We Claim:

1. A method for producing multiple distillate products from a single mineral oil feedstock, the method comprising:

exposing a distillate fuel boiling range mineral oil feedstock having a boiling point range of about 200ºF to about 680ºF and a sulfur content of less than about 10 wppm and a nitrogen content of less than about 5 wppm to a dewaxing catalyst comprising a molecular sieve, wherein the molecular sieve comprises ZSM-48 with a silica to alumina ratio of 70 to 1 to about 110 to 1, and a Group VIII noble metal hydrogenation component comprising about 0.05 wt % to about 0.35 wt % of a Group VIII noble metal under effective dewaxing conditions to produce a dewaxed effluent having a cloud point that is reduced by at least about 25ºF (14ºC) relative to a feedstock cloud point; and

fractionating the dewaxed effluent to produce at least a diesel fuel product having a cloud point of about -4ºF (-20ºC) or less and a jet fuel product having a lower boiling range than the diesel fuel product and having a freeze point of less than about -40ºF (-40ºC), a fractionation cut point temperature between the diesel fuel product and the jet fuel product having the lower boiling range being at least 500ºF (260ºC).

2. The method of claim 1, wherein the effective dewaxing conditions comprise a pressure of from about 200 psig (1.4 MPa) to about 1500 psig (10.4 MPa), a temperature of from about 321ºC (610ºF) to about 399ºC (750ºF), a hydrogen treat gas rate of about 500 scf/bbl (84 Nm^3/m^3) to about 4000 scf/bbl (674 Nm^3/m^3) or less, and a space velocity of from about 0.3 hr^{-1} to about 4.9 hr^{-1}.

3. The method of claim 1, wherein the metal hydrogenation component comprises Pt, Pd, or a combination thereof.

4. The method of claim 1, wherein the molecular sieve has a silica to alumina ratio of about 90 to 1.

5. The method of claim 1, wherein the feedstock has the sulfur content of less than about 5 wppm or less and the nitrogen content of less than about 1 wppm or less.

6. The method of claim 1, wherein the effective dewaxing conditions produce a dewaxed effluent having a cloud point that is reduced relative to a cloud point of the feedstock by at least about 80ºF (44ºC).

7. The method of claim 1, wherein the effective dewaxing conditions produce a dewaxed effluent having a cloud point that is reduced relative to a cloud point of the feedstock by at least about 100ºF (56ºC).

8. The method of claim 1, wherein the fractionation cut point temperature between the distillate product having the lower boiling range and the diesel fuel product is at least about 545ºF (285ºC).

9. The method of claim 1, wherein a T5 boiling point for the diesel fuel product is at least about 550ºF (288ºC).

10. The method of claim 1, wherein the distillate fuel boiling range feedstock has a T5 boiling point of at least about 280ºF (140ºC).

11. The method of claim 1, wherein the diesel fuel product has a cloud point of about -76ºF (-60ºC) or less.

12. The method of claim 1, further comprising exposing the dewaxed effluent to a hydrofinishing catalyst under effective hydrofinishing conditions, wherein the effective hydrofinishing conditions comprise a pressure of from about 200 psig (1.4 MPa) to about 1500 psig (10.4 MPa), a temperature of from about 500ºF (260ºC) to about 750ºF (399ºC), a hydrogen treat gas rate of about 500 scf/bbl (84 Nm^3/m^3) to about 4000 scf/bbl (674 Nm^3/m^3) or less, and a space velocity of from about 0.3 hr^{-1} to about 5.0 hr^{-1}.

13. A method for producing a diesel fuel product and a jet fuel product from a single mineral oil feedstock, the method comprising:

exposing a distillate fuel boiling range mineral oil feedstock having a boiling point range of about 200ºF to about 680ºF and a sulfur content of less than about 15 wppm and a nitrogen content of less than about 50 wppm to a dewaxing catalyst comprising a 10-member ring 1-D molecular sieve, wherein the molecular sieve comprises ZSM-48 with a silica to alumina ratio of 70 to 1 to about 110 to 1, and a metal hydrogenation component under effective dewaxing conditions to produce a dewaxed effluent,

wherein the effective dewaxing conditions comprise a pressure of from about 200 psig (1.4 MPa) to about 1500 psig (10.4 MPa),

wherein the dewaxing catalyst has an amount of metal hydrogenation component comprising about 0.05 wt % to about 0.35 wt % of a Group VIII noble metal, and

wherein the dewaxed effluent, when fractionated, produces the diesel fuel product and the jet fuel product; and

fractionating the dewaxed effluent to produce at least the diesel fuel product having a cloud point of about 14ºF (-10ºC) or less and the jet fuel product having a lower boiling range than the diesel fuel product and having a freeze point of less than about -40ºF (-40ºC), a fractionation cut point temperature between the diesel fuel product and the jet fuel product having the lower boiling range being at least 500ºF (260ºC).

14. The method of claim 1, wherein the mineral oil feedstock has a boiling point range of about 200ºF to about 650ºF.

15. The method of claim 13, wherein the effective dewaxing conditions comprise a temperature of from about 321ºC (610ºF) to about 399ºC (750ºF), a hydrogen treat gas rate of about 500 scf/bbl (84 Nm^3/m^3) to about 4000 scf/bbl (674 Nm^3/m^3) or less, and a space velocity of from about 0.3 hr^{-1} to about 4.9 hr^{-1}.

16. The method of claim 13, wherein the mineral oil feedstock has a boiling point range of about 200ºF to about 650ºF.

17. A method for producing multiple distillate products from a single feedstock, the method comprising:

exposing a distillate fuel boiling range feedstock having a boiling point range of about 200ºF to about 680ºF and a sulfur content of less than about 10 wppm and a nitrogen content of less than about 5 wppm to a dewaxing catalyst comprising a molecular sieve, wherein the molecular sieve comprises ZSM-48 with a silica to alumina ratio of 70 to 1 to about 110 to 1, and a Group VIII noble metal hydrogenation component comprising about 0.05 wt % to about 0.35 wt % of a Group VIII noble metal under effective dewaxing conditions to produce a dewaxed effluent having a cloud point that is reduced by at least about 25ºF (14ºC) relative to a feedstock cloud point, wherein the effective dewaxing conditions comprise a pressure of from about 200 psig (1.4 MPa) to about 1500 psig (10.4 MPa); and

fractionating the dewaxed effluent to produce at least a diesel fuel product having a cloud point of about -7.6ºF (-22ºC) or less and a jet fuel product having a lower boiling range than the diesel fuel product and having a freeze point of less than about -40ºF (-40ºC), a fractionation cut point temperature between the diesel fuel product and the jet fuel product having the lower boiling range being at least 500ºF (260ºC).