mixture to degrade quality of a polymer composition obtained in the end. Further, the fully filled condition enables all of the inner volume of the reactor to be used as a reaction space, and thereby a high productivity can be attained.

20 When the effluent port 11b of the first reactor 10 is located at the reactor's top as in this embodiment, the fully filled condition is conveniently realized simply by conducting the supply to and the taking from the first reactor 10, continuously. The locating of the effluent
25 port at the reactor's top is especially preferable for

continuously polymerizing a methacrylic ester monomer.

Further in the first polymerization step, the continuous polymerization is conducted under the adiabatic condition. This is especially suitable to the continuous bulk polymerization. The adiabatic condition can prevent beforehand the problems such as that gel adheres to and grows on the inner surface of the reactor, and that this gel is immixed into the reaction mixture to degrade quality of a polymer composition obtained in the end. Further, the adiabatic condition enables the polymerization reaction to become stable, and self regulating characteristics for suppressing a runaway reaction can be brought about.

The adiabatic condition can be realized by making the temperature of the inside of the first reactor 10 and the temperature of the outer surface thereof generally equal to each other. More specifically, this can be realized, with the use of the above described control unit (not shown in the drawings), by adjusting the supply amounts of the raw material monomer and the polymerization initiator to the first reactor 10 with operating the pumps 5 and 7 such that the temperature of the outer surface of the first reactor 10 set for the jacket (temperature regulating means) 13 and the temperature in the first reactor 10 detected by the temperature sensor (temperature detecting means) T correspond to each other. It is not preferable to set the

temperature of the outer surface of the reactor much higher than the temperature in the reactor since it adds extra amount of heat into the reactor. The smaller the difference between the temperature in the reactor and the temperature of the outer surface of the reactor is, the better it is. More specifically, it is preferable to adjust the temperature difference within the range of $\pm 5^{\circ}\text{C}$.

The heat generated in the first reactor 10 such as polymerization heat and stirring heat is generally carried away on taking the first polymer fraction from the first reactor 10. The amount of the heat carried away by the first polymer fraction is determined by the flow rate and the specific heat of the first polymer fraction, and the temperature of the polymerization reaction.

The temperature of the continuous polymerization in the first polymerization step is understood as the temperature in the first reactor 10 (detected by the temperature sensor T). This temperature changes according to various conditions until it reaches a static state, and is not particularly limited, but for example, about 100 to 180°C.

The pressure of the continuous polymerization in the first polymerization step is understood as the pressure in the first reactor 10. This pressure is a pressure not less

than a vapor pressure of the raw material monomer at the temperature in the reactor to prevent gas of the raw material monomer from generating in the reactor, and is generally about 1.0 to 2.0 MPa in gauge pressure.

5 A time period subjected to the continuous polymerization in the first polymerization step is understood as an average residence time in the first reactor 10. The average residence time can be set according to the productivity of the polymer in the first
10 polymer fraction and so on, and is not particularly limited, but, for example, from 15 minutes to 6 hours. This average residence time can be adjusted by using the pumps 5 and 7 to change the supply amount (supply flow rate) of the raw material monomer or the like to the first reactor 10.
15 However, since the average residence time depends in a large part on the inner volume of the first reactor 10, how the inner volume of the first reactor 10 and the inner volume of the second reactor 20 are designed is important as hereinafter described.

20 As described in the above, the first polymer fraction is taken from the effluent port 11b of the first reactor 10. The obtained first polymer fraction comprises the generated polymer, and may further comprise the unreacted raw material monomer, the unreacted polymerization initiator,
25 decomposed substance of the polymerization initiator, and

so on.

