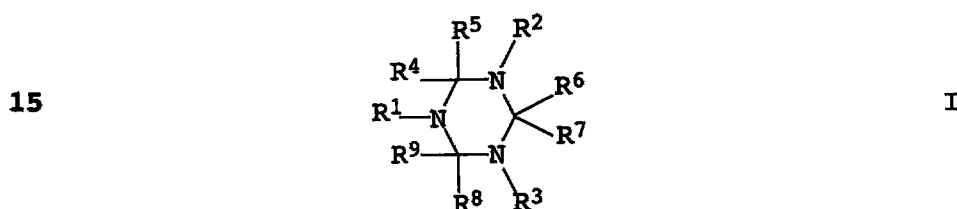


Oligomerization catalyst

The present invention relates to an oligomerization catalyst for
5 olefins, obtainable from

- a) a chromium compound CrX_3 and the at least equimolar amount,
based on the chromium compound CrX_3 , of a ligand L or from an
existing chromium complex CrX_3L , in which the groups X are,
10 independently of one another, abstractable counterions and L
is a 1,3,5-triazacyclohexane of the formula I



- 20 where the groups R^1 to R^9 are, independently of one another:
hydrogen or organosilicon or substituted or unsubstituted
carboorganic groups having from 1 to 30 carbon atoms, where
two geminal or vicinal radicals R^1 to R^9 may also be joined to
form a five- or six-membered ring, and
25 b) at least one activating additive.

The present invention further relates to a process for preparing
oligomers of olefins using the novel catalysts, to the oligomers
30 obtainable in this way and to the oxo alcohols obtainable from
these oligomers.

Olefin oligomers having up to 30 carbon atoms have great economic
importance as copolymers [sic] for plastics (e.g. 1-hexene) or as
35 precursors of oxo alcohols (e.g. 1-hexene and the decenes and
tetradecenes), where the latter are in turn constituents of
surfactants and plasticizers for plastics. In an integrated
chemical production complex, oligomerization processes are a
central step from the industrial olefin streams coming, for
40 example, from the steam crackers to products used in daily life.

The use of catalysts comprising compounds of chromium, amines and
aluminum compounds in the oligomerization of α -olefins is
generally known:

According to EP-A 780 353, olefins can be oligomerized, in particular trimerized, in the presence of a chromium source, a pyrrole-containing compound and a metal alkyl. However, the pretreatment of the catalyst is associated with a loss of active constituents.

DE-A 196 07 888 discloses an oligomerization catalyst for α -olefins which comprises a chromium compound and an aluminum compound together with at least one nitrogen-containing compound which may be a pyrrole. Here too, the catalyst pretreatment as described in EP-A 780 353 causes considerable losses.

EP-A 537 609 teaches a process in which ethylene is reacted in the presence of a chromium complex having a coordinated polydentate ligand and an aluminoxane to give a mixture of α -olefins having a relatively high proportion of 1-hexene. However, owing to the low catalyst activity together with a low trimerization selectivity, the economics of the process described are unsatisfactory.

Experiments on the selective trimerization of ethylene to 1-hexene using an N,N,N-trioctyltriaza-cyclohexane-chromium complex and methylaluminoxane were reported at the 215th ACS National Meeting, March 29 - April 2, 1998 in Dallas, Texas. However, the catalyst has only moderate activity and it also leads to considerable amounts of polymeric products, which is a disadvantage for the economics of the process.

It is an object of the present invention to provide stable catalysts which can be obtained more inexpensively and have improved activity and selectivity in respect of low molecular weight oligomers of olefins.

We have found that this object is achieved by the oligomerization catalysts mentioned at the outset.

We have also found a process for preparing oligomers of olefins using the novel catalysts. The invention further provides the oligomers obtainable in this way and the oxo alcohols obtainable from these oligomers.

The oligomerization catalysts of the present invention makes it possible to obtain oligomers of olefins in high yields and with a small proportion of by-products whose molar mass M_w is greater than 500. In particular, the catalyst has a high selectivity in respect of the trimerization of α -olefins and especially ethene.

- Triazacyclohexane and its derivatives, which differ in terms of different substitution patterns on the ring atoms, have been known for a long time and are used in a variety of ways in industry, since they can usually be prepared from readily available starting materials in a simple and inexpensive manner. Thus, triazacyclohexane derivatives are used, for example, in the desulfurization of kerosene. However, the use of triazacyclohexane and its derivatives as ligands in the preparation of organic metal complexes is not very widespread.
- 10 Only a few complexes containing these ligands have been described in the literature, for example in J. Chem. Soc., Dalton Trans. (1997), 1363-1368; Z. Naturforsch., part B50 (1995), 1038-1043; Angew. Chem. Int. Ed. Engl. 33 (1994), 1877-1878; J. Organomet. Chem. 501 (1995), 303-307; Chem. Ber. 129 (1996), 25-27; J. Organomet. Chem. 520 (1996), 121-129; Inorg. Chem. 36 (1997), 6064-6069; Chem. Ber. 129 (1996), 1327-1333.

Varying the substituents on the 1,3,5-triazacyclohexane ring allows the properties of the catalyst of the present invention to be influenced. Thus, the catalyst activity can normally be increased by substituents, in particular on the nitrogen atoms. The number and geometry of the substituents additionally enables the accessibility of the central atom to the α -olefins which are to be reacted and thus also the selectivity of the reaction in respect of various starting olefins to be controlled. The chemical structure of the substituents R^1 to R^9 can therefore be varied within a wide range in order to obtain a catalyst tailored to the particular reaction.

30 Possible substituted or unsubstituted carboorganic groups on the 1,3,5-triazacyclohexane ring are, for example:

- C_1 - C_{18} -alkyl, preferably C_1 - C_{12} -alkyl, e.g. methyl, ethyl, N,N-dimethylaminoethyl, n-propyl, i-propyl, butyl, pentyl, hexyl, 2-ethylhexyl, heptyl, octyl, nonyl, decyl, dodecyl, 1,1-dimethyldodecyl,
- 5- to 7-membered cycloalkyl which may in turn bear a C_1 - C_{10} -aryl group as substituent, e.g. cyclopentyl and cyclohexyl,
- C_6 - C_{15} -aryl such as phenyl, o-tolyl, p-tolyl, m-tolyl, 1-naphthyl and 2-naphthyl or
- 45 - C_6 - C_{15} -arylalkyl, preferably C_6 - C_8 -arylalkyl such as benzyl and 1-phenylethyl.

Possible organosilicon groups are, for example: trialkylsilyl groups having from 1 to 10 carbon atoms in identical or different alkyl radicals, in particular trimethylsilyl groups.

