

HIGHER DENSITY POLYOLEFINS WITH IMPROVED STRESS CRACK RESISTANCE

BACKGROUND OF THE INVENTION

5 Polyolefins such as high density polyethylene (HDPE) homopolymer and linear
low density polyethylene (LLDPE) copolymer can be produced using various
combinations of catalyst systems and polymerization processes. Chromium-based
catalyst systems can, for example, produce olefin polymers having good extrusion
processibility and polymer melt strength, typically due to their broad molecular weight
10 distribution (MWD).

In some end-use applications, it can be beneficial to have the processibility and
melt strength similar to that of an olefin polymer produced from a chromium-based
catalyst system, as well as improvements in stress crack resistance (e.g., higher notched
tensiles, lower natural draw ratios) at equal or higher polymer densities. Accordingly,
15 it is to these ends that the present invention is directed.

SUMMARY OF THE INVENTION

This summary is provided to introduce a selection of concepts in a simplified
form that are further described below in the detailed description. This summary is not
intended to identify required or essential features of the claimed subject matter. Nor is
20 this summary intended to be used to limit the scope of the claimed subject matter.

The present invention generally relates to new catalyst compositions, methods
for preparing catalyst compositions, methods for using the catalyst compositions to
polymerize olefins, the polymer resins produced using such catalyst compositions, and
articles produced using these polymer resins. In particular, aspects of the present
25 invention are directed to catalyst compositions employing two or three metallocene
catalyst components. The first catalyst component can comprise an unbridged
zirconium or hafnium based metallocene compound, while the second catalyst
component can comprise a bridged zirconium or hafnium based metallocene compound
with a fluorenyl group. If used, the third catalyst component can comprise a titanium
30 or chromium half-metallocene compound. Such catalyst compositions can be used to
produce, for example, ethylene-based copolymers having medium densities and
improved stress crack resistance.

The present invention also contemplates and encompasses olefin polymerization processes. Such processes can comprise contacting a catalyst composition with an olefin monomer and optionally an olefin comonomer under polymerization conditions to produce an olefin polymer. Generally, the catalyst composition employed can
5 comprise any of the catalyst component I metallocene compounds, any of the catalyst component II metallocene compounds, any of the optional catalyst component III metallocene compounds, and any of the activators and optional co-catalysts disclosed herein. For example, organoaluminum compounds can be utilized in the catalyst compositions and/or polymerization processes.

10 Polymers produced from the polymerization of olefins, resulting in homopolymers, copolymers, terpolymers, etc., can be used to produce various articles of manufacture. A representative and non-limiting example of an olefin polymer (e.g., an ethylene copolymer) consistent with aspects of this invention can be characterized as having the following properties: a density from about 0.930 to about 0.948 g/cm³, a
15 zero-shear viscosity greater than about 5×10^5 Pa-sec, a CY-a parameter in a range from about 0.01 to about 0.40, a peak molecular weight in a range from about 30,000 to about 130,000 g/mol, and a reverse comonomer distribution. Another representative and non-limiting ethylene-based polymer described herein can have a density from about 0.930 to about 0.948 g/cm³, a single point notched constant tensile load of at least
20 6,500 hours, and a natural draw ratio of less than or equal to about 525 %. Yet another representative and non-limiting ethylene-based polymer described herein can have a density from about 0.930 to about 0.948 g/cm³, and a relationship between natural draw ratio (NDR, %) and density (g/cm³) defined by the equation, $NDR < 7800(\text{density}) - 6800$ or, additionally or alternatively, $NDR < 13404(\text{density}) - 12050$.

25 Both the foregoing summary and the following detailed description provide examples and are explanatory only. Accordingly, the foregoing summary and the following detailed description should not be considered to be restrictive. Further, features or variations may be provided in addition to those set forth herein. For example, certain aspects and embodiments may be directed to various feature
30 combinations and sub-combinations described in the detailed description.

BRIEF DESCRIPTION OF THE FIGURES

FIG. 1 presents a plot of the molecular weight distribution and short chain branch distribution of the polymer of Example 4.

5 **FIG. 2** presents a plot of the molecular weight distribution and short chain branch distribution of the polymer of Example 10.

FIG. 3 presents a plot of the molecular weight distribution and short chain branch distribution of the polymer of Example 12.

10 **FIG. 4** presents a dynamic rheology plot (viscosity versus frequency) at 190 °C for the polymers of Examples 1 and 7.

FIG. 5 presents a dynamic rheology plot (viscosity versus frequency) at 190 °C for the polymers of Examples 1 and 9.

FIG. 6 presents a dynamic rheology plot (viscosity versus frequency) at 190 °C for the polymers of Examples 1 and 10.

15 **FIG. 7** presents a dynamic rheology plot (viscosity versus frequency) at 190 °C for the polymers of Examples 13 and 14.

FIG. 8 presents a dynamic rheology plot (viscosity versus frequency) at 190 °C for the polymers of Examples 18 and 21.

20 **FIG. 9** presents a plot of the molecular weight distributions of the polymers of Examples 1 and 7.

FIG. 10 presents a plot of the molecular weight distributions of the polymers of Examples 1 and 10.

FIG. 11 presents a plot of the molecular weight distributions of the polymers of Examples 13 and 14.

25 **FIG. 12** presents a plot of the molecular weight distributions of the polymers of Examples 18 and 21.

FIG. 13 presents a plot of the molecular weight distributions of the polymers of Examples 4 and 23-25.

30 **FIG. 14** presents a plot of the natural draw ratio versus the density for certain polymers described in the Examples.

FIG. 15 presents a plot of the natural draw ratio versus the density for certain polymers described in the Examples.

DEFINITIONS

To define more clearly the terms used herein, the following definitions are provided. Unless otherwise indicated, the following definitions are applicable to this disclosure. If a term is used in this disclosure but is not specifically defined herein, the definition from the IUPAC Compendium of Chemical Terminology, 2nd Ed (1997) can be applied, as long as that definition does not conflict with any other disclosure or definition applied herein, or render indefinite or non-enabled any claim to which that definition is applied. To the extent that any definition or usage provided by any document incorporated herein by reference conflicts with the definition or usage provided herein, the definition or usage provided herein controls.

While compositions and methods are described herein in terms of “comprising” various components or steps, the compositions and methods can also “consist essentially of” or “consist of” the various components or steps, unless stated otherwise. For example, a catalyst composition consistent with aspects of the present invention can comprise; alternatively, can consist essentially of; or alternatively, can consist of; (i) catalyst component I, (ii) catalyst component II, (iii) an activator, and (iv) optionally, a co-catalyst.

The terms “a,” “an,” “the,” etc., are intended to include plural alternatives, e.g., at least one, unless otherwise specified. For instance, the disclosure of “an activator-support” or “a metallocene compound” is meant to encompass one, or mixtures or combinations of more than one, activator-support or metallocene compound, respectively, unless otherwise specified.

Generally, groups of elements are indicated using the numbering scheme indicated in the version of the periodic table of elements published in *Chemical and Engineering News*, 63(5), 27, 1985. In some instances, a group of elements can be indicated using a common name assigned to the group; for example, alkali metals for Group 1 elements, alkaline earth metals for Group 2 elements, transition metals for Group 3-12 elements, and halogens or halides for Group 17 elements.

For any particular compound disclosed herein, the general structure or name presented is also intended to encompass all structural isomers, conformational isomers, and stereoisomers that can arise from a particular set of substituents, unless indicated otherwise. Thus, a general reference to a compound includes all structural isomers

unless explicitly indicated otherwise; e.g., a general reference to pentane includes n-pentane, 2-methyl-butane, and 2,2-dimethylpropane, while a general reference to a butyl group includes an n-butyl group, a sec-butyl group, an iso-butyl group, and a tert-butyl group. Additionally, the reference to a general structure or name encompasses all
5 enantiomers, diastereomers, and other optical isomers whether in enantiomeric or racemic forms, as well as mixtures of stereoisomers, as the context permits or requires. For any particular formula or name that is presented, any general formula or name presented also encompasses all conformational isomers, regioisomers, and stereoisomers that can arise from a particular set of substituents.

10 The term “substituted” when used to describe a group, for example, when referring to a substituted analog of a particular group, is intended to describe any non-hydrogen moiety that formally replaces a hydrogen in that group, and is intended to be non-limiting. A group or groups can also be referred to herein as “unsubstituted” or by equivalent terms such as “non-substituted,” which refers to the original group in which
15 a non-hydrogen moiety does not replace a hydrogen within that group. Unless otherwise specified, “substituted” is intended to be non-limiting and include inorganic substituents or organic substituents as understood by one of ordinary skill in the art.

The term “hydrocarbon” whenever used in this specification and claims refers to a compound containing only carbon and hydrogen. Other identifiers can be utilized
20 to indicate the presence of particular groups in the hydrocarbon (e.g., halogenated hydrocarbon indicates the presence of one or more halogen atoms replacing an equivalent number of hydrogen atoms in the hydrocarbon). The term “hydrocarbyl group” is used herein in accordance with the definition specified by IUPAC: a univalent group formed by removing a hydrogen atom from a hydrocarbon (that is, a
25 group containing only carbon and hydrogen). Non-limiting examples of hydrocarbyl groups include alkyl, alkenyl, aryl, and aralkyl groups, amongst other groups.

The term “polymer” is used herein generically to include olefin homopolymers, copolymers, terpolymers, and so forth. A copolymer is derived from an olefin monomer and one olefin comonomer, while a terpolymer is derived from an olefin
30 monomer and two olefin comonomers. Accordingly, “polymer” encompasses copolymers, terpolymers, etc., derived from any olefin monomer and comonomer(s) disclosed herein. Similarly, an ethylene polymer would include ethylene

homopolymers, ethylene copolymers, ethylene terpolymers, and the like. As an example, an olefin copolymer, such as an ethylene copolymer, can be derived from ethylene and a comonomer, such as 1-butene, 1-hexene, or 1-octene. If the monomer and comonomer were ethylene and 1-hexene, respectively, the resulting polymer can be categorized as an ethylene/1-hexene copolymer.

In like manner, the scope of the term "polymerization" includes homopolymerization, copolymerization, terpolymerization, etc. Therefore, a copolymerization process can involve contacting one olefin monomer (e.g., ethylene) and one olefin comonomer (e.g., 1-hexene) to produce a copolymer.

The term "co-catalyst" is used generally herein to refer to compounds such as aluminosilane compounds, organoboron or organoborate compounds, ionizing ionic compounds, organoaluminum compounds, organozinc compounds, organomagnesium compounds, organolithium compounds, and the like, that can constitute one component of a catalyst composition, when used, for example, in addition to an activator-support. The term "co-catalyst" is used regardless of the actual function of the compound or any chemical mechanism by which the compound may operate.

The terms "chemically-treated solid oxide," "treated solid oxide compound," and the like, are used herein to indicate a solid, inorganic oxide of relatively high porosity, which can exhibit Lewis acidic or Brønsted acidic behavior, and which has been treated with an electron-withdrawing component, typically an anion, and which is calcined. The electron-withdrawing component is typically an electron-withdrawing anion source compound. Thus, the chemically-treated solid oxide can comprise a calcined contact product of at least one solid oxide with at least one electron-withdrawing anion source compound. Typically, the chemically-treated solid oxide comprises at least one acidic solid oxide compound. The "activator-support" of the present invention can be a chemically-treated solid oxide. The terms "support" and "activator-support" are not used to imply these components are inert, and such components should not be construed as an inert component of the catalyst composition. The term "activator," as used herein, refers generally to a substance that is capable of converting a metallocene component into a catalyst that can polymerize olefins, or converting a contact product of a metallocene component and a component that provides an activatable ligand (e.g., an alkyl, a hydride) to the metallocene, when the

metallocene compound does not already comprise such a ligand, into a catalyst that can polymerize olefins. This term is used regardless of the actual activating mechanism. Illustrative activators include activator-supports, aluminoxanes, organoboron or organoborate compounds, ionizing ionic compounds, and the like. Aluminoxanes, organoboron or organoborate compounds, and ionizing ionic compounds generally are referred to as activators if used in a catalyst composition in which an activator-support is not present. If the catalyst composition contains an activator-support, then the aluminoxane, organoboron or organoborate, and ionizing ionic materials are typically referred to as co-catalysts.

10 The term “metallocene” as used herein describes compounds comprising at least one η^3 to η^5 -cycloalkadienyl-type moiety, wherein η^3 to η^5 -cycloalkadienyl moieties include cyclopentadienyl ligands, indenyl ligands, fluorenyl ligands, and the like, including partially saturated or substituted derivatives or analogs of any of these. Possible substituents on these ligands may include H, therefore this invention
15 comprises ligands such as tetrahydroindenyl, tetrahydrofluorenyl, octahydrofluorenyl, partially saturated indenyl, partially saturated fluorenyl, substituted partially saturated indenyl, substituted partially saturated fluorenyl, and the like. In some contexts, the metallocene is referred to simply as the “catalyst,” in much the same way the term “co-catalyst” is used herein to refer to, for example, an organoaluminum compound.

20 The terms “catalyst composition,” “catalyst mixture,” “catalyst system,” and the like, do not depend upon the actual product or composition resulting from the contact or reaction of the initial components of the disclosed or claimed catalyst composition/mixture/system, the nature of the active catalytic site, or the fate of the co-catalyst, the metallocene compound(s), any olefin monomer used to prepare a
25 precontacted mixture, or the activator (e.g., activator-support), after combining these components. Therefore, the terms “catalyst composition,” “catalyst mixture,” “catalyst system,” and the like, encompass the initial starting components of the composition, as well as whatever product(s) may result from contacting these initial starting components, and this is inclusive of both heterogeneous and homogenous catalyst
30 systems or compositions. The terms “catalyst composition,” “catalyst mixture,” “catalyst system,” and the like, can be used interchangeably throughout this disclosure.

The term "contact product" is used herein to describe compositions wherein the components are contacted together in any order, in any manner, and for any length of time. For example, the components can be contacted by blending or mixing. Further, contacting of any component can occur in the presence or absence of any other component of the compositions described herein. Combining additional materials or components can be done by any suitable method. Further, the term "contact product" includes mixtures, blends, solutions, slurries, reaction products, and the like, or combinations thereof. Although "contact product" can include reaction products, it is not required for the respective components to react with one another. Similarly, the term "contacting" is used herein to refer to materials which can be blended, mixed, slurried, dissolved, reacted, treated, or otherwise contacted in some other manner.

The term "precontacted" mixture is used herein to describe a first mixture of catalyst components that are contacted for a first period of time prior to the first mixture being used to form a "postcontacted" or second mixture of catalyst components that are contacted for a second period of time. Typically, the precontacted mixture can describe a mixture of a metallocene compound (one or more than one), olefin monomer (or monomers), and organoaluminum compound (or compounds), before this mixture is contacted with an activator-support(s) and optional additional organoaluminum compound. Thus, precontacted describes components that are used to contact each other, but prior to contacting the components in the second, postcontacted mixture. Accordingly, this invention can occasionally distinguish between a component used to prepare the precontacted mixture and that component after the mixture has been prepared. For example, according to this description, it is possible for the precontacted organoaluminum compound, once it is contacted with the metallocene compound and the olefin monomer, to have reacted to form at least one chemical compound, formulation, or structure different from the distinct organoaluminum compound used to prepare the precontacted mixture. In this case, the precontacted organoaluminum compound or component is described as comprising an organoaluminum compound that was used to prepare the precontacted mixture.

Additionally, the precontacted mixture can describe a mixture of metallocene compound(s) and organoaluminum compound(s), prior to contacting this mixture with an activator-support(s). This precontacted mixture also can describe a mixture of

metallocene compound(s), olefin monomer(s), and activator-support(s), before this mixture is contacted with an organoaluminum co-catalyst compound or compounds.

Similarly, the term “postcontacted” mixture is used herein to describe a second mixture of catalyst components that are contacted for a second period of time, and one constituent of which is the “precontacted” or first mixture of catalyst components that were contacted for a first period of time. Typically, the term “postcontacted” mixture is used herein to describe the mixture of metallocene compound(s), olefin monomer(s), organoaluminum compound(s), and activator-support(s) formed from contacting the precontacted mixture of a portion of these components with any additional components added to make up the postcontacted mixture.

Although any methods, devices, and materials similar or equivalent to those described herein can be used in the practice or testing of the invention, the typical methods, devices and materials are herein described.

All publications and patents mentioned herein are incorporated herein by reference for the purpose of describing and disclosing, for example, the constructs and methodologies that are described in the publications, which might be used in connection with the presently described invention. The publications discussed throughout the text are provided solely for their disclosure prior to the filing date of the present application. Nothing herein is to be construed as an admission that the inventors are not entitled to antedate such disclosure by virtue of prior invention.

Applicants disclose several types of ranges in the present invention. When Applicants disclose or claim a range of any type, Applicants’ intent is to disclose or claim individually each possible number that such a range could reasonably encompass, including end points of the range as well as any sub-ranges and combinations of sub-ranges encompassed therein. For example, when the Applicants disclose or claim a chemical moiety having a certain number of carbon atoms, Applicants’ intent is to disclose or claim individually every possible number that such a range could encompass, consistent with the disclosure herein. For example, the disclosure that a moiety is a C₁ to C₁₈ hydrocarbyl group, or in alternative language, a hydrocarbyl group having from 1 to 18 carbon atoms, as used herein, refers to a moiety that can have 1, 2, 3, 4, 5, 6, 7, 8, 9, 10, 11, 12, 13, 14, 15, 16, 17, or 18 carbon atoms, as well as any range between these two numbers (for example, a C₁ to C₈ hydrocarbyl group), and also

including any combination of ranges between these two numbers (for example, a C₂ to C₄ and a C₁₂ to C₁₆ hydrocarbyl group).

Similarly, another representative example follows for the peak molecular weight (Mp) of an olefin polymer produced in an aspect of this invention. By a disclosure that
5 the Mp can be in a range from about 30,000 to about 130,000 g/mol, Applicants intend to recite that the Mp can be any molecular weight in the range and, for example, can be equal to about 30,000, about 40,000, about 50,000, about 60,000, about 70,000, about 80,000, about 90,000, about 100,000, about 110,000, about 120,000, or about 130,000 g/mol. Additionally, the Mp can be within any range from about 30,000 to about
10 130,000 (for example, from about 40,000 to about 80,000), and this also includes any combination of ranges between about 30,000 and about 130,000 (for example, the Mp can be in a range from about 30,000 to about 75,000, or from about 90,000 to about 125,000). Likewise, all other ranges disclosed herein should be interpreted in a manner similar to these two examples.

15 Applicants reserve the right to proviso out or exclude any individual members of any such group, including any sub-ranges or combinations of sub-ranges within the group, that can be claimed according to a range or in any similar manner, if for any reason Applicants choose to claim less than the full measure of the disclosure, for example, to account for a reference that Applicants may be unaware of at the time of
20 the filing of the application. Further, Applicants reserve the right to proviso out or exclude any individual substituents, analogs, compounds, ligands, structures, or groups thereof, or any members of a claimed group, if for any reason Applicants choose to claim less than the full measure of the disclosure, for example, to account for a reference that Applicants may be unaware of at the time of the filing of the application.

