a SAR in the range 22 to 90, such as 30 to 90, 22 to 60 or 30 to 60.

12. A process according to any one of claims 1 to 11 wherein the methyl acetate feedstock is derived from a process for the zeolite catalysed carbonylation of dimethyl ether to produce methyl acetate.

13. A process according to any one of claims 1 to 12 wherein the catalyst composition comprises at least one inorganic oxide binder.

14. A process according to claim 13 wherein the binder is an alumina.

15. A process according to claim 13 or claim 14 wherein the catalyst composition is in the form of an extrudate.

16. A process according to any one of claims 1 to 15 wherein the methanol and methyl acetate are in a molar ratio in the range 1: 0.1 to 1:40.

17. A process according to any one of claims 1 to 16 wherein water is introduced into the reaction zone, suitably in an amount in the range 0.1 to 60 mol%, such as 3 to 40 mol%, for example 5 to 30 mol%, based on the total feed to the reaction zone (including any recycles).

18. A process according to any one of claims 1 to 17 wherein the process is operated in the vapour phase.

~~19. A catalyst composition having improved lifetime in a process for the co-production~~ of acetic acid and dimethyl ether from a mixture of methanol and methyl acetate conducted at a temperature from 200 to 260 °C wherein said catalyst composition comprises a zeolite which has a 2-dimensional channel system comprising at least one channel having a 10-membered ring and a silica : alumina molar ratio of at least 22 : 1.

20. A catalyst composition according to claim 19 wherein the zeolite is ferrierite, preferably in the hydrogen form, bound with an alumina binder and, suitably may be in the ~~form of an extrudate.~~