

Fig.1

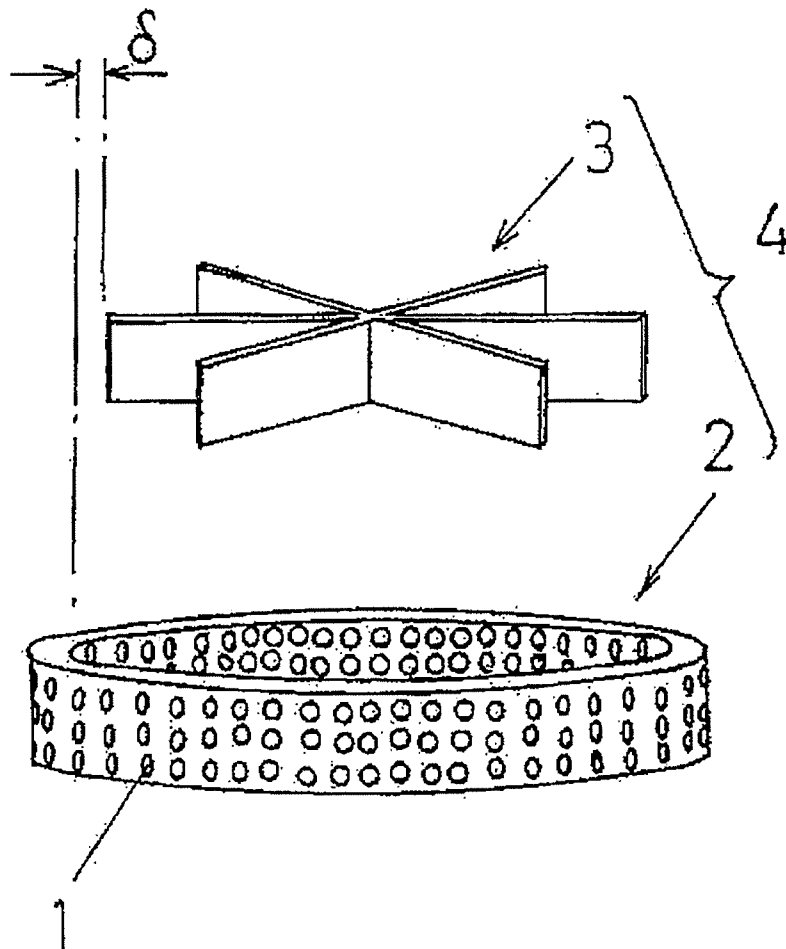
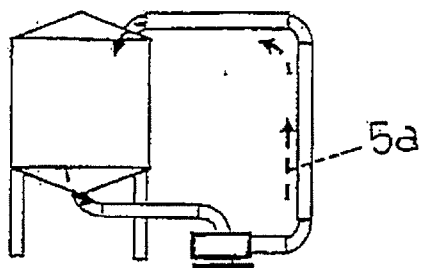


Fig.2

External Circulation



Internal Circulation

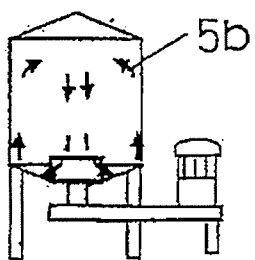


Fig.3

Mixer (Rotor-Stator Type)

