

METHOD AND PLANT FOR PROCESSING WATER BY BALLASTED
FLOCCULATION AND DEPOSITION

This invention relates to the field of water treatment.

Water treatment, primarily the potabilisation of water and the treatment of urban or industrial wastewater to be depolluted, frequently uses a process consisting of coagulating the water filled with impurities to be treated with a coagulant often constituted by a trivalent metal salt, flocculating the coagulated water with a flocculating reagent usually constituted by an organic polymer, and settling the floc formed in a settling tank, the sludge being partially extracted from the bottom portion of the settling tank, and the treated water being extracted from the top portion of the settling tank.

Such a technique makes it possible to remove the dissolved or suspended colloidal impurities constituted by organic matter, micropollutants and microorganisms, in particular, from the treated water.

The invention more specifically relates to technology referred to as flocculation-settling with

ballasted floc, which implements a ballast constituted by a fine and dense granular material such as microsand, for example, injected into the flocculation zone, in order to increase the speed of floc formation, serving
5 as a flocculation initiator, and also to increase, by increasing the density, the rate of settling of the floc formed during the flocculation phase, which makes it possible to reduce the size of the structures.

In practice, the coagulated water is placed in
10 contact in a reactor with a flocculating reagent, such as a polymer, and a ballast, and closely mixed therewith by agitation means. The time of contact between the water with the flocculant and the ballast must be sufficient to allow for the formation and
15 increase in size of the floc constituted by the aggregated impurities by means of the flocculant around the ballast.

Microsand, with a mean diameter of between around 20 and 400 micrometers, and usually 80 and 300
20 micrometers, is the ballast used most often for reasons of availability and cost.

The ballasted flocculation-settling technology is described in particular in the following patents:

- patent application FR-A-2627704, published on 1
25 September 1989;

- patent application FR-A-2719234, published on 3 November 1995.

In this technology, the ballast is usually separate from the sludge extracted from the settling
30 structure so as to be capable of being recycled, by recirculation means, in the process.

During the recycling, a small portion of the ballast goes with the sludge. It is therefore necessary to periodically inject new ballast intended to compensate for the loss of ballast.

5 It is important to control the loss of ballast with the sludge in order to minimise the amount spent on new ballast. In addition, excessive recirculation can cause a deterioration in the quality of the sludge extracted, i.e. it can result in excessively-diluted
10 extracted sludge, corresponding to "water losses".

To minimise these losses, the separation of the ballast from the sludge in order to recycle said ballast in the process is generally performed by hydrocyclone separation of the sludge/ballast mixture.

15 However, the risks of hydrocyclone malfunction increase rapidly beyond a given solids content in the underflow (often around 40 % solid by volume).

Finally, significant ballast losses may take place when the underflow of the hydrocyclone is clogged, and
20 the ballast then goes in overflow.

In an attempt to solve these problems, the prior art, namely patent application WO-A-03053862, published on 3 July 2003, suggests pump extracting the mixture of sludge and ballast from the bottom portion of the
25 settling tank and routing it to an agitated intermediate mixing zone, extracting the mixture of sludge and ballast present in said intermediate mixing zone and subjecting it to a step of sludge/ballast separation by hydrocyclone separation, and
30 recirculating a portion of the sludge by adjusting the rate of said recirculation.

However, the implementation of this technique quickly leads to a deterioration in the quality of the treated water, if it is desirable to implement the step of separation of the ballast and the sludge under
5 conditions leading to the recycling, in the flocculation zone, of the cleanest possible ballast. Indeed, the influx of additional solids tends to pollute the quality of the treated water.

In any case, this process described in WO-A-
10 03053862, as well as those described in FR-A-2627704 and FR-A-2719234 do not make it possible to optimise the amounts of ballast to be implemented according to the load of material to be flocculated from the water to be treated. This optimisation would make it possible
15 simultaneously to:

- perform the flocculation of impurities to be removed,
- minimise the ballast losses,
- reduce the water losses,
- 20 obtain high-quality treated water,
- without considerably increasing the energy needed for the formation of floc and for the recirculation of sludge.

The objective of this invention is to provide a
25 technique making it possible to approach or to achieve such an optimisation.

This objective is achieved by the invention, which relates to a process for treating water filled with dissolved or suspended colloidal impurities, in a
30 treatment plant, including steps consisting of:

- 5 - contacting, in a flocculation zone, said water, at least one ballast constituted by at least one insoluble granular material that is heavier than water, and at least one flocculating reagent so as to enable the floc to form;
- introducing the mixture of water and floc thus formed into a settling zone;
- 10 - separating the water treated in the top portion of said settling zone from a sludge and ballast mixture in the bottom portion of said settling zone and routing it to an agitated intermediate mixing zone;
- 15 - extracting the mixture of sludge and ballast present in said intermediate mixing zone and subject it to a step of sludge/ballast separation by hydrocyclone separation,
- recycling the underflow of the hydrocyclone separation step in said flocculation zone;
- 20 - extracting a portion of the sludge coming from the overflow of the hydrocyclone separation step and recirculating the other part of said sludge in said agitated intermediate mixing zone;
- 25 characterised in that it includes:
 - a step consisting of continuously measuring at least one parameter representing the concentration of impurities in the water before or when it enters said flocculation zone;
 - 30 - a step consisting of using the results of said measurement thus performed so as to

continuously deduce the amount of ballast that needs to be implemented to obtain treated water of a predetermined quality.

Such a process makes it possible to know, at any
5 time, the amount of ballast needed according to the pollutant load to obtain the flocculation of the entire pollutant load while minimising the losses of ballast.

The process according to the invention preferably includes:

- 10 - a step consisting of continuously measuring the ballast concentration in the mixture extracted from said settling zone or in the mixture present in said flocculation zone;
- a step consisting of deducing, from the
15 continuous measurement of the concentration of mixture extracted from said settling zone, the concentration of ballast actually present in said plant;
- a step consisting of refilling the
20 flocculation zone with ballast when said concentration of ballast actually present in said plant is lower than a predetermined threshold.

