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METHOD AND DEVICE FOR PRODUCING SOFT SOLDER POWDER ✓

The invention relates to a method for producing soft
5 solder powder without pressure, in particular exactly
spherical fine metal particles with a grain range between
1 to 100 μm and with a liquidus temperature of $<250\text{ }^{\circ}\text{C}$
from massive solder, whereby the solder existing in a
container is melted in an oil which remains stable at high
10 temperature and dispersed, while the density ratio
solder/oil is $\geq 2,5$.

The invention relates further to a device for the
pressureless production of soft solder powder, in
15 particular exactly spherical fine metal particles in a
grain size range of 1 to 100 μm and with a liquidus
temperature $<250\text{ }^{\circ}\text{C}$ from massive solder, with a heatable
container for melting the solder in an oil stable at high
temperature.

20 It is known to produce soft solder powder by using massive
solder metals through flow dispersion in liquids in
rapidly rotating agitators.

So for instance DD 237 575 A3 describes a method for
25 producing solder paste, whereby a solder carrier
consisting of colophonium, and organic solvent, a compound
with reducing action and triethanolamine is mixed with
soldermetal. In a receiver which can be cooled or heated
by choice with an agitator the solder carrier is produced
30 at $50\text{ }^{\circ}\text{C}$ by stirring. The solder metal is added in a
compact form to the receiver, while heating the latter to
a temperature which surpasses the melting point of the
solder metal by approximately $10\text{ }^{\circ}\text{C}$ and the melted mass
is dispersed by being agitated at a high speed of
35 approximately 10000 rpm.

After that it is cooled down to approximately 20 °C below the melting point of the solder metal and the agitator is kept at a low number of rotations per minute until it is cooled to room temperature. This known process has the disadvantages that the obtained particle size of approximately 150 µm does not result in fine metal powder. Besides the dispersed solder particles have also different diameters, i.e. they have by far a too broad grain distribution range. Therefore the known method has not proven itself on a large industrial scale, especially because it does not work continuously.

It is also known to use shearing devices working according to the rotor/stator principle for the production of emulsions (liquid/liquid) and suspensions (solid/liquid) IKA Maschinenbau-Prospekt "Dispergieren", pages 22-24, 1997). These devices are used for lacquers, dyes, pharmaceutical products, metal oxide suspensions and coated masses.

According to this known principle, as a rule, it has to be insured that in the case of highly viscous media the media flow has to be sustained by conveyor aggregates.

Furthermore from DE 44 02 042 A1 a process is known for producing microparticulate reflow-solder agents, whose solder metal content is present in a small grain size range. The compact solder metal is melted into an organic liquid which can be heated to high temperature, such as castor oil, and by means of a flow dispersion process, brought to a spherical symmetrical grain size range of preferably 3 to 10 µm in diameter, and the organic liquid is then removed to the extent that the metal particulate remains covered, so that it can be introduced in an emulsion and the individual particles of the suspension and emulsion are covered according to the method of

complex coacervation with a melamine polymerisate within the layer thickness range of 50 to 250 nm.

The microparticulate organic phase is then quantitatively
5 separated from the microparticulated metal phase. This microparticulate metal powders are protected by a duroplastic polymer system, however they can be released again only through the action of a highly activated fluxing agent. These fluxing agents lead to the
10 destruction of the microelectronic switching circuits and are therefore unsuitable.

Besides this method has been used only in laboratories and is not capable to insure a uniform sphere diameter from charge to charge.

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Another known solution (US Patent 4 648 820) melts metal such as aluminium in a crucible, feeds the melted metal to a cooling chamber filled with cooling fluids, wherein by means of spinning disks the liquids metal is dispersed in
20 drops, which again are drawn together with the cooling fluid into a recirculation cycle, whereby the latter is returned to the cooling chamber.

According to US Patent 5 411 602 the solder is melted and
25 the melted solder is divided into drops by means of inert gas. This state of the art is also plagued by the drawback that the produced metal particles do not have uniform sphere diameters, so that in any case sorting processes are necessary in order to select metal particles of an
30 approximately equal size having the same sphere diameter. That renders this known solution inefficient.

Given this state of the art, it is the object of the invention to improve a method and a device of the kind
35 mentioned in the introduction, so that the metal powders

produced according to the flow dispersion principle reach
a narrow grain size range clearly below 100 μm , a precise
5 spherical shape with an almost constant diameter, by
avoiding any screening and at low cost in a quasi-
continuous process.