25 DETAILED DESCRIPTION OF THE INVENTION

The present invention is directed generally to new catalyst compositions, methods for preparing catalyst compositions, methods for using the catalyst compositions to polymerize olefins, the polymer resins produced using such catalyst compositions, and articles produced using these polymer resins. In particular, the
30 present invention relates to catalyst compositions containing two or more metallocene components, to polymerization processes utilizing such catalyst compositions, and to the resulting olefin polymers produced from the polymerization processes.

CATALYST COMPONENT I

Catalyst component I can comprise an unbridged zirconium or hafnium based metallocene compound and/or an unbridged zirconium and/or hafnium based dinuclear metallocene compound. In one aspect, for instance, catalyst component I can comprise
 5 an unbridged zirconium or hafnium based metallocene compound containing two cyclopentadienyl groups, two indenyl groups, or a cyclopentadienyl and an indenyl group. In another aspect, catalyst component I can comprise an unbridged zirconium or hafnium based metallocene compound containing two cyclopentadienyl groups. In yet another aspect, catalyst component I can comprise an unbridged zirconium or hafnium
 10 based metallocene compound containing two indenyl groups. In still another aspect, catalyst component I can comprise an unbridged zirconium or hafnium based metallocene compound containing a cyclopentadienyl and an indenyl group.

In some aspects, catalyst component I can comprise an unbridged zirconium based metallocene compound containing two cyclopentadienyl groups, two indenyl
 15 groups, or a cyclopentadienyl and an indenyl group, while in other aspects, catalyst component I can comprise a dinuclear unbridged metallocene compound with an alkenyl linking group.

Catalyst component I can comprise, in particular aspects of this invention, an unbridged metallocene compound having formula (I):



Within formula (I), M, Cp^A, Cp^B, and each X are independent elements of the unbridged metallocene compound. Accordingly, the unbridged metallocene compound having formula (I) can be described using any combination of M, Cp^A, Cp^B, and X disclosed herein.

25 Unless otherwise specified, formula (I) above, any other structural formulas disclosed herein, and any metallocene complex, compound, or species disclosed herein are not designed to show stereochemistry or isomeric positioning of the different moieties (e.g., these formulas are not intended to display cis or trans isomers, or R or S

diastereoisomers), although such compounds are contemplated and encompassed by these formulas and/or structures.

In accordance with aspects of this invention, the metal in formula (I), M, can be Ti, Zr, or Hf. In one aspect, for instance, M can be Zr or Hf, while in another aspect, M
5 can be Ti; alternatively, M can be Zr; or alternatively, M can be Hf.

Each X in formula (I) independently can be a monoanionic ligand. In some aspects, suitable monoanionic ligands can include, but are not limited to, H (hydride), BH₄, a halide, a C₁ to C₃₆ hydrocarbyl group, a C₁ to C₃₆ hydrocarboxy group, a C₁ to C₃₆ hydrocarbylaminy group, a C₁ to C₃₆ hydrocarbylsilyl group, a C₁ to C₃₆
10 hydrocarbylaminylsilyl group, —OBR¹₂, or —OSO₂R¹, wherein R¹ is a C₁ to C₃₆ hydrocarbyl group. It is contemplated that each X can be either the same or a different monoanionic ligand.

In one aspect, each X independently can be H, BH₄, a halide (e.g., F, Cl, Br, etc.), a C₁ to C₁₈ hydrocarbyl group, a C₁ to C₁₈ hydrocarboxy group, a C₁ to C₁₈
15 hydrocarbylaminy group, a C₁ to C₁₈ hydrocarbylsilyl group, or a C₁ to C₁₈ hydrocarbylaminylsilyl group. Alternatively, each X independently can be H, BH₄, a halide, OBR¹₂, or OSO₂R¹, wherein R¹ is a C₁ to C₁₈ hydrocarbyl group. In another aspect, each X independently can be H, BH₄, a halide, a C₁ to C₁₂ hydrocarbyl group, a C₁ to C₁₂ hydrocarboxy group, a C₁ to C₁₂ hydrocarbylaminy group, a C₁ to C₁₂
20 hydrocarbylsilyl group, a C₁ to C₁₂ hydrocarbylaminylsilyl group, OBR¹₂, or OSO₂R¹, wherein R¹ is a C₁ to C₁₂ hydrocarbyl group. In another aspect, each X independently can be H, BH₄, a halide, a C₁ to C₁₀ hydrocarbyl group, a C₁ to C₁₀ hydrocarboxy group, a C₁ to C₁₀ hydrocarbylaminy group, a C₁ to C₁₀ hydrocarbylsilyl group, a C₁ to C₁₀ hydrocarbylaminylsilyl group, OBR¹₂, or OSO₂R¹, wherein R¹ is a C₁ to C₁₀
25 hydrocarbyl group. In yet another aspect, each X independently can be H, BH₄, a halide, a C₁ to C₈ hydrocarbyl group, a C₁ to C₈ hydrocarboxy group, a C₁ to C₈ hydrocarbylaminy group, a C₁ to C₈ hydrocarbylsilyl group, a C₁ to C₈ hydrocarbylaminylsilyl group, OBR¹₂, or OSO₂R¹, wherein R¹ is a C₁ to C₈ hydrocarbyl group. In still another aspect, each X independently can be a halide or a C₁
30 to C₁₈ hydrocarbyl group. For example, each X can be Cl.

The hydrocarbyl group which can be an X in formula (I) can be a C₁ to C₃₆ hydrocarbyl group, including, but not limited to, a C₁ to C₃₆ alkyl group, a C₂ to C₃₆

alkenyl group, a C₄ to C₃₆ cycloalkyl group, a C₆ to C₃₆ aryl group, or a C₇ to C₃₆ aralkyl group. For instance, each X independently can be a C₁ to C₁₈ alkyl group, a C₂ to C₁₈ alkenyl group, a C₄ to C₁₈ cycloalkyl group, a C₆ to C₁₈ aryl group, or a C₇ to C₁₈ aralkyl group; alternatively, each X independently can be a C₁ to C₁₂ alkyl group, a C₂ to C₁₂ alkenyl group, a C₄ to C₁₂ cycloalkyl group, a C₆ to C₁₂ aryl group, or a C₇ to C₁₂ aralkyl group; alternatively, each X independently can be a C₁ to C₁₀ alkyl group, a C₂ to C₁₀ alkenyl group, a C₄ to C₁₀ cycloalkyl group, a C₆ to C₁₀ aryl group, or a C₇ to C₁₀ aralkyl group; or alternatively, each X independently can be a C₁ to C₅ alkyl group, a C₂ to C₅ alkenyl group, a C₅ to C₈ cycloalkyl group, a C₆ to C₈ aryl group, or a C₇ to C₈ aralkyl group.

Accordingly, in some aspects, the alkyl group which can be an X in formula (I) can be a methyl group, an ethyl group, a propyl group, a butyl group, a pentyl group, a hexyl group, a heptyl group, an octyl group, a nonyl group, a decyl group, a undecyl group, a dodecyl group, a tridecyl group, a tetradecyl group, a pentadecyl group, a hexadecyl group, a heptadecyl group, or an octadecyl group; or alternatively, a methyl group, an ethyl group, a propyl group, a butyl group, a pentyl group, a hexyl group, a heptyl group, an octyl group, a nonyl group, or a decyl group. In some aspects, the alkyl group which can be an X in formula (I) can be a methyl group, an ethyl group, a n-propyl group, an iso-propyl group, a n-butyl group, an iso-butyl group, a sec-butyl group, a tert-butyl group, a n-pentyl group, an iso-pentyl group, a sec-pentyl group, or a neopentyl group; alternatively, a methyl group, an ethyl group, an iso-propyl group, a tert-butyl group, or a neopentyl group; alternatively, a methyl group; alternatively, an ethyl group; alternatively, a n-propyl group; alternatively, an iso-propyl group; alternatively, a tert-butyl group; or alternatively, a neopentyl group.

Suitable alkenyl groups which can be an X in formula (I) can include, but are not limited to, an ethenyl group, a propenyl group, a butenyl group, a pentenyl group, a hexenyl group, a heptenyl group, an octenyl group, a nonenyl group, a decenyl group, a undecenyl group, a dodecenyl group, a tridecenyl group, a tetradecenyl group, a pentadecenyl group, a hexadecenyl group, a heptadecenyl group, or an octadecenyl group. Such alkenyl groups can be linear or branched, and the double bond can be located anywhere in the chain. In one aspect, each X in formula (I) independently can be an ethenyl group, a propenyl group, a butenyl group, a pentenyl group, a hexenyl

group, a heptenyl group, an octenyl group, a nonenyl group, or a decenyl group, while in another aspect, each X in formula (I) independently can be an ethenyl group, a propenyl group, a butenyl group, a pentenyl group, or a hexenyl group. For example, an X can be an ethenyl group; alternatively, a propenyl group; alternatively, a butenyl group; alternatively, a pentenyl group; or alternatively, a hexenyl group. In yet another aspect, an X can be a terminal alkenyl group, such as a C₃ to C₁₈ terminal alkenyl group, a C₃ to C₁₂ terminal alkenyl group, or a C₃ to C₈ terminal alkenyl group. Illustrative terminal alkenyl groups can include, but are not limited to, a prop-2-en-1-yl group, a but-3-en-1-yl group, a pent-4-en-1-yl group, a hex-5-en-1-yl group, a hept-6-en-1-yl group, an oct-7-en-1-yl group, a non-8-en-1-yl group, a dec-9-en-1-yl group, and so forth.

Each X in formula (I) can be a cycloalkyl group, including, but not limited to, a cyclobutyl group, a substituted cyclobutyl group, a cyclopentyl group, a substituted cyclopentyl group, a cyclohexyl group, a substituted cyclohexyl group, a cycloheptyl group, a substituted cycloheptyl group, a cyclooctyl group, or a substituted cyclooctyl group. For example, an X in formula (I) can be a cyclopentyl group, a substituted cyclopentyl group, a cyclohexyl group, or a substituted cyclohexyl group. Moreover, each X in formula (I) independently can be a cyclobutyl group or a substituted cyclobutyl group; alternatively, a cyclopentyl group or a substituted cyclopentyl group; alternatively, a cyclohexyl group or a substituted cyclohexyl group; alternatively, a cycloheptyl group or a substituted cycloheptyl group; alternatively, a cyclooctyl group or a substituted cyclooctyl group; alternatively, a cyclopentyl group; alternatively, a substituted cyclopentyl group; alternatively, a cyclohexyl group; or alternatively, a substituted cyclohexyl group. Substituents which can be utilized for the substituted cycloalkyl group are independently disclosed herein and can be utilized without limitation to further describe the substituted cycloalkyl group which can be an X in formula (I).

In some aspects, the aryl group which can be an X in formula (I) can be a phenyl group, a substituted phenyl group, a naphthyl group, or a substituted naphthyl group. In an aspect, the aryl group can be a phenyl group or a substituted phenyl group; alternatively, a naphthyl group or a substituted naphthyl group; alternatively, a phenyl group or a naphthyl group; alternatively, a substituted phenyl group or a

substituted naphthyl group; alternatively, a phenyl group; or alternatively, a naphthyl group. Substituents which can be utilized for the substituted phenyl groups or substituted naphthyl groups are independently disclosed herein and can be utilized without limitation to further describe the substituted phenyl groups or substituted naphthyl groups which can be an X in formula (I).

In an aspect, the substituted phenyl group which can be an X in formula (I) can be a 2-substituted phenyl group, a 3-substituted phenyl group, a 4-substituted phenyl group, a 2,4-disubstituted phenyl group, a 2,6-disubstituted phenyl group, a 3,5-disubstituted phenyl group, or a 2,4,6-trisubstituted phenyl group. In other aspects, the substituted phenyl group can be a 2-substituted phenyl group, a 4-substituted phenyl group, a 2,4-disubstituted phenyl group, or a 2,6-disubstituted phenyl group; alternatively, a 3-substituted phenyl group or a 3,5-disubstituted phenyl group; alternatively, a 2-substituted phenyl group or a 4-substituted phenyl group; alternatively, a 2,4-disubstituted phenyl group or a 2,6-disubstituted phenyl group; alternatively, a 2-substituted phenyl group; alternatively, a 3-substituted phenyl group; alternatively, a 4-substituted phenyl group; alternatively, a 2,4-disubstituted phenyl group; alternatively, a 2,6-disubstituted phenyl group; alternatively, a 3,5-disubstituted phenyl group; or alternatively, a 2,4,6-trisubstituted phenyl group. Substituents which can be utilized for these specific substituted phenyl groups are independently disclosed herein and can be utilized without limitation to further describe these substituted phenyl groups which can be an X group(s) in formula (I).

In some aspects, the aralkyl group which can be an X group in formula (I) can be a benzyl group or a substituted benzyl group. In an aspect, the aralkyl group can be a benzyl group or, alternatively, a substituted benzyl group. Substituents which can be utilized for the substituted aralkyl group are independently disclosed herein and can be utilized without limitation to further describe the substituted aralkyl group which can be an X group(s) in formula (I).

In an aspect, each non-hydrogen substituent(s) for the substituted cycloalkyl group, substituted aryl group, or substituted aralkyl group which can be an X in formula (I) independently can be a C₁ to C₁₈ hydrocarbyl group; alternatively, a C₁ to C₈ hydrocarbyl group; or alternatively, a C₁ to C₅ hydrocarbyl group. Specific hydrocarbyl groups are independently disclosed herein and can be utilized without

limitation to further describe the substituents of the substituted cycloalkyl groups, substituted aryl groups, or substituted aralkyl groups which can be an X in formula (I). For instance, the hydrocarbyl substituent can be an alkyl group, such as a methyl group, an ethyl group, a n-propyl group, an isopropyl group, a n-butyl group, a sec-butyl group, an isobutyl group, a tert-butyl group, a n-pentyl group, a 2-pentyl group, a 3-pentyl group, a 2-methyl-1-butyl group, a tert-pentyl group, a 3-methyl-1-butyl group, a 3-methyl-2-butyl group, or a neo-pentyl group, and the like. Furthermore, the hydrocarbyl substituent can be a benzyl group, a phenyl group, a tolyl group, or a xylyl group, and the like.

A hydrocarboxy group is used generically herein to include, for instance, alkoxy, aryloxy, aralkoxy, -(alkyl, aryl, or aralkyl)-O-(alkyl, aryl, or aralkyl) groups, and -O(CO)-(hydrogen or hydrocarbyl) groups, and these groups can comprise up to about 36 carbon atoms (e.g., C₁ to C₃₆, C₁ to C₁₈, C₁ to C₁₀, or C₁ to C₈ hydrocarboxy groups). Illustrative and non-limiting examples of hydrocarboxy groups which can be an X in formula (I) can include, but are not limited to, a methoxy group, an ethoxy group, an n-propoxy group, an isopropoxy group, an n-butoxy group, a sec-butoxy group, an isobutoxy group, a tert-butoxy group, an n-pentoxy group, a 2-pentoxy group, a 3-pentoxy group, a 2-methyl-1-butoxy group, a tert-pentoxy group, a 3-methyl-1-butoxy group, a 3-methyl-2-butoxy group, a neo-pentoxy group, a phenoxy group, a toloxy group, a xyloxy group, a 2,4,6-trimethylphenoxy group, a benzoxy group, an acetylacetonate group (acac), a formate group, an acetate group, a stearate group, an oleate group, a benzoate group, and the like. In an aspect, the hydrocarboxy group which can be an X in formula (I) can be a methoxy group; alternatively, an ethoxy group; alternatively, an n-propoxy group; alternatively, an isopropoxy group; alternatively, an n-butoxy group; alternatively, a sec-butoxy group; alternatively, an isobutoxy group; alternatively, a tert-butoxy group; alternatively, an n-pentoxy group; alternatively, a 2-pentoxy group; alternatively, a 3-pentoxy group; alternatively, a 2-methyl-1-butoxy group; alternatively, a tert-pentoxy group; alternatively, a 3-methyl-1-butoxy group; alternatively, a 3-methyl-2-butoxy group; alternatively, a neo-pentoxy group; alternatively, a phenoxy group; alternatively, a toloxy group; alternatively, a xyloxy group; alternatively, a 2,4,6-trimethylphenoxy group; alternatively, a benzoxy group; alternatively, an acetylacetonate group; alternatively, a formate group;

alternatively, an acetate group; alternatively, a stearate group; alternatively, an oleate group; or alternatively, a benzoate group.

The term hydrocarbylaminy group is used generically herein to refer collectively to, for instance, alkylaminy, arylaminy, aralkylaminy, dialkylaminy, diarylaminy, diaralkylaminy, and $-(\text{alkyl, aryl, or aralkyl})-\text{N}-(\text{alkyl, aryl, or aralkyl})$ groups, and unless otherwise specified, the hydrocarbylaminy groups which can be an X in formula (I) can comprise up to about 36 carbon atoms (e.g., C_1 to C_{36} , C_1 to C_{18} , C_1 to C_{10} , or C_1 to C_8 hydrocarbylaminy groups). Accordingly, hydrocarbylaminy is intended to cover both (mono)hydrocarbylaminy and dihydrocarbylaminy groups. In some aspects, the hydrocarbylaminy group which can be an X in formula (I) can be, for instance, a methylaminy group ($-\text{NHCH}_3$), an ethylaminy group ($-\text{NHCH}_2\text{CH}_3$), an n-propylaminy group ($-\text{NHCH}_2\text{CH}_2\text{CH}_3$), an iso-propylaminy group ($-\text{NHCH}(\text{CH}_3)_2$), an n-butylaminy group ($-\text{NHCH}_2\text{CH}_2\text{CH}_2\text{CH}_3$), a t-butylaminy group ($-\text{NHC}(\text{CH}_3)_3$), an n-pentylaminy group ($-\text{NHCH}_2\text{CH}_2\text{CH}_2\text{CH}_2\text{CH}_3$), a neo-pentylaminy group ($-\text{NHCH}_2\text{C}(\text{CH}_3)_3$), a phenylaminy group ($-\text{NHC}_6\text{H}_5$), a tolylaminy group ($-\text{NHC}_6\text{H}_4\text{CH}_3$), or a xylylaminy group ($-\text{NHC}_6\text{H}_3(\text{CH}_3)_2$); alternatively, a methylaminy group; alternatively, an ethylaminy group; alternatively, a propylaminy group; or alternatively, a phenylaminy group. In other aspects, the hydrocarbylaminy group which can be an X in formula (I) can be, for instance, a dimethylaminy group ($-\text{N}(\text{CH}_3)_2$), a diethylaminy group ($-\text{N}(\text{CH}_2\text{CH}_3)_2$), a di-n-propylaminy group ($-\text{N}(\text{CH}_2\text{CH}_2\text{CH}_3)_2$), a di-iso-propylaminy group ($-\text{N}(\text{CH}(\text{CH}_3)_2)_2$), a di-n-butylaminy group ($-\text{N}(\text{CH}_2\text{CH}_2\text{CH}_2\text{CH}_3)_2$), a di-t-butylaminy group ($-\text{N}(\text{C}(\text{CH}_3)_3)_2$), a di-n-pentylaminy group ($-\text{N}(\text{CH}_2\text{CH}_2\text{CH}_2\text{CH}_2\text{CH}_3)_2$), a di-neo-pentylaminy group ($-\text{N}(\text{CH}_2\text{C}(\text{CH}_3)_3)_2$), a di-phenylaminy group ($-\text{N}(\text{C}_6\text{H}_5)_2$), a di-tolylaminy group ($-\text{N}(\text{C}_6\text{H}_4\text{CH}_3)_2$), or a di-xylylaminy group ($-\text{N}(\text{C}_6\text{H}_3(\text{CH}_3)_2)_2$); alternatively, a dimethylaminy group; alternatively, a di-ethylaminy group; alternatively, a di-n-propylaminy group; or alternatively, a di-phenylaminy group.