According to an advantageous alternative, said
25 step consisting of refilling the flocculation zone with ballast when said amount of ballast actually present in said plant is lower than a predetermined threshold is performed automatically.

The process also advantageously includes a step
30 consisting of using the results of said measurement of said at least one parameter representing the

concentration of impurities in the water so as also to deduce the amount of said flocculating reagent that needs to be dispensed into the flocculation zone in order to obtain treated water having said predetermined
5 quality.

According to an alternative, the process also includes a preliminary step consisting of continuously injecting into said water, before it enters the flocculation zone, at least one coagulating reagent
10 according to a predetermined amount, and, as the case may be, at least one reagent intended to adjust its pH according to a predetermined amount. This step of injecting the coagulating reagent and adjusting the pH is very generally necessary. However, there are
15 occasional cases in which it is not absolutely essential, in particular when the water to be treated contains very little organic matter.

Said parameter representing the concentration of impurities in the water used to implement the proposed
20 process is preferably the concentration (X) of the so-called "overall SS" in the water, with the so-called "overall SS" concentration being calculating by taking into account all or some of the following parameters:

- 25 - the concentration in said water of suspended solids,
- the concentration in said water of organic matter,
- the concentration of microorganisms in the raw water,
- 30 - the concentration of micropollutants in the raw water,

- said predetermined amount of coagulating reagent,

- said predetermined amount of reagent intended to adjust the pH.

5 According to an alternative of the process disclosed, the amount of ballast that needs to be suspended in the flocculation tank in order to obtain treated water of said predetermined quality is determined on the basis of the concentration Y of
10 ballast necessary for said so-called "overall SS" concentration X calculated according to the formula I: $Y = aX^b + c$ (in which a is between 0.4 and 1, b is between 0.3 and 1 and c is between 0 and 2) and on the basis of the approximate volume of water present in
15 said plant.

 The process proposed preferably includes a step also consisting of continuously adjusting the amount of said flocculating reagent dispensed into said flocculation zone according to said concentration of
20 ballast that needs to be implemented in order to obtain treated water of a predetermined quality.

 Said step consisting of extracting the mixture of sludge and ballast from the bottom portion of said settling zone and routing it to an intermediate mixing
25 zone is preferably performed using at least one endless screw. Such an endless screw enables much more regular routing of the mixture of sludge and ballast coming from the bottom portion of the settling tank to the intermediate zone, which the use of a simple pipeline
30 with a pump would not allow.

According to an advantageous alternative, the process also includes a step consisting of adjusting the flow rate of the sludge coming from the overflow of the hydrocyclone separation step, recirculated to said
5 intermediate mixing zone so as to maintain a predetermined level of sludge and ballast in said intermediate mixing zone.

In such a case, the process also preferably includes a step consisting of storing the sludge coming
10 from the overflow of the hydrocyclone separation step in a tank having an overflow pipe, measuring the level of sludge and ballast mixture present in the intermediate mixing zone, and releasing at least some of said tank into said intermediate mixing zone when
15 the measured value is lower than a predetermined threshold.

According to a preferred aspect of the technique disclosed, said step of hydrocyclone separation of the sludge and ballast mixture coming from said settling
20 zone is performed by implementing an injection of additional liquid tangentially to said sludge.

Said additional liquid is injected in an amount corresponding to 5 to 100 % by volume, and typically 5 to 20 % of the volume of the sludge and ballast mixture
25 introduced in the hydrocyclone separation step.

The use of such an additional liquid makes it possible to obtain a cleaner ballast in the hydrocyclone underflow, essentially free of the gangue of impurities surrounding it when it enters the
30 hydrocyclone.

According to an alternative of the process described, said step consisting of contacting, in a flocculation zone, said water, at least one ballast constituted by at least one insoluble granular material
5 heavier than water, and at least one flocculating reagent in order to allow floc to form, includes:

- 10 - a step consisting of defining, in the flocculation zone, by means of a fully immersed flow-guide structure, an internal zone in which, by agitation, a turbulent axial flow is created of the mixture of the water to be treated, the ballast and the flocculant in an axial direction of said flow-guide structure,
- 15 - a step consisting of injecting said flocculating reagent by means of a hydraulic distribution device in said axial flow,
- a step consisting of distributing this flow, by means of a static device opposing the rotation of said flow and arranged at the
20 outlet of this flow-guide structure;
- a step consisting of allowing said mixture to circulate in a peripheral zone surrounding said flow-guide structure, in an opposite direction up to the inlet of said internal zone; and
- 25 - a step consisting of moving said mixture to said settling zone.

The use of agitation means provided in the internal zone defined by the flow-guide structure allows for an intense mixture of the ballast with the
30 flocculant and the suspended solid involved in a good formation of floc in the peripheral zone. The partition

of the flocculation zone into an internal zone and a peripheral zone makes it possible to prevent the mechanical destruction of this floc by the agitation means from which the floc is protected by the flow-guide structure.

The process preferably includes a step consisting of converting the flow leaving said flow-guide structure into an axial flow by means of a flow-distributing static device. This device can be separate from the flow-guide structure, for example attached to the base of the flocculation zone. However, the flow-distributing static device will preferably be provided within the actual flow-guide structure.

The process described makes it possible to provide a contact time between the water to be treated, the flocculating reagent and the ballast in said flocculation zone, from one to several minutes.

Said ballast is preferably microsand with a mean diameter of between around 20 and 400 micrometers.

According to an alternative of the process, a granular material with adsorption properties, such as active carbon powder, or a granular material with ion or molecule exchange properties, such as a resin, is introduced into the flocculation zone or upstream of the flocculation zone so as to allow for a sufficient contact time of said material with the water to be treated.

This material may, where appropriate, constitute said ballast or a second ballast.

The settling step of the process is preferably a lamellar settling step.