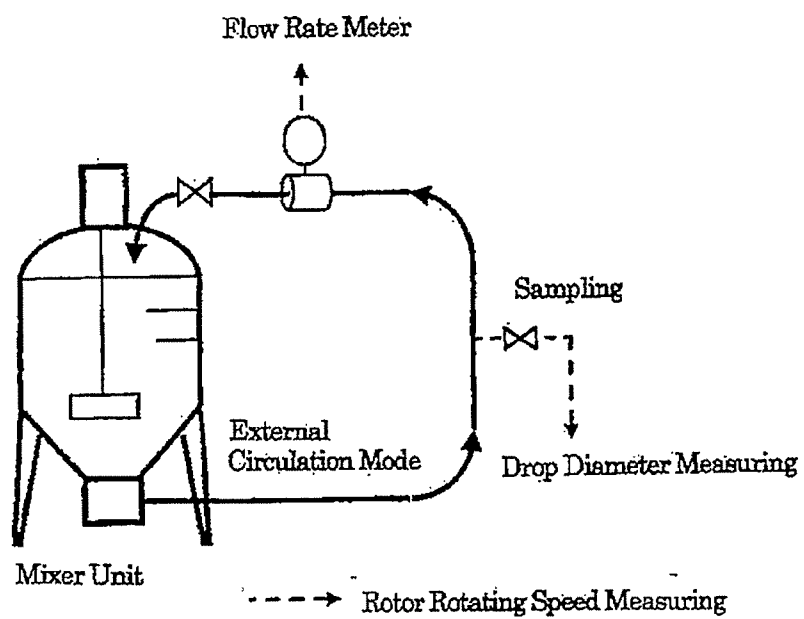


Fig.4

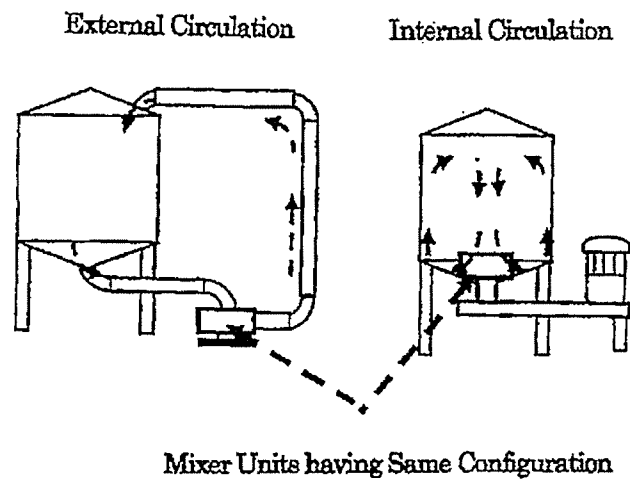
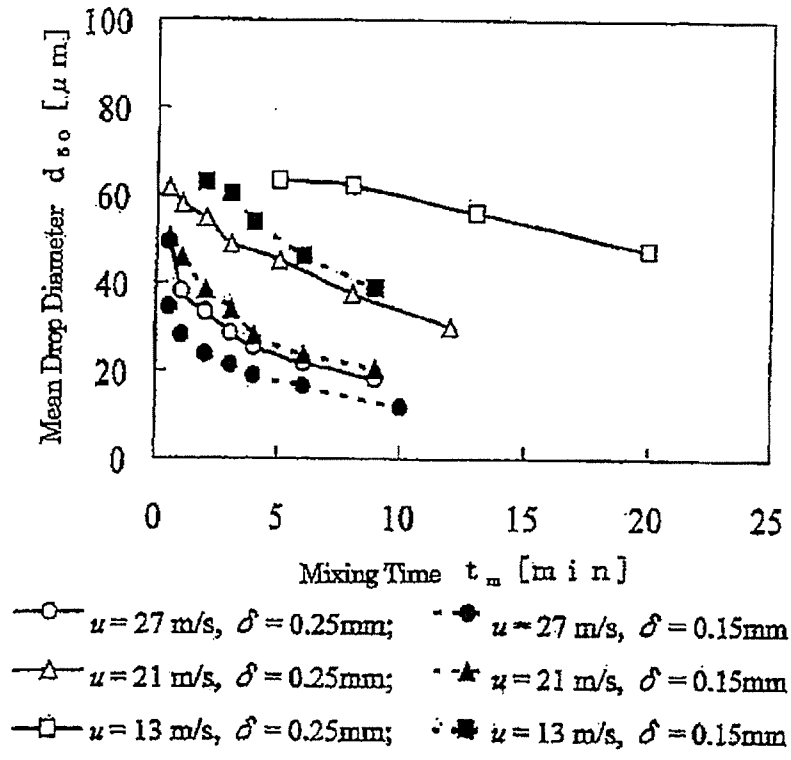
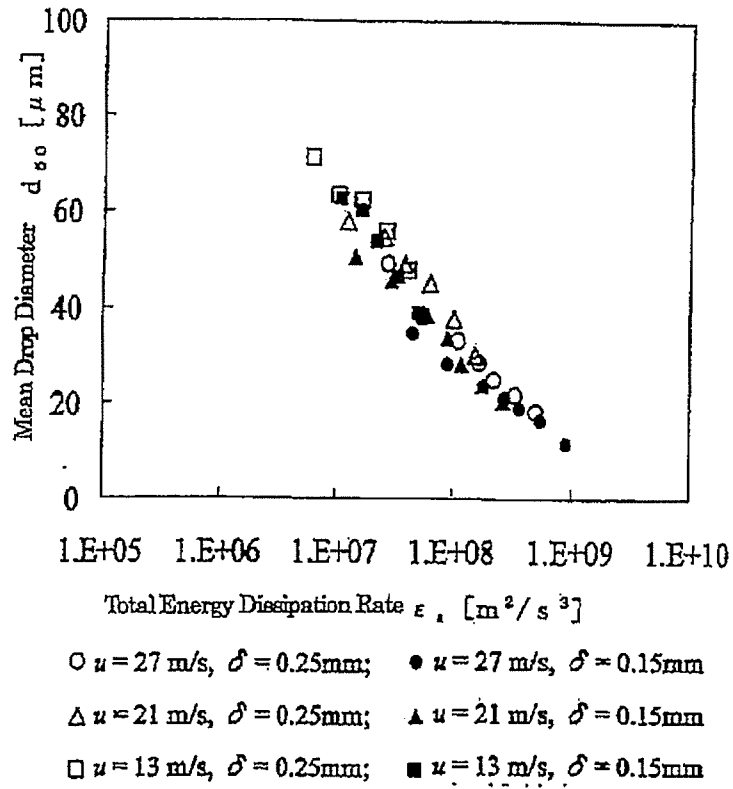