Although this embodiment is not limited thereto, the polymerization rate in the first polymer fraction is, for example, 5 to 90% by weight, and preferably 30 to 80% by weight. The polymerization rate in the first polymer fraction generally corresponds to the content ratio of the polymer in the first polymer fraction. The higher the polymerization rate, the higher the productivity of the polymer, but also the higher the viscosity of the polymer fraction, resulting in the larger the necessary power for stirring. The lower the polymerization rate, the lower the productivity of the polymer, resulting in the larger the load for recovering the unreacted raw material monomer. Therefore, it is preferable to set an appropriate polymerization rate as a target or a guide for the first polymer fraction.

- Second polymerization Step

The second polymerization step is conducted in parallel to the first polymerization step.

Hereinafter, explanations similar to those for the first polymerization step apply unless otherwise explained.

The raw material monomer and the polymerization initiator are supplied to the second reactor 20 through the supply port 21a from the raw material monomer tank 1' and

the polymerization initiator tank 3' as the supply source of the raw material monomer and the polymerization initiator. More specifically, the raw material monomer is supplied from the raw material monomer tank 1' by the pump 5', and the polymerization initiator is supplied from the polymerization initiator tank 3' by the pump 7', and they merge together through the raw material supply line 9' into the second reactor 20 via the supply port 21a.

For supplying the polymerization initiator to the second reactor 20, when the mixture of the raw material monomer and the polymerization initiator is prepared in the polymerization initiator tank 3' and supplied therefrom, it is preferable to adjust a ratio $A' : B'$ in a range from 80:20 to 98:2 wherein A' represents the supply flow rate (kg/h) of the raw material monomer from the raw material monomer tank 1', and B' represents the supply flow rate (kg/h) of the mixture of the raw material monomer and the polymerization initiator (of which content ratio of the polymerization initiator is 0.002 to 10% by weight) from the polymerization initiator tank 3'.

The temperature of the raw material monomer and the polymerization initiator supplied to the second reactor 20 is not particularly limited. However, this is one of factors which may change the polymerization temperature by losing a heat balance in the reactor, and therefore it is

preferable to adjust that temperature appropriately by a heater/cooler (not shown in the drawings) before the supply to the reactor 20.

5 The raw material monomer and the polymerization initiator supplied to the second reactor 20 as described in the above are subjected to continuous polymerization, continuous bulk polymerization in this embodiment, under an adiabatic condition in the second reactor 20. This second polymerization step is to subject the raw material monomer and the polymerization initiator to continuous
10 polymerization and let the polymerization reaction proceed to the desired polymerization rate, and a second polymer fraction (or polymerization syrup) is taken from the effluent port 21b of the second reactor 20.

15 Also in the second polymerization step, the continuous polymerization is preferably conducted under a fully filled condition. This is especially suitable to the continuous bulk polymerization. The fully filled condition can prevent beforehand the problems such as that gel adheres to and grows on the inner surface of the reactor, and that
20 this gel is immixed into the reaction mixture to degrade quality of the polymer composition obtained in the end. Further, the fully filled condition enables all of the inner volume of the reactor to be used as a reaction space, and thereby a high productivity can be attained.
25

When the effluent port 21b of the second reactor 20 is located at the reactor's top as in this embodiment, the fully filled condition is conveniently realized simply by conducting the supply to and the taking from the second reactor 20, continuously. The locating of the effluent port at the reactor's top is especially preferable for continuously polymerizing a methacrylic ester monomer.

Also, further in the second polymerization step, the continuous polymerization is conducted under the adiabatic condition. This is especially suitable to the continuous bulk polymerization. The adiabatic condition can prevent beforehand the problems such as that gel adheres to and grows on the inner surface of the reactor, and that this gel is immixed into the reaction mixture to degrade quality of the polymer composition obtained in the end. Further, the adiabatic condition enables the polymerization reaction to become stable, and self regulating characteristics for suppressing a runaway reaction can be brought about.

