

7. The method of claim 5, wherein the temperature in step (i) range from 380 °C to 450 °C.
8. The method of claim 5, wherein said pressure in step (i) ranges from 50 Bar to 180 Bar.
9. A method for treating a hydrocarbon containing feedstock which has a boiling point greater than 300 °C, comprising:
 - (i) simultaneously combining said feedstock with an upgrading catalyst precursor, wherein said catalyst precursor contains one or more of a Group VI, Group VII, Group VIIIB, alkali, or alkaline metal, on an alumina, alumina silica, silica, or zeolite support, water and hydrogen to form a mixture;
 - (ii) transporting said mixture to a decomposition reactor;
 - (iii) heating said mixture to form an upgrading catalyst;
 - (iv) transporting said mixture to an upgrading reactor;
 - (v) upgrading said mixture at a pressure of from 30-200 Bar, to form an effluent of (a) contaminant gases, (b) hydrocarbon gases having a boiling point of from 36 °C to 180 °C, (c) gas oil having a boiling point of from 180 °C to 375 °C, and (d) unconverted bottoms;
 - (vi) fractionating (a), (b), and (c) from said unconverted bottoms in a fractionation zone;
 - (vii) transporting said unconverted bottoms to a hydrotreating reactor which contains a hydrotreating catalyst, and hydrotreating said unconverted bottoms at a temperature of from about 300 °C to about 500 °C, an LHSV of from 0.1 to 20h⁻¹ and a pressure of from about 1 Bar to about 200 Bar, to form a fractionate of (a), (b), and (c) and unconverted bottoms;
 - (viii) transporting (a), (b), and (c) produced in step (v) and (vii) to a fractionation zone to separate (a), (b), and (c) from each other, and
 - (ix) recycling any unconverted bottoms from (vii) to said decomposition reactor for further processing.

10. The method of claim 9, wherein said temperature in step (vii) ranges from 380 °C to 450 °C.
11. The method of claim 9, wherein said pressure in step (vii) ranges from 50 Bar to 180 Bar.
12. The method of claim 9, wherein said hydrotreating reactor is a fixed bed, moving bed, slurry, plug flow, or CSTR.
13. The method of claim 9, wherein each reactor is a single or multiple reactors.
14. The method of claim 9, further comprising hydrotreating said unconverted bottoms at a pressure of from 50 Bar to 200 Bar.
15. The method of claim 9, wherein said pressure is from 30 to 100 Bar.
16. The method of claim 9, wherein said catalyst contains an alkali or alkaline metal.
17. The method of claim 16, wherein said catalyst is an alkali metal.
18. The method of claim 16, wherein said catalyst is an alkaline metal.