CLAIMS:

1. A method for processing a feedstock to form a distillate product, comprising:

exposing a feedstock having a T50 boiling point of at least 430°F (221°C), a first aromatics content of at least 5 wt%, and a sulfur content of 500 wppm or less to a hydrocracking catalyst and an aromatic saturation catalyst under effective hydrocracking conditions to produce a hydrocracked effluent, the effective hydrocracking conditions being effective for converting at least 5 wt% to 20 wt% of the feedstock relative to a conversion temperature of 430°F (221°C) such that molecules boiling above that conversion temperature are converted to molecules boiling below that temperature, the hydrocracked effluent having a second aromatics content, a ratio of the second aromatics content to the first aromatics content being 0.6 or less,

the hydrocracking catalyst comprising at least one Group VIII non-noble metal, at least one Group VIB metal, or a combination thereof,

the aromatic saturation catalyst comprising a Group VIII noble metal,

wherein the feedstock is exposed to the hydrocracking catalyst and the aromatic saturation catalyst in a single reaction stage in a single reactor with no intermediate separation being performed between exposing the feedstock to the catalysts, and

wherein the hydrocracked effluent comprises at least a naphtha fuel product fraction and a distillate fuel product fraction.

2. The method of claim 1, further comprising fractionating at least a portion of the hydrocracked effluent to form at least a naphtha product fraction and a bottoms fraction.

3. The method of claim 2, wherein the feedstock comprises at least a portion of the bottoms fraction.

4. The method of claim 2, wherein the bottoms fraction comprises at least a portion of the distillate fuel product fraction.

5. The method of claim 2, further comprising dewaxing the hydrocracked effluent prior to fractionating the at least a portion of the hydrocracked effluent.

6. The method of any preceding claim, further comprising exposing a feed having a sulfur content of greater than 500 wppm to a hydroprocessing catalyst under effective hydroprocessing conditions to form a hydroprocessed effluent; and

separating the hydroprocessed effluent to form at least a hydroprocessed fraction having a T95 boiling point of 1050°F (566°C) or less,

wherein the feedstock having a T50 boiling point of at least 430°F (221°C) comprises at least a portion of the hydroprocessed fraction having a T95 boiling point of 1050°F (566°C) or less.

7. The method of claim 6, wherein separating the hydroprocessed effluent comprises fractionating the hydroprocessed effluent, the fractionating optionally further forming a second naphtha fuel product fraction.

8. The method of claim 6 or claim 7, wherein the hydroprocessed effluent and the hydrocracked effluent are fractionated in a common fractionation process.

9. The method of any of claims 6 to 8, wherein exposing the feed having a sulfur content of at least 500 wppm to a hydroprocessing catalyst under effective hydroprocessing conditions comprises:

exposing the feed having a sulfur content of greater than 500 wppm to a hydrotreating catalyst under effective hydrotreating conditions, exposing the feed having a sulfur content of greater than 500 wppm to a hydrocracking catalyst under effective hydrocracking conditions, or a combination thereof.

10. The method of any of claims 6 to 9, wherein the feed having a sulfur content of greater than 500 wppm has a T5 boiling point of at least 430°F (221°C) and a T95 boiling point of 1050°F (566°C) or less.

11. The method of any of claims 6 to 10, wherein at least about 50 wt% of the feedstock having a T50 boiling point of at least 430°F (221°C) comprises the at least a portion of the hydroprocessed fraction having a T95 boiling point of 1050°F (566°C) or less.

12. The method of any preceding claim, wherein aromatic saturation catalyst comprises about 0.1 wt% to 1.8 wt% of Pt, Pd, or a combination thereof.

13. The method of any preceding claim, wherein the second aromatics content is less than 10 wt%, the first aromatics content is at least 15 wt%, or a combination thereof.

14. The method of any preceding claim, wherein the feedstock has a T5 boiling point of at least 430°F (221°C), a T95 boiling point of 800°F (427°C) or less, or a combination thereof.