CLAIMS

1. A method of producing a (meth)acrylic resin composition, wherein the method comprises the steps of:

continuously feeding a reaction raw material comprising a chain transfer agent, a radical polymerization initiator and a monomer mixture comprising 80 to 100 % by mass of methyl methacrylate and 20 to 0 % by mass of an alkyl acrylate to ~~a~~ tank reactor through two or more feeding ports;

bulk polymerizing the monomer mixture in the tank reactor until a polymerization conversion of 40 to 70 % by mass to prepare a reaction product; and

removing the monomer mixture from the reaction product,

wherein the perfect mixing time (θ_M [hr]) of the tank reactor, the half-life ($\tau_{1/2}$ [hr]) of the radical polymerization initiator at the temperature in the tank reactor, the stirring power (P_V [kW/m^3]) of the tank reactor, the mean residence time (θ [hr]) of the reaction raw material in the tank reactor, and the concentration (I [ppm]) of the radical polymerization initiator in the reaction raw material satisfy the following relationships:

$\theta_M > \tau_{1/2}$, and

$P_V \times \theta \times I \times \tau_{1/2} < 4$.

2. The method according to Claim 1, wherein the temperature in the tank reactor is 110°C to 160°C; and

CLAIMS

1. A method of producing a (meth)acrylic resin composition, wherein the method comprises the steps of:

continuously feeding a reaction raw material comprising a chain transfer agent, a radical polymerization initiator and a monomer mixture comprising 80 to 100 % by mass of methyl methacrylate and 20 to 0 % by mass of an alkyl acrylate to one tank reactor through two or more feeding ports;

bulk polymerizing the monomer mixture in the tank reactor until a polymerization conversion of 40 to 70 % by mass to prepare a reaction product; and

removing the monomer mixture from the reaction product,

wherein the perfect mixing time (θ_M [hr]) of the tank reactor, the half-life ($\tau_{1/2}$ [hr]) of the radical polymerization initiator at the temperature in the tank reactor, the stirring power (P_V [kW/m^3]) of the tank reactor, the mean residence time (θ [hr]) of the reaction raw material in the tank reactor, and the concentration (I [ppm]) of the radical polymerization initiator in the reaction raw material satisfy the following relationships:

$\theta_M > \tau_{1/2}$, and

$P_V \times \theta \times I \times \tau_{1/2} < 4$.

2. The method according to Claim 1, wherein the temperature in the tank reactor is 110°C to 160°C; and