In accordance with some aspects disclosed herein, each X independently can be a C_1 to C_{36} hydrocarbylsilyl group; alternatively, a C_1 to C_{24} hydrocarbylsilyl group; alternatively, a C_1 to C_{18} hydrocarbylsilyl group; or alternatively, a C_1 to C_8 hydrocarbylsilyl group. In an aspect, each hydrocarbyl (one or more) of the hydrocarbylsilyl group can be any hydrocarbyl group disclosed herein (e.g., a C_1 to C_5

alkyl group, a C₂ to C₅ alkenyl group, a C₅ to C₈ cycloalkyl group, a C₆ to C₈ aryl group, a C₇ to C₈ aralkyl group, etc.). As used herein, hydrocarbylsilyl is intended to cover (mono)hydrocarbylsilyl (–SiH₂R), dihydrocarbylsilyl (–SiHR₂), and trihydrocarbylsilyl (–SiR₃) groups, with R being a hydrocarbyl group. In one aspect, the hydrocarbylsilyl group can be a C₃ to C₃₆ or a C₃ to C₁₈ trihydrocarbylsilyl group, such as, for example, a trialkylsilyl group or a triphenylsilyl group. Illustrative and non-limiting examples of hydrocarbylsilyl groups which can be an X group(s) in formula (I) can include, but are not limited to, trimethylsilyl, triethylsilyl, tripropylsilyl (e.g., triisopropylsilyl), tributylsilyl, tripentylsilyl, triphenylsilyl, allyldimethylsilyl, and the like.

A hydrocarbylaminylsilyl group is used herein to refer to groups containing at least one hydrocarbon moiety, at least one N atom, and at least one Si atom. Illustrative and non-limiting examples of hydrocarbylaminylsilyl groups which can be an X can include, but are not limited to –N(SiMe₃)₂, –N(SiEt₃)₂, and the like. Unless otherwise specified, the hydrocarbylaminylsilyl groups which can be X can comprise up to about 36 carbon atoms (e.g., C₁ to C₃₆, C₁ to C₁₈, C₁ to C₁₂, or C₁ to C₈ hydrocarbylaminylsilyl groups). In an aspect, each hydrocarbyl (one or more) of the hydrocarbylaminylsilyl group can be any hydrocarbyl group disclosed herein (e.g., a C₁ to C₅ alkyl group, a C₂ to C₅ alkenyl group, a C₅ to C₈ cycloalkyl group, a C₆ to C₈ aryl group, a C₇ to C₈ aralkyl group, etc.). Moreover, hydrocarbylaminylsilyl is intended to cover –NH(SiH₂R), –NH(SiHR₂), –NH(SiR₃), –N(SiH₂R)₂, –N(SiHR₂)₂, and –N(SiR₃)₂ groups, among others, with R being a hydrocarbyl group.

In an aspect, each X independently can be –OBR¹₂ or –OSO₂R¹, wherein R¹ is a C₁ to C₃₆ hydrocarbyl group, or alternatively, a C₁ to C₁₈ hydrocarbyl group. The hydrocarbyl group in OBR¹₂ and/or OSO₂R¹ independently can be any hydrocarbyl group disclosed herein, such as, for instance, a C₁ to C₁₈ alkyl group, a C₂ to C₁₈ alkenyl group, a C₄ to C₁₈ cycloalkyl group, a C₆ to C₁₈ aryl group, or a C₇ to C₁₈ aralkyl group; alternatively, a C₁ to C₁₂ alkyl group, a C₂ to C₁₂ alkenyl group, a C₄ to C₁₂ cycloalkyl group, a C₆ to C₁₂ aryl group, or a C₇ to C₁₂ aralkyl group; or alternatively, a C₁ to C₈ alkyl group, a C₂ to C₈ alkenyl group, a C₅ to C₈ cycloalkyl group, a C₆ to C₈ aryl group, or a C₇ to C₈ aralkyl group.

In one aspect, each X independently can be H, BH₄, a halide, or a C₁ to C₃₆ hydrocarbyl group, hydrocarboxy group, hydrocarbylaminyll group, hydrocarbylsilyl group, or hydrocarbylaminylsilyl group, while in another aspect, each X independently can be H, BH₄, or a C₁ to C₁₈ hydrocarboxy group, hydrocarbylaminyll group, hydrocarbylsilyl group, or hydrocarbylaminylsilyl group. In yet another aspect, each X independently can be a halide; alternatively, a C₁ to C₁₈ hydrocarbyl group; alternatively, a C₁ to C₁₈ hydrocarboxy group; alternatively, a C₁ to C₁₈ hydrocarbylaminyll group; alternatively, a C₁ to C₁₈ hydrocarbylsilyl group; or alternatively, a C₁ to C₁₈ hydrocarbylaminylsilyl group. In still another aspect, each X can be H; alternatively, F; alternatively, Cl; alternatively, Br; alternatively, I; alternatively, BH₄; alternatively, a C₁ to C₁₈ hydrocarbyl group; alternatively, a C₁ to C₁₈ hydrocarboxy group; alternatively, a C₁ to C₁₈ hydrocarbylaminyll group; alternatively, a C₁ to C₁₈ hydrocarbylsilyl group; or alternatively, a C₁ to C₁₈ hydrocarbylaminylsilyl group.

Each X independently can be, in some aspects, H, a halide, methyl, phenyl, benzyl, an alkoxy, an aryloxy, acetylacetate, formate, acetate, stearate, oleate, benzoate, an alkylaminyll, a dialkylaminyll, a trihydrocarbylsilyl, or a hydrocarbylaminylsilyl; alternatively, H, a halide, methyl, phenyl, or benzyl; alternatively, an alkoxy, an aryloxy, or acetylacetate; alternatively, an alkylaminyll or a dialkylaminyll; alternatively, a trihydrocarbylsilyl or hydrocarbylaminylsilyl; alternatively, H or a halide; alternatively, methyl, phenyl, benzyl, an alkoxy, an aryloxy, acetylacetate, an alkylaminyll, or a dialkylaminyll; alternatively, H; alternatively, a halide; alternatively, methyl; alternatively, phenyl; alternatively, benzyl; alternatively, an alkoxy; alternatively, an aryloxy; alternatively, acetylacetate; alternatively, an alkylaminyll; alternatively, a dialkylaminyll; alternatively, a trihydrocarbylsilyl; or alternatively, a hydrocarbylaminylsilyl. In these and other aspects, the alkoxy, aryloxy, alkylaminyll, dialkylaminyll, trihydrocarbylsilyl, and hydrocarbylaminylsilyl can be a C₁ to C₃₆, a C₁ to C₁₈, a C₁ to C₁₂, or a C₁ to C₈ alkoxy, aryloxy, alkylaminyll, dialkylaminyll, trihydrocarbylsilyl, and hydrocarbylaminylsilyl.

Moreover, each X independently can be, in certain aspects, a halide or a C₁ to C₁₈ hydrocarbyl group; alternatively, a halide or a C₁ to C₈ hydrocarbyl group; alternatively, F, Cl, Br, I, methyl, benzyl, or phenyl; alternatively, Cl, methyl, benzyl,

or phenyl; alternatively, a C₁ to C₁₈ alkoxy, aryloxy, alkylaminyl, dialkylaminyl, trihydrocarbylsilyl, or hydrocarbylaminylsilyl group; alternatively, a C₁ to C₈ alkoxy, aryloxy, alkylaminyl, dialkylaminyl, trihydrocarbylsilyl, or hydrocarbylaminylsilyl group; or alternatively, methyl, ethyl, propyl, butyl, pentyl, hexyl, heptyl, octyl, nonyl, decyl, ethenyl, propenyl, butenyl, pentenyl, hexenyl, heptenyl, octenyl, nonenyl, decenyl, phenyl, tolyl, benzyl, naphthyl, trimethylsilyl, triisopropylsilyl, triphenylsilyl, or allyldimethylsilyl.

In formula (I), Cp^A and Cp^B independently can be a substituted or unsubstituted cyclopentadienyl or indenyl group. In one aspect, Cp^A and Cp^B independently can be an unsubstituted cyclopentadienyl or indenyl group. Alternatively, Cp^A and Cp^B independently can be a substituted indenyl or cyclopentadienyl group, for example, having up to 5 substituents.

If present, each substituent on Cp^A and Cp^B independently can be H, a halide, a C₁ to C₃₆ hydrocarbyl group, a C₁ to C₃₆ halogenated hydrocarbyl group, a C₁ to C₃₆ hydrocarboxy group, or a C₁ to C₃₆ hydrocarbylsilyl group. Importantly, each substituent on Cp^A and/or Cp^B can be either the same or a different substituent group. Moreover, each substituent can be at any position on the respective cyclopentadienyl or indenyl ring structure that conforms with the rules of chemical valence. In an aspect, the number of substituents on Cp^A and/or on Cp^B and/or the positions of each substituent on Cp^A and/or on Cp^B are independent of each other. For instance, two or more substituents on Cp^A can be different, or alternatively, each substituent on Cp^A can be the same. Additionally or alternatively, two or more substituents on Cp^B can be different, or alternatively, all substituents on Cp^B can be the same. In another aspect, one or more of the substituents on Cp^A can be different from the one or more of the substituents on Cp^B, or alternatively, all substituents on both Cp^A and/or on Cp^B can be the same. In these and other aspects, each substituent can be at any position on the respective cyclopentadienyl or indenyl ring structure. If substituted, Cp^A and/or Cp^B independently can have one substituent, two substituents, three substituents, four substituents, and so forth.

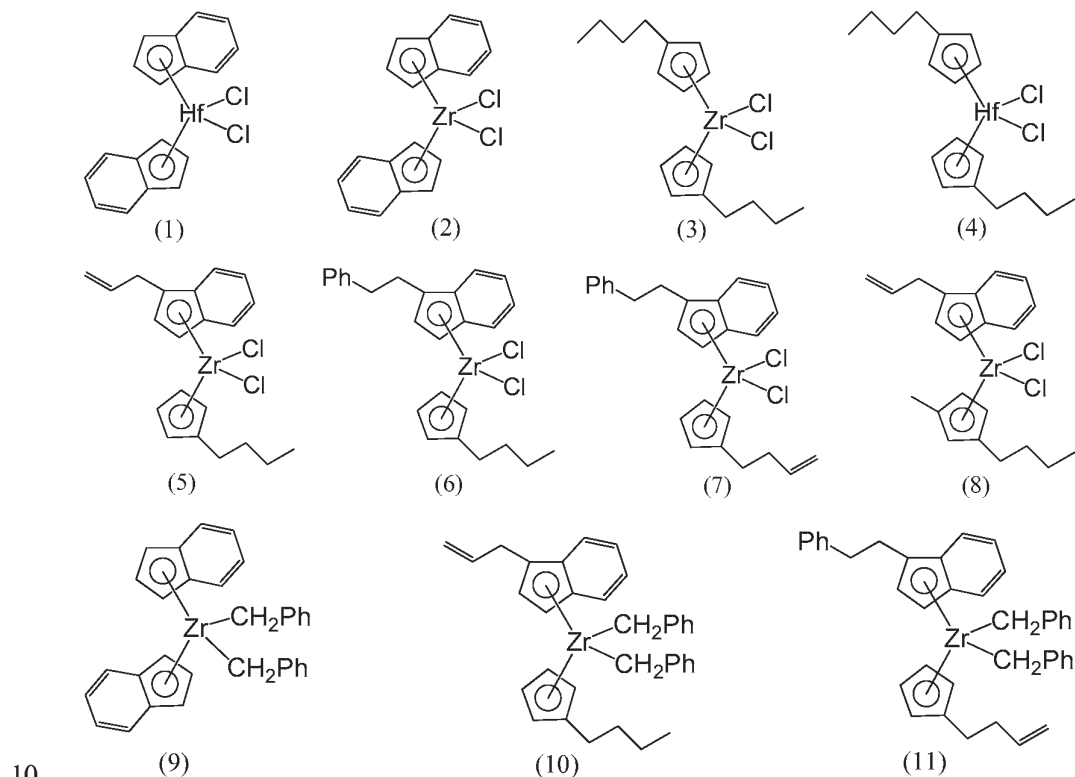
In formula (I), each substituent on Cp^A and/or on Cp^B independently can be H, a halide, a C₁ to C₃₆ hydrocarbyl group, a C₁ to C₃₆ halogenated hydrocarbyl group, a C₁ to C₃₆ hydrocarboxy group, or a C₁ to C₃₆ hydrocarbylsilyl group. In some aspects,

each substituent independently can be H; alternatively, a halide; alternatively, a C₁ to C₁₈ hydrocarbyl group; alternatively, a C₁ to C₁₈ halogenated hydrocarbyl group; alternatively, a C₁ to C₁₈ hydrocarboxy group; alternatively, a C₁ to C₁₈ hydrocarbysilyl group; alternatively, a C₁ to C₁₂ hydrocarbyl group or a C₁ to C₁₂ hydrocarbysilyl group; or alternatively, a C₁ to C₈ alkyl group or a C₃ to C₈ alkenyl group. The halide, C₁ to C₃₆ hydrocarbyl group, C₁ to C₃₆ hydrocarboxy group, and C₁ to C₃₆ hydrocarbysilyl group which can be a substituent on Cp^A and/or on Cp^B in formula (I) can be any halide, C₁ to C₃₆ hydrocarbyl group, C₁ to C₃₆ hydrocarboxy group, and C₁ to C₃₆ hydrocarbysilyl group described herein (e.g., as pertaining to X in formula (I)). A substituent on Cp^A and/or on Cp^B in formula (I) can be, in certain aspects, a C₁ to C₃₆ halogenated hydrocarbyl group, where the halogenated hydrocarbyl group indicates the presence of one or more halogen atoms replacing an equivalent number of hydrogen atoms in the hydrocarbyl group. The halogenated hydrocarbyl group often can be a halogenated alkyl group, a halogenated alkenyl group, a halogenated cycloalkyl group, a halogenated aryl group, or a halogenated aralkyl group. Representative and non-limiting halogenated hydrocarbyl groups include pentafluorophenyl, trifluoromethyl (CF₃), and the like.

As a non-limiting example, if present, each substituent on Cp^A and/or Cp^B independently can be H, Cl, CF₃, a methyl group, an ethyl group, a propyl group, a butyl group (e.g., t-Bu), a pentyl group, a hexyl group, a heptyl group, an octyl group, a nonyl group, a decyl group, an ethenyl group, a propenyl group, a butenyl group, a pentenyl group, a hexenyl group, a heptenyl group, an octenyl group, a nonenyl group, a decenyl group, a phenyl group, a tolyl group (or other substituted aryl group), a benzyl group, a naphthyl group, a trimethylsilyl group, a triisopropylsilyl group, a triphenylsilyl group, or an allyldimethylsilyl group; alternatively, H; alternatively, Cl; alternatively, CF₃; alternatively, a methyl group; alternatively, an ethyl group; alternatively, a propyl group; alternatively, a butyl group; alternatively, a pentyl group; alternatively, a hexyl group; alternatively, a heptyl group; alternatively, an octyl group, a nonyl group; alternatively, a decyl group; alternatively, an ethenyl group; alternatively, a propenyl group; alternatively, a butenyl group; alternatively, a pentenyl group; alternatively, a hexenyl group; alternatively, a heptenyl group; alternatively, an octenyl group; alternatively, a nonenyl group; alternatively, a decenyl group;

alternatively, a phenyl group; alternatively, a tolyl group; alternatively, a benzyl group; alternatively, a naphthyl group; alternatively, a trimethylsilyl group; alternatively, a triisopropylsilyl group; alternatively, a triphenylsilyl group; or alternatively, an allyldimethylsilyl group.

- 5 Illustrative and non-limiting examples of unbridged metallocene compounds having formula (I) and/or suitable for use as catalyst component I can include the following compounds (Ph = phenyl):

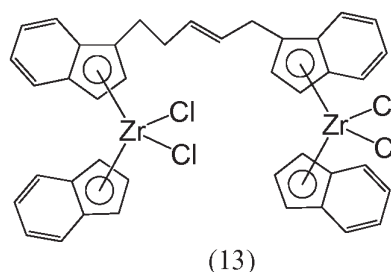
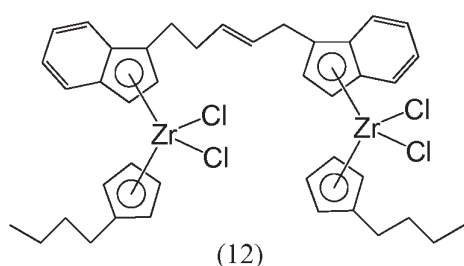


and the like, as well as combinations thereof.

- Catalyst component I is not limited solely to unbridged metallocene compounds such as described above, or to suitable unbridged metallocene compounds disclosed in U.S. Patent Nos. 7,199,073, 7,226,886, 7,312,283, and 7,619,047, which are incorporated herein by reference in their entirety. For example, catalyst component I can comprise an unbridged zirconium and/or hafnium based dinuclear metallocene compound. In one aspect, catalyst component I can comprise an unbridged zirconium based homodinuclear metallocene compound. In another aspect, catalyst component I can comprise an unbridged hafnium based homodinuclear metallocene compound. In
- 15

yet another aspect, catalyst component I can comprise an unbridged zirconium and/or hafnium based heterodinuclear metallocene compound (i.e., dinuclear compound with two hafniums, or two zirconiums, or one zirconium and one hafnium). Catalyst component I can comprise unbridged dinuclear metallocenes such as those described in

5 U.S. Patent Nos. 7,919,639 and 8,080,681, the disclosures of which are incorporated herein by reference in their entirety. Illustrative and non-limiting examples of dinuclear metallocene compounds suitable for use as catalyst component I can include the following compounds:



10 and the like, as well as combinations thereof.

