

POLYURETHANE FOAMS

001] The present invention relates to polyurethane foams prepared from polyester polyols obtained by polymerization of diol monomers and diacid monomers, the latter being synthesized from a mixture of dinitrile compounds obtained as by-products in the manufacture of adiponitrile by hydrocyanation of butadiene.

002] Polyurethane foams are used in many applications. Mention may be made, by way of example, of the manufacture of soles for shoes, and also internal soles or mid-soles.

003] According to the applications of these foams, they have to exhibit predetermined properties which require the use of specific starting materials for the synthesis of the polyester polyols and polyisocyanates. Thus, the polyurethane foams used in particular in the field of footwear are often obtained by using, as base products, polyester polyols synthesized from diol monomers, such as glycol or diethylene glycol, and diacid monomers, such as adipic acid. For other uses, it is also possible to make use of the polyester polyols obtained from diacid monomers composed of a mixture of diacids, namely adipic acid, glutaric acid and succinic acid. This mixture of diacids is a by-product obtained in the processes for the manufacture of adipic acid by oxidation of cyclohexane.

004] There still exists a need to find novel compounds or products for manufacturing polyurethanes and in particular polyurethane foams in order to obtain foams with novel properties and/or to widen the list of starting materials capable of producing polyurethane foams with properties suitable for the known applications.

005] The manufacture of adiponitrile, a major chemical intermediate used in particular in the synthesis of hexamethylenediamine and caprolactam (monomers for the manufacture of polyamides), by hydrocyanation of butadiene generates a stream of dinitrile by-products comprising predominantly branched dinitrile compounds, such as 2-methylglutaronitrile or ethylsuccinonitrile. This mixture of branched dinitrile compounds is obtained by distillation in order to separate it from adiponitrile. As the separation cannot be complete, the mixture of branched dinitrile compounds also comprises a small proportion of adiponitrile.

006] Several solutions have been proposed for giving added value to these by-products or mixtures. One of these consists in hydrogenating the dinitrile compounds to give primary amines, in particular in order to produce methylpentamethylenediamine (MPMD), used as monomer in the manufacture of specific polyamides. This process requires stages of purification, either of the methylglutaronitrile or of the methylpentamethylenediamine.

007] In industry, these by-products are also given added value in the form of steam or of energy by combustion. However, this combustion can require a treatment of the gases in order to remove the nitrogen oxides produced and produces carbon dioxide gas, which is discharged to the atmosphere.

008] There thus exists a significant demand and a need to find novel ways of giving added value to and converting these dinitrile compounds or mixtures to give chemical compounds which can be put to use and which are economically advantageous.

009] Unless otherwise mentioned, the percentages and parts given in the text below are expressed by weight.

010] One of the aims of the present invention is specifically to provide a polyurethane foam prepared from polyester polyols which are obtained with starting materials resulting from the conversion of the mixture of abovementioned branched dinitrile compounds. These polyurethane foams have properties comparable to those of the polyurethane foams of the prior art.

10 011] To this end, the invention provides a process for the preparation of polyurethane foam obtained by reaction between:

- a) at least one polyisocyanate and
- b) at least one polyester polyol produced by polymerization of diol monomers and diacid monomers, the diacid monomers comprising at least one mixture of diacids, referred to hereinafter as mixture M, the composition by weight of which is:

methyglutaric acid (MGA): 50-99%
20 ethylsuccinic acid (ESA): 0-30%
adipic acid (AA): 0-50%.

012] The invention is also targeted at the polyurethane foams thus prepared.

25 013] In the mixture of diacids used as diacid monomers, all or part of said diacids can be in the form of anhydrides.

30 014] Preferably, the mixture of diacids or mixture M exhibits the following composition by weight:

methyglutaric acid (MGA): 75-95%, advantageously 80-95%
ethylsuccinic acid (ESA): 0-12%, advantageously 0-10%
adipic acid (AA): 0-20%, advantageously 5-15%.

35 015] The diacid monomers used for the synthesis of the polyester polyol can also comprise other diacids, such as adipic acid, phthalic acids, the mixture of glutaric/succinic/adipic acids resulting from the

manufacture of adipic acid, or the like.

016] According to the invention, the above mixture M is obtained by conversion of a mixture of dinitrile compounds, referred to hereinafter as mixture N, to give acids by hydrolysis of the nitrile functional groups. This mixture N of dinitrile compounds is advantageously a mixture of branched dinitrile compounds separated and recovered in the process for the manufacture of adiponitrile by double hydrocyanation of butadiene.