The adiabatic condition can be realized by making the temperature of the inside of the second reactor 20 and the temperature of the outer surface thereof generally equal to each other. More specifically, this can be realized, with the use of the above described control unit (not shown in the drawings), by adjusting the supply amounts of the raw material monomer and the polymerization initiator to the

second reactor 20 with operating the pumps 5' and 7' such that the temperature of the outer surface of the second reactor 20 set for the jacket (temperature regulating means) 23 and the temperature in the second reactor 20
5 detected by the temperature sensor (temperature detecting means) T correspond to each other. It is not preferable to set the temperature of the outer surface of the reactor much higher than the temperature in the reactor since it adds extra amount of heat into the reactor. The smaller
10 the difference between the temperature in the reactor and the temperature of the outer surface of the reactor is, the better it is. More specifically, it is preferable to adjust the temperature difference within the range of $\pm 5^{\circ}\text{C}$.

15 The heat generated in the second reactor 20 such as polymerization heat and stirring heat is generally carried away on taking the second polymer fraction from the second reactor 20. The amount of the heat carried away by the second polymer fraction is determined by the flow rate and
20 the specific heat of the second polymer fraction, and the temperature of the polymerization reaction.

The temperature of the continuous polymerization in the second polymerization step is understood as the temperature in the second reactor 20. This temperature is,
25 for example, about 100 to 200°C. The temperature in the

second polymerization step may be equal to the temperature in the first polymerization step, but preferably different from it.

5 The pressure of the continuous polymerization in the second polymerization step is understood as the pressure in the second reactor 20. This pressure is generally about 1.0 to 2.0 MPa in gauge pressure, and may be equal to the pressure in the first polymerization step.

10 A time period subjected to the continuous polymerization in the second polymerization step is understood as an average residence time in the second reactor 20. The average residence time can be set according to the productivity of the polymer in the second polymer fraction and so on, and is not particularly limited,
15 but, for example, from 15 minutes to 6 hours. The average residence time in the second polymerization step may be equal to the average residence time in the first polymerization step, but preferably different from it. The average residence time in the second polymerization step
20 can be adjusted by using the pumps 5' and 7' to change the supply amount (supply flow rate) of the raw material monomer or the like to the second reactor 20. However, since the average residence time depends in a large part on the inner volume of the second reactor 20, how the inner
25 volume of the first reactor 10 and the inner volume of the

second reactor 20 are designed is important as hereinafter described.

As described in the above, the second polymer fraction is taken from the effluent port 21b of the second reactor 20. The obtained second polymer fraction comprises the generated polymer, and may further comprise the unreacted raw material monomer, the unreacted polymerization initiator, decomposed substance of the polymerization initiator, and so on.

Although this embodiment is not limited thereto, the polymerization rate in the second polymer fraction is, for example, 5 to 90% by weight, and preferably 30 to 80% by weight. The polymerization rate in the second polymer fraction generally corresponds to the content ratio of the polymer in the second polymer fraction. The higher the polymerization rate, the higher the productivity of the polymer, but also the higher the viscosity of the polymer fraction, resulting in the larger the necessary power for stirring. The lower the polymerization rate, the lower the productivity of the polymer, resulting in the larger the load for recovering the unreacted raw material monomer. Therefore, it is also preferable to set an appropriate polymerization rate as a target or a guide for the second polymer fraction.

- Blending Step

The first polymer fraction taken out of the first reactor 10 through the effluent line 15 and the second polymer fraction taken out of the second reactor 20 through the effluent line 25 are blended together by the mixer 26 to obtain a polymer composition (polymerization syrup) from the common effluent line 27.

Thus obtained polymer composition has properties which are resulted by combining (summing or compounding) the properties of the first polymer fraction and the properties of the second polymer fraction.

By conducting the continuous polymerization (continuous bulk polymerization) in two lines as in this embodiment, the polymerization reaction conditions, more specifically, the temperature, the time period (average residence time), the amount of the polymerization initiator (a ratio of the polymerization initiator to the raw material monomer) and so on can be set for the first polymerization step and the second polymerization step, independently.