Fig.5



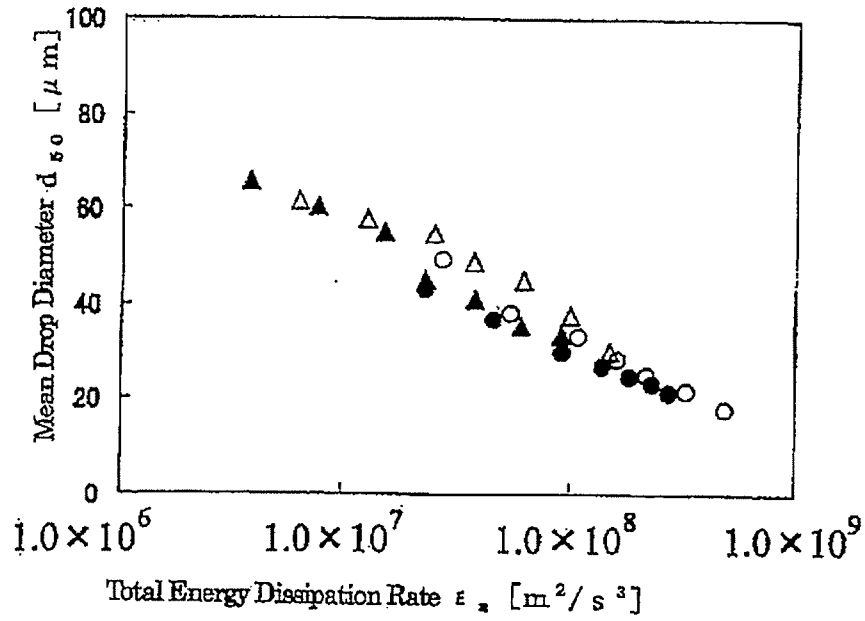
Relationship between Processing (Mixing) Time and Drop Diameter for Mixers A-1 and A-2

Fig.6



Relationship between Mean Drop Diameter and Total Energy Dissipation Rate for Mixer A-1 and A-2

Fig.7



○ Lab,  $u = 27$  m/s,  $\delta = 0.25\text{mm}$

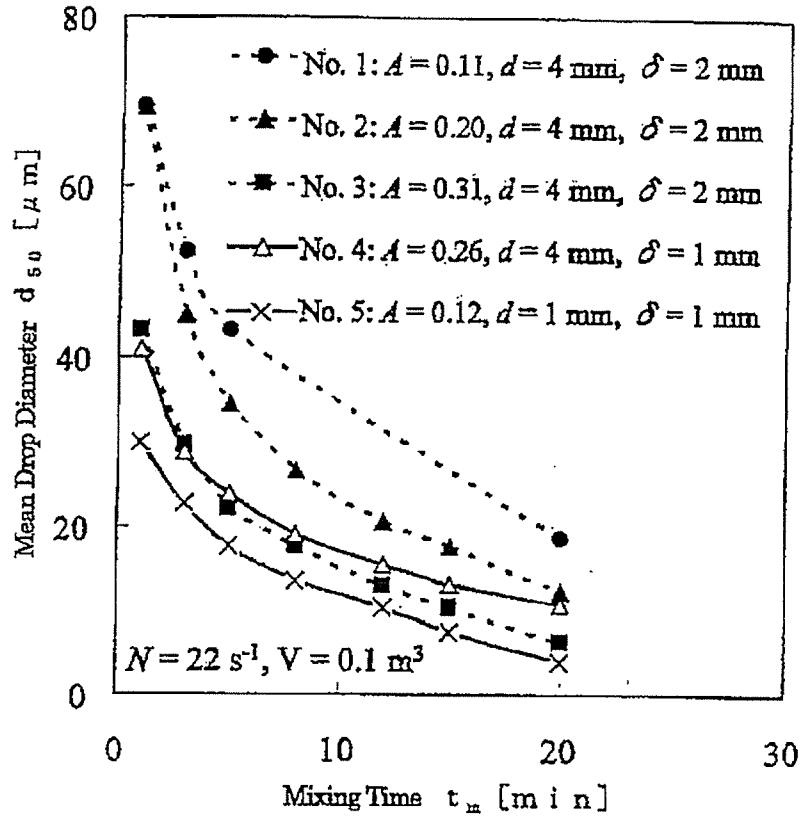
△ Lab,  $u = 21$  m/s,  $\delta = 0.25\text{mm}$

