CLAIMS

1. A method for cracking a hydrocarbon feed stream, the method comprising:

contacting the hydrocarbon feed stream with a cracking catalyst in a reactor unit, where the hydrocarbon feed stream has an API gravity of at least 40 degrees, and where the cracking catalyst comprises:

one or more binder materials in an amount of from 5 wt.% to 30 wt.% of the total cracking catalyst;

one or more matrix materials in an amount of from 30 wt.% to 60 wt.% of the total cracking catalyst;

*BEA framework type zeolite in an amount of from 5 wt.% to 45 wt.% of the total cracking catalyst;

FAU framework type zeolite in an amount of from 5 wt.% to 45 wt.% of the total cracking catalyst; and

MFI framework type zeolite in an amount of from 5 wt.% to 45 wt.% of the total cracking catalyst.

2. The method of claim 1, where the hydrocarbon feed stream has an API gravity of from 45 degrees to 60 degrees.

3. The method of claims 1 or 2, where one or more of the MFI framework type zeolite, *BEA framework type zeolite, and FAU framework type zeolite comprise phosphorous pentoxide.

4. The method of claims 1 or 2, where at least one of the one or more binder materials is pseudoboehmite.

5. The method of claims 1 or 2, where one or more of the matrix materials is kaolin.

6. The method of claims 1 or 2, where the catalyst to oil weight ratio is from 7 to 10.

7. The method of claims 1 or 2, where the contacting of the hydrocarbon feed stream with the cracking catalyst produces a product stream comprising at least 20 wt.% of light olefins selected from ethylene, propylene, and butene.

8. The method of claims 1 or 2, where the hydrocarbon feed stream is gas condensate.

9. A system for cracking a hydrocarbon feed stream, the system comprising:

a reactor;

a hydrocarbon feed stream entering the reactor, where the hydrocarbon feed stream has an API gravity of at least 40 degrees;

a product stream exiting the reactor; and

a cracking catalyst positioned at least in the reactor, where the cracking catalyst comprises:

one or more binder materials in an amount of from 5 wt.% to 30 wt.% of the total cracking catalyst;

one or more matrix materials in an amount of from 30 wt.% to 60 wt.% of the total cracking catalyst;

*BEA framework type zeolite in an amount of from 5 wt.% to 45 wt.% of the total cracking catalyst;

FAU framework type zeolite in an amount of from 5 wt.% to 45 wt.% of the total cracking catalyst; and

MFI framework type zeolite in an amount of from 5 wt.% to 45 wt.% of the total cracking catalyst.

10. The system of claim 9, where the hydrocarbon feed stream has an API gravity of from 45 degrees to 60 degrees.

11. The system of claims 9 or 10, where one or more of the MFI framework type zeolite, *BEA framework type zeolite, and FAU framework type zeolite comprise phosphorous pentoxide.

12. The system of claims 9 or 10, where one or more of the MFI framework type zeolite, *BEA framework type zeolite, and FAU framework type zeolite comprise from 1 wt.% to 20 wt.% of phosphorous pentoxide.

13. The system of claims 9 or 10, where the catalyst to oil weight ratio is from 7 to 10.

14. The system of claims 9 or 10, where the *BEA framework type zeolite comprises less than 0.5 wt.% of transition metal.

15. The system of claims 9 or 10, where the *BEA framework type zeolite comprises less than 0.5 wt.% of transition metal.