For example, it becomes possible by differentiating between the first reactor and the second reactor in the polymerization reaction conditions, more specifically, the temperature, the time period (average residence time), the amount of the polymerization initiator (a ratio of the

polymerization initiator to the raw material monomer) and so on, to differentiate a molecular weight distribution of the first polymer fraction from a molecular weight distribution of the second polymer fraction, and it becomes possible by blending them to obtain a polymer composition of which molecular weight distribution is controlled. In general, the higher the molecular weight, the higher the mechanical strength and heat resistance, but the lower the molding processability. On the other hand, the lower the molecular weight, the higher the molding processability, but sufficient mechanical strength and heat resistance can not be obtained. Thus, a polymer fraction of a high molecular weight and a polymer fraction of a low molecular weight are obtained as the first polymer fraction and the second polymer fraction described above and mixed (blended) together, so that a polymer composition of a broad or bimodal molecular weight distribution can be obtained. Therefore, a polymer composition having good molding processability (e.g. flowability, injection molding formability, and so on) and high mechanical strength and heat resistance.

According to this embodiment, it is possible to obtain a polymer composition having a bimodal molecular weight distribution, more effectively. In the melt kneading method described in JP 2008-538794 A, for example, a

polymer of a high molecular weight and a polymer of a low molecular weight are separately produced and made in an appropriate form for blending (generally, pellets) beforehand, and they are subjected to melt blending, that is, mixed at a certain ratio and charged into an extruder to be melt kneaded, and then arranged into a certain form (generally, pelletized). In contrast, according to this embodiment, the first polymer fraction and the second polymer fraction respectively obtained in the first reactor and the second reactor are directly mixed together. Therefore, in comparison to the melt kneading method in which polymers once formed are subjected to melt blending followed by being formed again (repelletized), this embodiment can be conducted by less number of steps, and can avoid the possibility of slight coloring by heating and of immixing of a foreign material during the melt kneading, and can continuously obtain the polymer composition of high quality with good productivity. Further, in the two stage polymerization method described in WO 2007/060891, for example, a first stage polymerization is conducted by supplying a certain raw material to a reactor and then a second stage polymerization is conducted by adding a certain raw material to this reactor, and such two stage polymerization method is generally conducted by suspension polymerization. In the suspension polymerization, a

suspension stabilizing agent is usually used, and an aqueous solution of sulfuric acid is sometimes added to dissolve and remove the suspension stabilizing agent after the polymerization. Also in the suspension polymerization, a polymer in the form of beads, which is obtained by dehydration and drying after the polymerization, is to be melt kneaded and pelletized in an extruder. In contrast, according to this embodiment, continuous bulk polymerization is conducted in the first reactor and the second reactor. Therefore, this embodiment can avoid the use of additives such as a suspension stabilizing agent and an aqueous solution of sulfuric acid, and does not require operations such as dehydration and drying, and thus, can avoid the possibility of immixing of a foreign material due to these additives and additional operations, and can continuously obtain the polymer composition of high quality with good productivity.

How the polymerization reaction conditions are set for each of the first polymerization step and the second polymerization step may vary according to the properties and productivity desired, and so on.

- Devolatilization Step

The polymer composition (polymerization syrup) obtained as described in the above may comprise the

unreacted raw material monomer and polymerization initiator and so on, in addition to the generated polymer. Although this embodiment is not limited thereto, such polymer composition is preferably subjected to, for example, devolatilization to separate and recover the raw material monomer.

More specifically, the polymer composition is transferred to the preheater 31 through the common effluent line 27. The polymer composition in the preheater 31 is added with a part or all of an amount of heat necessary to volatilize the volatile component which is mainly composed of the unreacted raw material monomer. Then, the polymer composition is transferred to the devolatilizing extruder 33 via the pressure adjusting valve (not shown in the drawings), and the volatile component is at least partially removed in the devolatilizing extruder, and a residual extruded object is formed into pellets and discharged from the discharge line 35. Thereby, the resin composition comprising a methacrylic ester polymer is produced in the form of the pellets.

