

Process for separating phenol from a mixture comprising at least hydroxyacetone, cumene, water and phenol

5 The invention relates to an improved process for separating phenol from a mixture comprising at least hydroxyacetone, cumene, water and phenol.

10 The process of acid-catalyzed cleavage of cumene hydroperoxide into phenol and acetone has been of particular industrial importance for a long time. In this preparation of phenol from cumene by the Hock process, cumene is oxidized to cumene hydroperoxide (CHP) in a first reaction step, known as the oxidation, and the CHP is subsequently concentrated to from 65 to 15 90% by weight in a vacuum distillation, known as the concentration. In a second reaction step, known as the cleavage, the CHP is cleaved into phenol and acetone by action of an acid, usually sulfuric acid. Apart from phenol and acetone, the cleavage product further 20 comprises additional compounds which can have been formed in the reaction steps preceding the cleavage and which are only partly transformed, if at all, in the cleavage. The most important compounds which may be present in the cleavage product in addition to phenol 25 and acetone are, in particular, α -methylstyrene (AMS), cumene and acetophenone. In addition, small amounts of dimethyl phenyl carbinol (DMPC) formed in the oxidation can be present in the cleavage product. Further impurities include compounds such as methylbenzofuran 30 (MBF), hydroxyacetone, mesityl oxide (MO) and carbonyl compounds such as acetaldehyde and 2-phenylpropionaldehyde. After neutralization of the cleavage product and possible removal of an aqueous phase, the cleavage product is worked up by distillation.

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Various processes for working up the cleavage product by distillation are known (Ullmann's Encyclopedia of Industrial Chemistry, 5th completely revised edition,



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Vol. A19, 1991, VCH Verlagsgesellschaft mbH, Weinheim). In principle, all these processes involve initial neutralization of the cleavage product using aqueous sodium hydroxide, amines or aqueous phenoxide solution.

5 After phase separation, the organic part of the neutralized cleavage product is transferred to a first column in which crude acetone is distilled off from the remaining cleavage product via the top of the column. This crude acetone is usually treated with alkali in a

10 scrubber and once again purified by distillation. However, the scrub is sometimes also carried out in the column. The bottom product from the first column is distilled in a second column from which AMS and cumene are taken off at the top and are usually passed to a

15 hydrogenation in which cumene is produced again. AMS and cumene can also be separated off by azeotropic distillation in the presence of water. The bottom product remaining in the second column is distilled in a crude phenol column.

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The crude phenol obtained can be purified further by extractive distillation using water or by treatment with an acid ion exchanger and subsequent distillation. In the latter process, compounds which are difficult to

25 separate from phenol by distillation, e.g. mesityl oxide and hydroxyacetone, are condensed to form higher-boiling compounds.

Such a process is described, for example, in US

30 5,064,507 (Allied). In this process, the cleavage product is firstly separated from the crude acetone in a crude acetone column. The bottom product is transferred to a cumene column in which cumene and AMS are separated from the cleavage product. The column is,

35 however, operated so that a certain proportion of AMS remains in the bottom product since this is required as reactant or solvent in the further processing of the phenol to remove MBF and other impurities. This bottom

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product is reacted with an amine, preferably hexamethylenediamine, in a reactor having plug flow characteristics in order to convert carbonyl compounds, e.g. acetol (hydroxyacetone) or MO, into higher-boiling compounds. The product which has been treated in this way is worked up further by distillation. However, it passes through a further four columns and two reaction zones before the purified end product phenol is obtained. The outlay for apparatus required for the removal of the hydroxyacetone from the phenol is relatively high in this process.

US 3,322,651 (UOP), too, describes the use of nitrogen compounds, in particular amines, for purifying phenol obtained in the cleavage of CHP. However, the amines added likewise have to be removed again from the products.