CATALYST COMPONENT II

Catalyst component II can comprise a bridged metallocene compound. In one aspect, for instance, catalyst component II can comprise a bridged zirconium or hafnium based metallocene compound. In another aspect, catalyst component II can

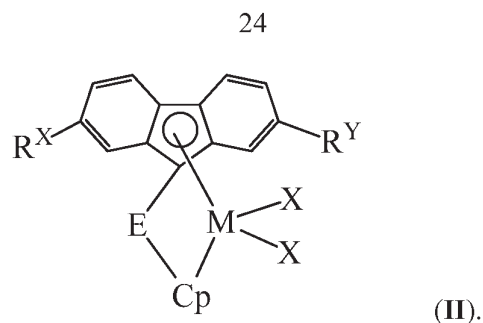
15 comprise a bridged zirconium or hafnium based metallocene compound with an alkenyl substituent. In yet another aspect, catalyst component II can comprise a bridged zirconium or hafnium based metallocene compound with an alkenyl substituent and a fluorenyl group. In still another aspect, catalyst component II can comprise a bridged zirconium or hafnium based metallocene compound with a cyclopentadienyl group and

20 a fluorenyl group, and with an alkenyl substituent on the bridging group and/or on the cyclopentadienyl group.

In some aspects, catalyst component II can comprise a bridged metallocene compound having an aryl group substituent on the bridging group, while in other aspects, catalyst component II can comprise a dinuclear bridged metallocene compound

25 with an alkenyl linking group.

Catalyst component II can comprise, in particular aspects of this invention, a bridged metallocene compound having formula (II):



Within formula (II), M, Cp, R^X, R^Y, E, and each X are independent elements of the bridged metallocene compound. Accordingly, the bridged metallocene compound having formula (II) can be described using any combination of M, Cp, R^X, R^Y, E, and X disclosed herein.

The selections for M and each X in formula (II) are the same as those described herein above for formula (I). In formula (II), Cp can be a substituted cyclopentadienyl, indenyl, or fluorenyl group. In one aspect, Cp can be a substituted cyclopentadienyl group, while in another aspect, Cp can be a substituted indenyl group.

In some aspects, Cp can contain no additional substituents, e.g., other than bridging group E, discussed further herein below. In other aspects, Cp can be further substituted with one substituent, two substituents, three substituents, four substituents, and so forth. If present, each substituent on Cp independently can be H, a halide, a C₁ to C₃₆ hydrocarbyl group, a C₁ to C₃₆ halogenated hydrocarbyl group, a C₁ to C₃₆ hydrocarboxy group, or a C₁ to C₃₆ hydrocarbylsilyl group. Importantly, each substituent on Cp can be either the same or a different substituent group. Moreover, each substituent can be at any position on the respective cyclopentadienyl, indenyl, or fluorenyl ring structure that conforms with the rules of chemical valence. In general, any substituent on Cp, independently, can be H or any halide, C₁ to C₃₆ hydrocarbyl group, C₁ to C₃₆ halogenated hydrocarbyl group, C₁ to C₃₆ hydrocarboxy group, or C₁ to C₃₆ hydrocarbylsilyl group described herein (e.g., as pertaining to substituents on Cp^A and Cp^B in formula (I)).

In one aspect, for example, each substituent on Cp independently can be a C₁ to C₁₂ hydrocarbyl group or a C₁ to C₁₂ hydrocarbylsilyl group. In another aspect, each substituent on Cp independently can be a C₁ to C₈ alkyl group or a C₃ to C₈ alkenyl group. In yet another aspect, each substituent on Cp^C independently can be H, Cl, CF₃, a methyl group, an ethyl group, a propyl group, a butyl group, a pentyl group, a hexyl

group, a heptyl group, an octyl group, a nonyl group, a decyl group, an ethenyl group, a propenyl group, a butenyl group, a pentenyl group, a hexenyl group, a heptenyl group, an octenyl group, a nonenyl group, a decenyl group, a phenyl group, a tolyl group, a benzyl group, a naphthyl group, a trimethylsilyl group, a triisopropylsilyl group, a triphenylsilyl group, or an allyldimethylsilyl group.

Similarly, R^X and R^Y in formula (II) independently can be H or any halide, C_1 to C_{36} hydrocarbyl group, C_1 to C_{36} halogenated hydrocarbyl group, C_1 to C_{36} hydrocarboxy group, or C_1 to C_{36} hydrocarbylsilyl group disclosed herein (e.g., as pertaining to substituents on Cp^A and Cp^B in formula (I)). In one aspect, for example, R^X and R^Y independently can be H or a C_1 to C_{12} hydrocarbyl group. In another aspect, R^X and R^Y independently can be a C_1 to C_{10} hydrocarbyl group. In yet another aspect, R^X and R^Y independently can be H, Cl, CF_3 , a methyl group, an ethyl group, a propyl group, a butyl group (e.g., t-Bu), a pentyl group, a hexyl group, a heptyl group, an octyl group, a nonyl group, a decyl group, an ethenyl group, a propenyl group, a butenyl group, a pentenyl group, a hexenyl group, a heptenyl group, an octenyl group, a nonenyl group, a decenyl group, a phenyl group, a tolyl group, a benzyl group, a naphthyl group, a trimethylsilyl group, a triisopropylsilyl group, a triphenylsilyl group, or an allyldimethylsilyl group, and the like. In still another aspect, R^X and R^Y independently can be a methyl group, an ethyl group, a propyl group, a butyl group, a pentyl group, a hexyl group, a heptyl group, an octyl group, a nonyl group, a decyl group, an ethenyl group, a propenyl group, a butenyl group, a pentenyl group, a hexenyl group, a heptenyl group, an octenyl group, a nonenyl group, a decenyl group, a phenyl group, a tolyl group, or a benzyl group.

Bridging group E in formula (II) can be (i) a bridging group having the formula $>E^A R^A R^B$, wherein E^A can be C, Si, or Ge, and R^A and R^B independently can be H or a C_1 to C_{18} hydrocarbyl group; (ii) a bridging group having the formula $—CR^C R^D—CR^E R^F—$, wherein R^C , R^D , R^E , and R^F independently can be H or a C_1 to C_{18} hydrocarbyl group; or (iii) a bridging group having the formula $—SiR^G R^H—E^5 R^I R^J—$, wherein E^5 can be C or Si, and R^G , R^H , R^I , and R^J independently can be H or a C_1 to C_{18} hydrocarbyl group.

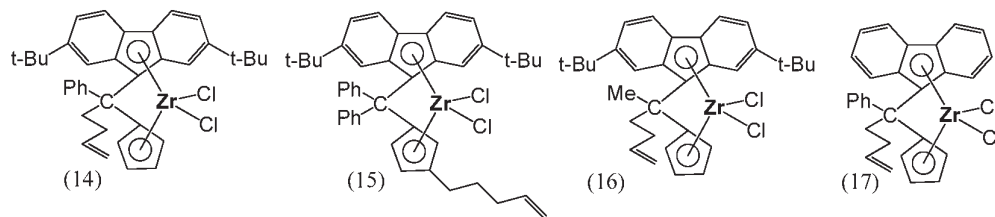
In the first option, the bridging group E can have the formula $>E^A R^A R^B$, wherein E^A can be C, Si, or Ge, and R^A and R^B independently can be H or any C_1 to C_{18}

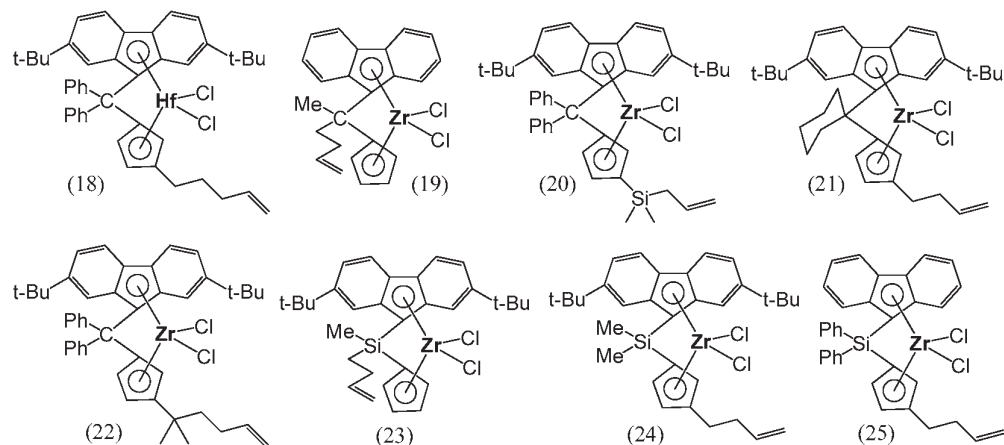
hydrocarbyl group disclosed herein. In some aspects of this invention, R^A and R^B independently can be a C_1 to C_{12} hydrocarbyl group; alternatively, R^A and R^B independently can be a C_1 to C_8 hydrocarbyl group; alternatively, R^A and R^B independently can be a phenyl group, a C_1 to C_8 alkyl group, or a C_3 to C_8 alkenyl group; alternatively, R^A and R^B independently can be a methyl group, an ethyl group, a propyl group, a butyl group, a pentyl group, a hexyl group, a heptyl group, an octyl group, a nonyl group, a decyl group, an ethenyl group, a propenyl group, a butenyl group, a pentenyl group, a hexenyl group, a heptenyl group, an octenyl group, a nonenyl group, a decenyl group, a phenyl group, a cyclohexylphenyl group, a naphthyl group, a tolyl group, or a benzyl group; or alternatively, R^A and R^B independently can be a methyl group, an ethyl group, a propyl group, a butyl group, a pentyl group, a hexyl group, a propenyl group, a butenyl group, a pentenyl group, a hexenyl group, a phenyl group, or a benzyl group. In these and other aspects, R^A and R^B can be either the same or different.

In the second option, the bridging group E can have the formula $—CR^C R^D—CR^E R^F—$, wherein R^C , R^D , R^E , and R^F independently can be H or any C_1 to C_{18} hydrocarbyl group disclosed herein. For instance, R^C , R^D , R^E , and R^F independently can be H or a methyl group.

In the third option, the bridging group E can have the formula $—SiR^G R^H—E^5 R^I R^J—$, wherein E^5 can be C or Si, and R^G , R^H , R^I , and R^J independently can be H or any C_1 to C_{18} hydrocarbyl group disclosed herein. For instance, E^5 can be Si, and R^G , R^H , R^I , and R^J independently can be H or a methyl group.

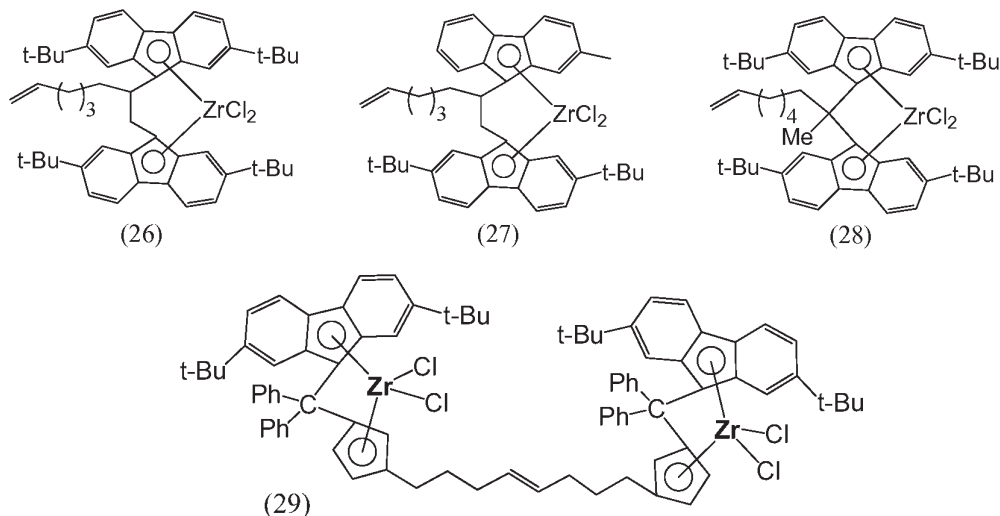
Illustrative and non-limiting examples of bridged metallocene compounds having formula (II) and/or suitable for use as catalyst component II can include the following compounds (Me = methyl, Ph = phenyl; t-Bu = tert-butyl):





and the like, as well as combinations thereof.

Further examples of bridged metallocene compounds having formula (II) and/or
 5 suitable for use as catalyst component II can include, but are not limited to, the following compounds:



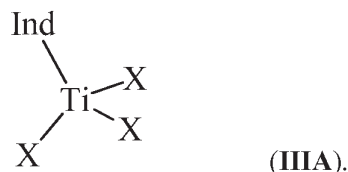
and the like, as well as combinations thereof.

10 Catalyst component II is not limited solely to the bridged metallocene compounds such as described above. Other suitable bridged metallocene compounds are disclosed in U.S. Patent Nos. 7,026,494, 7,041,617, 7,226,886, 7,312,283, 7,517,939, and 7,619,047, which are incorporated herein by reference in their entirety.

CATALYST COMPONENT III

15 In some aspects, the catalyst composition can contain catalyst component III, which can comprise a half-metallocene compound. Catalyst component III can

comprise, in particular aspects of this invention, a half-metallocene compound having formula (IIIA):



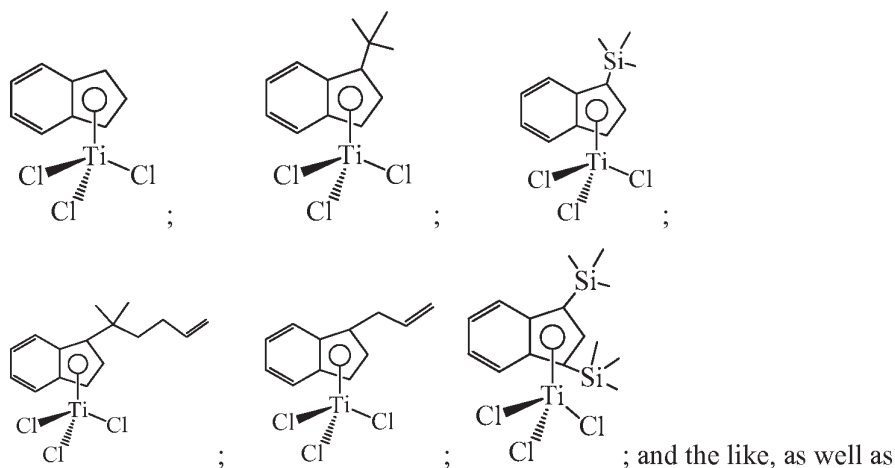
Within formula (IIIA), Ind and each X are independent elements of the half-metallocene compound. Accordingly, the half-metallocene compound having formula (IIIA) can be described using any combination of Ind and X disclosed herein. The selections for each X in formula (IIIA) are the same as those described hereinabove for formula (I), i.e., independently, any monoanionic ligand disclosed herein.

In formula (IIIA), Ind can be a substituted or unsubstituted indenyl group. In one aspect, Ind can be an unsubstituted indenyl group. Alternatively, Ind can be a substituted indenyl group, having one substituent, two substituents, three substituents, four substituents, five substituents, six substituents, or seven substituents. If present, each substituent on Ind independently can be H, a halide, a C₁ to C₃₆ hydrocarbyl group, a C₁ to C₃₆ halogenated hydrocarbyl group, a C₁ to C₃₆ hydrocarboxy group, or a C₁ to C₃₆ hydrocarbylsilyl group. Importantly, each substituent on Ind can be either the same or a different substituent group. Moreover, each substituent can be at any position on the indenyl ring structure that conforms with the rules of chemical valence. In general, any substituent on Ind, independently, can be H or any halide, C₁ to C₃₆ hydrocarbyl group, C₁ to C₃₆ halogenated hydrocarbyl group, C₁ to C₃₆ hydrocarboxy group, or C₁ to C₃₆ hydrocarbylsilyl group described herein (e.g., as pertaining to substituents on Cp^A and Cp^B in formula (I)).

In one aspect, for example, each substituent on Ind independently can be a C₁ to C₁₂ hydrocarbyl group or a C₁ to C₁₂ hydrocarbylsilyl group. In another aspect, each substituent on Ind independently can be H, Cl, CF₃, a methyl group, an ethyl group, a propyl group, a butyl group, a pentyl group, a hexyl group, a heptyl group, an octyl group, a nonyl group, a decyl group, an ethenyl group, a propenyl group, a butenyl group, a pentenyl group, a hexenyl group, a heptenyl group, an octenyl group, a nonenyl group, a decenyl group, a phenyl group, a tolyl group, a benzyl group, a

naphthyl group, a trimethylsilyl group, a triisopropylsilyl group, a triphenylsilyl group, or an allyldimethylsilyl group.

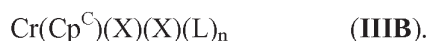
Illustrative and non-limiting examples of half-metallocene compounds having formula (IIIA) and/or suitable for use as catalyst component III can include, but are not limited to, the following compounds:



combinations thereof.

Half-metallocene compounds having formula (IIIA) can be synthesized using any suitable procedure, such as disclosed in Weiss et al., *Organometallics* **2005**, *24*, 2577-2581, which is incorporated herein by reference in its entirety.

Catalyst component III can comprise, in certain aspects of this invention, a half-metallocene compound having formula (IIIB):



Within formula (IIIB), Cp^{C} , n , each X and L are independent elements of the half-metallocene compound. Accordingly, the half-metallocene compound having formula (IIIB) can be described using any combination of Cp^{C} , n , X, and L disclosed herein. The selections for each X in formula (IIIB) are the same as those described hereinabove for formula (I), i.e., independently, any monoanionic ligand disclosed herein.

In formula (IIIB), Cp^{C} can be a substituted or unsubstituted cyclopentadienyl, indenyl, or fluorenyl group. In one aspect, Cp^{C} can be an unsubstituted cyclopentadienyl, indenyl, or fluorenyl group; alternatively, an unsubstituted cyclopentadienyl group; alternatively, an unsubstituted indenyl group; or alternatively,

an unsubstituted fluorenyl group. In another aspect, Cp^{C} can be a substituted cyclopentadienyl, indenyl, or fluorenyl group; alternatively, a substituted cyclopentadienyl group; alternatively, a substituted indenyl group; or alternatively, a substituted fluorenyl group. Cp^{C} can be a substituted cyclopentadienyl, indenyl, or
 5 fluorenyl group, having one substituent, two substituents, three substituents, four substituents, five substituents, and so forth; each substituent on Cp^{C} can be either the same or a different substituent group; and each substituent can be at any position on the ring structure that conforms with the rules of chemical valence.

When present, each substituent independently can be H, a halide, a C_1 to C_{36}
 10 hydrocarbyl group, a C_1 to C_{36} halogenated hydrocarbyl group, a C_1 to C_{36} hydrocarboxy group, or a C_1 to C_{36} hydrocarbysilyl group. In general, any substituent on Cp^{C} , independently, can be H or any halide, C_1 to C_{36} hydrocarbyl group, C_1 to C_{36} halogenated hydrocarbyl group, C_1 to C_{36} hydrocarboxy group, or C_1 to C_{36} hydrocarbysilyl group described herein (e.g., as pertaining to substituents on Cp^{A} and
 15 Cp^{B} in formula (I)).