The invention also relates to any plant for implementing such a process, including:

- at least one flocculation tank provided with at least one agitator;
- 5 - a pipeline supplying water to be treated in said flocculation tank;
- a settling tank provided with an outlet for the treated water in the bottom part;
- a pipeline connecting the bottom portion of
10 the settling tank to an intermediate tank provided with at least one agitator;
- a pipeline connecting said intermediate tank to a hydrocyclone;
- a pipeline for recirculation of some of the
15 overflow of the hydrocyclone to said intermediate tank;

characterised in that it includes:

at least one first sensor intended to continuously measure at least one parameter representing the
20 concentration of impurities in the water entering said plant;

a calculator making it possible to continuously deduce, from measurements taken by said first sensor, the amount of ballast that must be implemented in order
25 to obtain treated water of a predetermined quality.

Such a plant preferably includes at least one second sensor provided in said flocculation tank or in said intermediate tank or at the level of said pipeline connecting said intermediate tank to said hydrocyclone
30 making it possible to continuously measure the ballast concentration in the mixture passing through one of

them, and in that said calculator makes it possible to continuously deduce, from the measurements taken by said second sensor, the amount of ballast actually present in said plant.

5 Such a plant advantageously includes an automatic ballast-refilling device.

 Said calculator is preferably designed to continuously deduce, from the measurements taken by said first sensor, the amount of flocculating reagent
10 that needs to be implemented in order to obtain treated water of said predetermined quality.

 According to an alternative, the plant also includes an automatic flocculating reagent dispenser connected to said calculator.

15 Said first sensor is preferably a sensor measuring the concentration in the raw water of suspended solids and/or the concentration in the raw water of organic matter such as the concentration of total organic carbon in said water.

20 According to an alternative, the plant includes at least one sensor intended to continuously measure the quality of the water treated by said plant. In other alternatives, this measurement can be performed only from time to time, and manually, as the case may be.

25 Said pipeline supplying water to the flocculation tank is preferably equipped with a static mixer for mixing the water to be treated with a coagulating reagent.

 Said discharge of the treated water from said
30 settling tank advantageously includes at least one spillway or a perforated tube.

Said settling tank is preferably equipped at its inlet with a siphoniform partition.

Also preferably, said settling tank is equipped at its inlet with a splitting structure. The latter
5 advantageously includes at least two plates parallel to one another arranged on each side of a submerged spillway provided between the flocculation tank and the settling tank, and plates arranged parallel to one
10 another between the other plates, overlapping said submerged spillway, said transverse plates constituting, with the other plates, the same number of flow channels between the flocculation tank and the settling tank.

According to an advantageous alternative, said pipeline connecting the bottom portion of the settling
15 tank to said intermediate tank is equipped with an endless screw.

According to another alternative, the plant includes a tank provided with an overflow pipe provided on said pipeline for recirculation of some of the
20 hydrocyclone overflow to said intermediate tank, and preferably a valve provided on said pipeline for recirculation of some of the hydrocyclone overflow to said intermediate tank, said valve being provided downstream of said tank.

25 Also preferably, the plant includes a sensor that senses the level of the sludge and ballast mixture present in said intermediate tank.

According to an alternative, the hydrocyclone used in the plant described has a cylindrical portion
30 provided with at least one tangential supply of the sludge and ballast mixture to be treated and a conical

portion, and, at the outlet of the conical portion, an additional liquid injection chamber having a tangential supply of additional liquid.

According to an alternative, the plant proposed
5 includes at least one dispenser of a material having ion or molecule exchange or adsorption properties in said flocculation tank.

Said settling tank is preferably a lamellar settling tank provided with vertical blades according
10 to one alternative.

According to an advantageous feature, said flocculation tank preferably comprises a flow-guide structure, open at its two ends and arranged at a distance from the base of said tank defining a median
15 zone equipped with said agitator and a peripheral zone and a static device distributing the flow leaving said flow-guide structure. This flow-guide structure is preferably a tube with a circular cross-section arranged vertically at a distance from the base of said
20 flocculation tank.

According to an advantageous alternative, such a static device is integrated in the lower portion of the flow-guide structure, preferably at least 200 mm below the agitator. Said device is advantageously constituted
25 by at least one diametral plate of height H defining at least two compartments. Said compartments formed by said at least one plate preferably have surfaces that are substantially equal, and the theoretical width B of each compartment is chosen so that there is a ratio H/B
30 between the height H of said at least one plate and

said theoretical width B between around 1 and around 2, typically equal to around 1.5.

The invention, as well as the various advantages that it has, can be more easily understood from the following detailed description of two preferred
5 embodiments provided in reference to the figures, in which:

- 10 - figure 1 shows a diagrammatic cross-section view of a first embodiment of a plant according to this invention;
- figure 2 shows an upper perspective view of the flow-distributing device provided at the outlet of the flow-guide tube of the plant shown in figure 1;
- 15 - figure 3 shows a lower partial perspective view of the splitting structure provided on the submerged spillway between the flocculation tank and the settling tank of the plant shown in figure 1;
- 20 - figure 4 shows a cross-section view of the hydrocyclone of this plant;
- figure 5 shows a diagrammatic cross-section view of a second embodiment of a plant according to this invention;
- 25 - figure 6 shows a cross-section view of the flow-guide tube and its integrated flow distributor of the plant shown in figure 5;
- figure 7 shows a cross-section view AA' of said flow distributor;
- 30 - figures 8 and 9 show cross-section views of other embodiments of a flow distributor.

In reference to figure 1, the embodiment example described here has a flocculation tank 1 provided with a mechanical agitator 2. This mechanical agitator 2 includes a rotatably-mounted vertical pin plunging into
5 the tank and equipped with blades at its ends.

The flocculation tank 1 in the preferred embodiment described here has an essentially parallelepiped shape, but can have other shapes, in particular circular, in other embodiments.

10 This flocculation tank 1 is equipped, in its central portion, with a flow-guide structure constituted by a cylindrical flow-guide tube 3 receiving the agitator 2. Said flow-guide tube 3 is provided at a distance from the base of the tank and
15 defines therein an central internal zone 1a, constituted by the hole of the flow-guide tube 3, and a peripheral zone 1b, between the external wall of said flow-guide tube 3 and the lateral walls 1c of the flocculation tank 1.