This object is achieved with following steps:

- 10 a) gravity feeding the melted solder in a further oil
container by setting a volume ratio of oil and solder
melt of at least 10:1,
- b) dispersion of the liquefied solder by agitating and
subsequent shearing in consecutive shearing steps
15 according to the rotor/stator principle at speeds of
1500 to 5000 rpm with the addition of oil from the
container of step a),
- c) circulating by at least 20 times of the solder/oil
mixture of step b) in a counterflow over the oil
20 container of step and shearing steps, whereby through
the control of the shearing speed the number of the
steps and the geometry of the rotor, the particle size
and particle distribution of the dispersed material in
the dispersant are set,
- 25 d) discharging the solder/oil mixture from the circuit of
step c) into a further oil receiver for the separation
of the dispersed material through sedimentation and
returning the oil to the container of step b) and/or
a) and
- 30 e) extracting and feeding the dispersed material of step
d) for subsequent cleaning.

According to a further preferred feature of the method of
the invention, vegetable or animal oils, preferably castor
35 oil are used as oils.

It has surprisingly been found that solder melts with an extremely high viscosity at a density rate between the dispersed material and the dispersant of ≥ 2.5 can be separated with a shearing device without jamming the rotors in the stators and without requiring further conveying aggregates. Therefore in a further preferred embodiment of the method of the invention, the solder/oil mixture flows through the consecutive shearing steps in direction of gravity.

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The solder/oil mixture is pressed by gravity into the inlet of the first shearing step, where it enters the inner space of the first rotor and reaches the crenelated shearing openings of the first rotors, flows through the slots of the stators surrounding the first rotor and thereby being radially pressed into the inlet space of the second shearing step. By moving the rotor slots past the stator slots, due to the high peripheral speeds very high shearing forces are created, which separate the solder enveloped by the oil. Depending on the number and breadth of the slot openings in the individual shearing steps, the speed and the geometry of the rotors, it is possible to control the size of the solder particles at selected temperatures. Due to the high shearing forces the special advantage persists that the solder/oil mixture is conveyed to the circuit of step c).

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After a circulation of at least 20 times, and consequently repeated shearing, particles of clearly less than 100 μm .

In a further preferred embodiment of the method of the invention, the process temperature in steps b) and c) is set by approximately a maximum 30 °C above the liquidus temperature of the solder and the oil temperature of step d) at approximately 90 to 130 °C through the heat-carrying medium.

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In the case the density ratio of dispersed material to the dispersant is higher than ≥ 2.5 , the solder/oil mixture is additionally agitated.

- 5 A further preferred embodiment of the method of the invention provides that the individual steps be supplied by separate heating/cooling circuits. Of course when several steps are combined, it is part of the method of the invention to have one common heating/cooling circuit
10 each.

It is also conceivable to use only a single heating/cooling circuit.

- 15 In a further preferred embodiment of the method of the invention, for the extraction of the dispersed material of step e) a solvent is added, forming a suspension through agitation, which is pumped to a not represented cleaning installation for washing. As a solvent for step e), fat-
20 dissolving solvents, preferably acetone, have proven to be particularly suitable. The extraction of the dispersed material according to step e) can also be accomplished through gravity collection.

- 25 Further more the object of the invention is attained with a device wherein in a compact module the melt container for the massive solder and a dispersion container for the dispersion of the solder melt in oil are arranged in cascade to each another and a sedimentation tank for the
30 separation of the dispersed solder material from oil is arranged underneath the dispersion container, and that the container are interconnected by pipe conduits, whereby within the compact module the melt container is located above the dispersion container and that to the dispersion

container a multiple step shearing device is assigned for the separation of the solder melt into drops, whereby the feeding pipe from the melt container to the dispersion
5 container is connected to the dispersion container by an inclined pipe segment in the manner of an injector leading to the container bottom area, at whose lowest point a connection piece with a flange is provided for connecting the shearing device, whose outlet is flanged to the
10 recirculation conduit returning to the upper part of the dispersion container, which via a branched-off segment ends in the sedimentation container, which in turn is connected via an ascending pipe with the upper part of the dispersion container via a pump with drain-off pipes, and
15 that all containers, pipe conduits, the shearing device and pump can be heated or cooled by at least one tempering device.

According to a further feature of the device of the
20 invention, all containers and pipe conduits are built as double-walled bodies of stainless steel, preferably V2A, whose intermediate spaces formed by inner and outer walls are acted upon from the tempering device with a high-temperature heat carrier oil.