Each L in formula (IIIB) independently can be a neutral ligand, and the integer n in formula (IIIB) can be 0, 1 or 2 (e.g., n can be 0 or 1). Suitable neutral ligands are described in U.S. Patent No. 8,501,882, the disclosure of which is incorporated herein by reference in its entirety. Typically, each neutral ligand, L, independently can be an
 20 ether, a thioether, an amine, a nitrile, or a phosphine. For example, each neutral ligand independently can be azetidine, oxetane, thietane, dioxetane, dithietane, tetrahydropyrrole, dihydropyrrole, pyrrole, indole, isoindole, tetrahydrofuran, 2-methyltetrahydrofuran, 2,5-dimethyltetrahydrofuran, dihydrofuran, furan, benzofuran, isobenzofuran, tetrahydrothiophene, dihydrothiophene, thiophene, benzothiophene, isobenzothiophene, imidazolidine, pyrazole, imidazole, oxazolidine, oxazole, isoxazole,
 25 thiazolidine, thiazole, isothiazole, benzothiazole, dioxolane, dithiolane, triazole, dithiazole, piperidine, pyridine, dimethyl amine, diethyl amine, tetrahydropyran, dihydropyran, pyran, thiane, piperazine, diazine, oxazine, thiazine, dithiane, dioxane, dioxin, triazine, triazinane, trioxane, oxepin, azepine, thiepin, diazepine, morpholine,
 30 quinoline, tetrahydroquinone, bicyclo[3.3.1]tetrasiloxane, or acetonitrile; alternatively, azetidine, oxetane, thietane, dioxetane, dithietane, tetrahydropyrrole, tetrahydrofuran, 2-methyltetrahydrofuran, 2,5-dimethyltetrahydrofuran, tetrahydrothiophene,

imidazolidine, oxazolidine, oxazole, thiazolidine, thiazole, dioxolane, dithiolane, piperidine, tetrahydropyran, pyran, thiane, piperazine, oxazine, thiazine, dithiane, dioxane, dioxin, triazinane, trioxane, azepine, thiepin, diazepine, morpholine, 1,2-thiazole, or bicyclo[3.3.1]tetrasiloxane; alternatively, tetrahydropyrrole, 5 tetrahydrofuran, 2-methyltetrahydrofuran, 2,5-dimethyltetrahydrofuran, tetrahydrothiophene, oxazolidine, thiazolidine, dioxolane, dithiolane, dithiazole, piperidine, tetrahydropyran, pyran, thiane, piperazine, dithiane, dioxane, dioxin, trioxane, or morpholine, and the like.

ACTIVATOR-SUPPORTS

10 The present invention encompasses various catalyst compositions containing an activator, such as activator-support. In one aspect, the activator-support can comprise a chemically-treated solid oxide, e.g., a solid oxide treated with an electron-withdrawing anion. Alternatively, in another aspect, the activator-support can comprise a clay mineral, a pillared clay, an exfoliated clay, an exfoliated clay gelled into another oxide 15 matrix, a layered silicate mineral, a non-layered silicate mineral, a layered aluminosilicate mineral, a non-layered aluminosilicate mineral, or combinations thereof.

Generally, chemically-treated solid oxides exhibit enhanced acidity as compared to the corresponding untreated solid oxide. The chemically-treated solid 20 oxide also can function as a catalyst activator as compared to the corresponding untreated solid oxide. While the chemically-treated solid oxide can activate a metallocene complex in the absence of co-catalysts, it is not necessary to eliminate co-catalysts from the catalyst composition. The activation function of the activator-support can enhance the activity of catalyst composition as a whole, as compared to a 25 catalyst composition containing the corresponding untreated solid oxide. However, it is believed that the chemically-treated solid oxide can function as an activator, even in the absence of organoaluminum compounds, aluminoxanes, organoboron or organoborate compounds, ionizing ionic compounds, and the like.

The chemically-treated solid oxide can comprise a solid oxide treated with an 30 electron-withdrawing anion. While not intending to be bound by the following statement, it is believed that treatment of the solid oxide with an electron-withdrawing component augments or enhances the acidity of the oxide. Thus, either the activator-

support exhibits Lewis or Brønsted acidity that is typically greater than the Lewis or Brønsted acid strength of the untreated solid oxide, or the activator-support has a greater number of acid sites than the untreated solid oxide, or both. One method to quantify the acidity of the chemically-treated and untreated solid oxide materials can be by comparing the polymerization activities of the treated and untreated oxides under acid catalyzed reactions.

Chemically-treated solid oxides of this invention generally can be formed from an inorganic solid oxide that exhibits Lewis acidic or Brønsted acidic behavior and has a relatively high porosity. The solid oxide can be chemically-treated with an electron-withdrawing component, typically an electron-withdrawing anion, to form an activator-support.

According to one aspect of the present invention, the solid oxide used to prepare the chemically-treated solid oxide can have a pore volume greater than about 0.1 cc/g. According to another aspect of the present invention, the solid oxide can have a pore volume greater than about 0.5 cc/g. According to yet another aspect of the present invention, the solid oxide can have a pore volume greater than about 1.0 cc/g.

In another aspect, the solid oxide can have a surface area of from about 100 to about 1000 m²/g. In yet another aspect, the solid oxide can have a surface area of from about 200 to about 800 m²/g. In still another aspect of the present invention, the solid oxide can have a surface area of from about 250 to about 600 m²/g.

The chemically-treated solid oxide can comprise a solid inorganic oxide comprising oxygen and one or more elements selected from Group 2, 3, 4, 5, 6, 7, 8, 9, 10, 11, 12, 13, 14, or 15 of the periodic table, or comprising oxygen and one or more elements selected from the lanthanide or actinide elements (See: Hawley's Condensed Chemical Dictionary, 11th Ed., John Wiley & Sons, 1995; Cotton, F.A., Wilkinson, G., Murillo, C. A., and Bochmann, M., Advanced Inorganic Chemistry, 6th Ed., Wiley-Interscience, 1999). For example, the inorganic oxide can comprise oxygen and an element, or elements, selected from Al, B, Be, Bi, Cd, Co, Cr, Cu, Fe, Ga, La, Mn, Mo, Ni, Sb, Si, Sn, Sr, Th, Ti, V, W, P, Y, Zn, and Zr.

Suitable examples of solid oxide materials or compounds that can be used to form the chemically-treated solid oxide can include, but are not limited to, Al₂O₃, B₂O₃, BeO, Bi₂O₃, CdO, Co₃O₄, Cr₂O₃, CuO, Fe₂O₃, Ga₂O₃, La₂O₃, Mn₂O₃, MoO₃, NiO,

P₂O₅, Sb₂O₅, SiO₂, SnO₂, SrO, ThO₂, TiO₂, V₂O₅, WO₃, Y₂O₃, ZnO, ZrO₂, and the like, including mixed oxides thereof, and combinations thereof. For example, the solid oxide can comprise silica, alumina, silica-alumina, silica-coated alumina, aluminum phosphate, aluminophosphate, heteropolytungstate, titania, zirconia, magnesia, boria, zinc oxide, mixed oxides thereof, or any combination thereof.

The solid oxide of this invention encompasses oxide materials such as alumina, "mixed oxides" thereof such as silica-alumina, materials where one oxide is coated with another, as well as any combinations and mixtures thereof. The mixed oxide compounds such as silica-alumina can be single or multiple chemical phases with more than one metal combined with oxygen to form a solid oxide compound. Examples of mixed oxides that can be used in the activator-support of the present invention, either singly or in combination, can include, but are not limited to, silica-alumina, silica-titania, silica-zirconia, zeolites, various clay minerals, alumina-titania, alumina-zirconia, zinc-aluminate, alumina-boria, silica-boria, aluminophosphate-silica, titania-zirconia, and the like. The solid oxide of this invention also encompasses oxide materials such as silica-coated alumina, as described in U.S. Patent No. 7,884,163, the disclosure of which is incorporated herein by reference in its entirety.

The electron-withdrawing component used to treat the solid oxide can be any component that increases the Lewis or Brønsted acidity of the solid oxide upon treatment (as compared to the solid oxide that is not treated with at least one electron-withdrawing anion). According to one aspect of the present invention, the electron-withdrawing component can be an electron-withdrawing anion derived from a salt, an acid, or other compound, such as a volatile organic compound, that serves as a source or precursor for that anion. Examples of electron-withdrawing anions can include, but are not limited to, sulfate, bisulfate, fluoride, chloride, bromide, iodide, fluorosulfate, fluoroborate, phosphate, fluorophosphate, trifluoroacetate, triflate, fluorozirconate, fluorotitanate, phospho-tungstate, and the like, including mixtures and combinations thereof. In addition, other ionic or non-ionic compounds that serve as sources for these electron-withdrawing anions also can be employed in the present invention. It is contemplated that the electron-withdrawing anion can be, or can comprise, fluoride, chloride, bromide, phosphate, triflate, bisulfate, or sulfate, and the like, or any combination thereof, in some aspects of this invention. In other aspects, the electron-

withdrawing anion can comprise sulfate, bisulfate, fluoride, chloride, bromide, iodide, fluorosulfate, fluoroborate, phosphate, fluorophosphate, trifluoroacetate, triflate, fluoro-zirconate, fluorotitanate, and the like, or combinations thereof.

Thus, for example, the activator-support (e.g., chemically-treated solid oxide) used in the catalyst compositions of the present invention can be, or can comprise, fluorided alumina, chlorided alumina, bromided alumina, sulfated alumina, fluorided silica-alumina, chlorided silica-alumina, bromided silica-alumina, sulfated silica-alumina, fluorided silica-zirconia, chlorided silica-zirconia, bromided silica-zirconia, sulfated silica-zirconia, fluorided silica-titania, fluorided silica-coated alumina, sulfated silica-coated alumina, phosphated silica-coated alumina, and the like, or combinations thereof. In one aspect, the activator-support can be, or can comprise, fluorided alumina, sulfated alumina, fluorided silica-alumina, sulfated silica-alumina, fluorided silica-coated alumina, sulfated silica-coated alumina, phosphated silica-coated alumina, and the like, or any combination thereof. In another aspect, the activator-support can comprise fluorided alumina; alternatively, chlorided alumina; alternatively, sulfated alumina; alternatively, fluorided silica-alumina; alternatively, sulfated silica-alumina; alternatively, fluorided silica-zirconia; alternatively, chlorided silica-zirconia; or alternatively, fluorided silica-coated alumina. In yet another aspect, the activator-support can comprise a fluorided solid oxide and/or a sulfated solid oxide.

When the electron-withdrawing component comprises a salt of an electron-withdrawing anion, the counterion or cation of that salt can be selected from any cation that allows the salt to revert or decompose back to the acid before and/or during calcining. Factors that dictate the suitability of the particular salt to serve as a source for the electron-withdrawing anion can include, but are not limited to, the solubility of the salt in the desired solvent, the lack of adverse reactivity of the cation, ion-pairing effects between the cation and anion, hygroscopic properties imparted to the salt by the cation, and the like, and thermal stability of the anion. Examples of suitable cations in the salt of the electron-withdrawing anion can include, but are not limited to, ammonium, trialkyl ammonium, tetraalkyl ammonium, tetraalkyl phosphonium, H^+ , $[H(OEt_2)_2]^+$, and the like.

Further, combinations of two or more different electron-withdrawing anions, in varying proportions, can be used to tailor the specific acidity of the activator-support to

the desired level. Combinations of electron-withdrawing components can be contacted with the oxide material simultaneously or individually, and in any order that affords the desired chemically-treated solid oxide acidity. For example, one aspect of this invention can employ two or more electron-withdrawing anion source compounds in
5 two or more separate contacting steps.

Thus, a process by which a chemically-treated solid oxide can be prepared is as follows: a selected solid oxide, or combination of solid oxides, can be contacted with a first electron-withdrawing anion source compound to form a first mixture; this first mixture can be calcined and then contacted with a second electron-withdrawing anion
10 source compound to form a second mixture; the second mixture then can be calcined to form a treated solid oxide. In such a process, the first and second electron-withdrawing anion source compounds can be either the same or different compounds.

According to another aspect of the present invention, the chemically-treated solid oxide can comprise a solid inorganic oxide material, a mixed oxide material, or a
15 combination of inorganic oxide materials, that is chemically-treated with an electron-withdrawing component, and optionally treated with a metal source, including metal salts, metal ions, or other metal-containing compounds. Non-limiting examples of the metal or metal ion can include zinc, nickel, vanadium, titanium, silver, copper, gallium, tin, tungsten, molybdenum, zirconium, and the like, or combinations thereof.
20 Examples of chemically-treated solid oxides that contain a metal or metal ion can include, but are not limited to, chlorided zinc-impregnated alumina, fluorided titanium-impregnated alumina, fluorided zinc-impregnated alumina, chlorided zinc-impregnated silica-alumina, fluorided zinc-impregnated silica-alumina, sulfated zinc-impregnated alumina, chlorided zinc aluminate, fluorided zinc aluminate, sulfated zinc aluminate,
25 silica-coated alumina treated with hexafluorotitanic acid, silica-coated alumina treated with zinc and then fluorided, and the like, or any combination thereof.

Any method of impregnating the solid oxide material with a metal can be used. The method by which the oxide is contacted with a metal source, typically a salt or metal-containing compound, can include, but is not limited to, gelling, co-gelling,
30 impregnation of one compound onto another, and the like. If desired, the metal-containing compound can be added to or impregnated into the solid oxide in solution form, and subsequently converted into the supported metal upon calcining.

Accordingly, the solid inorganic oxide can further comprise a metal selected from zinc, titanium, nickel, vanadium, silver, copper, gallium, tin, tungsten, molybdenum, and the like, or combinations of these metals. For example, zinc often can be used to impregnate the solid oxide because it can provide improved catalyst activity at a low cost.

The solid oxide can be treated with metal salts or metal-containing compounds before, after, or at the same time that the solid oxide is treated with the electron-withdrawing anion. Following any contacting method, the contacted mixture of solid compound, electron-withdrawing anion, and the metal ion can be calcined. Alternatively, a solid oxide material, an electron-withdrawing anion source, and the metal salt or metal-containing compound can be contacted and calcined simultaneously.

Various processes can be used to form the chemically-treated solid oxide useful in the present invention. The chemically-treated solid oxide can comprise the contact product of one or more solid oxides with one or more electron-withdrawing anion sources. It is not required that the solid oxide be calcined prior to contacting the electron-withdrawing anion source. Typically, the contact product can be calcined either during or after the solid oxide is contacted with the electron-withdrawing anion source. The solid oxide can be calcined or uncalcined. Various processes to prepare solid oxide activator-supports that can be employed in this invention have been reported. For example, such methods are described in U.S. Patent Nos. 6,107,230, 6,165,929, 6,294,494, 6,300,271, 6,316,553, 6,355,594, 6,376,415, 6,388,017, 6,391,816, 6,395,666, 6,524,987, 6,548,441, 6,548,442, 6,576,583, 6,613,712, 6,632,894, 6,667,274, and 6,750,302, the disclosures of which are incorporated herein by reference in their entirety.

According to one aspect of the present invention, the solid oxide material can be chemically-treated by contacting it with an electron-withdrawing component, typically an electron-withdrawing anion source. Further, the solid oxide material optionally can be treated with a metal ion, and then calcined to form a metal-containing or metal-impregnated chemically-treated solid oxide. According to another aspect of the present invention, the solid oxide material and electron-withdrawing anion source can be contacted and calcined simultaneously.

The method by which the oxide is contacted with the electron-withdrawing component, typically a salt or an acid of an electron-withdrawing anion, can include, but is not limited to, gelling, co-gelling, impregnation of one compound onto another, and the like. Thus, following any contacting method, the contacted mixture of the solid
5 oxide, electron-withdrawing anion, and optional metal ion, can be calcined.

The solid oxide activator-support (i.e., chemically-treated solid oxide) thus can be produced by a process comprising:

- 1) contacting a solid oxide (or solid oxides) with an electron-withdrawing anion source compound (or compounds) to form a first mixture; and
10 2) calcining the first mixture to form the solid oxide activator-support.

According to another aspect of the present invention, the solid oxide activator-support (chemically-treated solid oxide) can be produced by a process comprising:

- 1) contacting a solid oxide (or solid oxides) with a first electron-withdrawing anion source compound to form a first mixture;
15 2) calcining the first mixture to produce a calcined first mixture;
- 3) contacting the calcined first mixture with a second electron-withdrawing anion source compound to form a second mixture; and
- 4) calcining the second mixture to form the solid oxide activator-support.

According to yet another aspect of the present invention, the chemically-treated
20 solid oxide can be produced or formed by contacting the solid oxide with the electron-withdrawing anion source compound, where the solid oxide compound is calcined before, during, or after contacting the electron-withdrawing anion source, and where there is a substantial absence of aluminoxanes, organoboron or organoborate compounds, and ionizing ionic compounds.

25 Calcining of the treated solid oxide generally can be conducted in an ambient atmosphere, typically in a dry ambient atmosphere, at a temperature from about 200 °C to about 900 °C, and for a time of about 1 minute to about 100 hours. Calcining can be conducted at a temperature of from about 300 °C to about 800 °C, or alternatively, at a temperature of from about 400 °C to about 700 °C. Calcining can be conducted for
30 about 30 minutes to about 50 hours, or for about 1 hour to about 15 hours. Thus, for example, calcining can be carried out for about 1 to about 10 hours at a temperature of from about 350 °C to about 550 °C. Any suitable ambient atmosphere can be employed

during calcining. Generally, calcining can be conducted in an oxidizing atmosphere, such as air. Alternatively, an inert atmosphere, such as nitrogen or argon, or a reducing atmosphere, such as hydrogen or carbon monoxide, can be used.

According to one aspect of the present invention, the solid oxide material can be
5 treated with a source of halide ion, sulfate ion, or a combination of anions, optionally treated with a metal ion, and then calcined to provide the chemically-treated solid oxide in the form of a particulate solid. For example, the solid oxide material can be treated with a source of sulfate (termed a "sulfating agent"), a source of bromide ion (termed a "bromiding agent"), a source of chloride ion (termed a "chloriding agent"), a source of
10 fluoride ion (termed a "fluoriding agent"), or a combination thereof, and calcined to provide the solid oxide activator. Useful acidic activator-supports can include, but are not limited to, bromided alumina, chlorided alumina, fluorided alumina, sulfated alumina, bromided silica-alumina, chlorided silica-alumina, fluorided silica-alumina, sulfated silica-alumina, bromided silica-zirconia, chlorided silica-zirconia, fluorided
15 silica-zirconia, sulfated silica-zirconia, fluorided silica-titania, alumina treated with hexafluorotitanic acid, silica-coated alumina treated with hexafluorotitanic acid, silica-alumina treated with hexafluorozirconic acid, silica-alumina treated with trifluoroacetic acid, fluorided boria-alumina, silica treated with tetrafluoroboric acid, alumina treated with tetrafluoroboric acid, alumina treated with hexafluorophosphoric acid, a pillared
20 clay, such as a pillared montmorillonite, optionally treated with fluoride, chloride, or sulfate; phosphated alumina or other aluminophosphates optionally treated with sulfate, fluoride, or chloride; or any combination of the above. Further, any of these activator-supports optionally can be treated or impregnated with a metal ion.