20 This flocculation tank 1 is also equipped, at the outlet of the flow-guide tube 3, and at a distance therefrom, with a static flow-distributing device 4 attached to its bottom wall 1d.

This static device 4 is shown in perspective in
25 figure 2. As can be seen in the figure, it is constituted by the association of two plates 4a and 4b together forming a cross.

It is noted that in other embodiments, this static device can be provided at the outlet of the flow-guide
30 tube, but integrated therein instead of being provided at a distance therefrom and attached to the base.

The plant described in figure 1 also includes a pipeline 5 supplying water to be treated to the flocculation tank described above, said pipeline 5 joining the lower portion of said tank.

5 This pipeline 5 is equipped with injection means 6, such as an injector, a coagulating reagent, for example, iron chloride, injection means 7, such as an injector, a reactor enabling the pH to be adjusted, for example lime, and a static mixer 8 making it possible to mix
10 the reagents brought to the pipeline by means 6 and means 7 with raw water so as to obtain, at the inlet of the flocculation tank, coagulated water with a predetermined pH.

 The plant described in figure 1 also includes
15 dispensing means 9, such as a dispenser, a granular material constituting a ballast, such as microsand, in the flocculation tank 1, and dispensing means 10, such as a dispenser, and a flocculating reagent, such as, for example, a polymer, in this same flocculation tank.

20 More specifically, the means 10 make it possible to dispense the flocculating reagent inside the flow-guide tube 3 in a portion thereof located below the blades of the agitator 2.

 The plant also includes a lamellar settling tank
25 11, provided downstream of the flocculation tank. In the context of this preferred embodiment, to enhance the compactness of plant, the settling tank has a wall 1c shared with the flocculation tank, said shared wall being equipped with a submerged spillway 16 equipped
30 with a splitting structure 17. The settling tank 11 is equipped with a siphoniform partition 18 forming, with

said submerged spillway 16 and said splitters, a passage 18a between the flocculation tank 1 and the settling tank 11.

5 This passage 18a is described in greater detail in reference to figure 3.

As can be seen in figure 3, the wall 1c shared by the flocculation tank 1 and the settling tank 11 is equipped in its upper portion with a submerged spillway 9. Said submerged spillway 9 is equipped with a
10 splitting structure 17. More specifically, this structure is constituted by two parallel plates 17a arranged on each side of the submerged spillway 16, and parallel plates 17b arranged between the other plates 17a, overlapping the submerged spillway 16. These
15 transverse plates 17b constitute, with plates 17a, the same number of flow channels between the flocculation tank 1 and the settling tank 11. These channels communicate with the passage 18a, which is defined by the siphoniform partition provided in the settling tank
20 11.

In reference to figure 1, the settling tank 11 of the plant is equipped in its lower portion with a rotating device 12 for scraping sludge, and in its upper portion with horizontal blades 13.

25 The prior art indeed proposed tilting the blades of the lamellar settling tanks used in the context of water treatment plants using ballasted floc so as to promote the settling of the floc. However, the inventors have discovered that the feature whereby
30 verticals blades are provided in the settling tank did not adversely affect the settling of the floc and had

the advantage of facilitating the handling of these plates. It is noted, however, that in other embodiments, the settling tank may have tilted blades or be blade-free.

5 The settling tank 11 has, in its bottom portion, a discharge channel 14 for sludge decanted therein, and, in its upper portion, a discharge outlet 15 for the treated water, constituted in this embodiment by a simple spillway. The treated water coming from this
10 spillway is picked up by a pipeline 15a on which a sensor 44 is provided, making it possible to take continuous or periodic measurements of one or more parameters relating to the quality of the treated water. It is noted that in other embodiments of the invention,
15 such measurements relating to the quality of the treated water can be obtained manually.

Still in reference to figure 1, the plant according to this invention also includes a so-called "intermediate tank", equipped with an agitator 20
20 constituted by a rotating pin on which the blades are mounted.

In this embodiment, for reasons of compactness, this intermediate tank 19 is attached to the flocculation tank 1. However, the base of this
25 intermediate tank 19 is at a lower level than that of the flocculation tank 1.

The plant shown in figure 1 also includes a pipeline 21 connecting the channel 14 of the settling tank 11 to the inside of the intermediate tank 19. This
30 pipeline 21 is equipped with an endless screw 22, the rotation of which is controlled by a motor 23.

The plant also includes a pipeline 25 provided with a pump 28 connecting the intermediate tank 19 to a hydrocyclone 26 of which the underflow 27 is provided above the flocculation tank 1.

5 The overflow 29 of the hydrocyclone 26 is connected to a recirculation pipeline 30 joined above the intermediate tank 19. A tank 31 is provided on this recirculation pipeline 30 and equipped with an overflow pipe 32 as well as a discharge pipeline 33 for this
10 overflow pipe. The portion of the pipeline 30 provided downstream of this tank 31 is equipped with a valve 34.

 The intermediate tank 19 is also equipped with a sensor 43 that senses the level of the sludge and ballast mixture present in the tank 19. This sensor 43
15 is connected to the valve 34.

 According to this preferred embodiment, the plant also includes a pipeline supplying service water 35 to the underflow 27 of the hydrocyclone. This pipeline is equipped with means 10a for supplying the flocculating
20 reagent, making it possible to optimise the mixture of the latter with the ballast. The hydrocyclone is shown in greater detail in the cross-section of figure 4.

 In reference to figure 4, the hydrocyclone 26 includes a cylindrical portion 50 provided in its upper
25 portion with a tangential supply of suspension to be treated. This tangential supply is connected to the recirculation pipeline 25.