- 5 Substituents in the C-organic groups or Si-organic groups on the 1,3,5-triazacyclohexane ring may in particular be alkyl groups with donor groups. The donor group may be neutral or anionic and may contain a heteroatom from groups 15-16 of the periodic system (according to IUPAC proposal 1985) or may be a carbanion. If it
- 10 is neutral, it may be coordinately bonded to the chromium. Preferably it is coordinated to the chromium. If the donor is formally anionic, then it is covalently bonded to the metal center. The bonds may be intramolecular or intermolecular; preferably, they are intramolecular. Preference is given to
- 15 neutral donors containing oxygen and/or nitrogen atoms which have free electron pairs, it also being possible for the oxygen and/or nitrogen atoms to have been inserted into an alkyl chain.

- Preference is given to 1,3,5-triazacyclohexane ligands in which
- 20 the groups R^1 , R^2 and R^3 are, independently of one another, substituted or unsubstituted C_1 - C_{12} -alkyl, C_6 - C_{15} -aryl or C_6 - C_8 -arylalkyl, in particular substituted or unsubstituted C_1 - C_{12} -alkyl or C_6 - C_8 -arylalkyl, e.g. methyl, ethyl, N,N -dimethylaminoethyl, n -propyl, n -butyl, *tert*-butyl, hexyl,
- 25 octyl, dodecyl, 1,1-dimethyldodecyl, 1-phenylethyl.

- In the process of the present invention, particular preference is given to using 1,3,5-triazacyclohexane ligands in which the groups R^4 , R^5 , R^6 , R^7 , R^8 and R^9 are, independently of one another,
- 30 hydrogen or C_1 - C_4 -alkyl, in particular hydrogen or methyl.

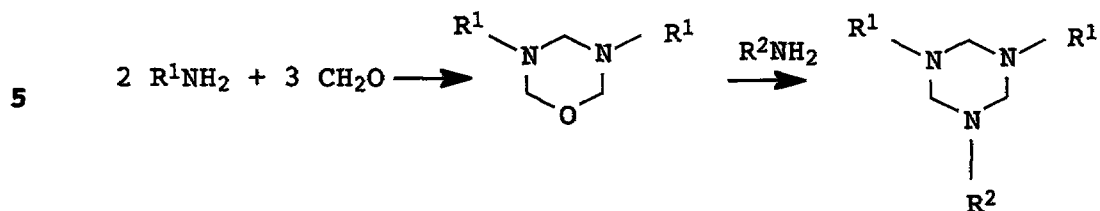
- Preferred 1,3,5-triazacyclohexanes are
- 1,3,5-tri-*tert*-butyl-1,3,5-triazacyclohexane,
- 1,3,5-triethyl-1,3,5-triazacyclohexane,
- 35 1,3,5-tris(1-phenylethyl)-1,3,5-triazacyclohexane,
- 1,3,5-tris(1,1-dimethyldodecyl)-1,3,5-triazacyclohexane and
- 1,3-di- n -dodecyl-5-[2-(N,N -dimethylamino)ethyl]-1,3,5-triazacyclohexane and particularly preferably 1,3,5-tri- n -octyl-1,3,5-triazacyclohexane, 1,3,5-tri- n -dodecyl-1,3,5-triazacyclohexane,
- 40 1,3,5-tribenzyl-1,3,5-triazacyclohexane,
- 1,3,5-tris(2-ethylhexyl)-1,3,5-triazacyclohexane,
- 1,3,5-tris(2- n -propylheptyl)-1,3,5-triazacyclohexane.

- The 1,3,5-triazacyclohexanes of the formula I in which the groups
- 45 R^4 to R^9 are hydrogen and the groups R^1 to R^3 are identical can be prepared in a manner known per se, for example by reacting primary amines of the R^1NH_2 type with formaldehyde or

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paraformaldehyde. Correspondingly, the 1,3,5-triazacyclohexanes, which bear one methyl group and one hydrogen atom on each of the carbon atoms of the ring are obtainable via acetaldehyde.

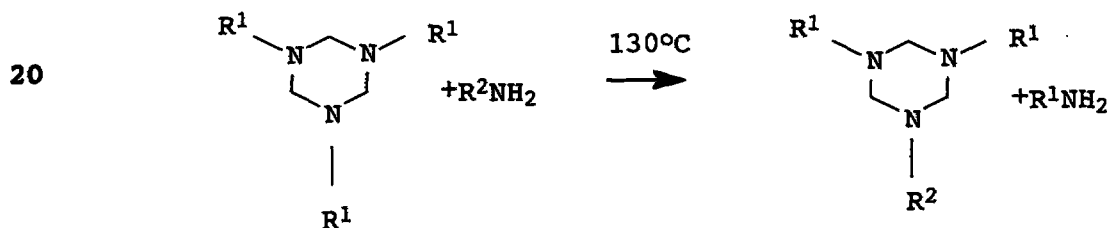
- 5 The 1,3,5-triazacyclohexanes of the formula I in which at least one of the radicals R^1 , R^2 and R^3 is different from the other radicals of this set can also be prepared in a manner known per se (cf., for example, Beilstein, "Handbook of Organic Chemistry", 4th Ed., Vth Suppl. Series, Springer-Verlag, Berlin, Vol. 26
- 10 (1986) 3 ff. and the references cited therein; R = octyl: J. Polym. Sci., Polym. Chem. Ed. 329 (1993), 1941-1958; J. Prakt. Chem. 327 (1985), 739-748; EP-A 620 266; DE-A 24 31 862; DE-A 41 00 856; Pharmazie 30 (1975), 699-706). A few of the known preparative methods are briefly outlined here by way of example:
- 15
- 1) The reaction of a mixture of two primary amines (R^1NH_2 and R^2NH_2) with formaldehyde (as aqueous solution or paraformaldehyde) leads to a mixture of various products which can be separated as follows:
- 20
- a) Distillation in the case of sufficiently small R^1 and R^2 .
- b) Carrying out the reaction using a large excess of the amine R^1NH_2 , if the symmetrical reaction product is
- 25 capable of being distilled off. After the distillation, the unsymmetrical product then remains.
- c) Selective crystallization of one product.
- 30 d) Complexation of the mixture of the 1,3,5-triazacyclohexanes with the chromium compound, for instance $CrCl_3$, and separation of the chromium complexes obtained, for instance by column chromatography.
- 35 2) Reaction of an amine R^1NH_2 with an excess of formaldehyde to give a mixture of symmetrically substituted 1,3,5-triazacyclohexane and the corresponding 1-oxa-3,5-diazacyclohexane: in a second step, the 1-oxa-3,5-diazacyclohexane is reacted with an amine R^2NH_2 (if
- 40 desired in the presence of an acid catalyst), resulting in the ring oxygen being replaced by an R^2N .



10

The product mixture can be separated as described under 1).

- 3) Reaction of a symmetrical 1,3,5-triazacyclohexane having a small R^1 (methyl or ethyl) at about 130°C with an amine R^2NH_2 .
 15 At this temperature, R^1NH_2 is given off and a mixture of unsymmetrical 1,3,5-triazacyclohexanes is formed.