017] Thus, by way of example, this mixture N comprises:

15 2-methylglutaronitrile (MGN): from 80 to 85%
 ethylsuccinonitrile (ESN): from 8 to 12%
 adiponitrile (AdN): from 3 to 5%

The remainder to 100% corresponds to various impurities.

20 018] The mixture of diacids is prepared by conversion of the compounds constituting the mixture N of dinitriles. This conversion can be carried out by several processes. By way of example, two processes are briefly described below.

019] According to a first process, the conversion of the nitrile functional groups to carboxyl functional groups is obtained by reaction of the nitrile compounds with a basic hydroxyl compound in solution in a solvent at a temperature of between 80 and 200°C, preferably between 80 and 150°C. The ammonia formed is removed. The salt obtained is reacted with an inorganic acid and the diacids formed are isolated and recovered. Such a process is, for example, described in French application No. 2 902 095. The basic hydroxyl compound is an alkali metal hydroxide, such as sodium hydroxide, potassium hydroxide or the like. Advantageously, an aqueous solution of this basic hydroxyl compound is

used. The concentration of basic compounds in the aqueous solution is advantageously between 5 and 30% by weight. The basic hydroxyl compound is employed with an excess of 3 to 20%, advantageously between 3 and 10%,
5 with respect to the stoichiometric amount necessary to convert the nitrile functional groups to carboxyl functional groups. The reaction is carried out either at atmospheric pressure at, advantageously, a temperature which makes it possible to have reflux of
10 the solvent, for example water, or under pressure with removal of the ammonia formed or without removal of this ammonia formed, which will be at least partially dissolved in the reaction medium. Mention may be made, as suitable inorganic acid, of sulfuric acid,
15 hydrochloric acid, organic acids exhibiting a pKa of less than or equal to 3, or their mixtures.

020] It is also possible to obtain the dicarboxylic acids constituting the mixture M according to another
20 process for the conversion of the nitrile functional groups to acid functional groups. This process consists in hydrating the nitrile functional groups of the compounds forming the mixture N, in order to form amide compounds, and in hydrolyzing the amide functional
25 groups to give carboxyl functional groups, as described in unpublished French patent application No. 06 10302, filed on 24 November 2006.

021] Briefly, according to this process, the mixture
30 M of diacids is prepared by:

- a) hydrating a corresponding mixture N comprising methylglutaronitrile (MGN), ethylsuccinonitrile (ESN) and adiponitrile (AdN) to give amide functional groups, and
- 35 b) hydrolyzing the amide functional groups to give carboxyl functional groups.

022] The hydration stage is carried out by reaction with water in the presence of a strong inorganic acid,

by using from 1 to 1.5 mol of water per mole of nitrile functional group to be hydrated in the presence of a strong inorganic acid at a temperature which makes it possible to maintain the reaction medium in the liquid state. The hydrolysis stage is carried out, with stirring, by using from 1 to 10 mol of water per mole of amide functional group to be hydrolyzed and an amount of strong inorganic acid, expressed in protons, corresponding to at least 1 mol of proton per mole of amide to be hydrolyzed, the temperature of the reaction medium being determined in order to maintain the reaction medium in the liquid state. The dicarboxylic acid formed is recovered by maintaining the reaction medium, without stirring, at a temperature greater than the melting point of the dicarboxylic acid and/or of the salt formed for separation by settling of the reaction medium, the upper phase comprising the carboxylic acid being separated.

023] The dicarboxylic acids thus obtained by these various processes are advantageously purified by the usual techniques, namely crystallization, distillation, refining or the like.

024] It is also possible to treat this mixture of diacids by processes which make it possible to separate some diacids and thus to modify the composition by weight of the mixture obtained by the processes for the conversion of dinitrile compounds described above. Thus, a process for the separation of diacides described in European patent 0 687 663 can be used. It consists in converting the diacids into the anhydride form and then separating the anhydrides by distillation. By the use of this process, it is possible to separate in particular the anhydride of ethylsuccinic acid and/or the anhydride of adipic acid and to recover a mixture comprising a high concentration of anhydride of methylglutaric acid. This mixture can be used as is or after reformation of the

acid form.