 The hydrocyclone 26 also includes a conical portion 52 extending from the cylindrical portion 50,
30 and which communicates with a cylindrical chamber 53. The cylindrical chamber 53 has a tangential supply 54

that communicates with the service water supply pipeline 35 mentioned above. The cylindrical chamber 53 communicates with the underflow 27 of the hydrocyclone. The overflow 29 of the hydrocyclone is provided in the upper portion of the cylindrical portion 50.

In reference to figure 1, the plant described includes sensors 40, 40a intended to continuously measure parameters representing the concentration of impurities in the raw water to be treated, entering the flocculation tank 1. These impurities may be of different types and/or in different forms (suspended solids, colloidal matter, dissolved matter, microorganisms, micropollutants, and so on). The parameters measured can be, for example, the concentration of suspended solids in the raw water or the concentration of organic matter in said raw water, measured as the TOC (total organic carbon), or the UV absorbency at 254 nm or the COD (chemical oxygen demand) or the oxygen consumed-permanganate (KmnO_4) or any other measurement making it possible to accurately estimate the OM (in particles or dissolved).

As will be explained below in greater detail, the measurement of these parameters, taken by sensors 40, 40, will be used to deduce the so-called "overall SS" concentration of the water entering the flocculation tank 1.

It is noted that in the embodiment described in figure 1, this sensor 40 is provided upstream of the static mixer 8 provided on the pipeline 5 for supplying water to be treated to the flocculation tank 1. The measurements taken by the sensor 40 are therefore done

on raw water. However, it is also possible to envisage, in other embodiments, taking measurements on the coagulated water, and therefore placing a corresponding sensor downstream of the water coagulation means.

5 The plant described also includes a sensor 41 provided at the level of the pipeline 25 connecting the intermediate tank 19 to the hydrocyclone 26. This sensor 41 makes it possible to continuously measure the ballast concentration (in the context of this
10 embodiment example, microsand) of the mixture of ballast and sludge passing through this pipeline 25. Such a ballast concentration corresponds to the ballast concentration present in the intermediate tank 19 and is proportional to the ballast concentration of the
15 mixture of water, ballast and polymer present in the flocculation tank 1.

It is also noted that in other embodiments, this ballast concentration sensor can be provided either in the intermediate tank 19 or in the flocculation tank 1.

20 The plant also includes a calculator 42 making it possible to collect the measurements taken by sensors 40, 40a and 41.

The operation of the plant described above in reference to figures 1 to 4 is as follows.

25 Raw water to be treated arrives by the pipeline 5. Coagulating reagent (for example, iron chloride) and reagent intended to adjust the pH (for example, lime) are injected in predetermined amounts into this raw water, by means 6 and 7 respectively, and mixed
30 therewith by the static mixer 8 so that the water arriving in the flocculation tank 1 is coagulated and

has an optimised pH according to the type of coagulant chosen.

The coagulated water arriving in the lower portion of the flocculation tank 1 follows an ascending path
5 into the peripheral zone 1b thereof defined by the lateral walls 1b of the flocculation tank 1 and the external wall of the flow-guide tube 3 (as shown in figure 1 by the arrows pointing upward in the flocculation tank 1), before penetrating said flow-
10 guide tube 3 through its upper opening and following a descending movement into the central internal zone 1a defined by the hole of said flow-guide tube 3 (as shown in figure 1 by the arrows pointing downward in the flow-guide tube 3d).

15 It is noted that in other embodiments, the coagulated water may arrive in the upper portion of the flocculation tank, with its flow then following a descending movement into the peripheral zone and an ascending movement into the internal zone.

20 When it descends into the flow-guide tube 3, the coagulated water follows a descending movement with a horizontal radial component due to the movement of the blades of the agitator 2.

As it leaves the flow-guide tube 3 through the
25 lower outlet thereof, the flow reaches the static flow-distributing device 4. This static flow-distributing device 4, by its configuration, makes it possible to strongly attenuate the radial component of the flow coming from the flow-guide tube 3 and to distribute
30 this flow in a substantially even manner in the entire peripheral zone 1b of the flocculation tank 1.

With the dispensing means 9, an amount of ballast, calculated as indicated below, is dispensed into the water present in the flocculation tank 1.

5 With the dispensing means 10, an amount of flocculating reagent, calculated as indicated below, is continuously dispensed inside the flow-guide tube 3 in the same water.

10 With the flow-guide tube 3 and the agitator 2, the mixture of said polymer and the microsand with the water is optimised.

In the flocculation tank 1, floc constituted by ballast is formed, and the impurities contained in the water agglutinate around said floc, owing to the flocculating reagent. The improvement of the mixture of
15 water and ballast and the flocculating reagent makes it possible to optimise the formation of floc as well.

20 With the sensors 40 and 40a, respectively, the suspended solids content and the concentration of organic matter (OM) in the raw water are measured continuously.

The corresponding measurements are sent to the calculator 42, which combines these measurements of the data concerning the predetermined amounts of coagulating reagent and the reagent intended to adjust
25 the pH used and the concentration of microalga in the raw water so as to deduce a concentration of so-called "overall SS" in the of the coagulated water entering the flocculation tank 1, representing the concentration of pollutants to be removed, contained in said water.

The calculator 42 then calculates the amount of flocculating reagent that needs to be implemented in the plant by means 9, according to:

- 5 - the flow rate of the raw water to be treated arriving in the plant through the pipeline 5,
- said so-called "overall SS" concentration in the water arriving in the flocculation tank 1,
- the particle size of the granular material constituting the ballast.

10 The calculator 42 calculates the amount of ballast that needs to be implemented in the plant in order to obtain treated water of a predetermined quality, said amount corresponding to a minimum ballast concentration in the flocculation tank.

15 In the context of this embodiment example, said ballast concentration Y is calculated by the calculator 42 using the formula:

$$Y = 0.4208 \times X^{0.3667}$$

20

in which X corresponds to the "overall SS" concentration.

In other embodiments, other methods for calculating this ballast concentration can be envisaged.

25 After having passed through the flocculation tank 1, the mixture formed by water and floc enters the settling tank 11 by passing over the submerged spillway 16.