GB 1 021 759 (Mitsui) describes the work-up of a cleavage product mixture which has been obtained in the acid-catalyzed cleavage of CHP and from which the catalyst has been removed by neutralization and scrubbing. To be able to obtain a phenol having a low hydroxyacetone content, the separation is carried out by feeding the cleavage product mixture into a distillation column at a side inlet and fractionating this mixture in one separation step to give a top fraction comprising water, acetone, hydroxyacetone and cumene and a bottom fraction comprising phenol having a hydroxyacetone content of less than 100 ppm. Depending on the composition of the cleavage product mixture, cumene was added in an amount so that the ratio of cumene to phenol in the feed to the column was at least 0.28 part by weight of cumene to 1 part by weight of phenol, since the process is based on the separation of an azeotropic mixture of hydroxyacetone and cumene from the phenol. The hydroxyacetone can be removed from the phenol by this process. However, a top fraction which

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comprises not only water, cumene and hydroxyacetone but also acetone is obtained. Phenol contamination may also be present in the top fraction. These products likewise have to be separated from one another.

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In US 4,251,325 (BP Chemicals), the work-up of a fraction which has been substantially freed of low boilers, water and acetone has been optimized by operating the cumene column in such a way that a
10 mixture comprising cumene, AMS and hydroxyacetone is taken off at the top, with this mixture being separated virtually completely from the crude phenol remaining in the bottoms and thus not having to be removed in a costly fashion during the work-up of the phenol. This
15 process gives phenol containing less than 30 ppm of hydroxyacetone. A disadvantage of this process is the fact that the input mixture has to be substantially freed of water, which is why an acetone fraction comprising low boilers and also the major part of the
20 water present in the cleavage product mixture has to be separated from the cleavage product mixture in the preceding separation step. The work-up of such an acetone fraction by methods of the prior art is relatively uneconomical, since a high outlay in terms
25 of apparatus is required.

It is therefore an object of the present invention to provide a simple process for separating phenol from a mixture comprising at least cumene, phenol and
30 hydroxyacetone, in which process a phenol having a hydroxyacetone content of less than 30 ppm is separated from the mixture with a low energy consumption, with a low outlay in terms of apparatus and in the presence of water.

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It has surprisingly been found that a mixture comprising at least phenol, water, hydroxyacetone and cumene can be worked up by means of a single fractional

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distillation step with subsequent phase separation to give phenol having a hydroxyacetone content of less than 30 ppm, with this fractional distillation step being able to be carried out with a lower energy consumption and a lower outlay in terms of apparatus than in conventional processes. Likewise surprisingly, it has been found that reversal of the order of the process steps also enables phenol having a hydroxyacetone content of less than 30 ppm to be separated from the abovementioned mixture.

The present invention accordingly provides a process as set forth in claim 1 for separating phenol from a mixture comprising at least hydroxyacetone, cumene, water and phenol, which comprises fractionating the mixture by means of at least one fractional distillation step and at least one phase separation step in such a way that at least one phenol-containing fraction containing less than 300 ppm of hydroxyacetone is obtained.

The present invention likewise provides an apparatus as set forth in claim 9 for separating phenol from a mixture comprising at least hydroxyacetone, cumene, water and phenol, which comprises at least one distillation column which is dimensioned so that an at least cumene- and/or α -methylstyrene-containing fraction can be taken off at the top of the column and a phenol-containing fraction having a hydroxyacetone content of less than 300 ppm can be taken off at the bottom of the column and at least one phase separation apparatus for separating organic phases from aqueous phases.

The invention also provides phenol obtained by means of a process as claimed in at least one of claims 1 to 8.

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The invention also provides a mixture of cumene and AMS obtained by means of a process as claimed in at least one of claims 1 to 8.

- 5 The advantage of the process of the invention is that the separation step chosen in the distillation substantially simplifies the further work-up of the cleavage product mixture or of the individual fractions obtained from the cleavage product mixture. In
10 particular, the joint removal of hydroxyacetone, AMS and cumene from the phenol-containing remainder of the cleavage product mixture substantially simplifies the work-up of the phenol-containing fraction, since the steps carried out in conventional processes in which
15 the hydroxyacetone remains in the phenol-rich fraction and is removed therefrom by reacting the hydroxyacetone with phenol to form compounds which have a boiling point higher than that of phenol and can be separated from the phenol by distillation become unnecessary.
- 20 Compared to conventional processes, the process of the invention has a significantly more favorable energy balance and also gives a higher total yield of phenol, based on the phenol content of the cleavage product
25 mixture. The conventional procedure requires a relatively high energy input. In addition, the yield of phenol is reduced since the hydroxyacetone reacts with the phenol, or it is necessary to add expensive chemicals such as amines, and these themselves or their
30 reaction products have to be removed from the process again, which is costly. The process of the invention, which circumvents this problem by separating the hydroxyacetone together with the cumene from the cleavage product mixture, also requires a significantly
35 lower outlay in terms of apparatus, since both the number of distillation columns required and also the number of reaction apparatuses necessary for reducing

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the contents of the various by-products in the fractions are reduced.