25

The separation can be carried out as described under 1).

- 4) Reaction of two different symmetrical
 30 1,3,5-triazacyclohexanes with one another, resulting in substituent exchange. The products can be separated as described under 1).

Suitable groups X in the chromium compounds CrX_3 or the chromium
 35 complexes CrX_3L are any abstractable counterions that are suitable for this purpose in organometallic chemistry, in particular

- halogen such as fluorine, bromine, iodine and especially chlorine,
- 40 - tosylate, triflate, tetrafluoroborate, hexafluorophosphate, hexafluoroantimonate, tetraphenylborate,
- C_1 - to C_{10} -carboxy, especially 2-ethylhexanoate,
- alkyl groups, for example methyl, ethyl, i-propyl, phenyl benzyl,
- 45 - bulky noncoordinating anions such as $\text{B}(\text{C}_6\text{F}_5)_4^-$.

The groups X are selected in particular such that the chromium compounds CrX_3 or chromium complexes CrX_3L in which they are present possess good solubility in the particular solvent used.

- 5 As starting materials for the chromium compounds CrX_3 and the chromium complexes CrX_3L , use is made of, for instance, chromium halides such as CrCl_3 , CrBr_3 , $\text{Cr}(\text{triflate})_3$, $\text{Cr}(\text{III})$ alkoxylates such as the 2-ethylhexanoate and also complexes of these chromium compounds with weakly bound, neutral complexing ligands which may
 10 be displaced by the 1,3,5-triazacyclohexane and possibly by the five-membered aromatic N-heterocycle, e.g. ether complexes such as $\text{CrCl}_3(\text{tetrahydrofuran})_3$, $\text{CrCl}_3(\text{dioxane})_3$, ester complexes such as $\text{CrCl}_3(\text{n-butyl acetate})$, $\text{CrCl}_3(\text{ethyl acetate})$, alcohol complexes such as $\text{CrCl}_3(\text{i-propanol})_3$, $\text{CrCl}_3(\text{2-ethylhexanol})_3$, amine complexes
 15 such as $\text{CrCl}_3(\text{pyridine})_3$, $\text{CrCl}_3(\text{i-propylamine})_2$, or nitrile complexes such as $\text{CrCl}_3(\text{acetonitrile})_3$. acetonitrile.

- In a preferred embodiment of the process of the present invention, use is made of oligomerization catalysts which have
 20 been prepared using chromium complexes CrX_3L which have been prepared and isolated beforehand in-house.

- The chromium complexes CrX_3L are moreover obtainable by methods known to those skilled in the art or by methods analogous to
 25 these (cf., for example, W. A. Herrmann, A. Salzer: "Synthetic Methods of Organometallic and Inorganic Chemistry", Vol. 1 - Literature, Laboratory Techniques, and Common Starting Materials, Thieme Verlag, Stuttgart, 1996).

- 30 The preparation of the chromium complexes CrX_3L in situ is generally carried out by dissolving or suspending the chromium compound CrX_3 in the reaction medium and adding the 1,3,5-triazacyclohexane either as such or in dissolved form.

- 35 In the oligomerization process of the present invention, preference is given to using chromium complexes CrX_3L in which X and L have the following meanings:

- X are, independently of one another: halogen, tosylate,
 40 triflate, alkyl,

- L is a 1,3,5-triazacyclohexane of the formula I, in which the groups R^4 , R^5 , R^6 , R^7 , R^8 and R^9 are, independently of one another, hydrogen or $\text{C}_1\text{-C}_4$ -alkyl, in particular hydrogen or
 45 methyl, and in which R^1 , R^2 and R^3 are, independently of one another, methyl, ethyl, N,N-dimethylaminoethyl, propyl,

n-butyl, tert-butyl, hexyl, octyl, dodecyl,
1,1-dimethyldodecyl or (1-phenyl)ethyl.

Particular preference is given to using chromium complexes CrX_3L ,
5 in which X and L have the following meanings:

X are, independently of one another: chlorine, tosylate,

10 L is a 1,3,5-triazacyclohexane of the formula I, in which the
groups R^4 , R^5 , R^6 , R^7 , R^8 and R^9 are, independently of one
another, hydrogen or methyl and in which R^1 , R^2 and R^3 are,
independently of one another, methyl, ethyl,
N,N-dimethylaminoethyl, propyl, n-butyl, tert-butyl, hexyl,
octyl, dodecyl, 1,1-dimethyldodecyl or 1-phenylethyl.

15 In one preferred embodiment of the process of the invention, the
activating additive is composed of an unsubstituted or
substituted five-membered aromatic N-heterocycle and at least one
aluminum alkyl, some of whose alkyl groups may have been replaced
20 by halogen and/or alkoxy.

Suitable five-membered aromatic N-heterocycles are ones having 1,
2, 3 or 4, preferably 1 or 2, nitrogen atoms in a five-membered
aromatic ring. The five-membered aromatic N-heterocycles may be
25 substituted on the ring carbons by groups which are inert under
the reaction conditions, e.g. alkyl groups, preferably methyl
and/or ethyl, or two adjacent carbon atoms of the five-membered
aromatic N-heterocycle may together be part of a fused-on
aromatic carbocyclic system which may in turn bear inert groups.
30 Examples of such N-heterocycles are unsubstituted and substituted
pyrroles, pyrazoles, imidazoles, triazoles and tetrazoles, e.g.
pyrrole, 2,5-dimethylpyrrole, indole, carbazole, pyrazole,
indazole, imidazole, benzimidazole. Preference is given to using
pyrroles and, in particular, alkyl-substituted pyrroles,
35 especially 2,5-dimethylpyrrole.

As aluminum alkyl, in which some of the alkyl groups may be
replaced by halogen and/or alkoxy, it is possible to use aluminum
alkyls of the formulae AlR_3 , AlR_2Hal , AlRHal_2 , $\text{AlR}_2\text{OR}'$, $\text{AlRHalOR}'$
40 and $\text{Al}_2\text{R}_3\text{Hal}_3$ and mixtures thereof, where R and R' are each,
independently of one another, methyl, ethyl or a straight-chain
or branched C_3 - C_8 -alkyl group and Hal is fluorine, bromine, iodine
or especially chlorine, for example trimethylaluminum,
triethylaluminum, tri-n-propylaluminum, tri-iso-propylaluminum,
45 tributylaluminum, diethylaluminum chloride, diethylaluminum
bromide, diethylaluminum ethoxide, diethylaluminum phenoxide,
ethylaluminum ethoxide chloride. Preference is given to using

aluminum alkyls of the AlR_3 and $AlRHal_2$ type, with triethylaluminum or a mixture of triethylaluminum and ethylaluminum dichloride being particularly preferred.

5 As an alternative to aluminum alkyls in which some of the alkyl groups are replaced by halogen and/or alkoxy, it is also possible to use mixtures of the corresponding aluminum alkyls and suitable cocatalysts, from which the desired mixed aluminum compounds are formed in situ in the reactor.