● MP10,  $u = 25$  m/s,  $\delta = 0.25\text{mm}$

▲ MP10,  $u = 20$  m/s,  $\delta = 0.25\text{mm}$

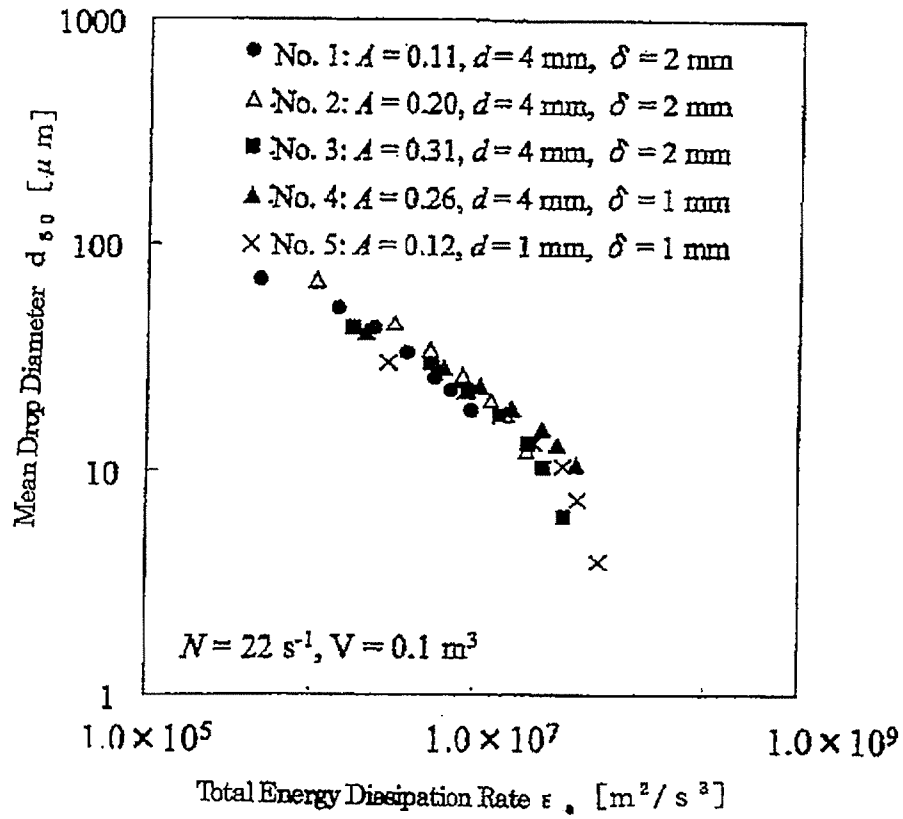
Relationship between Mean Drop Diameter and Total Energy Dissipation Rate for Mixer B