As a method for transferring the above polymer composition, a method described in JP 4-48802 B is preferable. As a method of using a devolatilizing extruder, methods described in, for example, JP 3-49925 A, JP 51-29914 B, JP 52-17555 B, JP 1-53682 B, JP 62-89710 A and so

on are preferable.

Further, during or after devolatilization of the polymer composition in the devolatilizing extruder described above, the polymer composition or the extruded
5 object can be added with a lubricating agent such as higher alcohols and higher fatty acid esters, an ultraviolet absorber, a heat stabilizer, a colorant, an antistatic agent and so on, in order to incorporate them into the resin composition, if necessary.

10 The volatile component removed in the devolatilizing extruder 33 consists primarily of the unreacted raw material monomer and includes impurities; e.g. impurities originally contained in the raw material monomer, additives used if necessary, volatile by-product(s) generated in the
15 process of polymerization, oligomer such as dimer and trimer, decomposed substance of the polymerization initiator, and so on. In general, a larger amount of the impurities make the obtained resin composition colored, which is not preferable. Then, the volatile component
20 removed in the devolatilizing extruder 33 (which consists primarily of the unreacted raw material monomer and includes impurities as described above) may be passed through a monomer recovery column (not shown in the drawings), and treated by means of distillation, adsorption
25 and so on in the monomer recovery column to remove the

impurities from the above described volatile component. Thereby, the unreacted raw material monomer can be recovered with high purity, so that it can be suitably reused as the raw material monomer for polymerization. For example, continuous distillation is conducted in the monomer recovery column to recover the unreacted raw material monomer with high purity as a distillate liquid from the top of the monomer recovery column, and it may be transferred and recycled to the raw material monomer tanks 1 and/or 1' after it is reserved in the recovery tank 37 once, or it may be transferred and recycled to the raw material monomer tanks 1 and/or 1' without being reserved in the recovery tank 37. On the other hand, the impurities removed in the monomer recovery column may be disposed as a waste.

In order to prevent the recovered raw material monomer from causing the polymerization reaction in the recovery tank 37 and/or the raw material monomer tanks 1 and/or 1', it is preferable that a polymerization inhibitor exists in the recovery tank 37 or the raw material monomer tanks 1 and/or 1' at a ratio of, for example, 2 to 8 ppm by weight with respect to the raw material monomer, and more preferably, in addition to this, an oxygen concentration in a gas phase in the recovery tank 37 or the raw material monomer tanks 1 and/or 1' is set at 2 to 8% by volume. If

the recovered raw material monomer is wanted to be preserved in the recovery tank 37 for a long time, it is preferable to reserve it at a low temperature of, for example, 0 to 5°C.

5

In this embodiment, the continuous bulk polymerization apparatus wherein the first reactor and the second reactor are both used to conduct the continuous bulk polymerization is described. However, the continuous polymerization apparatus of the present invention is not limited thereto, 10 one or both of the first reactor and the second reactor may be used to conduct continuous solution polymerization. In such embodiment, since a solvent is used for the solution polymerization, the continuous polymerization apparatus is provided, in addition to a similar configuration to the 15 continuous polymerization apparatus described in the above with reference to Fig. 1, with a solvent tank and a supply line and a pump (supply means) associated with the solvent tank to supply the solvent to a certain reactor for conducting the solution polymerization. The solvent tank 20 and the supply line and the pump (supply means) associated with the solvent tank are not particularly limited, those similar to conventionally used ones can be used. The solvent can be supplied to the certain reactor for 25 conducting the solution polymerization after being mixed