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Suitable cocatalysts are alkyl halides, alkylsilicon halides and Lewis-acid metal halides, preferably n-butyl chloride, n-butyl iodide, trimethylsilyl chloride, trimethylsilyl bromide, tin tetrachloride, germanium chloride and especially n-butyl bromide.

15

In the system comprising aluminum alkyl, some of whose alkyl groups may be replaced by halogen and/or alkoxy, and cocatalyst, the two components are present in a molar ratio of from 1 : 3 to 30 : 1, preferably from 1 : 1 to 15 : 1.

20

In the process of the present invention, the amount of chromium compound CrX_3 or chromium complex CrX_3L is normally in the range from 1×10^{-7} to 1 mol, preferably from 1×10^{-6} to 0.1 mol and in particular from 1×10^{-5} to 0.01 mol per kg of reaction mixture.

25

The amount of five-membered aromatic N-heterocycle is normally in the range from 1×10^{-8} to 100 mol, preferably from 1×10^{-7} to 1 mol and in particular from 1×10^{-5} to 0.05 mol per kg of reaction mixture.

30

The amount of aluminum alkyl in which some of the alkyl groups may be replaced by halogen and/or alkoxy is normally in the range from 1×10^{-8} to 500 mol, preferably from 1×10^{-7} to 10 mol and in particular from 5×10^{-5} to 0.5 mol, per kg of reaction

35 mixture.

In the process of the present invention, the molar ratio of the components (a), (b) and (c) is 1 : 0.1-100 : 0.1-500, preferably 1 : 0.1-10 : 1-100 and in particular 1 : 1-5 : 5-50.

40

Very particular preference is given to a catalyst consisting of (a) (1,3,5-tri-n-octyl-1,3,5-triazacyclohexane) $CrCl_3$ or (1,3,5-tribenzyl-1,3,5-triazacyclohexane) $CrCl_3$, (b) 2,5-dimethylpyrrole and (c) triethylaluminum and ethylaluminum

45 dichloride, where these components are present in a molar ratio of 1 : 0.1-10 : 0.1-100, preferably 1 : 1-5 : 5-50. The molar

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ratio of triethylaluminum and ethylaluminum dichloride in component (c) is 1-50:1, preferably 3-20:1.

The oligomerization is preferably carried out in a solvent.

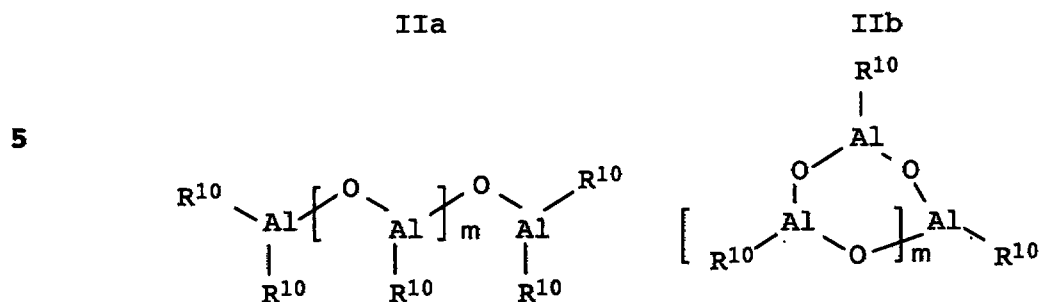
- 5 Solvents which can be used for the oligomerization are straight-chain, branched or alicyclic saturated hydrocarbons having from 1 to 20 carbon atoms, e.g. butane, pentane, 3-methylpentane, hexane, heptane, 2-methylhexane, octane, cyclohexane, methylcyclohexane, 2,2,4-trimethylpentane, or
- 10 decalin, straight-chain or branched halogenated hydrocarbons such as dichloroethane, aromatic hydrocarbons such as benzene, toluene, xylene, ethylbenzene, mesitylene, or tetralin and the oligomeric reaction products which are liquid under the reaction conditions, e.g. 1-hexene itself. The solvents can be used either
- 15 individually or as mixtures.

Preferred oligomerization catalysts in accordance with the invention are also those comprising an alkylalumoxane as the activating additive.

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- In this context, very particular preference is given to those ligands L in which the groups R^1 , R^2 and R^3 in part or in whole, and independently of one another, are a group which carries a substituent attached via a carbon atom, in particular an alkyl,
- 25 aryl or silyl group, in the β position or in a position even more remote from the nitrogen atom of the 1,3,5-triazacyclohexane ring. With particular preference, this substituent is in the β position. With further particular preference, this substituent is a β -alkyl substituted alkyl, especially 2-ethylhexyl or
- 30 2-n-propylheptyl. Among these ligands L, very particular preference in turn is given to those in which the groups R^4 , R^5 , R^6 , R^7 , R^8 and R^9 are hydrogen.

- Suitable alkylalumoxanes are known, for example, from DE-A 30 07
- 35 725, their structures being largely unelucidated. They are products of the careful partial hydrolysis of aluminum alkyls (cf. DE-A 30 07 725). These products are evidently not present in their pure form but are instead mixtures of open-chain and cyclic structures of type IIa and IIb which are presumably in dynamic
- 40 equilibrium with one another.



In the formulae IIa and IIb, the groups R^{10} are identical or different and independently of one another are C_1 - C_{12} -alkyl such as methyl, ethyl, n-propyl, i-propyl, n-butyl, i-butyl, sec-butyl, tert-butyl, n-pentyl, i-pentyl, sec-pentyl, neopentyl, 1,2-dimethylpropyl, i-amyl, n-hexyl, i-hexyl, sec-hexyl, n-heptyl, i-heptyl, n-octyl, n-nonyl, n-decyl, and n-dodecyl; preferably C_1 - C_6 -alkyl such as methyl, ethyl, n-propyl, i-propyl, n-butyl, i-butyl, sec-butyl, tert-butyl, n-pentyl, i-pentyl, sec-pentyl, neopentyl, 1,2-dimethylpropyl, i-amyl, n-hexyl, i-hexyl, sec-hexyl, with methyl being particularly preferred. m is an integer from 0 to 40, preferably from 0 to 25, and with particular preference from 0 to 22.

25 In the literature, cage-like structures for alumoxanes are also discussed (cf. Organometallics 1996, 15, pages 2213-26; Macromol. Symp. 1995, 97, pages 15-25).

The alkylalumoxanes are effective as activating additives in the context of the present invention independently of their structural constitution.

The amount of the activating alkylalumoxane used is dependent on its nature. The ratio of chromium compound CrX_3 and/or chromium complex CrX_3L to the activating alkylalumoxane is generally from 1:0.1 to 1:10 000, preferably from 1:1 to 1:1 000.

