CLAIMS

1. A method for heating one or more streams from a refinery process, chosen from a crude tower inlet, a vacuum tower inlet, a catalytic reformer inlet, a coker inlet, a thermal cracker inlet and a hydrocracker inlet, said method comprising a step of transferring, in a heat exchanger, heat from one or more streams from a petro-chemistry process, chosen from a steam cracker charge gas, a propane dehydrogenation charge gas and a butane dehydrogenation charge gas to said one or more streams from a refinery process for obtaining one or more heated streams, wherein the temperature of said one or more streams from the petro-chemistry process is above the temperature of said one or more streams from a refinery process before said step of heat exchanging has taken place,

wherein the crude tower inlet is heated by transferring, in a heat exchanger, heat from the steam cracker charge gas to said crude tower inlet for obtaining a heated crude tower inlet.

2. The method according to claim 1, wherein said step of heating further comprises a step of additionally heating said crude tower inlet in a crude furnace, wherein said step of additionally heating takes place after transferring heat from steam cracker charge gas.

3. The method according to claim 1, wherein said step of heating further comprises a step of additionally heating said crude tower inlet in a crude furnace, wherein said step of additionally heating takes place before transferring heat from steam cracker charge gas.

4. The method according to claim 1, wherein the vacuum tower inlet is heated by transferring, in a heat exchanger, heat from said steam cracker charge gas to said vacuum tower inlet for obtaining a heated vacuum tower inlet stream.

5. The method according to claim 1, wherein the temperature at an inlet of said heat exchanger is at least 10 °C higher than the temperature at an outlet of said heat exchanger.

6. The method according to claim 1, wherein temperature of said at least one or more streams from the petro-chemistry process is in the range of from 350 °C to 600 °C.

7. The method according to claim 1, wherein said step of heating further comprises a step of additionally heating said crude tower inlet in a crude furnace.

8. The method according to claim 2, wherein the temperature at an inlet of said heat exchanger is at least 10 °C higher than the temperature at an outlet of said heat exchanger.

9. The method according to claim 3, wherein the temperature at an inlet of said heat exchanger is at least 10 °C higher than the temperature at an outlet of said heat exchanger.

10. The method according to claim 4, wherein the temperature at an inlet of said heat exchanger is at least 10 °C higher than the temperature at an outlet of said heat exchanger.

11. The method according to claim 6, wherein the temperature at an inlet of said heat exchanger is at least 10 °C higher than the temperature at an outlet of said heat exchanger.

12. The method according to claim 2, wherein temperature of said at least one or more streams from the petro-chemistry process is in the range of from 350 °C to 600 °C.

13. The method according to claim 3, wherein temperature of said at least one or more streams from the petro-chemistry process is in the range of from 350 °C to 600 °C.

14. The method according to claim 4, wherein temperature of said at least one or more streams from the petro-chemistry process is in the range of from 350 °C to 600 °C.

15. The method according to claim 4, wherein said step of heating further comprises a step of additionally heating said crude tower inlet in a crude furnace.

16. The method according to claim 5, wherein said step of heating further comprises a step of additionally heating said crude tower inlet in a crude furnace.

17. The method according to claim 6, wherein said step of heating further comprises a step of additionally heating said crude tower inlet in a crude furnace.