In an aspect, the chemically-treated solid oxide can comprise a fluorided solid
25 oxide in the form of a particulate solid. The fluorided solid oxide can be formed by contacting a solid oxide with a fluoriding agent. The fluoride ion can be added to the oxide by forming a slurry of the oxide in a suitable solvent such as alcohol or water including, but not limited to, the one to three carbon alcohols because of their volatility and low surface tension. Examples of suitable fluoriding agents can include, but are
30 not limited to, hydrofluoric acid (HF), ammonium fluoride (NH_4F), ammonium bifluoride (NH_4HF_2), ammonium tetrafluoroborate (NH_4BF_4), ammonium silicofluoride (hexafluorosilicate) ($(\text{NH}_4)_2\text{SiF}_6$), ammonium hexafluorophosphate (NH_4PF_6),

hexafluorotitanic acid (H_2TiF_6), ammonium hexafluorotitanic acid ($(\text{NH}_4)_2\text{TiF}_6$), hexafluorozirconic acid (H_2ZrF_6), AlF_3 , NH_4AlF_4 , analogs thereof, and combinations thereof. Triflic acid and ammonium triflate also can be employed. For example, ammonium bifluoride (NH_4HF_2) can be used as the fluoriding agent, due to its ease of use and availability.

If desired, the solid oxide can be treated with a fluoriding agent during the calcining step. Any fluoriding agent capable of thoroughly contacting the solid oxide during the calcining step can be used. For example, in addition to those fluoriding agents described previously, volatile organic fluoriding agents can be used. Examples of volatile organic fluoriding agents useful in this aspect of the invention can include, but are not limited to, freons, perfluorohexane, perfluorobenzene, fluoromethane, trifluoroethanol, and the like, and combinations thereof. Calcining temperatures generally must be high enough to decompose the compound and release fluoride. Gaseous hydrogen fluoride (HF) or fluorine (F_2) itself also can be used with the solid oxide if fluorided while calcining. Silicon tetrafluoride (SiF_4) and compounds containing tetrafluoroborate (BF_4^-) also can be employed. One convenient method of contacting the solid oxide with the fluoriding agent can be to vaporize a fluoriding agent into a gas stream used to fluidize the solid oxide during calcination. Other suitable fluoriding agents and procedures for preparing fluorided solid oxides are well known to those of skill in the art.

Similarly, in another aspect of this invention, the chemically-treated solid oxide can comprise a chlorided solid oxide in the form of a particulate solid. The chlorided solid oxide can be formed by contacting a solid oxide with a chloriding agent. The chloride ion can be added to the oxide by forming a slurry of the oxide in a suitable solvent. The solid oxide can be treated with a chloriding agent during the calcining step. Any chloriding agent capable of serving as a source of chloride and thoroughly contacting the oxide during the calcining step can be used, such as SiCl_4 , SiMe_2Cl_2 , TiCl_4 , BCl_3 , and the like, including mixtures thereof. Volatile organic chloriding agents can be used. Examples of suitable volatile organic chloriding agents can include, but are not limited to, certain freons, perchlorobenzene, chloromethane, dichloromethane, chloroform, carbon tetrachloride, trichloroethanol, and the like, or any combination thereof. Gaseous hydrogen chloride or chlorine itself also can be used

with the solid oxide during calcining. One convenient method of contacting the oxide with the chloriding agent can be to vaporize a chloriding agent into a gas stream used to fluidize the solid oxide during calcination. Other suitable chloriding agents and procedures for preparing chlorided solid oxides are well known to those of skill in the art.

The amount of fluoride or chloride ion present before calcining the solid oxide generally can be from about 1 to about 50% by weight, where the weight percent is based on the weight of the solid oxide, for example, silica-alumina, before calcining. According to another aspect of this invention, the amount of fluoride or chloride ion present before calcining the solid oxide can be from about 1 to about 25% by weight, and according to another aspect of this invention, from about 2 to about 20% by weight. According to yet another aspect of this invention, the amount of fluoride or chloride ion present before calcining the solid oxide can be from about 4 to about 10% by weight. Once impregnated with a halide, the halided oxide can be dried by any suitable method including, but not limited to, suction filtration followed by evaporation, drying under vacuum, spray drying, and the like, although it is also possible to initiate the calcining step immediately without drying the impregnated solid oxide.

The silica-alumina used to prepare the treated silica-alumina typically can have a pore volume greater than about 0.5 cc/g. According to one aspect of the present invention, the pore volume can be greater than about 0.8 cc/g, and according to another aspect of the present invention, greater than about 1.0 cc/g. Further, the silica-alumina generally can have a surface area greater than about 100 m²/g. According to another aspect of this invention, the surface area can be greater than about 250 m²/g. Yet, in another aspect, the surface area can be greater than about 350 m²/g.

The silica-alumina utilized in the present invention typically can have an alumina content from about 5 to about 95% by weight. According to one aspect of this invention, the alumina content of the silica-alumina can be from about 5 to about 50%, or from about 8% to about 30%, alumina by weight. In another aspect, high alumina content silica-alumina compounds can be employed, in which the alumina content of these silica-alumina compounds typically ranges from about 60% to about 90%, or from about 65% to about 80%, alumina by weight. According to yet another aspect of

this invention, the solid oxide component can comprise alumina without silica, and according to another aspect of this invention, the solid oxide component can comprise silica without alumina.

The sulfated solid oxide can comprise sulfate and a solid oxide component, such as alumina or silica-alumina, in the form of a particulate solid. Optionally, the sulfated oxide can be treated further with a metal ion such that the calcined sulfated oxide comprises a metal. According to one aspect of the present invention, the sulfated solid oxide can comprise sulfate and alumina. In some instances, the sulfated alumina can be formed by a process wherein the alumina is treated with a sulfate source, for example, sulfuric acid or a sulfate salt such as ammonium sulfate. This process generally can be performed by forming a slurry of the alumina in a suitable solvent, such as alcohol or water, in which the desired concentration of the sulfating agent has been added. Suitable organic solvents can include, but are not limited to, the one to three carbon alcohols because of their volatility and low surface tension.

According to one aspect of this invention, the amount of sulfate ion present before calcining can be from about 0.5 to about 100 parts by weight sulfate ion to about 100 parts by weight solid oxide. According to another aspect of this invention, the amount of sulfate ion present before calcining can be from about 1 to about 50 parts by weight sulfate ion to about 100 parts by weight solid oxide, and according to still another aspect of this invention, from about 5 to about 30 parts by weight sulfate ion to about 100 parts by weight solid oxide. These weight ratios are based on the weight of the solid oxide before calcining. Once impregnated with sulfate, the sulfated oxide can be dried by any suitable method including, but not limited to, suction filtration followed by evaporation, drying under vacuum, spray drying, and the like, although it is also possible to initiate the calcining step immediately.

According to another aspect of the present invention, the activator-support used in preparing the catalyst compositions of this invention can comprise an ion-exchangeable activator-support including, but not limited to, silicate and aluminosilicate compounds or minerals, either with layered or non-layered structures, and combinations thereof. In another aspect of this invention, ion-exchangeable, layered aluminosilicates such as pillared clays can be used as activator-supports. When the acidic activator-support comprises an ion-exchangeable activator-support, it can

optionally be treated with at least one electron-withdrawing anion such as those disclosed herein, though typically the ion-exchangeable activator-support is not treated with an electron-withdrawing anion.

According to another aspect of the present invention, the activator-support of
5 this invention can comprise clay minerals having exchangeable cations and layers capable of expanding. Typical clay mineral activator-supports can include, but are not limited to, ion-exchangeable, layered aluminosilicates such as pillared clays. Although the term “support” is used, it is not meant to be construed as an inert component of the catalyst composition, but rather can be considered an active part of the catalyst
10 composition, because of its intimate association with the metallocene component.

According to another aspect of the present invention, the clay materials of this invention can encompass materials either in their natural state or that have been treated with various ions by wetting, ion exchange, or pillaring. Typically, the clay material activator-support of this invention can comprise clays that have been ion exchanged
15 with large cations, including polynuclear, highly charged metal complex cations. However, the clay material activator-supports of this invention also can encompass clays that have been ion exchanged with simple salts, including, but not limited to, salts of Al(III), Fe(II), Fe(III), and Zn(II) with ligands such as halide, acetate, sulfate, nitrate, or nitrite.

According to another aspect of the present invention, the activator-support can
20 comprise a pillared clay. The term “pillared clay” is used to refer to clay materials that have been ion exchanged with large, typically polynuclear, highly charged metal complex cations. Examples of such ions can include, but are not limited to, Keggin ions which can have charges such as 7+, various polyoxometallates, and other large
25 ions. Thus, the term pillaring can refer to a simple exchange reaction in which the exchangeable cations of a clay material are replaced with large, highly charged ions, such as Keggin ions. These polymeric cations then can be immobilized within the interlayers of the clay and when calcined are converted to metal oxide “pillars,” effectively supporting the clay layers as column-like structures. Thus, once the clay is
30 dried and calcined to produce the supporting pillars between clay layers, the expanded lattice structure can be maintained and the porosity can be enhanced. The resulting pores can vary in shape and size as a function of the pillaring material and the parent

clay material used. Examples of pillaring and pillared clays are found in: T.J. Pinnavaia, *Science* 220 (4595), 365-371 (1983); J.M. Thomas, *Intercalation Chemistry*, (S. Whittington and A. Jacobson, eds.) Ch. 3, pp. 55-99, Academic Press, Inc., (1972); U.S. Patent No. 4,452,910; U.S. Patent No. 5,376,611; and U.S. Patent No. 4,060,480; 5 the disclosures of which are incorporated herein by reference in their entirety.

The pillaring process can utilize clay minerals having exchangeable cations and layers capable of expanding. Any pillared clay that can enhance the polymerization of olefins in the catalyst composition of the present invention can be used. Therefore, suitable clay minerals for pillaring can include, but are not limited to, allophanes; 10 smectites, both dioctahedral (Al) and tri-octahedral (Mg) and derivatives thereof such as montmorillonites (bentonites), nontronites, hectorites, or laponites; halloysites; vermiculites; micas; fluoromicas; chlorites; mixed-layer clays; the fibrous clays including but not limited to sepiolites, attapulgites, and palygorskites; a serpentine clay; illite; laponite; saponite; and any combination thereof. In one aspect, the pillared clay 15 activator-support can comprise bentonite or montmorillonite. The principal component of bentonite is montmorillonite.

The pillared clay can be pretreated if desired. For example, a pillared bentonite can be pretreated by drying at about 300 °C under an inert atmosphere, typically dry nitrogen, for about 3 hours, before being added to the polymerization reactor. 20 Although an exemplary pretreatment is described herein, it should be understood that the preheating can be carried out at many other temperatures and times, including any combination of temperature and time steps, all of which are encompassed by this invention.

The activator-support used to prepare the catalyst compositions of the present 25 invention can be combined with other inorganic support materials, including, but not limited to, zeolites, inorganic oxides, and the like. In one aspect, typical support materials that can be used include, but are not limited to, silica, silica-alumina, alumina, titania, zirconia, magnesia, boria, thoria, aluminophosphate, aluminum phosphate, silica-titania, coprecipitated silica/titania, mixtures thereof, or any combination thereof.

30 According to another aspect of the present invention, one or more of the metallocene compounds can be precontacted with an olefin monomer and an organoaluminum compound for a first period of time prior to contacting this mixture

with the activator-support. Once the precontacted mixture of metallocene complex(es), olefin monomer, and organoaluminum compound is contacted with the activator-support, the composition further comprising the activator-support can be termed a “postcontacted” mixture. The postcontacted mixture can be allowed to remain in
5 further contact for a second period of time prior to being charged into the reactor in which the polymerization process will be carried out.

According to yet another aspect of the present invention, one or more of the metallocene compounds can be precontacted with an olefin monomer and an activator-support for a first period of time prior to contacting this mixture with the
10 organoaluminum compound. Once the precontacted mixture of the metallocene complex(es), olefin monomer, and activator-support is contacted with the organoaluminum compound, the composition further comprising the organoaluminum can be termed a “postcontacted” mixture. The postcontacted mixture can be allowed to remain in further contact for a second period of time prior to being introduced into the
15 polymerization reactor.

CO-CATALYSTS

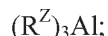
In certain aspects directed to catalyst compositions containing a co-catalyst, the co-catalyst can comprise a metal hydrocarbyl compound, examples of which include non-halide metal hydrocarbyl compounds, metal hydrocarbyl halide compounds, non-
20 halide metal alkyl compounds, metal alkyl halide compounds, and so forth. The hydrocarbyl group (or alkyl group) can be any hydrocarbyl (or alkyl) group disclosed herein. Moreover, in some aspects, the metal of the metal hydrocarbyl can be a group 1, 2, 11, 12, 13, or 14 metal; alternatively, a group 13 or 14 metal; or alternatively, a group 13 metal. Hence, in some aspects, the metal of the metal hydrocarbyl (non-
25 halide metal hydrocarbyl or metal hydrocarbyl halide) can be lithium, sodium, potassium, rubidium, cesium, beryllium, magnesium, calcium, strontium, barium, zinc, cadmium, boron, aluminum, or tin; alternatively, lithium, sodium, potassium, magnesium, calcium, zinc, boron, aluminum, or tin; alternatively, lithium, sodium, or potassium; alternatively, magnesium or calcium; alternatively, lithium; alternatively,
30 sodium; alternatively, potassium; alternatively, magnesium; alternatively, calcium; alternatively, zinc; alternatively, boron; alternatively, aluminum; or alternatively, tin. In some aspects, the metal hydrocarbyl or metal alkyl, with or without a halide, can

comprise a lithium hydrocarbyl or alkyl, a magnesium hydrocarbyl or alkyl, a boron hydrocarbyl or alkyl, a zinc hydrocarbyl or alkyl, or an aluminum hydrocarbyl or alkyl.

In particular aspects directed to catalyst compositions containing a co-catalyst (e.g., the activator can comprise a solid oxide treated with an electron-withdrawing anion), the co-catalyst can comprise an aluminoxane compound, an organoboron or organoborate compound, an ionizing ionic compound, an organoaluminum compound, an organozinc compound, an organomagnesium compound, or an organolithium compound, and this includes any combinations of these materials. In one aspect, the co-catalyst can comprise an organoaluminum compound. In another aspect, the co-catalyst can comprise an aluminoxane compound, an organoboron or organoborate compound, an ionizing ionic compound, an organozinc compound, an organomagnesium compound, an organolithium compound, or any combination thereof. In yet another aspect, the co-catalyst can comprise an aluminoxane compound; alternatively, an organoboron or organoborate compound; alternatively, an ionizing ionic compound; alternatively, an organozinc compound; alternatively, an organomagnesium compound; or alternatively, an organolithium compound.

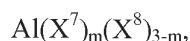
ORGANOALUMINUM COMPOUNDS

In some aspects, catalyst compositions of the present invention can comprise one or more organoaluminum compounds. Such compounds can include, but are not limited to, compounds having the formula:



wherein each R^Z independently can be an aliphatic group having from 1 to 10 carbon atoms. For example, each R^Z independently can be methyl, ethyl, propyl, butyl, hexyl, or isobutyl.

Other organoaluminum compounds which can be used in catalyst compositions disclosed herein can include, but are not limited to, compounds having the formula:



wherein each X^7 independently can be a hydrocarbyl; each X^8 independently can be an alkoxide or an aryloxide, a halide, or a hydride; and m can be from 1 to 3, inclusive. Hydrocarbyl is used herein to specify a hydrocarbon radical group and includes, for instance, aryl, alkyl, cycloalkyl, alkenyl, cycloalkenyl, cycloalkadienyl, alkynyl, aralkyl, aralkenyl, and aralkynyl groups.

In one aspect, each X^7 independently can be any hydrocarbyl having from 1 to about 18 carbon atoms disclosed herein. In another aspect of the present invention, each X^7 independently can be any alkyl having from 1 to 10 carbon atoms disclosed herein. For example, each X^7 independently can be methyl, ethyl, propyl, n-butyl, sec-butyl, isobutyl, or hexyl, and the like, in yet another aspect of the present invention.

According to one aspect of the present invention, each X^8 independently can be an alkoxide or an aryloxy, any one of which has from 1 to 18 carbon atoms, a halide, or a hydride. In another aspect of the present invention, each X^8 can be selected independently from fluorine and chlorine. Yet, in another aspect, X^8 can be chlorine.

In the formula, $Al(X^7)_m(X^8)_{3-m}$, m can be a number from 1 to 3, inclusive, and typically, m can be 3. The value of m is not restricted to be an integer; therefore, this formula can include sesquihalide compounds or other organoaluminum cluster compounds.

Examples of organoaluminum compounds suitable for use in accordance with the present invention can include, but are not limited to, trialkylaluminum compounds, dialkylaluminum halide compounds, dialkylaluminum alkoxide compounds, dialkylaluminum hydride compounds, and combinations thereof. Specific non-limiting examples of suitable organoaluminum compounds can include trimethylaluminum (TMA), triethylaluminum (TEA), tri-n-propylaluminum (TNPA), tri-n-butylaluminum (TNBA), triisobutylaluminum (TIBA), tri-n-hexylaluminum, tri-n-octylaluminum, diisobutylaluminum hydride, diethylaluminum ethoxide, diethylaluminum chloride, and the like, or combinations thereof.

The present invention contemplates a method of precontacting a metallocene compound (or compounds) with an organoaluminum compound and an optional olefin monomer to form a precontacted mixture, prior to contacting this precontacted mixture with an activator-support to form a catalyst composition. When the catalyst composition is prepared in this manner, typically, though not necessarily, a portion of the organoaluminum compound can be added to the precontacted mixture and another portion of the organoaluminum compound can be added to the postcontacted mixture prepared when the precontacted mixture is contacted with the solid oxide activator-support. However, the entire organoaluminum compound can be used to prepare the

catalyst composition in either the precontacting or postcontacting step. Alternatively, all the catalyst components can be contacted in a single step.

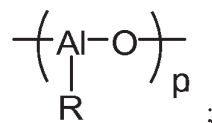
Further, more than one organoaluminum compound can be used in either the precontacting or the postcontacting step. When an organoaluminum compound is added in multiple steps, the amounts of organoaluminum compound disclosed herein include the total amount of organoaluminum compound used in both the precontacted and postcontacted mixtures, and any additional organoaluminum compound added to the polymerization reactor. Therefore, total amounts of organoaluminum compounds are disclosed regardless of whether a single organoaluminum compound or more than one organoaluminum compound is used.

ALUMINOXANE COMPOUNDS

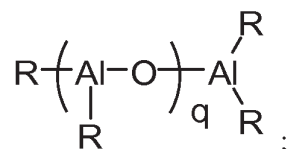
Certain aspects of the present invention provide a catalyst composition which can comprise an aluminoxane compound. As used herein, the terms “aluminoxane” and “aluminoxane compound” refer to aluminoxane compounds, compositions, mixtures, or discrete species, regardless of how such aluminoxanes are prepared, formed or otherwise provided. For example, a catalyst composition comprising an aluminoxane compound can be prepared in which aluminoxane is provided as the poly(hydrocarbyl aluminum oxide), or in which aluminoxane is provided as the combination of an aluminum alkyl compound and a source of active protons such as water. Aluminoxanes also can be referred to as poly(hydrocarbyl aluminum oxides) or organoaluminoxanes.