Suitable solvents when using an oligomerization catalyst comprising CrX_3 , a ligand L and the alkylalumoxane, or comprising CrX_3L and the alkylalumoxane, are aprotic solvents, examples being the aliphatic or aromatic hydrocarbons cited earlier above as solvents, and especially toluene.

In another preferred embodiment of the process of the invention, an oligomerization catalyst is used which comprises as activating additive at least one boron compound and at least one aluminum

alkyl, some of whose alkyl groups may have been replaced by halogen and/or alkoxy.

- Examples of suitable boron compounds are those containing
- 5 electron-withdrawing radicals (e.g. trispentafluorophenylborane, N,N-dimethylanilinium tetrakis(pentafluorophenyl)borate, tri-n-butylammonium tetrakis(pentafluorophenyl)borate, N,N-dimethylanilinium tetrakis(3,5-bis(perfluoromethyl)-phenyl)borate, tri-n-butylammonium
 - 10 tetrakis(3,5-bis(perfluoromethyl)phenyl)borate, and tritylium tetrakis(pentafluorophenyl)borate). These activating additives are known from EP-A 468 537 and also EP-A 426 638. Preference is given to tritylium tetrakis(pentafluorophenyl)borate, trispentafluorophenylborane, and especially dimethylanilinium
 - 15 tetrakis(pentafluorophenyl)borate.

The amount of the activating boron compound used is dependent on its nature. The ratio of chromium compound CrX_3 and/or chromium complex CrX_3L to the activating boron compound is generally from

20 1:0.1 to 1:10 000, preferably from 1:1 to 1:1 000.

Suitable aluminum alkyls some of whose alkyl groups may be replaced by halogen and/or alkoxy are the representatives of this class of substance cited on earlier on above, in the amounts

25 specified there relative to the chromium compound CrX_3 and/or the chromium complex CrX_3L .

Suitable solvent in this context are aprotic solvents, examples being the aliphatic or aromatic hydrocarbons cited earlier on

30 above as solvents, and especially toluene.

Preferred olefins for oligomerization by the process of the invention are straight-chain and branched α -olefins having preferably from 2 to 10, in particular from 2 to 6 and especially

35 from 2 to 4, carbon atoms and mixtures thereof, and with very particular preference, in each case on its own: 1-propene, 1-butene, 1-hexene, 1-decene, and especially ethene, 1-butene, especially 1-butene in the mixture with its isomers such as is present, for instance, in the raffinate II.

40

Owing to the tendency of the aluminum compounds in particular and possibly the cocatalysts to hydrolyze, the oligomerization is generally to be carried out with very substantial exclusion of moisture. Techniques known per se can be employed for this

45 purpose. The oligomerization is preferably carried out under protective gas using baked-out apparatuses. Protective gases which can be used are all gases which are chemically inert under

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the reaction conditions, advantageously nitrogen or argon. In addition, the α -olefin to be reacted can itself assume the function of a protective gas as long as it has a sufficiently high vapor pressure under the reaction conditions.

5

The oligomerization is preferably carried out at from 1 to 120°C, in particular from 70 to 110°C, and preferably at a pressure in the range from 3 to 120 bar. The pressure is advantageously selected so that the reaction mixture is liquid at the

10 temperature set.

The process of the present invention can be carried out batchwise or continuously, with the continuous mode being preferred on an industrial scale.

15

Reactors suitable for carrying out the process of the present invention continuously are well known to those skilled in the art, for example from Ullmann's Enzyklopädie der technischen Chemie, Volume 1, 3rd edition, 1951, page 743 ff.; pressure-rated

20 reactors are also described there on page 769 ff.

The remaining boundary conditions of such oligomerization reactions are set by a person skilled in the art on the basis of his general technical knowledge, which he can, for example,

25 derive from DE-A 196 07 888.

The deactivation of the catalyst at the end of the reaction can be carried out using, in principle, a number of substances which all have the ability to hydrolyze aluminum alkyl compounds, for

30 example water and monoalcohols having from 1 to 10 carbon atoms. Mineral acids may also be added to these substances.

The products of the oligomerization of the present invention are advantageously purified by distillation. In this way, for

35 example, the reaction product from the ethene oligomerization can be fractionated to give not only the main (hexene) fraction consisting predominantly of 1-hexene but also a decene fraction and a tetradecene fraction. The latter two fractions consist predominantly of branched, internal olefins.

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To achieve a high total conversion in the process of the present invention, unreacted starting material can be recovered and returned to the reaction.

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Preferred products of the process of the present invention are trimers of α -olefins, especially of α -olefins having from 2 to 6 carbon atoms, and particularly preferably the 1-hexene obtainable from ethene.

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The oligomers obtainable with the process of the invention are especially suitable for preparing monoalcohols for plasticizers and surfactants. For this purpose the oligomers are appropriately subjected to hydroformylation, in the course of which mixtures of
10 the aldehydes and alcohols, chain-extended by one carbon atom, are formed, these mixtures being subsequently hydrogenated to give the desired alcohols. The implementation of the hydroformylation and hydrogenation is known per se to the skilled worker and therefore requires no further elucidation (cf., e.g.,
15 Beller et al., Journal of Molecular Catalysis A 104 (1995) pages 17-85).

The following examples illustrate the invention.

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Examples

A) Catalysts

- 5 2,5-Dimethylpyrrol, $\text{CrCl}_3(\text{THF})_3$, 1,3,5-tribenzyl-1,3,5-triazacyclohexane and triethylaluminum were procured from Aldrich Chemical Company Ltd. and kieselguhr from Riedel de Haen AG.

10 Preparation of the 1,3,5-triazacyclohexanes

Preparation of 1,3,5-tri-n-octyl-1,3,5-triazacyclohexane

- 100 g (0.774 mol) of n-octylamine were added in small portions to
 15 a suspension of 20.2 g (0.673 mol) of paraformaldehyde in 500 ml of toluene which was cooled to 0°C. On subsequent heating of the mixture to the boiling point, the paraformaldehyde went into solution. Water and toluene were then distilled off. The residue was freed of volatile constituents at 1 mbar, taken up in 100 ml
 20 of methanol and filtered through a 1 cm thick layer of silica gel. The volatile constituents of the filtrate were subsequently removed at 1 mbar, giving 82.3 g (83% yield) of the title compound as a viscous, clear liquid.