25 A further preferred embodiment of the device of the invention provides that the dispersion container is incorporated in a separate heating/cooling circuit, and the pump, the ascending pipe and drain-off pipe are
30 incorporated in a further separate heating/cooling circuit, the melt container with drain-off pipe, the shearing device and recirculation pipe conduit again in a separate heating/cooling circuit and additionally in a cooling circuit with a cooling container, the

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sedimentation container with the branched-off pipe are connected together in a separate heating/cooling circuit, whereby flexible, heatstable metal hoses constitute the
5 respective connecting pipe conduits and are respectively connected to a common distributor, which is connected with the tempering device through a flow line and a return line.

10 However it is also possible to incorporate all containers, pipe conduits, setting members, connection pieces, flanges and the shearing device in a common heating/cooling circuit, without leaving the framework of the invention. Also it pertains to the invention to use an electric
15 heating device instead of an oil heating device.

In a further suitable development of the device of the invention, the pipe conduits and the connection piece are provided with locking elements, preferably ball valves
20 made of stainless steel.

In a particularly advantageous further development of the invention, the shearing device consists of several,
25 preferably three rotors arranged corotationally on a drive shaft which have teeth spaced apart by slots, whereby the rotors are inserted into a stator separating the shearing steps from each other and insured against rotation, which has teeth spaced apart by slots, whereby during the
30 rotation of the rotor, the slots in the rotor and stator clear passage openings for the passage of the solder/oil mixture into the subsequent shearing step.

In a further preferred embodiment of the device of the
35 invention, the teeth of the rotor and stator form circles

of teeth, which are arranged concentrically with respect to each other and fitted into each other.

5 According to a further preferred feature of the device of the invention, the shearing device is arranged in a vertical position in alignment with the axis of the dispersion container, whereby the solder/oil mixture is independently sucked axially into the inlet of the
10 shearing device and pressed radially through the slots of the rotor-stator arrangement.

At bigger density differences between dispersed material and dispersant, particularly at a ratio ≥ 2.5 , the
15 dispersion container is suitably provided with an agitator.

In the sedimentation container there is an insert with a collection basket for collection and separation of the
20 solder particles from the process. Thereby the collection basket is located close to the bottom of the sedimentation container, so that due to gravity the solder particles drop into the collection basket, which can then later be removed from the sedimentation container.

25 According to a further preferred feature, instead of the drain-off pipe and the collection basket an agitator leading through the container cover of the sedimentation container and a height-adjustable dip pipe which reaches
30 down with one end close to the container bottom of the sedimentation container, and is connected at the other end to a pump with variable direction of rotation for aspiring the suspended dispersed material, respectively for feeding the solvent into the container, can be provided.

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In order to maintain the process temperature by at least 30 °C above the liquidus temperature, in all containers and pipe conduits temperature sensors are provided close
5 to the solder. This insures that the viscosity of the solder melt remains approximately the same in all stages.

In a further preferred embodiment of the device of the invention, the compact module consists of a housing frame
10 with a bottom plate, wherein table-like support stands for the preliminary assembly of the containers, pipe conduits, distributor and the pump are provided.

All containers, pipe conduits, flow and return lines,
15 locking members, the pump, shearing device, the metal hoses and the distributor are heated-insulated.

In a further preferred embodiment of the device of the invention, the tempering device is mobile and arranged
20 outside the compact module. However the tempering device can be just as well arranged in the compact module.

The invention distinguishes itself over all heretofore-
25 known flow dispersion processes in that the soft solder powder can be produced with exact spherical shape and within a narrow grain size range quasi-continuously on a large industrial scale. By simply exchanging the shearing device, by changing the slot dimensions, the variation of
30 the number of shearing steps, the rotational speeds and the number of the recirculations, the sphere diameters of the solder particles can be kept within a narrow grain size range, at low cost and with high precision.

The device of the invention is of compact construction,
35 user-friendly and requires little maintenance.

Further advantages and detail result from the following description with reference to the enclosed drawing.

The invention is subsequently described in more details
5 with aid of an embodiment example.

It shows:

- Fig. 1 the device of the invention illustrated in
10 The principle,
Fig. 2 a three-step shearing device in a sectioned
 representation,
Fig. 3 a variant of the sedimentation container
 for the removal of the dispersed material
15 as a detail according to fig. 1,
Fig. 4 and 5 a diagram of the heating/cooling circuit of
 the individual process steps and
Fig. 6 a diagram of the method of the invention.

