WHAT IS CLAIMED IS:

1. A process for making a renewable product from a biofeedstock, the process comprising contacting a biofeedstock with a hydroconversion catalyst under hydroconversion conditions, wherein the biofeedstock comprises one or more biocomponents, and the hydroconversion catalyst comprises a hydrotreating catalyst and a hydroisomerization catalyst.
2. A process according to claim 1, wherein the hydroconversion catalyst comprises zeolite SSZ-91.
3. A process according to claims 1-2, wherein the hydroisomerization catalyst comprises SSZ-91.
4. A process according to claims 1-3, wherein the biofeedstock contains only renewable biocomponents.
5. A process according to claims 1-4, wherein a fossil fuel component is not used along with the biofeedstock in the process.
6. A process according to claims 1-5, wherein the process is a single-stage process.
7. A process according to claim 6, wherein the single stage process is carried out in a single reactor.
8. A process according to claim 6, wherein the single-stage process is carried out in two or more reactors connected in series, with a first reactor comprising a hydrotreating section and a reactor downstream from the first reactor comprising a hydroisomerization section.
9. A process according to claims 1-8, wherein the hydroconversion catalyst is or comprises a precious metal catalyst or a combination of a base metal catalyst and a precious metal catalyst.
10. A process according to claims 1-9, wherein the hydroconversion catalyst comprises a base metal catalyst and a precious metal catalyst.
11. A process according to claims 9-10, wherein the base metal is selected from Mo, Ni, W, Co, and combinations thereof.
12. A process according to claim 11, wherein the base metal is Mo or a combination of Mo and Ni.
13. A process according to claims 9-12, wherein the precious metal is selected from Pt, Pd, and a combination thereof.
14. A process according to claims 1-13, wherein the process comprises a hydrotreating section and a hydroisomerization section and all of the products from the hydrotreating section are directly passed to the hydroisomerization section.
15. A process according to claims 1-14, wherein the renewable product comprises a middle distillate product, a base oil product, or a combination thereof.

16. A process according to claim 15, wherein the renewable product comprises a naphtha, kerosene, jet fuel, diesel fuel, base oil, or a combination thereof.

17. A process according to any of claims 1-16, wherein a hydrocracking catalyst is not used to produce the renewable product.

18. A process according to claims 1-17, wherein the hydroconversion conditions comprise:
a temperature in the range of 300°F to 800°F (149°C to 427°C);
a pressure in the range of 15 to 3000 psig (0.10 to 20.68 MPa gauge);
a feed rate of biofeedstock in the range from 0.1 to 20 h^{-1} LHSV; and
hydrogen and biofeedstock feed rates in a ratio from 1000 to 10,000 standard cubic feet H_2 per barrel biofeedstock (from 180 to 1800 m^3 H_2/m^3 feed).

19. A process according to claim 18, wherein the hydroconversion conditions are hydrotreating or hydroisomerization.

20. A process according to claims 1-19, wherein the hydroconversion catalyst comprises zeolite SSZ-91 and a Group 8-10 metal.

21. A process according to claims 1-20, wherein the hydroconversion catalyst comprises zeolite SSZ-91, wherein the zeolite SSZ-91 has, in its calcined form, an X-ray diffraction pattern substantially as shown in the following Table:

2-Theta[(a)]	d-spacing (nm)	Relative Intensity[(b)]
7.67	1.152	M
8.81	1.003	W
12.61	0.701	W
15.30	0.579	W
21.25	0.418	VS
23.02	0.386	VS
24.91	0.357	W
26.63	0.334	W
29.20	0.306	W
31.51	0.284	W

[(a)] ± 0.20

[(b)] wherein powder XRD patterns provided are based on a relative intensity scale in which the strongest line in the X-ray pattern is assigned a value of 100: W = weak (> 0 to ≤ 20); M = medium (> 20 to ≤ 40); S = strong (> 40 to ≤ 60); VS = very strong (> 60 to ≤ 100).

22. A process according to claims 1-21, wherein the hydroconversion catalyst comprises zeolite SSZ-91 having a silicon oxide to aluminum oxide ratio of 40 to 220, or 70 to 160, or 80 to 160, or 80 to 140, or 100 to 160.

23. A process according to claims 1-22, wherein the hydroconversion catalyst comprises zeolite SSZ 91 having at least 80% polytype 6 of the total ZSM-48-type material present in the zeolite SSZ-91, or at least 90% polytype 6 of the total ZSM-48-type material present in the zeolite SSZ-91.

24. A process according to claims 1-23, wherein the hydroconversion catalyst comprises zeolite SSZ-91 and the zeolite SSZ-91 comprises 0.1 to 4.0 wt.% EUO-type molecular sieve phase.

25. A process according to claims 1-24, wherein the hydroconversion catalyst comprises zeolite SSZ-91 comprising 0.1 to 4.0 wt.% EU-1.

26. A process according to claims 1-25, wherein the hydroconversion catalyst comprises zeolite SSZ-91 having a morphology characterized as polycrystalline aggregates comprising crystallites collectively having an average aspect ratio of 1 to 4.

27. A process according to claims 1-26, wherein the hydroconversion catalyst comprises zeolite SSZ-91 having:
    a silicon oxide to aluminum oxide ratio of 40 to 220 or 70 to 160;
    a morphology characterized as polycrystalline aggregates comprising crystallites collectively having an average aspect ratio in the range of 1 to 4;
    at least 80% polytype 6 of the total ZSM-48-type material present in the zeolite SSZ-91; and, 0.1 to 4.0 wt.% EUO-type molecular sieve phase.

28. A process according to claims 1-27, wherein the hydroconversion catalyst comprises from 5 to 95 wt.% zeolite SSZ-91, and from 0.05 to 2.0 wt.% of a metal modifier.

29. A process according to claims 1-28, wherein the biofeedstock comprises or is a biocomponent feed selected from lipids, vegetable oils and animal fats which comprise triglycerides and free fatty acids, for example wherein the biocomponent feed is selected from canola oil, corn oil, soy oils, castor oil, camelina oil, palm oil and a combination thereof.

30. A process according to claims 1-29, wherein the biofeedstock comprises or is a biocomponent feed selected from canola oil, corn oil, soy oils, castor oil, camelina oil, palm oil, rapeseed oil, soybean oil, colza oil, tall oil, sunflower oil, hempseed oil, olive oil, linseed oil, coconut oil, castor oil, peanut oil, palm oil, mustard oil, cottonseed oil, tallow, yellow and brown greases, lard, train oil, fats in milk, fish oil, algal oil, sewage sludge, cuphea oil, camelina oil, jatropha oil, curcas oil, babassu oil, palm kernel oil, crambe oil, and the like.

31. A process according to claims 1-30, wherein the process produces a diesel fuel exhibiting a lower cloud point compared to the cloud point of the hydrotreated biofeedstock.

32. A process according to claim 31, wherein the diesel fuel has a cloud point at least 10°C lower than the cloud point of the hydrotreated biofeedstock, or a cloud point at least 20°C lower than the cloud

point of the biofeedstock, or a cloud point at least 30°C lower than the cloud point of the hydrotreated biofeedstock.

33. A process according to claims 31-32, wherein the diesel fuel has a pour point at least 10°C lower than the pour point of the hydrotreated biofeedstock, or a pour point at least 20°C lower than the pour point of the hydrotreated biofeedstock, or a pour point at least 30°C lower than the pour point of the hydrotreated biofeedstock.