025] The polyester polyols are obtained, for example, according to a manufacturing process comprising two stages, a first stage of esterification and a second stage of polycondensation.

026] The esterification stage is carried out by mixing the diacids of the mixture M with polyols, preferably diols and/or polyether diols, such as, for example, a mixture of ethylene glycol and diethylene glycol, with a diol/diacid molar ratio of between 1.2 and 1.5.

The suitable diols are chosen from the group consisting of ethylene glycol, 1,4-butanediol, 1,5-pentanediol, 1,6-hexanediol, 1,10-decanediol, 2,2-dimethyl-1,3-propanediol, 1,3-propanediol, trimethylpropanol and bisphenol, the polyether diols being chosen from the group consisting of diethylene glycol, dipropylene glycol and 1,1,3-trimethyltriethylenediol.

027] The reaction temperature in this first stage is gradually increased during the progression of the reaction. By way of example, the start of the reaction is carried out at a temperature of 160°C to arrive at a temperature of 220°C at the end of the reaction.

028] The second stage of polycondensation is carried out with addition of a catalyst, such as tetrabutyl titanate (TBT), with a concentration by weight of 0.003%, with respect to the weight of diacids involved. The polymerization temperature is 200°C under a pressure of between 10 and 20 mbar.

029] The polyester polyol obtained is characterized by the hydroxyl number (I_{OH}), corresponding to the number of mg of potassium hydroxide per gram of polyol to convert the hydroxyl functional groups to alkoxide functional groups, and the acid number (I_A), which

represents the number of mg of KOH necessary to neutralize 1 g of polyol.

030] The polyester polyol is also characterized by
5 the viscosity and by its molecular weight.

031] Advantageously, an additive which limits or prevents the hydrolysis of the ester functional groups is added to the polyester polyols, such as carboimides,
10 for example cyanamides; hydrogen cyanamide; carbimides; cyanogenamides; amidocyanogens.

032] It can also be advantageous to add, to the polyester polyols, additives which stabilize against UV
15 radiation, such as hindered amines, antioxidants, flame retardants or the like.

033] It can be advantageous, in order to modify the mechanical properties of the polyurethane foams, to add
20 a dispersed particulate inorganic filler.

034] Mention may be made, as suitable particulate inorganic fillers, by way of example, of the fillers exhibiting particles with a size of less than 60 μm ,
25 preferably of less than 20 μm and more advantageously still of less than 10 μm .

035] Thus, mention may be made, as suitable fillers, of powders formed of aluminosilicate, of silica, in particular obtained by precipitation, of titanium
30 oxides, of talc, of kaolin or of calcium carbonate, for example.

036] According to a preferred embodiment, these
35 inorganic fillers are present in a dispersed manner in the polyester polyol before reacting with the polyisocyanate. This dispersion of the inorganic filler can be obtained by addition of the latter to the polyester polyol or to the medium for polymerization of

the polyester polyol. It is also possible to disperse the inorganic filler in the polyol monomer before the addition to the process for the manufacture of the polyester polyol. More advantageously still, the inorganic filler can be mixed with the mixture M of diacids before feeding to the polymerization process.

037] The amount of inorganic filler in the suspension in the polyol, the polyester polyol or as a mixture with the diacids is chosen according to the concentration of inorganic filler desired in the polyurethane foam. Thus, concentrations between 1 and 80% by weight of filler in the mixture with the diacids can be used.

038] The polyurethanes of the invention are obtained according to the conventional and normal processes. Thus, the polyester polyols of the invention are mixed with optionally a chain-extending agent and the polyisocyanate in the presence of a foam-forming or blowing agent and a catalyst.

039] Use may be made, as foam-forming agent, of water, hydrocarbons, chlorofluorocarbons or hydrofluorocarbons, alone or as a mixture. Water is the preferred foam-forming or blowing agent.

040] Mention may be made, as catalysts suitable for the invention, of tertiary amines, such as 1,4-diazabicyclo[2.2.2]octane, N,N,N',N'-tetramethylhexamethylenediamine, N,N,N',N'-tetramethylpropylenediamine, N,N,N',N',N''-pentamethyldiethylenetriamine, trimethylaminoethylpiperazine, N,N-dimethylcyclohexylamine, N,N-dimethylbenzylamine, N-methylmorpholine, N-ethylmorpholine, triethylamine, tributylamine, bis(dimethylaminoalkyl)piperazines, N,N,N',N'-tetramethylethylenediamine, N,N-diethylbenzylamine, bis(N,N-diethylaminoalkyl) adipate, N,N,N',N'-tetramethyl-1,3-butanediamine, N,N-dimethyl- β -phenylethyldiamine, 1,2-

dimethylimidazole, 2-methylimidazole and the like. Other catalysts can be used, such as organometallic compounds, for example dibutyltin dilaurate, tin oleate, cobalt naphthenate or lead naphthenate.