- 25 The following 1,3,5-triazacyclohexanes were prepared in an analogous manner:

- 1,3,5-tri-n-dodecyl-1,3,5-triazacyclohexane
- 1,3,5-tri-tert-butyl-1,3,5-triazacyclohexane
- 30 - 1,3,5-triethyl-1,3,5-triazacyclohexane
- 1,3,5-tris(1-phenylethyl)-1,3,5-triazacyclohexane
- 1,3,5-tris(1,1-dimethyldodecyl)-1,3,5-triazacyclohexane
- 1,3-di-n-dodecyl-5-[2-(N,N-dimethylamino)ethyl]-1,3,5-triazacyclohexane
- 35 - 1,3,5-tris(2-ethylhexyl)-1,3,5-triazacyclohexane
- 1,3,5-tris(2-n-propylheptyl)-1,3,5-triazacyclohexane

Preparation of the catalysts

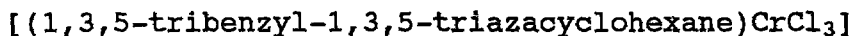
- 40 Preparation of "chromium complex 1": [(1,3,5-tri-n-octyl-1,3,5-triazacyclohexane) CrCl_3]

- 662 mg (1.768 mmol) of the tetrahydrofuran complex $\text{CrCl}_3(\text{THF})_3$ and 728 mg (1.855 mmol) of 1,3,5-tri-n-octyl-1,3,5-triazacyclohexane
 45 (see above) were placed in a reaction flask at 25°C. At -78°C, 100 ml of diethyl ether which had been dried over sodium were condensed into this mixture. The suspension obtained in this way

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was stirred for about 30 minutes at 25°C. It was then filtered through a frit and the filter residue was washed with diethyl ether until the washings were no longer green. The residue was then dried at 25°C and 1 mbar, giving 885 mg of the title compound 5 (98% yield).

Preparation of "chromium complex 2":



- 10 10 ml of dry diethyl ether were placed under argon in a baked-out glass apparatus at 25°C. 749 mg (20 mmol) of the tetrahydrofuran complex $\text{CrCl}_3(\text{THF})_3$ were suspended therein, and a solution of 715 mg (20 mmol) of 1,3,5-tribenzyl-1,3,5-triazacyclohexane in 2 ml of diethyl ether were added dropwise to the mixture while
- 15 stirring. The mixture was subsequently stirred for another 30 minutes at 20°C and then filtered under argon through a frit. The filter residue was washed three times with 10 ml each time of diethyl ether and then dried at 25°C and 1 mbar. This gave 0.64 g of the title compound as a violet solid.

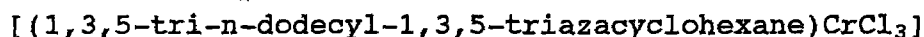
20

Preparation of the "chromium complexes 3 - 10"

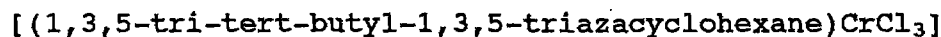
Using a method analogous to the preparation of the complexes 1 and 2, the following complexes of chromium(III) chloride were

25 prepared:

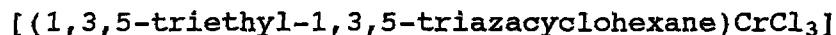
"chromium complex 3":



30 "chromium complex 4":

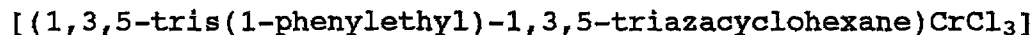


"chromium complex 5":

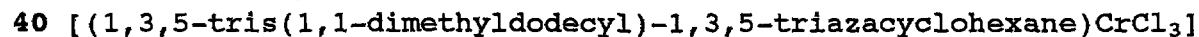


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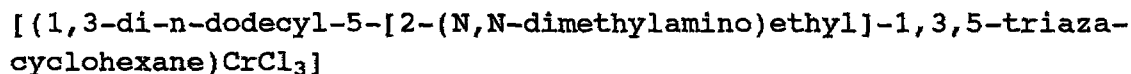
"chromium complex 6":



"chromium complex 7":



"chromium complex 8":



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"chromium complex 9"

$[(1,3,5\text{-tris(2-ethylhexyl)-1,3,5-triazacyclohexane})\text{CrCl}_3]$

"chromium complex 10"

5 $[(1,3,5\text{-tris(2-n-propylheptyl)-1,3,5-triazacyclohexane})\text{CrCl}_3]$

B) Oligomerizations

Example 1: Oligomerization of ethene in the presence of "complex
10 1" and 2,5-dimethylpyrrole

A steel autoclave having a capacity of 100 ml was baked out at 105°C in a stream of argon for 60 minutes. 14.5 mg of "chromium complex 1" were subsequently introduced at 25°C, followed by 25 ml
15 of n-heptane which had been dried over sodium and 0.5 ml of a solution of 143 mg of 2,5-dimethylpyrrole in 10 ml of n-heptane, corresponding to 0.075 mmol of 2,5-dimethylpyrrole. The autoclave was subsequently flushed three times with ethene at atmospheric pressure. 0.75 ml of a 1 molar solution of triethylaluminum in
20 n-heptane was then added, followed by pressurization with 25 bar of ethene. The temperature was subsequently increased to 80°C and the ethene pressure was increased to 40 bar. The contents of the autoclave were stirred for 2 hours under these conditions, after which the autoclave was cooled and vented. The catalyst was
25 deactivated by addition of 1 ml of water to the reaction mixture. The constituents insoluble in the reaction mixture were separated off, dried and weighed. The productivity was 18.6 kg per 1 g of chromium in the catalyst. The relative amounts of the products obtained were determined by gas chromatography using n-heptane as
30 internal standard:

hexenes	44.4% by weight
decenes	33.1% by weight
tetradecenes	10.9% by weight
35 "polymers"	1.5% by weight

Examples 2 to 11

Examples 2 to 11 were carried out using a method analogous to
40 Example 1. n-Butyl bromide (n-BuBr) and ethylaluminum dichloride (EADC) were used as 0.1M solutions in n-heptane. The starting materials, the associated amounts and the results of the experiments are shown in Table 1 below.

Table 1: Data on Examples 2 to 11

Ex.	Chromium complex CrX ₃ L	Cat [μmol]	DMP [μmol]	TEA [μmol]	Cocat [μmol]	n-Heptane [ml]	C6 [% by weight]	C10 [% by weight]	C14 [% by weight]	Polym [% by weight]	Productivity [kg/g Cr]
2	2	25	75	750	-	25	56.1	27.5	6.5	7.3	27.4
3	2	10	30	300	-	10	62.1	21.7	4.7	7.6	44.8
4	3	10	30	300	-	10	53.5	25.0	6.3	9.1	33.5
5	4	10	30	300	-	10	59.4	24.4	7.3	2.6	21.1
6	5	10	30	300	-	10	63.3	21.1	5.3	8.8	16.4
7	6	10	30	300	-	10	55.6	23.9	7.0	4.4	19.3
8	7	10	30	300	-	10	61.7	23.5	6.0	4.9	28.0
9	8	10	30	300	-	10	48.3	23.0	7.0	10.5	24.8
10	2	10	30	300	n-BuBr 30	10	68.1	20.7	6.2	2.2	75.3
11	2	10	30	300	EADC 30	10	82.8	14.3	2.1	0.3	106.1

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Abbreviations:

