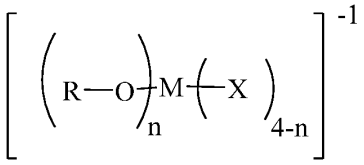
CLAIMS

1. A process of polymerizing olefins, the process comprising contacting ethylene and a (C_3–C_{40})alpha-olefin comonomer in the presence of a catalyst system to produce an ethylene-based polymer, the catalyst system comprising a procatalyst and an ionic metallic activator complex, the ionic metallic activator complex comprising an anion and a countercation, the anion having a structure according to formula (I):



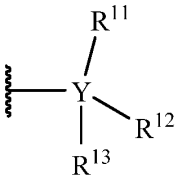
(I)

where:

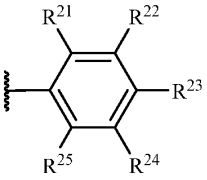
M is aluminum, boron, or gallium;

n is 2, 3, or 4;

each R is independently selected from the group consisting of radicals having formula (II) and radicals having formula (III):



(II)



(III)

each Y is independently carbon or silicon;

each R^{11}, R^{12}, R^{13}, R^{21}, R^{22}, R^{23}, R^{24}, and R^{25} is independently chosen from (C_1–C_{40})alkyl, (C_6–C_{40})aryl, –OR^C, –O–, –SR^C, –H, or –F, wherein when R is a radical according to formula (III), at least one of R^{21}, R^{22}, R^{23}, R^{24}, or R^{25} is a halogen-substituted (C_1–C_{40})alkyl , a halogen-substituted (C_6–C_{40})aryl, or –F; and

provided that:

when each R is a radical according to formula (II) and Y is carbon, at least one of R^{11}, R^{12}, or $R^{13}$is a halogen-substituted (C_1–C_{40})alkyl , a halogen-substituted (C_6–C_{40})aryl, or –F; or

when M is aluminum and n is 4 and each R is a radical according to formula (II), and each Y is carbon:

each R^{11}, R^{12}, and R^{13} of each R is a halogen- substituted $(C_1–C_{40})$alkyl, a halogen-substituted $(C_6–C_{40})$aryl, or –F; or

a total number of halogen atoms in R^{11}, R^{12}, and R^{13} of each R is at least six;

each X is a monodentate ligand independently chosen from halogen-substituted $(C_1–C_{20})$alkyl, $(C_1–C_{20})$alkyl, halogen-substituted $(C_6–C_{40})$aryl, $(C_6–C_{40})$aryl, triflate, or $–S(O)_3R^C$;

optionally, two groups R in formula (I) are covalently connected;

each R^C is independently $(C_1–C_{30})$hydrocarbyl or –H.

2. The polymerization process according to claim 1, wherein the procatalyst is a bis(phenylphenoxy) metal–ligand complex.

3. The polymerization process according to claim 1 or claim 2, wherein n is 4 and each R is independently $–C(H)(CF_3)_2$, $–C_6F_5$, or $–C(CF_3)_3$.

4. The polymerization process according to claim 1 or claim 2, wherein n is 3 and X is chosen from –OH, triflate (–OTf), methyl, or halogen.

5. The polymerization process according to claim 1 or claim 2, wherein n is 4, and three of the four groups R are $–C(CF_3)_3$ and one of the four groups R is $–C_6F_5$.

6. The polymerization process according to any one of the following claims, wherein the countercation has a formal change of positive one (+1).

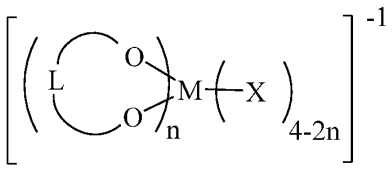
7. The polymerization process according to any one of claims 1–6, wherein the countercation is $^+N(H)R^N{}_3$, where each R^N is chosen from $(C_1–C_{20})$alkyl or $(C_6–C_{20})$aryl.

8. The polymerization process according to claim 6, wherein the countercation is $^+N(H)R^N{}_3$, where each where at least two R^N are chosen from $(C_{10}–C_{20})$alkyl.

9. The polymerization process according to any one of claims 1–6, wherein the countercation is $^+C(C_6H_5)_3$.

10. The polymerization process according to any one of claims 1–6, wherein the countercation is $^{+}C(C_6H_4R^C)_3$, where R^C is $(C_1–C_{20})$alkyl.

11. The polymerization process according to claim 1, wherein two groups R are covalently connected and the anion has a structure according to formula (IV):



(IV)

where:

M and X are as defined in formula (I);

n is 1 or 2;

L represents the two groups R that are covalently connected;

each L is independently chosen from $(C_2–C_{40})$alkylene, $(C_2–C_{40})$heteroalkylene or or $–(Si(R^C)_2–O)_z–Si(R^C)_2–$, where z is 0, 1, 2, or 3; and wherein R^C is independently $(C_1–C_{30})$hydrocarbyl or –H; and

when n is 1, X is a monodentate ligand independently chosen from halogen, halogenated-$(C_1–C_{20})$alkyl, or triflate.

15. The polymerization process according to any one of the preceding claims, wherein the ionic metallic activator complex in a high-boiling-point fully saturated hydrocarbon solution having a concentration of 200 micromoles of ionic metallic activator complex and 20 millimoles of water in a high-boiling-point fully saturated hydrocarbon solution has a percent dissipation factor of less than or equal to 0.1 as measured by the Hydrocarbon Conductivity Test.