[0075] Prior to incorporation into the finished catalysts, the conventional USY and HNPV USY zeolites were analyzed by transmission electron microscopy (TEM). The TEM images for the conventional USY and HNPV USY are presented in Figures 1 and 2, respectively.

[0076] In addition, the pore size distributions were determined for the conventional USY and HNPV zeolites. A plot of the pore size distributions for the two zeolites is presented in Figure 3.

[0077] OD acidity was determined by the amount of bridged hydroxyl groups exchanged with deuterated benzene at 80°C, which is measured by FT-IR.

TABLE 7

USY	conventional USY	HNPV USY
Mesopore volume (cc/g)	0.11	0.18
NPV - 8 nm - 20 nm (%)	49.5	25.7
NPV - 20 nm - 50 nm (%)	20.8	53.2
NPV - > 50 nm (%)	18.1	21.1
unit cell size (Å)	24.28	24.29
silica/alumina ratio	30	30-

TABLE 8

	conventional USY	HNPV USY
Brönsted acid sites determined by FTIR after H-D exchange (mmol/g)		
HF(OD)	0.184	0.153
HF'(OD)	0.027	0.017
LF(OD)	0.096	0.0507
LF'(OD)	0.008	0.006
Total	0.316	0.227
ASDI	0.13	0.11

What is claimed is:

1. A hydrocracking catalyst, comprising:

a support;

an amorphous silica alumina material;

a stabilized Y zeolite having a pore volume in the 20 nm to 50 nm range of 0.15 to 0.6 cc/g, a Brønsted acidity of 0.2-1.2 mmole/g, and an acid site distribution index factor of between 0.02 and 0.12.; and

at least one metal selected from the group consisting of elements from Group 6 and Groups 8 through 10 of the Periodic Table,

wherein the stabilized Y zeolite meets one or more of the following conditions:

20 to 30% of the pores are in the 8 nm to 20 nm range;

40 to 60% of the pores are in the 20 nm to 50 nm range;

15 to 25% of the pores are greater than 50 nm.

2. The hydrocracking catalyst of Claim 1, wherein the stabilized Y zeolite has an acid site distribution index factor of between 0.06 and 0.12.

3. The hydrocracking catalyst of Claim 1, wherein the stabilized Y zeolite has an acid site distribution index factor of between 0.08 and 0.11.

4. The hydrocracking catalyst of Claim 1, wherein 20 to 30% of the pores are in the 8 nm to 20 nm range.

5. The hydrocracking catalyst of Claim 1, wherein 40 to 60% of the pores are in the 20 nm to 50 nm range.

6. The hydrocracking catalyst of Claim 1, wherein 15 to 25% of the pores are greater than 50 nm.

7. A process for hydrocracking a hydrocarbonaceous feedstock, comprising contacting the feedstock with a hydrocracking catalyst under hydrocracking conditions to produce a hydrocracked effluent;

the hydrocracking catalyst comprising: a support;

an amorphous silica alumina material;

a stabilized Y zeolite having a pore volume in the 20 nm to 50 nm range of 0.15 to 0.6 cc/g and an acid site distribution index factor of between 0.02 and 0.12; and

at least one metal selected from the group consisting of elements from Group 6 and Groups 8 through 10 of the Periodic Table,

wherein the stabilized Y zeolite meets one or more of the following conditions:

20 to 30% of the pores are in the 8 nm to 20 nm range;

40 to 60% of the pores are in the 20 nm to 50 nm range;

15 to 25% of the pores are greater than 50 nm.

8. The process of Claim 7, wherein the stabilized Y zeolite has an acid site distribution index factor of between 0.06 and 0.12.

9. The process of Claim 7, wherein the stabilized Y zeolite has an acid site distribution index factor of between 0.08 and 0.11.

10. The process of Claim 7, wherein 20 to 30% of the pores are in the 8 nm to 20 nm range.

11. The process of Claim 7, wherein 40 to 60% of the pores are in the 20 nm to 50 nm range.

12. The process of Claim 7, wherein 15 to 25% of the pores are greater than 50 nm.

13. The process of Claim 7, wherein the hydrocracked effluent is a heavy middle distillate product in the 380 to 700°F range.