20 As can be seen in detail from Fig. 1, the device of the invention consists of a container-like compact module 1, which lodges all essential components. The compact module 1 has a somewhat rectangular bottom plate 2, upon which vertical and horizontal struts 3 are connected to form a
25 parallelepipedic housing frame 4. The struts 3 consist of angle sections made of steel or aluminium. All lateral surfaces and the cover surface of the parallelepipedic housing frame 4 are lined with wall plates 5, which on their inside are provided with heat and sound insulating
30 plates 6, consisting of an appropriate sound-absorbing material coated with aluminium foil.

In the compact module 1 table-like support stands 7, 8 and 9 are inserted preassembled for the main components of the
35 device of the invention.

The support stand 7, also made of angle sections, receives the melt container 1 at its upper area 10 of the cover area of the compact module 1. In the middle and lower area of the support stand there are heat distributors 12 and 13
5 for the supply of the individual components with the heating medium. The melt container 11 has a curved bottom 14, at whose lowest point a vertically engaging drain-off pipe is connected. The drain-off pipe 15 is shaped as a 60° arc for the connection of a ball valve 17,
10 by means of which the drain-off pipe 15 can be opened and closed.

The ball valve 17 continues on the outlet side with a conduit segment 18, which reaches injector-like into the bottom area of the dispersion container 19 at an angle of
15 60°. The dispersion container 19 is supported by the support stand 8 and is positioned so that it is located sufficiently deeper than the deepest point of the melt container 11, so that the solder melt can reach the dispersion container 19 due to gravity.

20 The dispersion container 19, just like the melt container 11, has a curved bottom area, where the solder melt collects. In the deepest point of the dispersion container 19 an outgoing connection piece 20 is provided in alignment with the container axis of the dispersion
25 container 19, for the connection with a ball valve 21 for opening and closing the connection piece 20. On the outgoing side the ball valve 21 is connected on a flange 22 to which the shearing device 23 is connected with its inlet flange 24 in vertical fitting position. The outlet
30 25 of the shearing device 23 is provided with an outlet flange 26, which is positioned perpendicularly with respect to the fitting position.

Besides that, on the support stand 8 a recirculation conduit 27 with a pre-mounted flange 28 releasably

connected with the connection flange 26 of the shearing device 23, is connected.

5 The shearing device 23 with its drive aggregate 29 is held by an insert movable on the bottom plate 2 in such a manner that the shearing device 23 can be screwed without tension to the flange 22 of the ball valve 21, respectively to the flange 28 of the recirculation conduit
10 27.

As shown in Fig. 2, the shearing device 23 consists of three shearing steps S1, S2 and S3 with six shearing spaces 58. Each shearing step is comprises a rotor 31 and a stator 32. The rotor sits corotationally on the drive
15 shaft 33 of the shearing device 23, which is driven by drive aggregate 29, for instance a motor. The rotor 31 rotates with the drive shaft 33 in the stator 32 with a speed of approximately 2500 rotations per minute and has teeth distributed coaxially with the shaft 33, which are
20 spaced apart by slots 34. The stator 32 also has teeth spaced apart by slots. The teeth are arranged coaxially with respect to each other. The slots 34 and 35 lead into the second shearing step S2.

The second shearing step is built just like the first one,
25 only that the number of teeth, and therewith the number of slots 34 in the stator 32 is bigger. Again the slots 34 in the stator 32 of the shearing step S2 lead into the space of the shearing step S3.

30 According to Fig. 1, the recirculation conduit 27 leads back into the upper area of the dispersion container 19, whereby this conduit ends above the liquid level of the filling medium in the dispersion container 19 and can be opened and closed by a ball valve 37 located approximately
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at the level of the container bottom. Approximately underneath this ball valve 37, recirculation conduit 27
5 has a horizontally running branched-off conduit 38 with flange 39, on which a ball valve 40 is flanged, which on the outgoing side engages in the upper area of a sedimentation container 41.

This sedimentation container is located clearly underneath
10 the dispersion container 19 and is received by the support stand 9, which is connected with the frame of the support stand 8. In the sedimentation container 41, at the bottom side an insert 42 with a collection basket 43 is inserted. Two outlet conduits 44 and 45 lead to the bottom area of
15 the sedimentation container 41 via a rotary piston pump 46 into an ascending conduit 47 fastened in the frame of the support stand 8, which is returned to the upper area of the dispersion container above the surface level of the filling medium. In the outlet conduits 44 and 45 ball
20 valves 48 and 49 are integrated, for opening and closing the conduits.