30 During this passage, said mixture passes through channels defined by plates 17, 17a of the splitting structure described in reference to figure 3.

This structure makes it possible to obtain, at the outlet of said channels, a flow of the mixture of water and floc that is better distributed over the length of the submerged spillway 16.

5 This mixture then passes through the passage 18a defined by the submerged spillway 16 and the siphoniform partition 18 to arrive in the settling tank 11.

10 In the settling tank 11, the floc formed by matter aggregated around the ballast settles and accumulates on the bottom wall of the settling tank 11 to form a mixture of sludge and ballast. This settling is improved by the presence of blades 13 provided in the upper portion of the settling tank 11.

15 The rotating scraping device 12 makes it possible to direct this mixture of sludge and sand into the channel 14 of the settling tank 11.

20 The treated water free of its impurities is discharged into the upper portion of the settling tank 11 by the discharge outlet 15.

25 The mixture of sludge and ballast present in the channel 14 of the settling tank 11 is extracted from said channel 14 through the pipeline 21 by means of the endless screw 22 provided in the pipeline 21, which endless screw is actuated by the motor 23.

30 This sludge and ballast mixture is routed at a primarily constant speed into the intermediate tank 19. This routing is facilitated by the fact that the base of the tank 19 is provided at a level lower than that of the flocculation tank 1, which enables the pipeline 21 to pass below it.

The sludge and ballast mixture is mixed by agitation means 20 provided in the tank 19, in which it follows an ascending, then descending movement (as indicated by the arrows pointing upward and downward).

5 This sludge and ballast mixture is continuously extracted from the intermediate tank 19 through the pipeline 25 by means of the pump 28 so as to be routed toward the hydrocyclone 26 intended to separate the ballast from the sludge contained in said mixture.

10 This separation is improved by the injection, through the pipeline 25, of service water into the hydrocyclone. This injection of service water makes it possible to obtain, in the underflow 27 of said hydrocyclone 26, a ballast that is essentially free of
15 organic matter. The ballast recovered in the underflow of the hydrocyclone 27 is redistributed in the flocculation tank 1.

 The overflow 29 of the hydrocyclone 26, constituted by diluted sludge, is routed through the
20 pipeline 30 to the tank 31 provided thereon. Said diluted sludge accumulates in said tank 31. A part of said diluted sludge is discharged through a pipeline 33 connected to an overflow pipe 32 provided in said tank, while another part is rerouted by way of the pipeline
25 30 to the intermediate tank 19. However, this recirculation is implemented only when the level of mixture present in the tank 19 and detected by the sensor 43 is lower than a predetermined value. In this case, the valve 34 provided on the pipeline 30 opens to
30 release some of the contents of tank 31 into tank 19 and closes when the sensor 43 detects that the level of

mixture in said tank 19 has reached the predetermined value.

This mechanism makes it possible to maintain an essentially constant ballast concentration in the tank
5 19.

The sensor 41 continuously measures this concentration and transmits it to the calculator 42, which deduces the amount of ballast actually present in the plant.

10 If this amount is lower than or excessively lower than the amount of ballast needed to obtain a predetermined water quality (amount calculated as indicated above from the ballast concentration Y), in other words, if this amount falls below a predetermined
15 value, the calculator 42 commands the dispensing means 9 to automatically fill the plant with an additional amount of ballast so as to obtain said necessary amount.

A second embodiment example is shown in reference to figures 5 to 7.

20 The plant described in figure 5 is completely identical to that shown in figure 1, except that:

- its flocculation tank 1 is equipped with a flow-guide tube 3a including a flow distributor 4a;
- 25 - and in that it includes a dispenser 9a of a second granular material (material having adsorption properties, or ion or molecule exchange properties) in the flocculation tank 1.

In reference to figure 6, the flow distributor
30 included in the tube is positioned more than 200 mm below the agitator 2 and is constituted by the

association of 8 plates 50 together forming a plurality of crosses, defining 25 channels 51 allowing for the passage of the fluid leaving the tube 3.

In reference to figures 8 and 9, this flow distributor can be constituted by a number of plates other than 8, for example 4 (figure 8) or 9 (figure 9).

The ratio between the height H of the plates 50 and their maximum width B is preferably between 1.5 and 2.

CLAIMS

1. Process for treating water filled with dissolved or suspended colloidal impurities, in a treatment plant, including steps consisting of:

- 5 - placing together in a flocculation zone, said water, at least one ballast constituted by at least one insoluble granular material that is heavier than water and at least one flocculating reagent so as to enable the floc to form;
- 10 - introducing the mixture of water and floc thus formed into a settling zone;
- separating the water treated in the top portion of said settling zone from a sludge and ballast mixture resulting from the settling of said
15 floc;
- extracting the mixture of sludge and ballast in the bottom portion of said settling zone and routing it to an agitated intermediate mixing zone;
- 20 - extracting the mixture of sludge and ballast present in said intermediate mixing zone and subjecting it to a step of sludge/ballast separation by hydrocyclone separation;
- recycling the underflow of the hydrocyclone
25 separation step in said flocculation zone;
- extracting a part of the sludge coming from the overflow of the hydrocyclone separation step and recirculating the other part of said sludge in said agitated intermediate mixing zone;

characterised in that it includes:

- a step consisting of continuously measuring at least one parameter representing the concentration of impurities in the water before or when it enters said flocculation zone;
- a step consisting of using the results of said measurement thus performed so as to continuously deduce the amount of ballast that needs to be implemented in order to obtain treated water of a predetermined quality.

2. Process according to claim 1, characterised in that it includes:

- a step consisting of continuously measuring the ballast concentration in the mixture extracted from said settling zone or in the mixture present in said flocculation zone;
- a step consisting of deducing, from the continuous measurement of the concentration of mixture extracted from said settling zone, the concentration of ballast actually present in said plant;
- a step consisting of refilling the flocculation zone with ballast when said concentration of ballast actually present in said plant is lower than a predetermined threshold.