5 A further advantage achieved by the process of the invention is that the hydroxyacetone is preferentially obtained in an aqueous phase and can easily be disposed of or worked up together with this.

10 For the purposes of the present invention, the total number of trays present in a column is defined as having a separation potential of 100% regardless of the number of trays, so that it is possible to indicate the region having a similar separation potential in columns having a differing number of trays. Accordingly, the
15 bottom of the column, i.e. the region below the first tray, has a separation potential of 0%. At the top of the column, i.e. the region above the uppermost tray, the separation potential is, in accordance with this definition, 100%. In accordance with this definition, a
20 column having 50 trays has a separation potential of 30% in the region of the 15th tray.

The process of the invention can be used for the work-up by distillation of mixtures obtained as part of the
25 cleavage product mixtures in the cleavage of cumene hydroperoxide (CHP) into acetone and phenol with subsequent work-up of the cleavage product mixture. The process of the invention is preferably used for separating phenols from a mixture which comprises at
30 least hydroxyacetone, cumene, water and phenol and is that part of a cleavage product mixture from the cleavage of CHP which is obtained after separation of crude acetone from the cleavage product mixture. The acetone content of such a mixture is preferably less
35 than 1% by weight, very particularly preferably less than 0.2% by weight.

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The process of the invention is described below by way of example for the work-up by distillation of a mixture obtained in the acid-catalyzed homogeneous cleavage of CHP and subsequent work-up of the cleavage product mixture, without the process being restricted to this embodiment. This mixture is obtained as part of the cleavage product mixture by separating a crude acetone fraction from the cleavage product mixture.

10 The process of the invention for separating phenol from a mixture comprising at least hydroxyacetone, cumene, water and phenol comprises fractionating the mixture by means of at least one fractional distillation step and at least one phase separation step in such a way that
15 at least one phenol-containing fraction containing less than 300 ppm of hydroxyacetone is obtained. This phenol-containing fraction is very particulary preferably obtained by a process in which a single fractional distillation step and a single phase
20 separation step are carried out.

Before the phenol is separated off, the mixture preferably has a phenol concentration of from 20 to 99% by weight, particularly preferably from 40 to 70% by weight. The mixture can have a hydroxyacetone
25 concentration of from 300 ppm to 5% by weight.

Apart from the compounds mentioned, the mixture may further comprise additional compounds such as α -methylstyrene (AMS), cumene, water, phenylbutenes, methylbenzofuran (MBF), dimethyl phenyl carbinol (DMPC), cresols, e.g. o-cresol, mesityl oxide (MO), n-propylbenzene, isopropylphenol, carbonyl compounds such as 3-methylcyclopentenone, (methyl) isobutyl ketones or
30 2-phenylpropionaldehyde, sec-butylbenzene, tert-butylbenzene, methylbenzenes, e.g. dimethylbenzene, or acetophenone (AP).

The process of the invention can be carried out in at least two different variants, but all of these comprise at least one distillation step and at least one phase separation step.

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In a first embodiment of the process of the invention, the mixture is fractionated in at least one fractional distillation step, preferably in only a single distillation step, in such a way that a phenol-
10 containing fraction containing less than 300 ppm of hydroxyacetone, preferably less than 100 ppm and very particularly preferably less than 10 ppm of hydroxyacetone, and a further fraction comprising at least hydroxyacetone, cumene and water are obtained and
15 the latter fraction is separated into an organic phase and an aqueous phase in a phase separation step.

In this embodiment of the process of the invention, the mixture from which phenol is to be separated is firstly
20 fed into a distillation apparatus, preferably a distillation column. The distillation column has to be configured so that it is possible to fractionate the mixture to give at least one phenol-containing fraction and at least one further fraction comprising at least
25 cumene, water and hydroxyacetone. The mixture is preferably fed into the column at a side inlet, preferably in a position at which the column has a separation potential of from 25 to 85%, particularly preferably from 40 to 60%. The column is operated so
30 that a phenol-containing fraction can be taken off in liquid form at the bottom of the column. It can be advantageous to feed part of this fraction back into the column. The phenol-containing fraction which is separated off at the bottom of the column and has a
35 hydroxyacetone concentration of less than 300 ppm is preferably passed as crude phenol to further work-up.