Instead of the collection basket 43 and instead of the outlet conduit 45, as shown in Fig. 3, an agitator 64 and a dip pipe 63 can be provided. The agitator 64 passes
25 through the container cover 62 of the sedimentation container 41 and reaches close to the level at which the horizontal branched-off pipe 38 enters the container 41. The dip pipe 63 also passes through container cover 62 and is height-adjustable fastened to it, so that the dipping
30 depth T of the dip pipe 63 in the sedimentation container is variable. The end of the dip pipe 62 (sic) which projects from the container cover is connected with a pump with variable rotation direction not shown in the drawing, so that by means of this dip pipe solder material

dispersed in the solvent are aspirated, respectively solvent can be pumped into the sedimentation container 41. By means of the agitator 64, the dispersed solder sinking due to gravity and the solvent are converted into a suspension.

Naturally, there is no need for specially mentioning that the outlet conduit 45 can be remain mounted, when the dispersed solder material is aspirated for being fed to a cleaning installation not shown in the drawing. The containers 11, 19, 41, the pipe conduits 15, 18, 27, 38, 44, 47 and 63, the heat distributors 12 and 13, the ball valves 17, 21, 37, 40, 48 and 49 are enveloped with a heat insulation not shown in the drawing.

Fig. 4 and 5 show the heating/cooling circuits for the containers and pipe conduits. All containers and pipe conduits are double-wall bodies made of stainless steel, for instance V2A.

The spaces between the outer wall and inner wall of the double-wall bodies are acted upon with a available heat carrier oil, which guarantees a temperature in use of 300 °C. From the tempering device 51 flexible metal hoses 56 as flow and return lines VL, respectively RL, to the heat distributor 12, which by means of equally flexible metal hoses 56 forms heating/cooling circuits I and II. The heating/cooling circuit I leads from the flow line VL of the distributor 12 via the rotary piston pump 46, the ascending pipe 47 and the outlet conduit 44 to the return line of the heat distributor 12. The heating/cooling circuit II supplies exclusively the dispersion container 19. The separate cooling circuit VI cools not illustrated slidable ring seals in the shearing device 23. From a cooling-medium container 61 provided with a pump

cooling fluid is sent according to the siphon principle via the supply line 59 to the shearing device 23 and
5 returned to the cooling-medium container 61 via drain 60.

The outer heat distributor 13 is connected with the tempering device 51 via flexible metal hoses 56. Altogether from the heat distributor 13 run the
10 heat/cooling circuits III, IV and V. In the heating/cooling circuit III the melt container 11 and the drain-off pipe 15 are integrated, in the heating/cooling circuit IV the shearing device 23 and the recirculation conduit 27, in the heating/cooling circuit V the
15 sedimentation container 41 with the branched-off pipe 38 and the branched-off pipe 45. Flexible metal hoses form here also the corresponding supply lines.

Fig. 6 represents the flow of the process according to the
20 invention. In the melt container 11 massive solder, for instance 10 kg of a Sn63Pb37 alloy, is introduced together with castor oil. The is completely covered by the oil and melted. The work temperature is kept approximately 60 °C above the liquidus temperature by means of the
25 heating/cooling circuit II.

In the melt container 11 a temperature sensor 52 is mounted for the precise temperature adjustment. This measured value serves for the control of the heating/cooling circuit.

30 After the massive solder has been melted, the ball valve 17 is opened and the solder melt flows together with the oil into the dispersion container 19, whose dimensions are selected so that the ratio is one part solder melt to ten parts oil. The solder melt sinks to the bottom area of the

dispersion container 19 and, when the ball valve 21 is open, reaches the shearing device 23 via outlet pipe 20 and the inlet 53. Thereby the solder melt flows axially towards the first shearing step S1, wherein the melt is caught by the rotor 31 of the shearing device and separated.

10 The rotor 31 rotates with the drive shaft 33 of the shearing device 23, which is driven by drive aggregate 29. The solder melt is radially diverted through the crenelated slots 34 of the rotor 31 and pressed into the crenelated slots 35 of the stator 32, when the slots 34 in the rotor 31 and the slots 35 in the stator 32 come to coincide, clearing an outlet opening. During the passage of the slot 34 the melt flow is being sheared. Melt droplets result. After completing the first shearing step S1, the melt/oil mixture reaches the second shearing step S2, where again an axial feeding and a radial deflection of the solder/oil mixture take place, before the third shearing step S3 is traversed.

Depending on the width, respectively geometry of the slots at the periphery of the rotor 31 and the stator 32, as well as on the rotational speed, it is possible to set the desired particle size of the separated solder melt particles.