Cat	Amount of chromium complex CrX ₃ L	C6	Proportion of hexenes in the product
DMP	Amount of 2,5-dimethylpyrrole	C10	Proportion of decenes in the product
TEA	Amount of triethylaluminum	C14	Proportion of tetradecenes in the product
Cocat	Cocatalyst and amount	Polym	Proportion of polymers in the product
n-Heptan	Amount of n-heptane		

Example 12: Trimerization of 1-butene in the presence of "chromium complex 9" and methylaluminoxane and hydroformylation of the resulting trimer to the corresponding oxo alcohol

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a) Trimerization

A steel autoclave of a volume of 2500 ml was baked out at 120°C under a stream of argon. At 25°C, 750 mg of "chromium complex 9",
10 and 500 g of toluene, dried over sodium, were charged to the autoclave which was then flushed three times with 1-butene. Thereafter, 50 g of a 1 M solution of methylalumoxane in toluene and, via an airlock, 500 g of 1-butene were introduced into the autoclave. The temperature in the autoclave was then raised to
15 40°C and the pressure was adjusted to 15 bar using nitrogen gas. After two hours of reaction under the conditions thus established, the autoclave was cooled and let down. The catalyst was deactivated by adding 2-propanol. Subsequent analysis by gas chromatography of the reactor discharge (800 g) found the only
20 oligomers present to be isomeric dodecenes. The dodecane mixture obtained by hydrogenation had an ISO index of 2.3.

b1) Hydroformylation in the presence of cobalt carbonyl

25 1.06 kg of the dodecene mixture prepared in accordance with section a) were hydroformylated with 4.0 g of $\text{Co}_2(\text{CO})_8$ at 185°C and 280 bar of CO/H_2 (1:1) with the addition of 100 g of water in a 2500 ml rotary stirred autoclave in 5 hours. The reaction discharge was subsequently decobalted oxidatively at 90°C using
30 10% strength acetic acid and with introduction of air. The oxo product thus obtained is hydrogenated over a fixed-bed Co/Mo catalyst in a 2500 ml tube reactor operated in downflow mode at 175°C and 280 bar of H_2 with the addition of 10% by weight of water, based on the organic phase. The alcohol mixture produced
35 in this reaction was worked up by distillation and the tridecanol mixture thus isolated had an OH number of 279 mg KOH/g. A mean degree of branching of 2.7 was found by $^1\text{H-NMR}$ spectroscopy.

b2) Hydroformylation with rhodium biscarbonyl
40 acetylacetonate/polyethyleneimine

50 mg of rhodium biscarbonyl acetylacetonate, 4.5 g of a polyethyleneimine of molecular mass $M_w = 460000$, in which 60% of all the nitrogen atoms had been amidated using lauric acid, 800 g
45 of the dodecene mixture prepared in accordance with section a) and 196 g of toluene were heated to 150°C in a 2500 ml stirred lift autoclave under CO/H_2 (1:1). A pressure of 280 bar was set by

means of C₀/H₂. After 7 hours, the autoclave was cooled, let down and emptied. An olefin conversion of 93% was found by gas chromatography. The oxo product thus obtained was hydrogenated in a 2500 ml tube reactor operated in downflow mode over a fixed-bed 5 Co/Mo catalyst at 175°C and 280 bar of H₂ with the addition of 10% by weight of water, based on the organic phase. The alcohol mixture produced in this reaction was worked up by distillation and the resulting tridecanol mixture had an OH number of 279 mg KOH/g. A mean degree of branching of 2.9 was measured by ¹H-NMR 10 spectroscopy.

Examples 13-22: Trimerization in the presence of "chromium complex 9" and methylaluminoxane

15 a) Alternative preparation of "chromium complex 9"

15 ml of (+/-)-2-ethylhexylamine (92 mmol) were dissolved in 200 ml toluene, and 2.75 g of paraformaldehyde (92 mmol) were added. After the mixture had been stirred for one hour, the 20 toluene/water azeotrope was distilled off until a boiling point of 110°C had been reached. The mixture was then cooled in a stream of argon to below the boiling point, and 4.82 g of anhydrous CrCl₃ (31 mmol) were added. After again distilling off a few ml of toluene and cooling under the stream of argon, 0.5 g zinc powder 25 is added. On further distillative removal of toluene, the suspension turned into a deep violet solution. Toluene was distilled off for 30 minutes more and the residue was cooled to 25°C. After the zinc powder had settled out, the deep violet solution was decanted off in air and the solvent was removed on a 30 rotary evaporator. The violet, somewhat oily solid residue was dissolved in acetone and the solution was filtered. The resulting deep violet solution was admixed with water until the solution above the violet precipitate had only a slight violet coloration. After filtration, the violet residue was dried for 40 hours under 35 reduced pressure (approximately 1 Pa) at 50°C toward the end. 13.12 g (74%) of the violet "chromium complex 9" were obtained.

b) Implementation of the trimerizations

40 The trimerizations were conducted in a 1 l four-necked flask equipped with contact thermometer, stirrer, heating mantle and gas inlet tube, into which from 30 to 50 µmol of "chromium complex 9" in 250 ml of toluene were introduced under argon at 40°C.

45 Methylaluminoxane ("MAO") was used in the form of a 1.6 M solution in toluene.

21

The boron compound used was dimethylanilinium tetrakis(pentafluorophenyl)borate ("DMAB"). Following its addition, the reaction mixture was heated to 70°C, then cooled to 40°C and admixed with triisobutylaluminum ("TIBAL").

5

From 20 to 40 l/h of ethene or 1-butene were passed through the pale green/yellow solution obtained following the addition of MAO or DMAB/TIBAL, or the corresponding amount of 1-hexene was added dropwise.

10

In the course of the experiment, the temperature was held constant at temperature T for the reaction time t. The reaction was ended by adding 15 ml of concentrated hydrochloric acid in 50 ml of methanol and the reaction mixture was subsequently stirred

15 for 15 min. Then 250 ml of methanol were added and stirring was continued for 15 mins more. Following filtration to remove any insoluble polymer forms, the product was washed three times with water and dried over sodium sulfate. Yield and product distribution were determined by gas chromatography from the
20 solution thus obtained. Further reactant data and the results of the experiments are given in Table 2.