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The temperature at the bottom of column is preferably from 140 to 200°C, particularly preferably from 170 to 190°C. The temperature at the top of the column is preferably from 60 to 160°C, particularly preferably from 65 to 100°C. The temperature at the top of the column is always selected so that the temperature at the top is lower than the temperature at the bottom. The pressure in the column can be from 0.1 to 4 bar. The distillation column is preferably under atmospheric pressure.

The fraction taken off at the top of the column, preferably in vapor form, comprises at least water, cumene and hydroxyacetone. If AMS is present in the original mixture, AMS is also present in the top fraction. The top fraction preferably comprises at least from 95% to 100%, preferably from 98% to 99.9%, of the cumene present in the mixture, from 95% to 100%, preferably from 98% to 99.9%, of the hydroxyacetone present in the mixture and from 97% to 99.9% of the water present in the mixture.

Part of the fraction taken off at the top of the column can be fed back into the column in liquid form as runback. Preference is given to transferring at least part of the fraction taken off at the top of the distillation column to a phase separation apparatus, e.g. a decanter, coalescer, phase separation vessel or extractor, in which the fraction can be separated into two phases, viz. an aqueous phase and an organic phase. It may be advantageous to return at least part of the organic phase of this fraction, at least part of the aqueous phase of this fraction or a mixture of organic and aqueous phase to the column as runback. The temperature at which phase separation is carried out is preferably from 20 to 100°C at atmospheric pressure.

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Very particular preference is given to returning at least part of the aqueous phase and part of the organic phase of the top fraction separated in the phase separation apparatus separately to the distillation column.

It may be advantageous to feed at least part of the aqueous phase back into the column in vapor or liquid form, preferably vapor form, at a point below the feed point.

The reflux ratio based on the amount of water taken off and the amount of water returned is preferably from 0.2 to 3, very particularly preferably from 0.4 to 2. The reflux ratio based on the amount of organic phase taken off and the amount of organic phase returned is preferably from 0.1 to 10, very particularly preferably from 0.5 to 5. The remainder of the organic part of the top fraction obtained from the phase separation apparatus is passed to further work-up. This organic part of the top fraction comprises at least cumene. The amount of hydroxyacetone in this organic part of the top fraction is from 0.01 to 10%, preferably from 0.1 to 2%, of the hydroxyacetone originally present in the top fraction.

The remainder of the aqueous part of the top fraction which is not recirculated to the distillation column can be passed to disposal or work-up. This aqueous part comprises the remaining hydroxyacetone from the top fraction which is not present in the organic part of the top fraction.

The advantage of the mode of operation according to the invention is that the hydroxyacetone present in the top fraction is concentrated in the water of this fraction. The predominant proportion (factor of 20-30) of the hydroxyacetone goes into the aqueous phase in the phase

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separation apparatus and can thus be discharged from the process in a simple manner with the aqueous part of the top fraction and does not have to be separated off from an organic phase as in the prior art
5 (US 4,251,325, US 3,322,651 or US 5,064,507).

In a second embodiment of the process of the invention, the mixture is separated into an organic phase and an aqueous phase in at least one phase separation step and
10 the organic phase obtained is fractionated in a fractional distillation step to give a phenol-containing fraction in which less than 300 ppm of hydroxyacetone are present.

15 In this embodiment of the process of the invention, the mixture from which phenol is to be separated is transferred to at least one phase separation apparatus, e.g. a decanter, coalescer, phase separation vessel or extractor, in which the mixture can be separated into
20 two phases, viz. an aqueous phase and an organic phase. The temperature at which the phase separation is carried out is preferably from 20 to 100°C at atmospheric pressure.

25 The aqueous phase of the mixture can be passed to disposal or work-up, e.g. a phenol removal from wastewater and a water treatment plant, as are known from the prior art. A large part of the hydroxyacetone from the mixture is present in this aqueous phase.

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The organic phase of the mixture obtained from the phase separation apparatus comprises at least cumene and phenol. The amount of hydroxyacetone in this organic phase of the mixture is from 10 to 60%,
35 preferably from 30 to 40%, of the hydroxyacetone originally present in the mixture.