with raw material monomer and/or the polymerization initiator, or can be supplied to the certain reactor for conducting the solution polymerization, directly. In the above certain reactor, the polymerization step is conducted
5 similarly (under an adiabatic condition) to the polymerization step described in the above with reference to Fig. 1, except that the solvent is used in the polymerization reaction. As to the solvent, it is appropriately selected according to the raw material
10 monomer of the solution polymerization reaction and so on, and not particularly limited, but examples thereof include toluene, xylene, ethyl benzene, methyl isobutyl ketone, methyl alcohol, ethyl alcohol, octane, decane, cyclohexane, decalin, butyl acetate, pentyl acetate, and so on. A ratio
15 C : D is, for example, 70:30 to 95:5, and preferably 80:20 to 90:10, but not limited thereto, wherein C represents a supply flow rate (kg/h) of the raw material monomer to the certain reactor for conducting the solution polymerization, and D represents a supply flow rate (kg/h) of the solvent
20 to this certain reactor.

The continuous polymerization apparatus and the process for producing the polymer composition of the present invention are hereinbefore described through the
25 embodiment of the present invention in detail. According

to the present invention, there is provided the novel continuous polymerization apparatus, and the use of such continuous polymerization apparatus can conduct the polymerization in at least two lines in parallel by using at least the first reactor and the second reactor, so that the polymerization reaction conditions, more specifically, the temperature, the time period (average residence time), the amount of the polymerization initiator (a ratio of the polymerization initiator to the raw material monomer) and so on can be set for the first polymerization step and the second polymerization step, independently. Thereby, it becomes possible to control a molecular weight distribution of the polymer contained in the resin composition obtained in the end, and to produce more efficiently the polymer composition which is suitable for obtaining the resin composition having a variety of properties, more specifically, good molding processability, high mechanical strength, high heat resistance, and so on.

However, the present invention is not limited to the above embodiment, and various modifications can be made. For example, three or more reactors can be used to conduct the polymerization in three or more lines in parallel. For example, the effluent port may be located on the reactor at other position than the reactor's top.

Industrial Applicability

The present invention can be used for producing a polymer composition which is suitable for obtaining a resin composition comprising a methacrylic ester polymer(s).

5

The present application claims priority to Japanese Patent Application No. 2011-14346 filed on January 26, 2011, entitled "CONTINUOUS POLYMERIZATION APPARATUS AND PROCESS FOR PRODUCING POLYMER COMPOSITION." The contents of that application are incorporated herein by the reference thereto in their entirety.

10

WHAT IS CLAIMED IS:

1. A continuous polymerization apparatus used for continuously polymerizing a methacrylic ester monomer, and comprising at least two reactors of a complete mixing type, characterized in that

each of the reactors is provided with a supply port and an effluent port;

the respective supply ports of the two reactors are independently connected to a supply source of a raw material monomer and a polymerization initiator; and

the respective effluent ports of the two reactors are connected to a common effluent line.

2. The continuous polymerization apparatus according to claim 1, wherein the effluent port of each of the reactors is located at a reactor's top.

3. The continuous polymerization apparatus according to claim 1 or 2, wherein the two reactors are both used to conduct continuous bulk polymerization.

4. The continuous polymerization apparatus according to any of claims 1 to 3, wherein the two reactors have an inner volume which is different from each other.

5. A process for producing a polymer composition conducted by using the continuous polymerization apparatus according to any of claims 1 to 4, which comprises

5 a first polymerization step of supplying a raw material monomer and a polymerization initiator to a first reactor of said two reactors through the supply port of the first reactor from the supply source of the raw material monomer and the polymerization initiator to be subjected to continuous polymerization under an adiabatic condition in
10 the first reactor, and taking a resultant first polymer fraction from the effluent port of the first reactor;

a second polymerization step of supplying a raw material monomer and a polymerization initiator to a second reactor of said two reactors through the supply port of the
15 second reactor from the supply source of the raw material monomer and the polymerization initiator to be subjected to continuous polymerization under an adiabatic condition in the second reactor, and taking a resultant second polymer fraction from the effluent port of the second reactor; and

20 a blending step of blending the first polymer fraction and the second polymer fraction to obtain a polymer composition.