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Declarations under Rule 4.17:

- as to applicant's entitlement to apply for and be granted a patent (Rule 4.17(ii))
- as to the applicant's entitlement to claim the priority of the earlier application (Rule 4.17(iii))
- of inventorship (Rule 4.17(iv))

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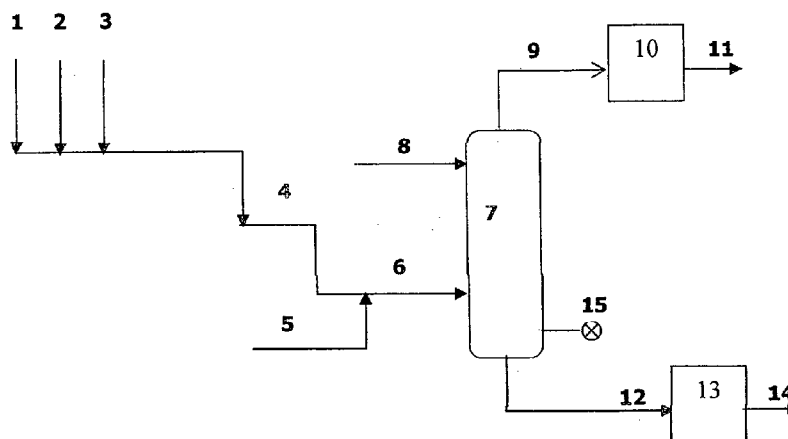
(54) **Title:** PROCESS TO PRODUCE PROCESS OIL WITH LOW POLYAROMATIC HYDROCARBON CONTENT

Figure 1.

(57) **Abstract:** Process for TDAE-1 and TDAE-2 production is initiated with production of DAE Feeds which have kinematic viscosity at 100°C ranges 24-67 cSt, followed by mixing them with solvent to yield Mixture of DAE Feed with density ranges 0.75-0.85 kg/liter and further contacting the Mixture of DAE Feed with solvent, like furfural, NMP and DMSO to facilitate a counter current liquid-liquid extraction, wherein the TDAE-1 and TDAE-2 are produced at ratio of polar solvent to Mixture of DAE Feed ranges 1.7-2.0 and 0.5-1.7, respectively. The PCA content of TDAE-1 and TDAE-2 are less than 3% weight and 3-20% weight. The amount of 8 Grimmer polyaromatics hydrocarbon content in the TDAE-1 and TDAE-2 are the same, that is, less than 10 mg/kg including Benzo (a) pyrene substance as much as less than 1 mg/kg.

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