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This organic phase of the mixture is then fed to a distillation apparatus, preferably a distillation column. The distillation column has to be configured so that it is possible to fractionate the mixture so as to
5 give at least one fraction comprising phenol and at least one further fraction comprising at least cumene. The mixture is preferably fed into the column via a side inlet, preferably in a position at which the column has a separation potential of from 25 to 85%,
10 particularly preferably from 40 to 60%. The column is operated so that a phenol-containing fraction can be taken off in liquid form at the bottom of the column. The phenol-containing fraction separated off at the bottom of the column, in which hydroxyacetone is
15 present in a concentration of less than 300 ppm, is preferably passed as crude phenol to further work-up.

The temperature at the bottom of the column is preferably from 140 to 200°C, particularly preferably
20 from 170 to 190°C. The temperature at the top of the column is preferably from 60 to 160°C, particularly preferably from 80 to 100°C. The temperature at the top of the column is always selected so that it is lower than the temperature at the bottom. The pressure in the
25 column can be from 0.1 to 4 bar. The distillation column is preferably under atmospheric pressure.

The fraction taken off at the top of the column, preferably in vapor form, comprises at least cumene and
30 hydroxyacetone. If AMS is present in the original mixture, AMS is also present in the top fraction. The top fraction preferably comprises from 95% to 100%, preferably from 98% to 99.9%, of the cumene present in the original mixture.

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Part of the fraction taken off at the top of the column can be fed back into the column in liquid form as runback.

The advantage of the mode of operation according to the invention is that the hydroxyacetone is concentrated in the water. A predominant part of the hydroxyacetone goes into the aqueous phase in the phase separation apparatus and can thus be discharged from the process in a simple manner. Further treatment of the top fraction in this embodiment of the process of the invention in a phase separation apparatus also enables, as in the first embodiment of the process of the invention, the hydroxyacetone from the top fraction to be discharged via an aqueous phase separated off from the top product by phase separation.

In both embodiments of the process of the invention, very particular preference is given to obtaining a phenol-containing fraction which preferably comprises from 95 to 99% by weight of phenol and has a hydroxyacetone content of less than 300 ppm, preferably less than 100 ppm and very particularly preferably less than 10 ppm.

In both embodiments of the process of the invention, it can be advantageous to take off a further fraction comprising at least one organic and/or inorganic acid from the distillation apparatus in the distillation step via a side offtake. Such a fraction is preferably taken off from a side offtake located below the feed point for the mixture and above the bottom of the column. In this way, the proportion of by-products in the fraction can be reduced further.

In both embodiments of the process of the invention, it can be advantageous for further amounts of compounds which are already present in the mixture to be treated to be added to this mixture. Particular preference is given to adding the compounds cumene and/or water or mixtures comprising cumene and/or water to the mixture

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to be treated. The addition can be carried out before or during the distillation step and/or before or during the phase separation step.

5 In the first embodiment of the process of the invention, it can be particularly advantageous to add such an amount of cumene and/or water to the mixture prior to the distillation that the water content of the mixture is from 1 to 14% by weight and the cumene
10 content is from 1 to 50% by weight.

In the second embodiment, it can be advantageous to add water to the mixture before or during the phase separation step. It can likewise be advantageous to add
15 cumene to the organic phase of the mixture prior to the distillation step. In the second embodiment, the cumene content of the organic part of the mixture before it is fed to the distillation step is preferably from 5 to 50% by weight.

20 In both embodiments of the process of the invention, the phenol obtained from the feed mixture not only contains less than 300 ppm of hydroxyacetone but is also depleted in impurities such as phenylbutenes, methylbenzofuran (MBF), mesityl oxide (MO), n-propyl-
25 benzene, isopropylphenol, carbonyl compounds such as 3-methylcyclopentenone, (methyl) isobutyl ketones or 2-phenylpropionaldehyde, sec-butylbenzene, tert-butylbenzene or methylbenzenes, e.g. dimethylbenzene. These
30 impurities are separated from the mixture together with α -methylstyrene (AMS), cumene and water via the top of the distillation column.

The fractions obtained according to the invention can
35 be worked up further by methods known from the prior art.