Fig.8



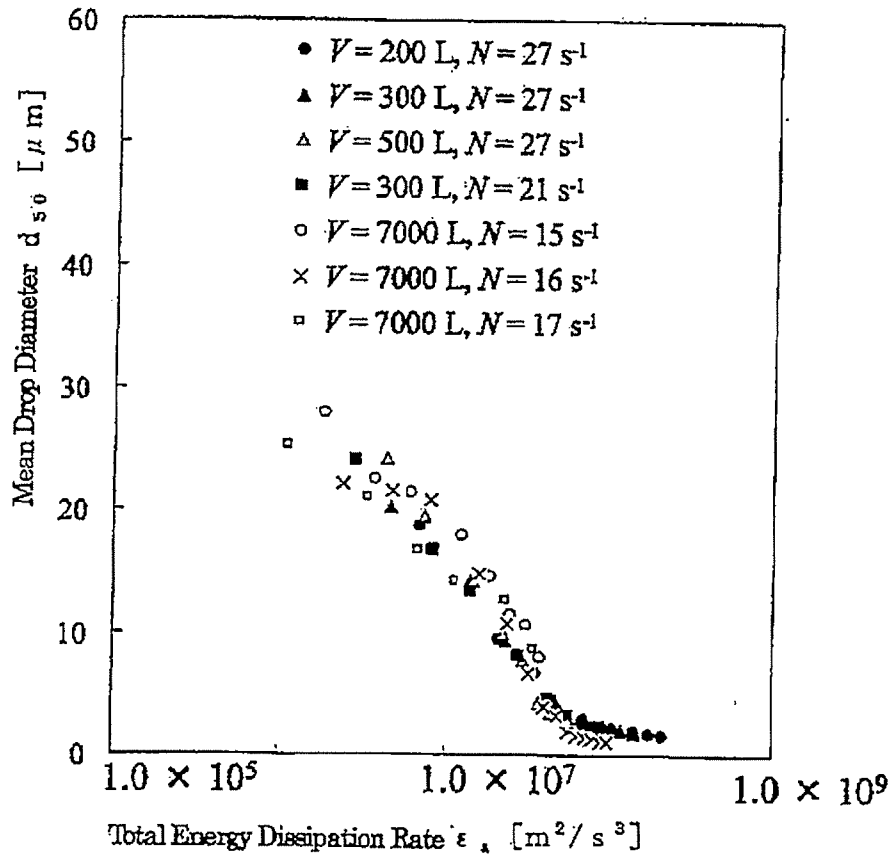
Relationship between Mixing Time and Liquid Drop Diameter under Running Conditions in Table 8 for Mixer C (Stators No. 1 to No.5)

Fig.9



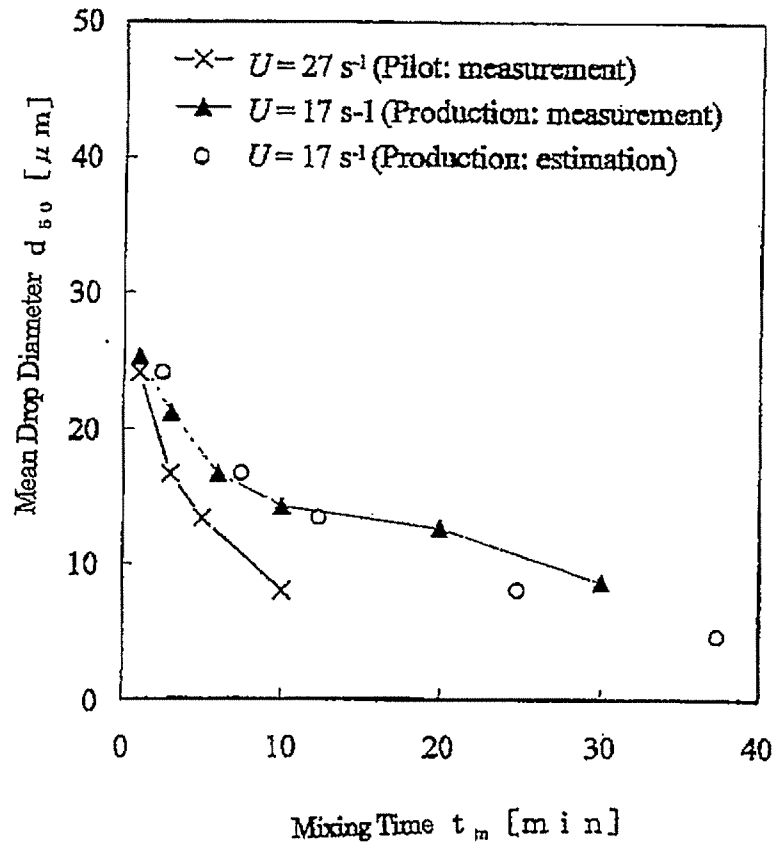
Relationship between Average Liquid Drop Diameter and Total Energy Dissipation Rate for Mixer C (Stators No. 1 to No.5)

Fig.10



Relationship between Mean Drop Diameter and Total Energy Dissipation Rate  
for Mixers D and E

Fig.11



Estimated Value and Actual Measured Value calculated from Equivalent Mixing Time

Fig.12