After the separation of the solder melt in the shearing steps S1, S2 and S3, the solder/oil mixture reaches the recirculation conduit 27 opened by means of ball valve 55, while the ball valve 40 of the branched-off pipe 38 is closed.

Now the solder/oil mixture is passed at least 20 times through the dispersion container 19 and the three-stage

shearing device 23. This insures the desired particle sizes of 1 to 100 μm can be set. If particle sizes of for instances 6 μm are desired, then with the method of the invention this size can be achieved without subsequent sorting.

A solder/oil dispersed phase results. The suction power of the shearing steps is sufficient for performing the recirculation without additional conveying aggregates. The ball valve 37 is closed and by opening the ball valve 40, the solder/oil phase is guided through the branched-off pipe 38 into the sedimentation container 41, due to gravity the solder particles sink into the collection basket 43 of the insert 42, thereby being separated from the excess oil, whereby the solder particles remain enveloped by oil. After closing the ball valve 40 and opening the ball valves 48, respectively 49, the oil is returned to the dispersion container 19 via the rotary piston pump 46 and the ascending pipe 47.

Naturally the removal of the solder particles from the sedimentation container 41 can also be done so that, after the solder particles have sunk, the excess oil is aspirated as previously described and returned to the dispersion container 19. The ball valve 49 is closed. Through the dip pipe 63 a fat dissolving solvent, for instance acetone, is introduced into sedimentation container 41 by means of a pump with variable direction of rotation, not shown in the drawing. The solvent and the solder particles are then agitated by an agitator 64 until a suspension which can be pumped is formed. After the rotation direction of the pump is reversed, the suspension is sucked out of the sedimentation container 41 and sent to a cleaning installation not shown in the drawing.

Through the heating circuit V in the sedimentation container 41 a temperature of about 100 °C is set, in

order to correspondingly cool down the solder particles prior removal. When the collection basket 43 is retrieved,
5 the ball valves 40, 48 and 49 are closed.

After the collection basket 43 is reinserted, the ball valve 40 of the branched-off pipe 38 remains closed and the ball valve 37 of the recirculation circuit 27 is opened, so that the aforementioned process can be
10 repeated.

With the heating/cooling circuits I to IV, a process temperature of about 60 °C above the liquidus temperature of the solder is maintained in the containers 11 and 19,
15 the pipe conduits 15, 18, 27, 38, 44, 45, the ball valves 17, 21, 37, 40, 48 and 49, as well as in the shearing device 23.

The soft solders produced with the method of the invention
20 achieve a narrow grain size range up to 100 µm, whereby sorting is completely eliminated. By selecting the number, shape of the slots in the shearing device as well as the speed of the rotors and the number of recirculations, it is possible also set an exact grain size of less than 100
25 µm.

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List of used reference numbers

Compact module	1
Bottom plate	2
struts of 1	3
housing frame	4
wall plates	5
heat and sound insulating plates	6
support stands	7, 8, 9
upper area of support stand 7	10
melt container	11
heat distributor	12, 13
bottom of 11	14
drain-off pipe 11	15
flange on 15	16
ball valve on 15	17
pipe conduit segment	18
dispersion container	19
connection piece on 19	20
ball valve	21
flange on 21	22
shearing device	23
inlet flange of 23	24
outlet on 23	25
outlet flange	26
recirculation conduit	27
flange of 27	28
drive aggregate of 23	29
mobile insert	30
rotor	31
stator	32
drive shaft	33
slots in 31	34
slots in 32	35

upper area of 19	36
ball valve of 27	37
branched-off pipe	38
flange of 38	39
ball valve of 38	40
sedimentation container	41
insert in 41	42
collection basket	43
outlet conduits	44, 45
rotary piston pump	46
ascending pipe	47
ball valve	48, 49
spaces	50
tempering device	51
temperature sensor	52
inlet of 23	53
passage opening	54
ball valve for 23	55
metal hoses	56
agitator in 19	57
shearing spaces	58
supply line for cooling fluid	59
drain for cooling fluid	60
container for cooling fluid	61
container cover of 41	62
dip pipe in 41	63
agitator in 41	64
shearing steps	S1, S2, S3
heating/cooling circuits	I, II, III, IV, V
cooling circuit	VI
flow line	VL
return line	RL
dipping depth	T