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The process of the invention for separating phenol from a mixture comprising at least hydroxyacetone, cumene, water and phenol is preferably carried out in an apparatus according to the invention.

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This apparatus of the invention comprises at least one distillation column which is dimensioned so that an at least cumene- and/or α -methylstyrene-containing fraction can be taken off at the top of the column and a phenol-containing fraction having a hydroxyacetone content of less than 300 ppm, preferably less than 100 ppm and very particularly preferably less than 10 ppm, can be taken off at the bottom of the column and at least one phase separation apparatus for separating organic phases from aqueous phases.

The distillation column particularly preferably has at least from 20 to 160, particularly preferably from 40 to 80, theoretical plates. In a particularly preferred embodiment of the apparatus of the invention, it has a side offtake at which a fraction comprising at least one organic acid can be taken off located between the feed point for the mixture and the bottom of the column. The organic acid present in the fraction can be, for example, acetic acid, oxalic acid, formic acid or butyric acid or a mixture comprising at least one of these acids.

As phase separation apparatus, the apparatus of the invention preferably has at least one decanter.

Phenol is obtainable by the process of the invention. This phenol has a hydroxyacetone content of less than 300 ppm, particularly preferably less than 100 ppm and very particularly preferably less than 10 ppm. A cumene- and/or AMS-containing mixture having a reduced hydroxyacetone content can likewise be obtained by means of the process of the invention.

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The process of the invention and the apparatus of the invention are shown by way of example in fig. 1 and fig. 2, without the process or the apparatus being
5 restricted to these embodiments.

Fig. 1 schematically shows an embodiment of the apparatus of the invention. The apparatus of the invention comprises a distillation column **K1'** which has
10 a side inlet through which the mixture **SP'** can be fed in for the purpose of separating off the phenol. At the top and at the bottom of the column, the top product **KP'** and the bottom product **SP1'**, respectively, can be taken off. The distillation column of the apparatus of
15 the invention has, at the bottom of the column, a heat exchanger **WT2'** by means of which the appropriate heat energy can be introduced into the column.

From the top of the column, the top product **KP'**
20 comprising at least cumene, hydroxyacetone and water is passed through a heat exchanger **WT3'** in which the top product is condensed, and the top product is transferred from there to a phase separation apparatus **PT1'**. Part of the organic phase formed in this phase
25 separation apparatus can be returned to the distillation column via **RO'**. The remaining part of the organic phase, which comprises at least cumene, can be passed to further work-up via **CA'**. Part of the aqueous phase can likewise be returned in liquid form to the
30 distillation column **K1'** via **RW1'**. A further part of the aqueous phase can be conveyed to the distillation column **K1'** in liquid or vapor form via **RW2'**. The remaining part of the aqueous phase, which comprises hydroxyacetone, can be passed via **W1'** to utilization or
35 work-up. The distillation column **K1'** may optionally have one or more side oftakes **SOS'** via which fractions comprising at least one organic acid can be discharged from the column.

Fig. 2 schematically shows a further embodiment of the process of the invention. A mixture to be treated **SP** is fed into a phase separation apparatus **PT1**. The organic phase of the mixture, which comprises at least cumene and phenol, can be fed into a distillation column **K1** at the side via **SCA**. The aqueous phase of the mixture, which comprises hydroxyacetone, can be passed via **W1** to utilization or work-up. If necessary or desired, an aqueous phase or water can be introduced into the phase separation vessel via **AW**.

The organic phase of the mixture which is fed into the column **K1** at the side via **SCA** is fractionated in the column to give a fraction which comprises at least cumene and is taken off at the top of the column as **KP1** and a fraction which comprises at least phenol and can be taken off at the bottom of the column as **SP1**. The distillation column of the apparatus of the invention has runback systems at the top and at the bottom of the column by means of which some or all of the top product or bottom product can be returned to the column. The heat exchangers **WT1** and **WT2** are installed in these runback systems and make it possible to introduce or remove heat energy into/from the bottom or top product returned to the column. The distillation column **K1** can optionally be provided with one or more side offtakes **SOS** via which fractions comprising at least one organic acid can be discharged from the column.

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Example 1:

A mixture comprising, inter alia, 73 parts of phenol, 20 parts of cumene, 3 parts of AMS, 1 part of acetophenone, 0.2 part of hydroxyacetone and 2 parts of water was fed at the side, at the height of the 40th theoretical plate, into a distillation column having 80 theoretical plates as shown in Fig. 1.