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Table 2: Data for Examples 13-22

Ex.	Amount of chromium complex 9		Atom ratio Al:Cr	Atom ratio B ¹):Cr	T [°C]	Monomer	DMP ³) [μmol]	t [min]
	[mg]	(μmol)						
13	16.6	33.6	300:1	-	40	C ₂ H ₄ +5 ml 1-hexene	-	60
14	19.0	32.6	350:1	-	40	C ₂ H ₄ ⁴	-	60
15	30.2	51.9	50:	2.2:1	40	C ₂ H ₄ ⁴	-	60
16	25.5	43.8	350:1	-	40	C ₂ H ₄ ⁴	-	60
17	23.8	40.9	50:1 ²)	2:1	40	500 ml 1-hexene	123	90
18	20.4	35.1	50:1	2:1	40	500 ml 1-hexene	60	-
19	21.2	36.4	300:1	-	40	500 ml 1-hexene	-	60
20	26.6	45.7	350:1	-	40	1-butene ⁴	-	60
21	22.2	38.1	50:1	10:1	40	1-butene ⁴	-	60
22	18.4	31.6	300:1	-	20	1-butene ⁴	-	60

Table 2 continued: Data for Examples 13-22

Ex.	Polymer [g]	Products [g]				Activity of the catalyst used [kg/(mol Cr*h)]					
		C ₆	C ₁₀	C ₁₄	C ₁₈	Polymer	C ₆	C ₁₀	C ₁₄	C ₁₈	Total
13	-	13.0	16.5	3.08	-	-	387	488	91	-	965
14	0.52	6.9	10	2.3	-	16	213	307	71	-	607
15	0.9	4.9	7.78	2.5	-	17	94	149	48	-	308
16	0.56	5.96	12.5	2.99	-	12.8	136	286	68	-	502
17	-	-	-	-	3.47	-	-	-	-	84	84
18	-	-	-	-	1.02	-	-	-	-	29.1	29.1
19	-	-	-	-	2.7	-	-	-	-	75.8	75.8
20	-	2.08				-	43.1				43.1
21	-	2.58				-	67				67
22	-	1.19				-	37.65				37.65

23

- 1 Activation is by addition of DMAB and TIBAL
- 2 Triethylaluminum was used instead of TIBAL
- 3 2,5-Dimethylpyrrole
- 4 Gas was passed through

24

Examples 23 to 26: Trimerization in the presence of "chromium complex 10" and methylalumoxane

5 a) Alternative preparation of "chromium complex 10"

The preparation took place in analogy to the alternative preparation of chromium complex 9 in accordance with Examples 13-22.

10

b) Implementation of the trimerizations

The trimerizations of Examples 23-25 were carried out in analogy to Examples 13-22 in toluene as the solvent.

15

The reaction of Example 26, on the other hand, took place in a 1000 ml autoclave under a pressure of 40 bar, again in toluene.

The further reactant data and the results of the experiments are
20 given in Table 3.

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Table 3: Data for Examples 23-26

Ex.	Amount of chromium complex 10		Atom ratio Al:Cr	Atom ratio B ¹⁾ :Cr	T [°C]	Monomer	DMP ³⁾ [μmol]	t [min]
	[mg]	(μmol)						
23	19.5	29.3	300 : 1	-	40	C ₂ H ₄ ⁴⁾	-	60
24	28.3	42.5	50 : 1 ⁵⁾	5.3 : 1	40	1-butene ⁴⁾	127.5	60
25	12.1	18.2	500 : 1	-	50	ethene	-	30
26	55	83	300 : 1	-	40	200 ml 1-butene	-	60

Ex.	Polymer [g]	Product [g]				Activity of the catalyst used [kg/(mol Cr*h)]					
		C ₆	C ₁₀	C ₁₄	C ₁₈	Polymer	C ₆	C ₁₀	C ₁₄	C ₁₈	Total
23	0.43	9.02	10.9	2.06	0.16	14.7	308	372	70	5.5	770
24	-	C ₁₂ : 2.31				-	C ₁₂ : 54,3				54.3
25	0.07	6.63	1.96	-	-	3.8	730	215	0	0	945
26	-	C ₁₀ : 0.24, C ₁₂ : 2.09				-	C ₁₀ : 2.9, C ₁₂ : 25.2				28.1

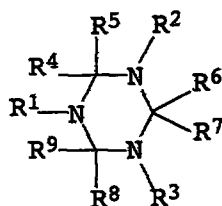
25

- 1 Activation takes place by addition of DMAB and TIBAL
- 2 Triethylaluminum was used instead of TIBAL
- 3 2,5-Dimethylpyrrole
- 4 Gas was passed through
- 5 Use of triethylaluminum



We claim

1. An oligomerization catalyst for olefins, obtainable from
5 a) a chromium compound CrX_3 and the at least equimolar amount, based on the chromium compound CrX_3 , of a ligand L or from an existing chromium complex CrX_3L , in which the groups X are, independently of one another, abstractable counterions and L
10 is a 1,3,5-triazacyclohexane of the formula I



I

- where the groups R^1 to R^9 are, independently of one
20 another: hydrogen or organosilicon or substituted or unsubstituted carboorganic groups having from 1 to 30 carbon atoms, where two geminal or vicinal radicals R^1 to R^9 may also be joined to form a five- or six-membered ring, and

- 25 b) at least one activating additive.

2. An oligomerization catalyst as claimed in claim 1, obtainable
30 using an activating additive comprising an unsubstituted or substituted five-membered aromatic N-heterocycle and at least one aluminum alkyl, some of whose alkyl groups may have been replaced by halogen and/or alkoxy.

3. An oligomerization catalyst as claimed in claim 1, obtainable
35 using at least one activating additive.

4. An oligomerization catalyst as claimed in claim 1, obtainable
40 using at least one boron compound and at least one aluminum alkyl, some of whose alkyl groups may have been replaced by halogen and/or alkoxy, as activating additive.

5. An oligomerization catalyst as claimed in any of claims 1 to
4, wherein the groups R^1 , R^2 and R^3 in the
1,3,5-triazacyclohexane I are, independently of one another,
45 unsubstituted or substituted C_1 - C_{12} -alkyl, C_6 - C_{15} -aryl or C_6 - C_8 -arylalkyl.



6. An oligomerization catalyst as claimed in claim 5, wherein the groups R^1 , R^2 and R^3 in the 1,3,5-triazacyclohexane I are, independently of one another, substituted or unsubstituted C_1 - C_{12} -alkyl or C_6 - C_8 -arylalkyl.
- 5 7. An oligomerization catalyst as claimed in any of claims 1 to 6, wherein the groups R^4 , R^5 , R^6 , R^7 , R^8 and R^9 in the 1,3,5-triazacyclohexane I are, independently of one another, hydrogen or methyl.
- 10 8. A process for preparing oligomers having up to 30 carbon atoms by reaction of an olefin or a mixture of olefins at from 0 to 150°C and pressures of from 1 to 200 bar in the presence of an oligomerization catalyst as claimed in any of
- 15 claims 1 to 7.
9. An oligomer obtainable by a process as claimed in claim 8.
10. An oxo alcohol obtainable by conventional hydroformulation
- 20 [sic] of the oligomers of claim 9.
11. [(1,3,5-Tris(2-n-propylheptyl)-1,3,5-triazacyclohexane)- $CrCl_3$].
- 25 12. [(1,3,5-A₃-1,3,5-triazacyclohexane) $CrCl_3$] in which A is an alkyl which is alkyl-substituted in position 2.

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