The other catalyst components typically can be contacted with the aluminoxane in a saturated hydrocarbon compound solvent, though any solvent that is substantially inert to the reactants, intermediates, and products of the activation step can be used. The catalyst composition formed in this manner can be collected by any suitable method, for example, by filtration. Alternatively, the catalyst composition can be introduced into the polymerization reactor without being isolated.

The aluminoxane compound of this invention can be an oligomeric aluminum compound comprising linear structures, cyclic structures, or cage structures, or mixtures of all three. Cyclic aluminoxane compounds having the formula:



wherein each R in this formula independently can be a linear or branched alkyl having from 1 to 10 carbon atoms, and p in this formula can be an integer from 3 to 20, are encompassed by this invention. The AlRO moiety shown here also can constitute the repeating unit in a linear aluminoxane. Thus, linear aluminoxanes having the formula:



wherein each R in this formula independently can be a linear or branched alkyl having from 1 to 10 carbon atoms, and q in this formula can be an integer from 1 to 50, are also encompassed by this invention.

Further, aluminoxanes can have cage structures of the formula $\text{R}^t_{5r+\alpha} \text{R}^b_r \alpha \text{Al}_4 \text{O}_{3r}$, wherein each R^t independently can be a terminal linear or branched alkyl group having from 1 to 10 carbon atoms; each R^b independently can be a bridging linear or branched alkyl group having from 1 to 10 carbon atoms; r can be 3 or 4; and α can be equal to $n_{\text{Al}(3)} - n_{\text{O}(2)} + n_{\text{O}(4)}$, wherein $n_{\text{Al}(3)}$ is the number of three coordinate aluminum atoms, $n_{\text{O}(2)}$ is the number of two coordinate oxygen atoms, and $n_{\text{O}(4)}$ is the number of 4 coordinate oxygen atoms.

Thus, aluminoxanes which can be employed in the catalyst compositions of the present invention can be represented generally by formulas such as $(\text{R-Al-O})_p$, $\text{R}(\text{R-Al-O})_q \text{AlR}_2$, and the like. In these formulas, each R group independently can be a linear or branched $\text{C}_1\text{-C}_6$ alkyl, such as methyl, ethyl, propyl, butyl, pentyl, or hexyl. Examples of aluminoxane compounds that can be used in accordance with the present invention can include, but are not limited to, methylaluminoxane, modified methylaluminoxane, ethylaluminoxane, n-propylaluminoxane, iso-propylaluminoxane, n-butylaluminoxane, t-butylaluminoxane, sec-butylaluminoxane, iso-butylaluminoxane, 1-pentylaluminoxane, 2-pentylaluminoxane, 3-pentylaluminoxane, isopentylaluminoxane, neopentylaluminoxane, and the like, or any combination thereof. Methylaluminoxane, ethylaluminoxane, and iso-butylaluminoxane can be prepared from trimethylaluminum, triethylaluminum, and triisobutylaluminum, respectively, and sometimes are referred to

as poly(methyl aluminum oxide), poly(ethyl aluminum oxide), and poly(isobutyl aluminum oxide), respectively. It is also within the scope of the invention to use an aluminoxane in combination with a trialkylaluminum, such as that disclosed in U.S. Patent No. 4,794,096, incorporated herein by reference in its entirety.

5 The present invention contemplates many values of p and q in the aluminoxane formulas $(R-Al-O)_p$ and $R(R-Al-O)_qAlR_2$, respectively. In some aspects, p and q can be at least 3. However, depending upon how the organoaluminoxane is prepared, stored, and used, the value of p and q can vary within a single sample of aluminoxane, and such combinations of organoaluminoxanes are contemplated herein.

10 In preparing a catalyst composition containing an aluminoxane, the molar ratio of the total moles of aluminum in the aluminoxane (or aluminoxanes) to the total moles of metallocene complexes in the composition generally can be between about 1:10 and about 100,000:1. In another aspect, the molar ratio can be in a range from about 5:1 to about 15,000:1. Optionally, aluminoxane can be added to a polymerization zone in
15 ranges from about 0.01 mg/L to about 1000 mg/L, from about 0.1 mg/L to about 100 mg/L, or from about 1 mg/L to about 50 mg/L.

 Organoaluminoxanes can be prepared by various procedures. Examples of organoaluminoxane preparations are disclosed in U.S. Patent Nos. 3,242,099 and 4,808,561, the disclosures of which are incorporated herein by reference in their
20 entirety. For example, water in an inert organic solvent can be reacted with an aluminum alkyl compound, such as $(R^Z)_3Al$, to form the desired organoaluminoxane compound. While not intending to be bound by this statement, it is believed that this synthetic method can afford a mixture of both linear and cyclic R-Al-O aluminoxane species, both of which are encompassed by this invention. Alternatively,
25 organoaluminoxanes can be prepared by reacting an aluminum alkyl compound, such as $(R^Z)_3Al$, with a hydrated salt, such as hydrated copper sulfate, in an inert organic solvent.

ORGANOBORON & ORGANOBORATE COMPOUNDS

 According to another aspect of the present invention, the catalyst composition
30 can comprise an organoboron or organoborate compound. Such compounds can include neutral boron compounds, borate salts, and the like, or combinations thereof.

For example, fluoroorgano boron compounds and fluoroorgano borate compounds are contemplated.

Any fluoroorgano boron or fluoroorgano borate compound can be utilized with the present invention. Examples of fluoroorgano borate compounds that can be used in the present invention can include, but are not limited to, fluorinated aryl borates such as N,N-dimethylanilinium tetrakis(pentafluorophenyl)borate, triphenylcarbenium tetrakis(pentafluorophenyl)borate, lithium tetrakis(pentafluorophenyl)borate, N,N-dimethylanilinium tetrakis[3,5-bis(trifluoromethyl)phenyl]borate, triphenylcarbenium tetrakis[3,5-bis(trifluoromethyl)phenyl]borate, and the like, or mixtures thereof.

Examples of fluoroorgano boron compounds that can be used as co-catalysts in the present invention can include, but are not limited to, tris(pentafluorophenyl)boron, tris[3,5-bis(trifluoromethyl)phenyl]boron, and the like, or mixtures thereof. Although not intending to be bound by the following theory, these examples of fluoroorgano borate and fluoroorgano boron compounds, and related compounds, can form “weakly-coordinating” anions when combined with a transition metal complex (see e.g., U.S. Patent 5,919,983, the disclosure of which is incorporated herein by reference in its entirety). Applicants also contemplate the use of diboron, or bis-boron, compounds or other bifunctional compounds containing two or more boron atoms in the chemical structure, such as disclosed in J. Am. Chem. Soc., 2005, 127, pp. 14756-14768, the content of which is incorporated herein by reference in its entirety.

Generally, any amount of organoboron compound can be used. According to one aspect of this invention, the molar ratio of the total moles of organoboron or organoborate compound (or compounds) to the total moles of metallocene compounds in the catalyst composition can be in a range from about 0.1:1 to about 15:1. Typically, the amount of the fluoroorgano boron or fluoroorgano borate compound used can be from about 0.5 moles to about 10 moles of boron/borate compound per mole of metallocene complexes. According to another aspect of this invention, the amount of fluoroorgano boron or fluoroorgano borate compound can be from about 0.8 moles to about 5 moles of boron/borate compound per mole of metallocene complexes.

IONIZING IONIC COMPOUNDS

In another aspect, catalyst compositions disclosed herein can comprise an ionizing ionic compound. An ionizing ionic compound is an ionic compound that can function as a co-catalyst to enhance the activity of the catalyst composition. While not
5 intending to be bound by theory, it is believed that the ionizing ionic compound can be capable of reacting with a metallocene complex and converting the metallocene complex into one or more cationic metallocene complexes, or incipient cationic metallocene complexes. Again, while not intending to be bound by theory, it is believed that the ionizing ionic compound can function as an ionizing compound by
10 completely or partially extracting an anionic ligand, such as monoanionic ligand X, from the metallocene complex. However, the ionizing ionic compound can be a co-catalyst regardless of whether it is ionizes the metallocene compound, abstracts a X ligand in a fashion as to form an ion pair, weakens the metal-X bond in the metallocene, simply coordinates to a X ligand, or activates the metallocene by some
15 other mechanism.

Further, it is not necessary that the ionizing ionic compound activate the metallocene compound only. The activation function of the ionizing ionic compound can be evident in the enhanced activity of catalyst composition as a whole, as compared to a catalyst composition that does not contain an ionizing ionic compound.

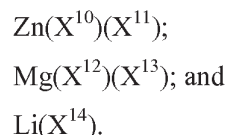
20 Examples of ionizing ionic compounds can include, but are not limited to, the following compounds: tri(n-butyl)ammonium tetrakis(p-tolyl)borate, tri(n-butyl)ammonium tetrakis(m-tolyl)borate, tri(n-butyl)ammonium tetrakis(2,4-dimethylphenyl)borate, tri(n-butyl)ammonium tetrakis(3,5-dimethylphenyl)borate, tri(n-butyl)ammonium tetrakis[3,5-bis(trifluoromethyl)phenyl]borate, tri(n-butyl)ammonium tetrakis(pentafluorophenyl)borate, N,N-dimethylanilinium tetrakis(p-tolyl)borate, N,N-dimethylanilinium tetrakis(m-tolyl)borate, N,N-dimethylanilinium tetrakis(2,4-dimethylphenyl)borate, N,N-dimethylanilinium tetrakis(3,5-dimethylphenyl)borate, N,N-dimethylanilinium tetrakis[3,5-bis(trifluoromethyl)phenyl]borate, N,N-dimethylanilinium tetrakis(pentafluorophenyl)borate, triphenylcarbenium
25 tetrakis(p-tolyl)borate, triphenylcarbenium tetrakis(m-tolyl)borate, triphenylcarbenium tetrakis(2,4-dimethylphenyl)borate, triphenylcarbenium tetrakis(3,5-dimethylphenyl)borate, triphenylcarbenium tetrakis[3,5-bis(trifluoromethyl)phenyl]
30

borate, triphenylcarbenium tetrakis(pentafluorophenyl)borate, tropylium tetrakis(p-tolyl)borate, tropylium tetrakis(m-tolyl)borate, tropylium tetrakis(2,4-dimethylphenyl)borate, tropylium tetrakis(3,5-dimethylphenyl)borate, tropylium tetrakis[3,5-bis(trifluoromethyl)phenyl]borate, tropylium tetrakis(pentafluorophenyl)
 5 borate, lithium tetrakis(pentafluorophenyl)borate, lithium tetraphenylborate, lithium tetrakis(p-tolyl)borate, lithium tetrakis(m-tolyl)borate, lithium tetrakis(2,4-dimethylphenyl)borate, lithium tetrakis(3,5-dimethylphenyl)borate, lithium tetrafluoroborate, sodium tetrakis(pentafluorophenyl)borate, sodium tetraphenylborate, sodium tetrakis(p-tolyl)borate, sodium tetrakis(m-tolyl)borate, sodium tetrakis(2,4-
 10 dimethylphenyl)borate, sodium tetrakis(3,5-dimethylphenyl)borate, sodium tetrafluoroborate, potassium tetrakis(pentafluorophenyl)borate, potassium tetraphenylborate, potassium tetrakis(p-tolyl)borate, potassium tetrakis(m-tolyl)borate, potassium tetrakis(2,4-dimethylphenyl)borate, potassium tetrakis(3,5-dimethylphenyl)borate, potassium tetrafluoroborate, lithium
 15 tetrakis(pentafluorophenyl)aluminate, lithium tetraphenylaluminate, lithium tetrakis(p-tolyl)aluminate, lithium tetrakis(m-tolyl)aluminate, lithium tetrakis(2,4-dimethylphenyl)aluminate, lithium tetrakis(3,5-dimethylphenyl)aluminate, lithium tetrafluoroaluminate, sodium tetrakis(pentafluorophenyl)aluminate, sodium tetraphenylaluminate, sodium tetrakis(p-tolyl)aluminate, sodium tetrakis(m-
 20 tolyl)aluminate, sodium tetrakis(2,4-dimethylphenyl)aluminate, sodium tetrakis(3,5-dimethylphenyl)aluminate, sodium tetrafluoroaluminate, potassium tetrakis(pentafluorophenyl)aluminate, potassium tetraphenylaluminate, potassium tetrakis(p-tolyl)aluminate, potassium tetrakis(m-tolyl)aluminate, potassium tetrakis(2,4-dimethylphenyl)aluminate, potassium tetrakis (3,5-dimethylphenyl)aluminate,
 25 potassium tetrafluoroaluminate, and the like, or combinations thereof. Ionizing ionic compounds useful in this invention are not limited to these; other examples of ionizing ionic compounds are disclosed in U.S. Patent Nos. 5,576,259 and 5,807,938, the disclosures of which are incorporated herein by reference in their entirety.

ORGANOZINC, ORGANOMAGNESIUM, & ORGANOLITHIUM COMPOUNDS

30 Other aspects are directed to catalyst compositions which can include an organozinc compound, an organomagnesium compound, an organolithium compound,

or a combination thereof. In some aspects, these compounds have the following general formulas:



In these formulas, X^{10} , X^{12} , and X^{14} independently can be a C_1 to C_{18} hydrocarbyl group, and X^{11} and X^{13} independently can be H, a halide, or a C_1 to C_{18} hydrocarbyl or C_1 to C_{18} hydrocarboxy group. It is contemplated X^{10} and X^{11} (or X^{12} and X^{13}) can be the same, or that X^{10} and X^{11} (or X^{12} and X^{13}) can be different.

In one aspect, X^{10} , X^{11} , X^{12} , X^{13} , and X^{14} independently can be any C_1 to C_{18} hydrocarbyl group, C_1 to C_{12} hydrocarbyl group, C_1 to C_8 hydrocarbyl group, or C_1 to C_5 hydrocarbyl group disclosed herein. In another aspect, X^{10} , X^{11} , X^{12} , X^{13} , and X^{14} independently can be any C_1 to C_{18} alkyl group, C_2 to C_{18} alkenyl group, C_6 to C_{18} aryl group, or C_7 to C_{18} aralkyl group disclosed herein; alternatively, any C_1 to C_{12} alkyl group, C_2 to C_{12} alkenyl group, C_6 to C_{12} aryl group, or C_7 to C_{12} aralkyl group disclosed herein; or alternatively, any C_1 to C_5 alkyl group, C_2 to C_5 alkenyl group, C_6 to C_8 aryl group, or C_7 to C_8 aralkyl group disclosed herein. Thus, X^{10} , X^{11} , X^{12} , X^{13} , and X^{14} independently can be a methyl group, an ethyl group, a propyl group, a butyl group, a pentyl group, a hexyl group, a heptyl group, an octyl group, a nonyl group, a decyl group, a undecyl group, a dodecyl group, a tridecyl group, a tetradecyl group, a pentadecyl group, a hexadecyl group, a heptadecyl group, an octadecyl group, an ethenyl group, a propenyl group, a butenyl group, a pentenyl group, a hexenyl group, a heptenyl group, an octenyl group, a nonenyl group, a decenyl group, a undecenyl group, a dodecenyl group, a tridecenyl group, a tetradecenyl group, a pentadecenyl group, a hexadecenyl group, a heptadecenyl group, an octadecenyl group, a phenyl group, a naphthyl group, a benzyl group, or a tolyl group, and the like. In yet another aspect, X^{10} , X^{11} , X^{12} , X^{13} , and X^{14} independently can be methyl, ethyl, propyl, butyl, or pentyl (e.g., neopentyl), or both X^{10} and X^{11} (or both X^{12} and X^{13}) can be methyl, or ethyl, or propyl, or butyl, or pentyl (e.g., neopentyl).

X^{11} and X^{13} independently can be H, a halide, or a C_1 to C_{18} hydrocarbyl or C_1 to C_{18} hydrocarboxy group (e.g., any C_1 to C_{18} , C_1 to C_{12} , C_1 to C_{10} , or C_1 to C_8 hydrocarboxy group disclosed herein). In some aspects, X^{11} and X^{13} independently can

be H, a halide (e.g., Cl), or a C₁ to C₁₈ hydrocarbyl or C₁ to C₁₈ hydrocarboxy group; alternatively, H, a halide, or a C₁ to C₈ hydrocarbyl or C₁ to C₈ hydrocarboxy group; or alternatively, H, Br, Cl, F, I, methyl, ethyl, propyl, butyl, pentyl (e.g., neopentyl), hexyl, heptyl, octyl, nonyl, decyl, ethenyl, propenyl, butenyl, pentenyl, hexenyl, heptenyl, octenyl, nonenyl, decenyl, phenyl, benzyl, tolyl, methoxy, ethoxy, propoxy, butoxy, pentoxy, phenoxy, toloxy, xyloxy, or benzoxy.

In other aspects, the organozinc and/or the organomagnesium compound can have one or two hydrocarbylsilyl moieties. Each hydrocarbyl of the hydrocarbylsilyl group can be any hydrocarbyl group disclosed herein (e.g., a C₁ to C₁₈ alkyl group, a C₂ to C₁₈ alkenyl group, a C₆ to C₁₈ aryl group, a C₇ to C₁₈ aralkyl group, etc.). Illustrative and non-limiting examples of hydrocarbylsilyl groups can include, but are not limited to, trimethylsilyl, triethylsilyl, tripropylsilyl (e.g., triisopropylsilyl), tributylsilyl, tripentylsilyl, triphenylsilyl, allyldimethylsilyl, trimethylsilylmethyl, and the like.

Exemplary organozinc compounds which can be used as co-catalysts can include, but are not limited to, dimethylzinc, diethylzinc, dipropylzinc, dibutylzinc, dineopentylzinc, di(trimethylsilyl)zinc, di(triethylsilyl)zinc, di(triisopropylsilyl)zinc, di(triphenylsilyl)zinc, di(allyldimethylsilyl)zinc, di(trimethylsilylmethyl)zinc, and the like, or combinations thereof.

Similarly, exemplary organomagnesium compounds can include, but are not limited to, dimethylmagnesium, diethylmagnesium, dipropylmagnesium, dibutylmagnesium, dineopentylmagnesium, di(trimethylsilylmethyl)magnesium, methylmagnesium chloride, ethylmagnesium chloride, propylmagnesium chloride, butylmagnesium chloride, neopentylmagnesium chloride, trimethylsilylmethylmagnesium chloride, methylmagnesium bromide, ethylmagnesium bromide, propylmagnesium bromide, butylmagnesium bromide, neopentylmagnesium bromide, trimethylsilylmethylmagnesium bromide, methylmagnesium iodide, ethylmagnesium iodide, propylmagnesium iodide, butylmagnesium iodide, neopentylmagnesium iodide, trimethylsilylmethylmagnesium iodide, methylmagnesium ethoxide, ethylmagnesium ethoxide, propylmagnesium ethoxide, butylmagnesium ethoxide, neopentylmagnesium ethoxide, trimethylsilylmethylmagnesium ethoxide, methylmagnesium propoxide, ethylmagnesium propoxide, propylmagnesium propoxide, butylmagnesium propoxide,

neopentylmagnesium propoxide, trimethylsilylmethylmagnesium propoxide, methylmagnesium phenoxide, ethylmagnesium phenoxide, propylmagnesium phenoxide, butylmagnesium phenoxide, neopentylmagnesium phenoxide, trimethylsilylmethylmagnesium phenoxide, and the like, or any combinations thereof.