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The temperature in the column was set so that the temperature at the top was 95°C and the temperature at the bottom was 182°C. The pressure in the distillation column corresponded to atmospheric pressure. The fraction taken off at the top of the distillation column had a water content of 8% by weight, a cumene content of 79% by weight, a hydroxyacetone content of 0.8% by weight and an AMS content of 12% by weight. This fraction was transferred to a decanter. In this decanter, an aqueous phase comprising the major part of the hydroxyacetone present in the fraction was separated off from the fraction. Part of the aqueous phase was discarded. The remainder of the aqueous phase was returned to the distillation column.

The organic phase separated from the aqueous phase in the separation vessel had a hydroxyacetone content of less than 400 ppm. Part of this organic phase was returned to the distillation column. The remaining part of the organic phase was fed to a cumene column for the purpose of further work-up.

The fraction taken off from the bottom of the first distillation column comprised, inter alia, 98.5% by weight of phenol and 1.4% by weight of acetophenone and only 13 ppm of hydroxyacetone. This fraction was fed into a crude phenol column for the purpose of further work-up.

Claims:

1. A process for separating phenol from a mixture comprising at least hydroxyacetone, cumene, water and phenol, which comprises fractionating the mixture by means of at least one fractional distillation step and at least one phase separation step in such a way that at least one phenol-containing fraction containing less than 300 ppm of hydroxyacetone is obtained.
2. The process as claimed in claim 1, wherein the mixture is separated into an organic phase and an aqueous phase in a phase separation step and the organic phase obtained is fractionated in a fractional distillation step in such a way that a phenol-containing fraction containing less than 300 ppm of hydroxyacetone is obtained.
3. The process as claimed in claim 1, wherein the mixture is fractionated in a fractional distillation step in such a way that a phenol-containing fraction containing less than 300 ppm of hydroxyacetone and a further fraction comprising at least hydroxyacetone, cumene and water are obtained and the latter fraction is separated into an organic phase and an aqueous phase.
4. The process as claimed in at least one of claims 1 to 3, wherein the phenol-containing fraction has a hydroxyacetone content of less than 30 ppm.
5. The process as claimed in at least one of claims 1 to 4, wherein the mixture comprises α -methylstyrene.

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6. The process as claimed in at least one of claims 1 to 5, wherein the mixture used is part of a cleavage product mixture obtained in the acid-catalyzed cleavage of cumene hydroperoxide.
- 5 7. The process as claimed in at least one of claims 1 to 6, wherein the mixture has a phenol concentration of from 20 to 90% by weight.
- 10 8. The process as claimed in at least one of claims 1 to 7, wherein the mixture has a hydroxyacetone concentration of from 300 ppm to 5% by weight.
- 15 9. An apparatus for separating phenol from a mixture comprising at least hydroxyacetone, cumene, water and phenol, which comprises at least one distillation column which is dimensioned so that at least one cumene- and/or α -methylstyrene-containing fraction can be taken off at the top of the column and a phenol-containing fraction having a hydroxyacetone content of less than 300 ppm can be taken off at the bottom of the column and at least one phase separation apparatus for separating organic phases from aqueous phases.
- 20 10. An apparatus as claimed in claim 9, wherein the column has at least 20 trays.
- 25 11. An apparatus as claimed in claim 9 or 10, wherein the column has a side offtake at which a fraction comprising at least one organic acid can be taken off between the feedpoint for the mixture and the bottom of the column.
- 30 12. An apparatus as claimed in any of claims 9 to 11, wherein the phase separation apparatus is a decanter.
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13. Phenol obtainable by a process as claimed in at least one of claims 1 to 8 which is depleted in impurities such as hydroxyacetone, water, cumene, α -methylstyrene, phenylbutenes, methylbenzofuran (MBF), mesityl oxide (MO), n-propylbenzene, isopropylbenzene, carbonyl compounds, 3-methylcyclopentenone, (methyl) isobutyl ketones, 2-phenylpropionaldehyde, sec-butylbenzene, tert-butylbenzene, methylbenzenes and/or dimethylbenzene.
14. A mixture which comprises cumene and α -methylstyrene and is obtainable by a process as claimed in at least one of claims 1 to 8.