Claims

1. Method for pressureless production of soft solder powder, particularly of exactly spherical fine metal particles in a grain size range of 1 to 100 μm and with a liquidus temperature $<250\text{ }^{\circ}\text{C}$ from massive solder, whereby the solder existing in a receiver is melted in an oil which remains stable at high temperature and subsequently dispersed whereby the solder/oil density ration is ≥ 2.5 , with following steps:
- a) gravity feeding the melted solder into a further oil container while setting volume ratio of oil to solder melt of at least 10:1,
 - b) dispersing the liquefied solder through agitating and mechanical shearing in consecutive shearing steps according the rotor-stator-principle at rotational speeds of 1500 to 5000 rpm, while adding oil from the container of step a),
 - c) recirculating the solder/oil mixture of step b) at least 20 times in a circuit against the flow direction through oil container of step a) and the shearing steps, whereby due to the control of the peripheral speed, the number of steps and the geometry of the rotor, the particle size distribution of the dispersed material is set,
 - d) discharging the solder/oil mixture from the circuit of step c) in a further container for the separation of the dispersed material through sedimentation and returning the oil to the container of step b) and/or a) and
 - e) removing the dispersed material of step d) for cleaning.



2. Method according to claim 1, characterized in that as oil vegetable and animal oils are used, preferably castor oil.
- 5 3. Method according to claim 1, characterized in that the solder/oil mixture flows through the succession of shearing steps in gravity direction.
4. Method according to claim 1 to 3, characterized
10 in that the circuit of step c) is self-feedingly entrained by the rotor/stator.
5. Method according to claim 1, characterized in that the process temperature is set by the oil temperature
15 in steps b) and d) at least by 30 °C above the liquidus temperature and the oil temperature after discharge of step d) is set at 20 to approximately 130 °C.
6. Method according to one or more of claims 1 to
20 5, characterized in that the process temperature in the individual steps is controlled through separate heating/cooling circuits.
7. Method according to one or more of claims 1 to
25 6, characterized in that the process temperature in all steps is set by a single heating/cooling circuit.
8. Method according to claim 1, characterized in that the removal of dispersed material of step e) is
30 performed by adding solvent to the dispersed material, agitating and producing a suspension and conveying the suspension for washing by pumping it out.
9. Method according to claim 1, characterized in
35 that the removal of the dispersed material of step e) is performed by gravity separation.



10. Method according to claim 8, characterized in that as solvent for step e) a fat-dissolving solvent, preferably acetone, is used.

5 11. Device for the pressureless production of soft solder powder, preferably exactly spherical fine particles in a grain size range of 1 to 100 μm and with a liquidus temperature $<250\text{ }^{\circ}\text{C}$ from massive solder, with a heatable container for melting the solder in an oil which remains
10 stable at high temperatures, characterized in that in a compact module (1) melt container (11) for the massive solder and a dispersion container (19) are arranged in a cascade to each other and a sedimentation container (41) for separating the dispersed solder material from the oil
15 is arranged underneath the dispersion container, all being interconnected by pipe conduits (15, 18, 27, 38, 44, 45, 47), whereby the melt container (11) is located above the dispersion container (19) in the compact module (1), and that the dispersion container (19) is associated with a
20 multistep shearing device (23) for the separation of the solder melt into melt droplets, whereby the conduit (15) from the melt container to the dispersion container (19) leads injector-like through a pipe segment (18) at an inclination into the bottom area of the dispersion
25 container, at whose deepest point a connection pipe (20) with a flange (22) for the connection the shearing device (23) is arranged, whose outlet (25) is flanged to the recirculation conduit (27) leading to the upper part of the dispersion container, which ends via a branched-off
30 pipe (38) in the sedimentation container (41), which in turn through an ascending pipe (47) is in contact with the upper part of the dispersion container (19) via a pump (46) with outlet conduits (44, 45), and that all containers (11, 19, 41), pipe conduits (15, 18, 27, 38,
35 44, 45, 47), the shearing device (23) and the pump (46) is heated by means of at least one tempering device (51).



12. Device according to claim 11, characterized in that all containers (11, 19, 41) and pipe conduits (15, 18, 27, 38, 44, 45, 47) are double-walled bodies made of stainless steel, preferably V2A, whose spaces (50) formed by the inner and outer walls are acted upon with a high temperature heat carrier oil by the tempering device (51).