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041] Other additives, such as regulators of the size and shape of the cells, pigments, coloring agents or antioxidants, can be added.

10 042] The mixture is injected into a mold in order to form the polyurethane foam and to obtain an article with the desired shape, such as soles, for example.

043] By adjusting the amount of foam-forming agent,
15 for example the amount of water, it is possible to obtain foams with different densities, for example of between 0.1 and 0.9 g/cm³, advantageously of between 0.2 and 0.5 g/cm³.

20 044] The polyurethane foams of the invention make it possible to produce articles exhibiting suitable properties similar to those of the polyurethane foams of the prior art, in particular those obtained with polyester polyols produced from diol monomers and
25 adipic acid. These properties are illustrated in the following examples.

045] Among these properties, the tensile strength, determined according to the standard DIN 53543, the
30 elongation at break, measured according to the standard DIN 53543, and the tear strength, measured according to the standard ASTM D3574-95, are important.

046] Other properties are also important for certain
35 applications. Thus, the abrasion resistance is determined according to the standard DIN 53516. The shrinkage during molding is measured according to the standard ASTM D3851, the compression set (CS) is measured according to the standard ASTM D395 and the

resilience is measured according to the standard ASTM D1054.

047] The advantages and details of the invention
5 will become apparent in more detail in the light of the
examples given below by way of indication and without
implied limitation.

048] Preparation of diacids from a mixture N of
10 dinitriles by basic hydrolysis

049] 108 g of a mixture N of dinitrile compounds
originating from the process for the manufacture of
adiponitrile by hydrocyanation of butadiene are added
15 over 30 min with stirring to 560 g of a 15% aqueous
sodium hydroxide solution heated beforehand to 80°C.

050] The mixture N of dinitrile compounds has the
following composition by weight:
20 methylglutaronitrile (MGN): 84.2%
ethylsuccinonitrile (ESN): 11%
adiponitrile (AdN): 4%

The remainder to 100% corresponds to various
impurities.

25 051] The mixture is subsequently heated in order to
obtain a reflux and is maintained at this temperature
for approximately 7 h. The ammonia which is given off
is recovered and trapped. The progress of the reaction
30 is monitored by potentiometric titration with a
hydrochloric acid solution. This titration makes it
possible to determine the amount of sodium hydroxide
remaining, the amount of dissolved ammonia and the
amount of salified carboxyl functional group
35 corresponding to the various jumps of pH observed
during the titration. The reaction medium is
subsequently cooled to ambient temperature and 80 g of
water are added before running in 105 g of 98% sulfuric
acid. The pH of the aqueous solution is of the order

of 3.

052] The aqueous phase is subsequently extracted with 3 times 200 ml of MTBE (methyl tert-butyl ether) at 40°C. The organic phases are combined and the MTBE is subsequently distilled off. 141.6 g of diacids are obtained with a purity, determined by potentiometric titration, of the order of 98.5%.

053] The mixture of diacids obtained is distilled in a batchwise distillation. After removal of the first top fractions comprising volatile compounds, the first fractions comprising methylglutaric acid and ethylsuccinic acid are combined in order to form a first example used to carry out example 1, the combination of the intermediate fractions is used to carry out example 2 and the final fractions form a third mixture comprising a higher proportion of adipic acid used to carry out example 3.

054] A second batch of mixture of diacids was manufactured according to the above procedure. A portion of the mixture obtained after extraction of the MTBE solvent was distilled in a continuous distillation; the distilled fraction, after removal of the volatile compounds, was used to carry out example 4 while the other undistilled portion of the mixture of diacids was used to carry out example 5.