3. Process according to claim 2, characterised in that said step consisting of refilling the flocculation zone with ballast when the amount of ballast actually present in said plant is lower than a predetermined threshold is performed automatically.

4. Process according to any one of claims 1 to 3, characterised in that it includes a step consisting of using the results of said measurement of said at least one parameter representing the concentration of
5 impurities in the water so as also to deduce the amount of said flocculating reagent that needs to be dispensed into the flocculation zone in order to obtain treated water having said predetermined quality.

5. Process according to any one of claims 1 to 4,
10 characterised in that it includes a preliminary step consisting of continuously injecting into said water, before it enters the flocculation zone, at least one coagulating reagent according to a predetermined amount, and, as the case may be, at least one reagent intended
15 to adjust the pH according to a predetermined amount.

6. Process according to any one of claims 1 to 5, characterised in that said parameter representing the concentration of impurities in the water is the concentration (X) of the so-called "overall SS" in the
20 water, said so-called "overall SS" concentration being calculating by taking into account all or some of the following parameters:

- the concentration in said water of suspended solids,
- 25 - the concentration in said water of organic matter,
- the concentration of microorganisms in the raw water,
- the concentration of micropollutants in the raw
30 water,

- said predetermined amount of coagulating reagent,
- said predetermined amount of reagent intended to adjust the pH.

5 7. Process according to claim 6, characterised in that the amount of ballast that needs to be suspended in the flocculation tank in order to obtain treated water of said predetermined quality is determined by: the concentration (Y) of ballast necessary for said so-called "overall SS" concentration (X) calculated
10 according to the formula (I):

$$Y = aX^b + c$$

in which a is between 0.4 and 1, b is between 0.3 and 1 and c is between 0 and 2,

15 and the approximate volume of water present in said plant.

8. Process according to any one of claims 1 to 7, characterised in that it includes a step consisting of continuously adjusting the amount of said
20 flocculating reagent dispensed into said flocculation zone according to said concentration of ballast that needs to be implemented in order to obtain treated water of a predetermined quality.

9. Process according to any one of claims 1
25 to 8, characterised in that said step consisting of extracting the mixture of sludge and ballast from the bottom portion of said settling zone and routing it to an intermediate mixing zone is performed using at least one endless screw.

30 10. Process according to any one of claims 1 to 9, characterised in that it includes a step consisting of

adjusting the flow rate of the sludge coming from the overflow of the hydrocyclone separation step, recirculated to said intermediate mixing zone so as to maintain a predetermined level of sludge and ballast in
5 said intermediate mixing zone.

11. Process according to claim 10, characterised in that it includes a step consisting of storing the sludge coming from the overflow of the hydrocyclone separation step in a tank having an overflow pipe,
10 measuring the level of sludge and ballast mixture present in the intermediate mixing zone, and releasing at least some of said tank into said intermediate mixing zone when the measured value is lower than a predetermined threshold.

12. Process according to any one of claims 1 to 11,
15 characterised in that said step of hydrocyclone separation of the sludge and ballast mixture coming from said settling zone is performed by implementing an injection of additional liquid tangentially to said
20 sludge.

13. Process according to claim 12, characterised in that said additional liquid is injected in an amount corresponding to 5 to 100 % by volume, and typically 5 to 20 % of the volume of the sludge and ballast mixture
25 introduced in the hydrocyclone separation step.

14. Process according to any one of claims 1 to 13, characterised in that said step consisting of contacting, in a flocculation zone, said water, at least one ballast constituted by at least one insoluble
30 granular material heavier than water, and at least one

flocculating reagent in order to allow floc to form, includes:

- 5 - a step consisting of defining, in the flocculation zone, by means of a fully immersed flow-guide structure, an internal zone in which, by agitation, a turbulent axial flow is created of the mixture of the water to be treated, the ballast and the flocculant in an axial direction of said flow-guide structure,
- 10 - a step consisting of injecting said flocculating reagent by means of a hydraulic distribution device in said axial flow,
- a step consisting of distributing this flow, by means of a static device opposing the rotation
15 of said flow and arranged at the outlet of this flow-guide structure;
- a step consisting of allowing said mixture to circulate in a peripheral zone surrounding said flow-guide structure, in an opposite direction
20 up to the inlet of said internal zone; and
- a step consisting of moving said mixture to said settling zone.

15. Process according to claim 14, characterised in that it includes a step consisting of converting the
25 flow leaving said flow-guide structure into an axial flow by means of a flow-distributing static device.

16. Process according to any one of claims 1 to 15, characterised in that said step consisting of converting the flow leaving said flow-guide structure
30 into an axial flow by means of a flow-distributing

static device is performed within the actual flow-guide structure.

17. Process according to any one of claims 1 to 16, characterised in that it consists of providing a
5 contact time between the water to be treated, the flocculating reagent and the ballast in said flocculation zone, from one to several minutes.

18. Process according to any one of claims 1 to 17, characterised in that said ballast is microsand.

10 19. Process according to any one of claims 1 to 18, characterised in that a granular material with adsorption properties, or a granular material with ion or molecule exchange properties, is introduced into the flocculation zone or upstream of the flocculation zone
15 so as to allow for a sufficient contact time of said material with the water to be treated.

20. Process according to claim 19, characterised in that said material with ion or molecule exchange properties is a resin.

20 21. Process according to claim 19, characterised in that said material with adsorption properties is active carbon powder.

22. Process according to one of claims 19 or 20, characterised in that said granular material with
25 adsorption properties, or ion or molecule exchange properties, constitutes said ballast.

23. Process according to one of claims 19 or 20, characterised in that said granular material with adsorption properties, or ion or molecule exchange
30 properties, constitutes a second ballast.

24. Process according to any one of claims 1 to 23, characterised in that said settling step is a lamellar settling step.

