CLAIMS:

1. A hydrocarbon conversion process comprising contacting a hydrocarbon stream with a catalyst at hydrocarbon conversion conditions to give a converted product, the catalyst comprising a modified UZM-43 microporous crystalline zeolite, wherein the modified UZM-43 has a three-dimensional framework of at least AlO_2 and SiO_2 tetrahedral units and an empirical composition on an anhydrous basis expressed by an empirical formula of:

$$M_m{}^+R1_{r1}R2_{r2}Al_{1-x}E_xSi_yO_z$$

where M represents sodium or a combination of sodium and potassium exchangeable cations, "m" is the mole ratio of M to (Al + E) and varies from 0.05 to 5, R1 is a singly charged propyltrimethylammonium cation, "r1" is the mole ratio of R to (Al +E) and has a value of 0.25 to 8.0, R2 is an amine, "r2" is the mole ratio of R to (Al +E) and has a value of 0.0 to 5, E is an element selected from the group consisting of gallium, iron, boron and mixtures thereof, "x" is the mole fraction of E and has a value from 0 to 1.0, "y" is the mole ratio of Si to (Al + E) and varies from greater than 5 to 40 and "z" is the mole ratio of O to (Al + E) and has a value determined by the equation:

$$z = (m + r1 + r2 + 3 + 4 \bullet y)/2$$

and is characterized in that it has the x-ray diffraction pattern having at least the d-spacings and intensities set forth in Table A:

TABLE A

2θ	d(Å)	I/I_0%
7.96-8.06	10.96-11.09	m
8.72-8.85	9.97-10.10	w
9.40-9.41	9.36-9.40	w
12.96-13.01	6.79-6.82	w
19.10-19.17	4.62-4.64	m
20.54-20.62	4.30-4.32	vs
22.23-22.33	3.97-3.99	m
23.29-23.42	3.79-3.81	m-w
23.97-24.08	3.69-3.70	m
26.01- 26.13	3.40-3.42	w
26.54-26.62	3.34-3.35	m
27.24-27.32	3.26-3.27	m
28.86-29.00	3.07-3.09	w
33.16-33.29	2.68-2.69	w
35.46-35.52	2.52	w

and is thermally stable up to a temperature of at least 600°C and has a BET surface area of less than 420 m^2/g.

2. The process of claim 1 wherein the hydrocarbon conversion process is selected from the group consisting of alkylation, de-alkylation, trans-alkylation of aromatics, isomerization of aromatics, alkylation of olefins with isoparaffin, olefin dimerization, olefin oligomerization, catalytic cracking, and dewaxing.

3. The process of claim 1 wherein the hydrocarbon conversion process is an aromatic conversion selected from the group consisting of xylene isomerization, toluene disproportionation, ring opening and cracking to remove benzene co-boilers and alkylation of aromatics with paraffins.

4. The process of claim 2 wherein said hydrocarbon conversion process is an alkylation process.

5. The process of claim 2 wherein said hydrocarbon conversion process is a catalytic cracking process.

6. The process of claim 1 wherein said modified UZM-43 microporous crystalline zeolite has an EUO-NES-NON framework structure comprising from 33-34 wt-% EUO, 24-31 wt-% NES and 34-43 wt-% NON.

7. The process of claim 1 wherein said catalyst further comprises alumina.

CLAIMS

The invention claimed is:

1. A hydrocarbon conversion process comprising contacting a hydrocarbon stream with a catalyst at hydrocarbon conversion conditions to give a converted product, the catalyst comprising a modified UZM-43 microporous crystalline zeolite, wherein the modified UZM-43 has a three-dimensional framework of at least AlO_2 and SiO_2 tetrahedral units and an empirical composition on an anhydrous basis expressed by an empirical formula of:

$$M_m+R1_{r1}R2_{r2}Al_{1-x}E_xSi_yO_z$$

where M represents sodium or a combination of sodium and potassium exchangeable cations, “m” is the mole ratio of M to (Al+E) and varies from about 0.05 to about 5, R1 is a singly charged propyltrimethylammonium cation, “r1” is the mole ratio of R to (Al+E) and has a value of about 0.25 to about 8.0, R2 is an amine, “r2” is the mole ratio of R to (Al+E) and has a value of about 0.0 to about 5, E is an element selected from the group consisting of gallium, iron, boron and mixtures thereof, “x” is the mole fraction of E and has a value from 0 to about 1.0, “y” is the mole ratio of Si to (Al+E) and varies from greater than 5 to about 40 and “z” is the mole ratio of 0 to (Al+E) and has a value determined by the equation:

$$z=(m+r1+r2+3+4\cdot y)/2$$

and is characterized in that it has the x-ray diffraction pattern having at least the d-spacings and intensities set forth in Table A:

TABLE A

2θ	d(Å)	I/I_0 %
7.96-8.06	10.96-11.09	m
8.72-8.85	9.97-10.10	w
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12.96-13.01	6.79-6.82	w
19.10-19.17	4.62-4.64	m
20.54-20.62	4.30-4.32	vs
22.23-22.33	3.97-3.99	m
23.29-23.42	3.79-3.81	m-w
23.97-24.08	3.69-3.70	m
26.01-26.13	3.40-3.42	w
26.54-26.62	3.34-3.35	m
27.24-27.32	3.26-3.27	m
28.86-29.00	3.07-3.09	w
33.16-33.29	2.68-2.69	w
35.46-35.52	2.52	w

and is thermally stable up to a temperature of at least 600° C. and has a BET surface area of less than about 420 m^2/g wherein said modified UZM-43 microporous crystalline zeolite has an EUO-NES-NON framework structure comprising from about 33-34 wt-% EUO, 24-31 wt-% NES and 34-43 wt-% NON.

2. The process of claim 1 wherein the hydrocarbon conversion process is selected from the group consisting of alkylation, de-alkylation, trans-alkylation of aromatics, isomerization of aromatics, alkylation of olefins with isoparaffin, olefin dimerization, olefin oligomerization, catalytic cracking, and dewaxing.

3. The process of claim 1 wherein said catalyst further comprises alumina.