055] The compositions by weight of the various mixtures of diacids described above are shown in table 1 below:

Table 1

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Components	Ex. 1	Ex. 2	Ex. 3	Ex. 4	Ex. 5
Methylglutaric acid, % by weight	91.5	93	85	87.9	87.9
Ethylsuccinic acid,	8.5	0	0	7.6	7.6

% by weight					
Adipic acid, % by weight	0	7	15	4.5	4.5

056] Preparation of the polyester polyol

057] The mixtures of diacids defined above in the
5 table are esterified by addition of a mixture of MEG
and DEG glycols according to an MEG/DEG molar ratio of
60/40, the glycol/diacid molar ratio being 1.30. After
esterification, the polymerization reaction is carried
out, after addition of 0.03 g/kg of tin catalyst, at
10 approximately 200°C for approximately 13 h.

058] The 5 polyester polyols obtained have the
physicochemical characteristics collated in table 2
below:

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Table 2

Polyester polyol	Ex. 1	Ex. 2	Ex. 3	Ex. 4	Ex. 5
Reaction time (h)	13.3	14.9	15.1	19.4	15.2
Yield (g polyester polyol/g acid)	1.43	1.40	1.42	1.33	1.34
Hydroxyl number (mg KOH/g)	58.7	57.5	58.9	65.9	59.4
Acid number (mg KOH/g)	0.60	1.0	0.58	0.15	0.47
Content of water (%)	0.04	0.04	0.06	0.05	0.06
Viscosity, mPa·s, at 35°C	3540	3252	3306	2927	3384

059] Preparation of the polyurethane foams

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060] The polyurethane foams are obtained from the
5 polyester polyols described above in table 2
(examples 1 to 5) and by mixing the products listed in
table 3 below, by injection of these products into an
injection molding machine and forming in a mold
25 according to the conditions shown in table 4. The

NCO/OH molar ratio is 1.02 for the polyol of example 1, 1.00 for the polyol of example 2, 0.98 for the polyol of example 3, 0.99 for the polyol of example 4 and 0.96 for the polyol of example 5.

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Table 3

	Parts by weight	% by weight
Polyol	100	88.73
MEG	10	8.87
Water	0.8	0.71
Dabco DC 1027*	0.56	0.50
Dabco EG*	0.84	0.75
Dabco DC 3043*	0.3	0.27
Dabco DC 3042*	0.2	0.18
Isocyanate prepolymer, sold under the name Elastopan SP 8020 by BASF (% NCO = 20.8)		

* Products sold by Air Products & Chemicals

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Table 4

Temperature of the polyol	40°C
Isocyanate prepolymer temperature	35°C
Rotation of the head mixer (rpm)	7700
Molding temperature	50°C
Density of the molding	0.45 g/cm ³
Removal time	4 min

061] The properties of the polyurethane foams obtained are determined according to the standardized methods described above and are collated in table 5

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below:

Table 5

	Ex. 1	Ex. 2	Ex. 3	Ex. 4	Ex. 5
Tensile strength kgf/cm ² (DIN 53543)	52.9	45.6	49.7	50.8	56.2
Tensile strength kgf/cm ² (DIN 53543) after 7 days at 70°C	52.3±5.7	44.2±2.7	55.8±2.6		
Elongation kgf/cm ² (DIN 53543)	297	326	291	289	310
Tear strength kgf/cm ² (ASTM D3574-95)	14.4	16.9	14.5	16.7	19.3
Abrasion (DIN 53516 force 10N)	380/353	310/336	280/302		

Abrasion (DIN 53516 force 5N)	108±20	103±30	75±10	116±20	97±5
CS (ASTM D-395) (%)	15-25	15-25	10-20	12-15	8-11
Resilience (ASTM D1054) (%)	22	26	25	13	12
Bending fatigue test (cycles)	>150 000	>150 000	>150 000		
Initial hardness (DIN 53545)	44±1	53±2	47±1		
Hardness after 7 days at 70°C (DIN 53545)	43±0	44±1.5	46±1	52±1.3	51.8±1

062] Table 5 reveals that the 5 polyurethane foams prepared from polyester polyols in accordance with the invention (examples 1 to 5) exhibit a level of physical properties which are high and comparable with those of the polyurethane foams normally used in industry, in particular in the footwear industry.