13. Device according to claim 11, characterized in that the dispersion container (19) is integrated in a separate heating/cooling circuit (II) and the pump (46), ascending pipe (47) and the outlet conduit (34) are integrated in a further heating/cooling circuit (I), and that the melt container (11) with drain-off pipe (15) are integrated in a separate heating/cooling circuit (III), the shearing device (23) and the recirculation conduit (27) are integrated in a separate heating/cooling circuit (IV) and additionally in a cooling circuit (VI) with the cooling-medium container (61), the sedimentation container (841) with branched-off pipe (38) and outlet conduit (45) are integrated in a separate heating/cooling conduit (V), whereby heat-resistant flexible metal hoses (56) form the connecting pipe conduits, each being connected to at least one common distributor (12, 13), which is connected to the tempering device (51) via a flow and return line.

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14. Device according to claim 11, characterized in that all containers (11, 19, 41), pipe conduits (15, 18, 27, 38, 44, 45, 47), locking members (17, 21, 37, 40, 48, 49, 55), flanges (16, 22, 24, 26, 28, 39) and the shearing device (23) are integrated in a single heating/cooling circuit.

15. Device according to claim 11, characterized in that all containers (11, 19, 41), pipe conduits (15, 18, 27, 38, 44, 45, 47), locking members (17, 21, 37, 40, 48, 49, 55), flanges (16, 22, 24, 26, 28, 39) and the shearing device (23) can be electrically heated, preferably by means of heating cuffs.



16. Device according to claim 11, characterized in that the pipe conduits (15, 18, 27, 38, 44, 45, 47) are provided with locking members, preferably ball valves.

17. Device according to one or more of claims 11 to 16, characterized in that the shearing device (23) consists of several, preferably three rotors (31) arranged consecutively on a drive shaft (33) corotationally with the same, having teeth spaced apart by slots (34), whereby the rotors (31) are set in a stator (32) secured against rotation, separating the shearing steps from each other, having teeth spaced apart by slots (35), whereby during rotation the slots (34, 35) in the rotor and stator leave passage openings (54) for the passage of solder/oil mixture to the following shearing step.

18. Device according to claim 17, characterized in that the teeth of the rotor (31) and the stator (32) form tooth circles which are arranged concentrically with respect to each other and interfitted.

19. Device according to one or more of claim 11 to 17, characterized in that the shearing device (23) is arranged in vertical position in alignment with the container axis of the dispersion container (19), whereby the solder/oil mixture is independently sucked axially into the inlet (53) of the shearing device (23) and pressed radially through the slots (34, 35) of the rotor-stator assembly.

20. Device according to one or more of claims 11 to 18, characterized in that the dispersion container (19) is provided with an agitator (57).



21. Device according to claim 11, characterized in that in the sedimentation container (41) an insert (42) with a collection basket (43) is arranged.

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22. Device according to claim 21, characterized in that the collection basket (43) has adjustable outlet openings at its periphery.

10 23. Device according to claim 11 and 21, characterized in that instead of the outlet conduit (45) and the collection basket (43), a dip pipe (63) passing through the container cover (62) of the sedimentation container (41) reaches with one end close to the container
15 bottom of the container (41) and on the other end is connected with a pump with variable direction of rotation for aspiring of the suspended dispersed material, respectively for the introduction of solvent in the container (41), and that the sedimentation container (41)
20 is provided with an agitator (64).

24. Device according to one or more of claims 11 to 23, characterized in that in the containers (11, 19, 41) and pipe conduits (15, 18, 27, 38, 44, 45, 47, 63)
25 temperature sensors (52) are arranged for measuring the temperature of the solder.

25. Device according to claim 11, characterized in that the compact module (1) consists of a housing frame
30 (4) with a bottom plate (2), wherein table-like support stands (7, 8, 9) are provided for the preliminary assembly of the containers (11, 19, 41), pipe conduits (27, 38, 44, 45, 47), the distributors (12, 13) and the pump (46).

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26. Device according to claim 11 and 25,
characterized in that the shearing device (23) is received
5 by an insert (30) movable on the bottom plate and is
tensionless held on the flange (22) of the ball valve (21)
and the flange (28) of the recirculation conduit (27).

27. Device according to claim 11 and 25,
10 characterized in that the housing frame (4) is provided
with wall plates whose inner sides have heat and sound
insulating plates (6) coated with aluminium foil.

28. Device according to claim 11, characterized in
15 that the containers (11, 19, 41), the pipe (15, 18, 20,
27, 38, 44, 45, 47, 63), the flow and return lines (VL;
RL), the locking organs (17, 21, 37, 40, 48, 49, 55), the
pump (46), the metal hoses (56) and the distributors (12,
13) are heat-insulated.

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29. Device according to claim 11, characterized in
that the tempering device (51) is mobile and can be
arranged outside the compact module (1).