25. Plant for implementing a process according to
5 any one of claims 1 to 24, including:

- at least one flocculation tank (1) provided with at least one agitator (2);
- a pipeline (5) supplying water to be treated in said flocculation tank (1);
- 10 - a settling tank (11) provided with a discharge outlet (15) for the treated water in the bottom portion;
- a pipeline (21) connecting the bottom portion of the settling tank to an intermediate tank
15 (19) provided with at least one agitator (20);
- a pipeline (25) connecting said intermediate tank (19) to a hydrocyclone (26);
- a pipeline (30) for recirculation of some of the overflow of the hydrocyclone (26) to said
20 intermediate tank (19);

characterised in that it includes:

at least one first sensor (40, 40a) intended to continuously measure at least one parameter representing the concentration of impurities in the
25 water entering said plant;

a calculator (42) making it possible to continuously deduce, from measurements taken by said first sensor, the amount of ballast that must be implemented in order to obtain treated water of a predetermined quality.

30 26. Plant according to claim 25, characterised in that it includes at least one second

sensor (41) provided in said flocculation tank or in said intermediate tank or at the level of said pipeline (25) connecting said intermediate tank to said hydrocyclone making it possible to continuously measure
5 the ballast concentration in the mixture passing through one of them, and in that said calculator (42) makes it possible to continuously deduce, from the measurements taken by said second sensor (41), the amount of ballast actually present in said plant.

10 27. Plant according to claim 25 or 26, characterised in that it includes an automatic ballast-refilling device (9).

28. Plant according to claim 27, characterised in that said calculator (42) is designed
15 to continuously deduce, from the measurements taken by said first sensor (40, 40a), the amount of flocculating reagent that needs to be implemented in order to obtain treated water of said predetermined quality.

29. Plant according to claim 28,
20 characterised in that said it includes an automatic flocculating reagent dispenser (10) connected to said calculator.

30. Plant according to any one of claims 25 to 29, characterised in that said first sensor (40, 40a)
25 is a sensor measuring the concentration in the raw water of suspended solids and/or the concentration in the raw water of organic matter such as the concentration of total organic carbon in said water.

31. Plant according to any one of claims 25
30 to 30, characterised in that it includes at least one

sensor (44) intended to continuously measure the quality of the water treated by said plant.

32. Plant according to any one of claims 25 to 31, characterised in that said pipeline (5) supplying water
5 to the flocculation tank (1) is equipped with a static mixer (8) for mixing the water to be treated with a coagulating reagent.

33. Plant according to any one of claims 25 to 32, characterised in that said discharge outlet (15) for
10 discharging the treated water from said settling tank includes at least one submerged spillway or a perforated tube.

34. Plant according to any one of claims 25 to 33, characterised in that said settling tank (11) is
15 equipped at its inlet with a siphoniform partition (18).

35. Plant according to one of claim 25 to 34, characterised in that said settling tank (11) is equipped at its inlet with a splitting structure (17).

36. Plant according to claim 35, characterised in
20 that said splitting structure (17) includes at least two plates (17a) parallel to one another arranged on each side of a submerged spillway (16) provided between the flocculation tank (1) and the settling tank (11), and plates (17b) arranged parallel to one another
25 between the plates (17a), overlapping said spillway (16), said transverse plates (17b) constituting, with the plates (17a), the same number of flow channels between the flocculation tank (1) and the settling tank (11).

30 37. Plant according to any one of claims 25 to 36, characterised in that said pipeline (21) connecting the

bottom portion of the settling tank to said intermediate tank is equipped with an endless screw (22).

38. Plant according to any one of claims 25 to 37,
5 characterised in that it includes a tank (31) provided with an overflow pipe (32) provided on said pipeline (30) for recirculation of some of the hydrocyclone (26) overflow to said intermediate tank (19).

39. Plant according to claim 38, characterised in
10 that it includes a valve (34) provided on said pipeline (30) for recirculation of some of the hydrocyclone (26) overflow to said intermediate tank (19), said valve (34) being provided downstream of said tank (31).

40. Plant according to one of claims 38 or 39,
15 characterised in that it includes a sensor (43) that senses the level of the sludge and ballast mixture present in said intermediate tank (19).

41. Plant according to any one of claims 25 to 40,
characterised in that said hydrocyclone (26) has a
20 cylindrical portion (50) provided with at least one tangential supply of the sludge and ballast mixture to be treated and a conical portion (52), and, at the outlet of the conical portion, an additional liquid injection chamber (53) having a tangential supply (54)
25 of additional liquid.

42. Plant according to any one of claims 25 to 41,
characterised in that it includes at least one
dispenser (9a) of a material having ion or molecule
exchange or adsorption properties in said flocculation
30 tank.

43. Plant according to any one of claims 25 to 42, characterised in that said settling tank (11) is a lamellar settling tank.

44. Plant according to claim 43, characterised in
5 that said lamellar settling tank (11) is provided with vertical blades.

45. Plant according to any one of claims 25 to 44, characterised in that said flocculation tank (1) comprises a flow-guide structure, open at its two ends
10 and arranged at a distance from the base of said tank (1) defining a median zone (1a) equipped with said agitator (2) and a peripheral zone (1b) and a static device (4, 4a) distributing the flow leaving said flow-guide structure.

15 46. Plant according to claim 45, characterised in that the flow-guide structure is a tube (3) with a circular cross-section arranged vertically at a distance from the base of said flocculation tank (1).

47. Plant according to one of claims 45 or 46,
20 characterised in that said static device (4a) is included in the lower portion of the flow-guide structure.

48. Plant according to claims 46 and 47, said static flow-distributing device (4a) included in said
25 flow-guide tube (3) is constituted by at least one diametral plate of height H defining at least two compartments.

49. Plant according to one of claims 47 or 48, characterised in that the static flow-distributing
30 device (4a) is provided at least 200 mm below the agitator.

50. Plant according to one of claims 48 or 49, characterised in that said compartments formed by said at least one plate have surfaces that are substantially equal, and in that the theoretical width B of each
5 compartment is chosen so that there is a ratio H/B between the height H of said at least one plate and said theoretical width B between around 1 and around 2, typically equal to around 1.5.