

9. The process according to one of claims 1 to 6, wherein the tubular reactor is constructed from at least two tubes joined together.
10. The process according to one of claims 1 to 6, wherein the tubular reactor is constructed from at least two tubes joined together, characterised in that the tubular reactor over the first 20 to 60% of its length has an internal diameter of the tubular reactor of 1.1 mm to < 100 mm, and over the second 80 to 40% of its length has an internal diameter of the tubular reactor of 100 mm to 500 mm.
11. The process according to one of claims 1 to 10, wherein the tubular reactor is free from several layers arranged in parallel one on top of the other so that each layer has a plurality of channels arranged parallel to one another which form a continuous flow path from one side of the plate to the opposite side thereof.
12. The process according to one of claims 1 to 10, wherein the tubular reactor is free from several layers arranged in parallel one on top of the other, which are microstructured so that each layer has a plurality of channels arranged parallel to one another which form a continuous flow path from one side of the plate to the opposite side thereof.
13. The process according to one of claims 1 to 12, wherein the H-functional starter substance is selected from at least one of the group consisting of polyether polyol, polyester polyol, polyether carbonate polyol, water, ethylene glycol, diethylene glycol, propylene glycol, dipropylene glycol, 1,3-propanediol, 1,4-butanediol, 1,4-butenediol, 1,4-butyne diol, neopentyl glycol, 1,5-pentanediol, 3-methyl-1,5-pentanediol, 1,6-hexanediol; 1,8-octanediol, 1,10-decanediol, 1,12-dodecanediol, 1,4-bis(hydroxymethyl)cyclohexane, triethylene glycol, tetraethylene glycol, dipropylene glycol, tripropylene glycol, dibutylene glycol trimethylolpropane, glycerol, tris(hydroxyethyl) isocyanurate, castor oil, pentaerythritol, sorbitol, hexitol, sucrose, starch, starch hydrolysate, cellulose, cellulose hydrolysate, hydroxyl-functionalised fats and hydroxyl-functionalised oils ~~is used~~.
14. The process according to one of claims 1 to 13, wherein the tubular reactor has a ratio of tube length L to tube diameter d_R of $L / d_R > 50$.