CLAIMS

1. A polyurethane foam, characterized in that it is capable of being obtained by reaction:
- 5 a) of a polyisocyanate and
b) of a polyester polyol obtained by polymerization of a mixture of polyol monomers and diacid monomers, said diacid monomers being composed of at least one mixture M of diacids exhibiting a following composition by
- 10 weight:
- | | |
|---------------------------|--------|
| methyglutaric acid (MGA): | 50-99% |
| ethylsuccinic acid (ESA): | 0-30% |
| adipic acid (AA): | 0-50%. |
- 15 2. The foam as claimed in claim 1, characterized in that the mixture M of diacids exhibits the composition by weight:
- | | |
|---------------------------|--------|
| methyglutaric acid (MGA): | 75-95% |
| ethylsuccinic acid (ESA): | 0-12% |
| 20 adipic acid (AA): | 0-20%. |
3. The foam as claimed in claim 2, characterized in that the mixture M of diacids exhibits the composition by weight:
- 25
- | | |
|---------------------------|--------|
| methyglutaric acid (MGA): | 80-95% |
| ethylsuccinic acid (ESA): | 0-10% |
| adipic acid (AA): | 5-15%. |
- 30 4. The foam as claimed in one of claims 1 to 3, characterized in that the diacids of the mixture M are partially or completely in the anhydride form.
5. The foam as claimed in one of claims 1 to 4, characterized in that the polyol monomers are chosen
- 35 from the group consisting of diols and polyether diols.
6. The foam as claimed in any one of the preceding claims, characterized in that the mixture M of diacids is obtained from a mixture N comprising 2-methyl-

glutaronitrile (MGN), ethylsuccinonitrile (ESN) and adiponitrile (AdN) by reaction with a basic hydroxyl compound in solution in a solvent at a temperature of between 80 and 200°C, removal of the ammonia formed and
5 reaction of the salt obtained with an inorganic acid.

7. The foam as claimed in any one of claims 1 to 5, characterized in that the mixture M of diacids is prepared by:

- 10 a) hydrating a mixture N comprising 2-methylglutaronitrile (MGN), ethylsuccinonitrile (ESN) and adiponitrile (AdN) to give amide functional groups, and
b) hydrolyzing the amide functional groups to give carboxyl functional groups.

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8. The foam as claimed in claim 7, characterized in that the hydration stage is carried out by reaction with water in the presence of a strong inorganic acid, by using from 1 to 1.5 mol of water per mole of nitrile
20 functional group to be hydrated in the presence of a strong inorganic acid, at a temperature which makes it possible to maintain the reaction medium in the liquid state.

- 25 9. The foam as claimed in claim 7 or 8, characterized in that the hydrolysis stage is carried out, with stirring, by using from 1 to 10 mol of water per mole of amide functional group to be hydrolyzed and an amount of strong inorganic acid, expressed in protons,
30 corresponding to at least 1 mol of proton per mole of amide to be hydrolyzed, the temperature of the reaction medium being determined in order to maintain the reaction medium in the liquid state.

- 35 10. The foam as claimed in one of claims 7 to 9, characterized in that the dicarboxylic acids formed are recovered by maintaining the reaction medium, without stirring, at a temperature greater than the melting point of the diacids and/or the salts formed in order

to make possible the separation by settling of the reaction medium, the upper phase comprising the diacids being separated.

- 5 11. The foam as claimed in one of claims 6 to 10, characterized in that the mixture N of dinitrile compounds is a mixture resulting from the process for the manufacture of adiponitrile by double hydrocyanation of butadiene.

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12. The foam as claimed in any one of the preceding claims, characterized in that the diol is chosen from the group consisting of ethylene glycol, 1,4-butanediol, 1,5-pentanediol, 1,6-hexanediol, 1,10-decanediol, 2,2-dimethyl-1,3-propanediol, 1,3-propanediol, trimethylpropanol and bisphenol.

13. The foam as claimed in one of the preceding claims, characterized in that the polyether diol is
20 chosen from the group consisting of diethylene glycol, dipropylene glycol and 1,1,3-trimethyltriethylenediol.

14. The foam as claimed in one of the preceding claims, characterized in that the polyurethane foam
25 comprises a dispersed particulate inorganic filler.

15. The foam as claimed in claim 14, characterized in that the dispersed particulate inorganic filler exhibits particles with a size of less than 60 μm .

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16. The foam as claimed in claim 15, characterized in that the dispersed particulate inorganic filler exhibits particles with a size of less than 20 μm .

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17. The foam as claimed in any one of claims 14 to 16, characterized in that the dispersed particulate inorganic filler is chosen from powders formed of aluminosilicate, of silica, in particular obtained by

precipitation, of titanium oxide, of talc, of kaolin
and of calcium carbonate.