5 Likewise, exemplary organolithium compounds can include, but are not limited to, methyllithium, ethyllithium, propyllithium, butyllithium (e.g., t-butyllithium), neopentyllithium, trimethylsilylmethyllithium, phenyllithium, tolyllithium, xylyllithium, benzylolithium, (dimethylphenyl)methyllithium, allyllithium, and the like, or combinations thereof.

10 OLEFIN MONOMERS

Unsaturated reactants that can be employed with catalyst compositions and polymerization processes of this invention typically can include olefin compounds having from 2 to 30 carbon atoms per molecule and having at least one olefinic double bond. This invention encompasses homopolymerization processes using a single olefin
15 such as ethylene or propylene, as well as copolymerization, terpolymerization, etc., reactions using an olefin monomer with at least one different olefinic compound. For example, the resultant ethylene copolymers, terpolymers, etc., generally can contain a major amount of ethylene (>50 mole percent) and a minor amount of comonomer (<50 mole percent), though this is not a requirement. Comonomers that can be
20 copolymerized with ethylene often can have from 3 to 20 carbon atoms, or from 3 to 10 carbon atoms, in their molecular chain.

Acyclic, cyclic, polycyclic, terminal (α), internal, linear, branched, substituted, unsubstituted, functionalized, and non-functionalized olefins can be employed in this invention. For example, typical unsaturated compounds that can be polymerized with
25 the catalyst compositions of this invention can include, but are not limited to, ethylene, propylene, 1-butene, 2-butene, 3-methyl-1-butene, isobutylene, 1-pentene, 2-pentene, 3-methyl-1-pentene, 4-methyl-1-pentene, 1-hexene, 2-hexene, 3-hexene, 3-ethyl-1-hexene, 1-heptene, 2-heptene, 3-heptene, the four normal octenes (e.g., 1-octene), the four normal nonenes, the five normal decenes, and the like, or mixtures of two or more
30 of these compounds. Cyclic and bicyclic olefins, including but not limited to, cyclopentene, cyclohexene, norbornylene, norbornadiene, and the like, also can be polymerized as described herein. Styrene can also be employed as a monomer in the

present invention. In an aspect, the olefin monomer can comprise a C₂-C₂₀ olefin; alternatively, a C₂-C₂₀ alpha-olefin; alternatively, a C₂-C₁₀ olefin; alternatively, a C₂-C₁₀ alpha-olefin; alternatively, the olefin monomer can comprise ethylene; or alternatively, the olefin monomer can comprise propylene.

- 5 When a copolymer (or alternatively, a terpolymer) is desired, the olefin monomer and the olefin comonomer independently can comprise, for example, a C₂-C₂₀ alpha-olefin. In some aspects, the olefin monomer can comprise ethylene or propylene, which is copolymerized with at least one comonomer (e.g., a C₂-C₂₀ alpha-olefin, a C₃-C₂₀ alpha-olefin, etc.). According to one aspect of this invention, the olefin
- 10 monomer used in the polymerization process can comprise ethylene. In this aspect, examples of suitable olefin comonomers can include, but are not limited to, propylene, 1-butene, 2-butene, 3-methyl-1-butene, isobutylene, 1-pentene, 2-pentene, 3-methyl-1-pentene, 4-methyl-1-pentene, 1-hexene, 2-hexene, 3-ethyl-1-hexene, 1-heptene, 2-heptene, 3-heptene, 1-octene, 1-decene, styrene, and the like, or combinations thereof.
- 15 According to another aspect of the present invention, the olefin monomer can comprise ethylene, and the comonomer can comprise a C₃-C₁₀ alpha-olefin; alternatively, the comonomer can comprise 1-butene, 1-pentene, 1-hexene, 1-octene, 1-decene, styrene, or any combination thereof; alternatively, the comonomer can comprise 1-butene, 1-hexene, 1-octene, or any combination thereof; alternatively, the comonomer can
- 20 comprise 1-butene; alternatively, the comonomer can comprise 1-hexene; or alternatively, the comonomer can comprise 1-octene.

- Generally, the amount of comonomer introduced into a polymerization reactor system to produce a copolymer can be from about 0.01 to about 50 weight percent of the comonomer based on the total weight of the monomer and comonomer. According
- 25 to another aspect of the present invention, the amount of comonomer introduced into a polymerization reactor system can be from about 0.01 to about 40 weight percent comonomer based on the total weight of the monomer and comonomer. In still another aspect, the amount of comonomer introduced into a polymerization reactor system can be from about 0.1 to about 35 weight percent comonomer based on the total weight of
- 30 the monomer and comonomer. Yet, in another aspect, the amount of comonomer introduced into a polymerization reactor system can be from about 0.5 to about 20 weight percent comonomer based on the total weight of the monomer and comonomer.

While not intending to be bound by this theory, where branched, substituted, or functionalized olefins are used as reactants, it is believed that a steric hindrance can impede and/or slow the polymerization process. Thus, branched and/or cyclic portion(s) of the olefin removed somewhat from the carbon-carbon double bond would not be expected to hinder the reaction in the way that the same olefin substituents situated more proximate to the carbon-carbon double bond might.

According to one aspect of the present invention, at least one monomer/reactant can be ethylene (or propylene), so the polymerization reaction can be a homopolymerization involving only ethylene (or propylene), or a copolymerization with a different acyclic, cyclic, terminal, internal, linear, branched, substituted, or unsubstituted olefin. In addition, the catalyst compositions of this invention can be used in the polymerization of diolefin compounds including, but not limited to, 1,3-butadiene, isoprene, 1,4-pentadiene, and 1,5-hexadiene.

CATALYST COMPOSITIONS

In some aspects, the present invention can employ catalyst compositions containing catalyst component I, catalyst component II, an activator (one or more than one), and optionally, a co-catalyst. In other aspects, the present invention can employ catalyst compositions containing catalyst component I, catalyst component II, catalyst component III, an activator (one or more than one), and optionally, a co-catalyst. These catalyst compositions can be utilized to produce polyolefins – homopolymers, copolymers, and the like – for a variety of end-use applications. Catalyst components I, II, and III are discussed hereinabove. In aspects of the present invention, it is contemplated that the catalyst composition can contain more than one catalyst component I metallocene compound, and/or more than one catalyst component II metallocene compound, and/or more than one catalyst component III metallocene compound. Further, additional catalytic compounds – other than those specified as catalyst component I, II, or III – can be employed in the catalyst compositions and/or the polymerization processes, provided that the additional catalytic compound(s) does not detract from the advantages disclosed herein. Additionally, more than one activator also may be utilized.

The metallocene compounds of catalyst component I are discussed hereinabove. For instance, in some aspects, catalyst component I can comprise (or consist essentially

of, or consist of) an unbridged metallocene compound having formula (I). The bridged metallocene compounds of catalyst component II also are discussed hereinabove. For instance, in some aspects, catalyst component II can comprise (or consist essentially of, or consist of) a metallocene compound having formula (II). Moreover, the half-

5 metallocene compounds of catalyst component III are discussed hereinabove. For instance, in some aspects, catalyst component III can comprise (or consist essentially of, or consist of) a half-metallocene compound having formula (IIIA) or formula (IIIB).

Generally, catalyst compositions of the present invention can comprise catalyst

10 component I, catalyst component II, and an activator, or alternatively, catalyst component I, catalyst component II, catalyst component III, and an activator. In aspects of the invention, the activator can comprise an activator-support (e.g., an activator-support comprising a solid oxide treated with an electron-withdrawing anion). Activator-supports useful in the present invention are disclosed hereinabove.

15 Optionally, such catalyst compositions can further comprise one or more than one co-catalyst compound or compounds (suitable co-catalysts, such as organoaluminum compounds, also are discussed hereinabove). Thus, a catalyst composition of this invention can comprise catalyst component I, catalyst component II, an activator-support (or catalyst component I, catalyst component II, catalyst component III, an

20 activator-support), and an organoaluminum compound. For instance, the activator-support can comprise (or consist essentially of, or consist of) fluorided alumina, chlorided alumina, bromided alumina, sulfated alumina, fluorided silica-alumina, chlorided silica-alumina, bromided silica-alumina, sulfated silica-alumina, fluorided silica-zirconia, chlorided silica-zirconia, bromided silica-zirconia, sulfated silica-

25 zirconia, fluorided silica-titania, fluorided silica-coated alumina, sulfated silica-coated alumina, phosphated silica-coated alumina, and the like, or combinations thereof; alternatively, the activator-support can comprise (or consist essentially of, or consist of) a fluorided solid oxide and/or a sulfated solid oxide. Additionally, the organoaluminum compound can comprise (or consist essentially of, or consist of) trimethylaluminum,

30 triethylaluminum, tri-n-propylaluminum, tri-n-butylaluminum, triisobutylaluminum, tri-n-hexylaluminum, tri-n-octylaluminum, diisobutylaluminum hydride, diethylaluminum ethoxide, diethylaluminum chloride, and the like, or combinations thereof.

Accordingly, a catalyst composition consistent with aspects of the invention can comprise (or consist essentially of, or consist of) an unbridged zirconium or hafnium based metallocene compound; a bridged zirconium or hafnium based metallocene compound with a fluorenyl group; optionally, a half-metallocene compound; sulfated alumina (or fluorided silica-alumina, or fluorided silica-coated alumina); and triethylaluminum (or triisobutylaluminum).

In another aspect of the present invention, a catalyst composition is provided which comprises catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator-support, and an organoaluminum compound, wherein this catalyst composition is substantially free of aluminoxanes, organoboron or organoborate compounds, ionizing ionic compounds, and/or other similar materials; alternatively, substantially free of aluminoxanes; alternatively, substantially free of organoboron or organoborate compounds; or alternatively, substantially free of ionizing ionic compounds. In these aspects, the catalyst composition has catalyst activity, discussed below, in the absence of these additional materials. For example, a catalyst composition of the present invention can consist essentially of catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator-support, and an organoaluminum compound, wherein no other materials are present in the catalyst composition which would increase/decrease the activity of the catalyst composition by more than about 10% from the catalyst activity of the catalyst composition in the absence of said materials.

However, in other aspects of this invention, these activators/co-catalysts can be employed. For example, a catalyst composition comprising catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), and an activator-support can further comprise an optional co-catalyst. Suitable co-catalysts in this aspect can include, but are not limited to, aluminoxane compounds, organoboron or organoborate compounds, ionizing ionic compounds, organoaluminum compounds, organozinc compounds, organomagnesium compounds, organolithium compounds, and the like, or any combination thereof; or alternatively, organoaluminum compounds, organozinc compounds, organomagnesium compounds,

organolithium compounds, or any combination thereof. More than one co-catalyst can be present in the catalyst composition.

In a different aspect, a catalyst composition is provided which does not require an activator-support. Such a catalyst composition can comprise catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), and an activator, wherein the activator comprises an aluminoxane compound, an organoboron or organoborate compound, an ionizing ionic compound, or combinations thereof.

In a particular aspect contemplated herein, the catalyst composition is a catalyst composition comprising an activator (one or more than one), only one catalyst component I metallocene compound, only one catalyst component II metallocene compound, and only one catalyst component III half-metallocene compound (if present). In these and other aspects, the catalyst composition can comprise an activator (e.g., an activator-support comprising a solid oxide treated with an electron-withdrawing anion); only one unbridged zirconium or hafnium based metallocene compound; only one bridged zirconium or hafnium based metallocene compound with a fluorenyl group; and optionally, only one half-metallocene compound.

This invention further encompasses methods of making these catalyst compositions, such as, for example, contacting the respective catalyst components in any order or sequence.

Catalyst component I, catalyst component II, or catalyst component III, or any combination thereof, can be precontacted with an olefinic monomer if desired, not necessarily the olefin monomer to be polymerized, and an organoaluminum compound for a first period of time prior to contacting this precontacted mixture with an activator-support. The first period of time for contact, the precontact time, between the metallocene compound(s), the olefinic monomer, and the organoaluminum compound typically ranges from a time period of about 1 minute to about 24 hours, for example, from about 3 minutes to about 1 hour. Precontact times from about 10 minutes to about 30 minutes also can be employed. Alternatively, the precontacting process can be carried out in multiple steps, rather than a single step, in which multiple mixtures can be prepared, each comprising a different set of catalyst components. For example, at least two catalyst components can be contacted forming a first mixture, followed by

contacting the first mixture with at least one other catalyst component forming a second mixture, and so forth.

Multiple precontacting steps can be carried out in a single vessel or in multiple vessels. Further, multiple precontacting steps can be carried out in series
5 (sequentially), in parallel, or a combination thereof. For example, a first mixture of two catalyst components can be formed in a first vessel, a second mixture comprising the first mixture plus one additional catalyst component can be formed in the first vessel or in a second vessel, which is typically placed downstream of the first vessel.

In another aspect, one or more of the catalyst components can be split and used
10 in different precontacting treatments. For example, part of a catalyst component can be fed into a first precontacting vessel for precontacting with at least one other catalyst component, while the remainder of that same catalyst component can be fed into a second precontacting vessel for precontacting with at least one other catalyst component, or can be fed directly into the reactor, or a combination thereof. The
15 precontacting can be carried out in any suitable equipment, such as tanks, stirred mix tanks, various static mixing devices, a flask, a vessel of any type, or combinations of these apparatus.

In another aspect of this invention, the various catalyst components (for example, a catalyst component I, II, and/or III metallocene, an activator-support, an
20 organoaluminum co-catalyst, and optionally an unsaturated hydrocarbon) can be contacted in the polymerization reactor simultaneously while the polymerization reaction is proceeding. Alternatively, any two or more of these catalyst components can be precontacted in a vessel prior to entering the reaction zone. This precontacting step can be continuous, in which the precontacted product can be fed continuously to
25 the reactor, or it can be a stepwise or batchwise process in which a batch of precontacted product can be added to make a catalyst composition. This precontacting step can be carried out over a time period that can range from a few seconds to as much as several days, or longer. In this aspect, the continuous precontacting step generally can last from about 1 second to about 1 hour. In another aspect, the continuous
30 precontacting step can last from about 10 seconds to about 45 minutes, or from about 1 minute to about 30 minutes.

In an aspect, once the precontacted mixture of catalyst component I and/or catalyst component II and/or catalyst component III, an olefin monomer (if used), and an organoaluminum co-catalyst is contacted with an activator-support, this composition (with the addition of the activator-support) can be termed the "postcontacted mixture."

- 5 The postcontacted mixture optionally can remain in contact for a second period of time, the postcontact time, prior to initiating the polymerization process. Postcontact times between the precontacted mixture and the activator-support generally range from about 1 minute to about 24 hours. In a further aspect, the postcontact time can be in a range from about 3 minutes to about 1 hour. The precontacting step, the postcontacting step, or both, can increase the productivity of the polymer as compared to the same catalyst composition that is prepared without precontacting or postcontacting. However, neither a precontacting step nor a postcontacting step is required.

- 15 The postcontacted mixture can be heated at a temperature and for a time period sufficient to allow adsorption, impregnation, or interaction of the precontacted mixture and the activator-support, such that a portion of the components of the precontacted mixture can be immobilized, adsorbed, or deposited thereon. Where heating is employed, the postcontacted mixture generally can be heated to a temperature of from between about 0 °F to about 150 °F, or from about 40 °F to about 95 °F.

- 20 According to an aspect of this invention, the weight ratio of catalyst component I to catalyst component II in the catalyst composition can be in a range from about 10:1 to about 1:10, from about 8:1 to about 1:8, from about 5:1 to about 1:5, from about 4:1 to about 1:4, from about 3:1 to about 1:3; from about 2:1 to about 1:2, from about 1.5:1 to about 1:1.5, from about 1.25:1 to about 1:1.25, or from about 1.1:1 to about 1:1.1. If present, the weight percentage of catalyst component III in the catalyst composition can be in a range from about 5 to about 50%, from about 5 to about 45%, from about 5 to about 40%, from about 10 to about 50%, from about 10 to about 40%, or from about 10 to about 30%. These weight percentages are based on the total weight of catalyst components I, II, and III equaling 100%, and does not include other components of the catalyst composition, e.g., activator, co-catalyst, etc.

- 30 When a precontacting step is used, the molar ratio of the total moles of olefin monomer to total moles of metallocene(s) in the precontacted mixture typically can be in a range from about 1:10 to about 100,000:1. Total moles of each component are

used in this ratio to account for aspects of this invention where more than one olefin monomer and/or more than one metallocene compound is employed in a precontacting step. Further, this molar ratio can be in a range from about 10:1 to about 1,000:1 in another aspect of the invention.

5 Generally, the weight ratio of organoaluminum compound to activator-support can be in a range from about 10:1 to about 1:1000. If more than one organoaluminum compound and/or more than one activator-support is employed, this ratio is based on the total weight of each respective component. In another aspect, the weight ratio of the organoaluminum compound to the activator-support can be in a range from about
10 3:1 to about 1:100, or from about 1:1 to about 1:50.

 In some aspects of this invention, the weight ratio of metallocene compounds (total of catalyst component I, II, and optionally III) to activator-support can be in a range from about 1:1 to about 1:1,000,000. If more than one activator-support is employed, this ratio is based on the total weight of the activator-support. In another
15 aspect, this weight ratio can be in a range from about 1:5 to about 1:100,000, or from about 1:10 to about 1:10,000. Yet, in another aspect, the weight ratio of the metallocene compounds to the activator-support can be in a range from about 1:20 to about 1:1000.

 Catalyst compositions of the present invention generally have a catalyst activity
20 greater than about 100 grams of polyethylene (homopolymer, copolymer, etc., as the context requires) per gram of activator-support per hour (abbreviated g/g/hr). In another aspect, the catalyst activity can be greater than about 150, greater than about 250, or greater than about 500 g/g/hr. In still another aspect, catalyst compositions of this invention can be characterized by having a catalyst activity greater than about 550,
25 greater than about 650, or greater than about 750 g/g/hr. Yet, in another aspect, the catalyst activity can be greater than about 1000 g/g/hr, greater than about 2000 g/g/hr, or greater than about 3000 g/g/hr, and often as high as 5000-10,000 g/g/hr. These activities are measured under slurry polymerization conditions, with a triisobutylaluminum co-catalyst, using isobutane as the diluent, at a polymerization
30 temperature of about 90 °C and a reactor pressure of about 390 psig. Moreover, in some aspects, the activator-support can comprise sulfated alumina, fluorided silica-alumina, or fluorided silica-coated alumina, although not limited thereto.

As discussed herein, any combination of catalyst component I, catalyst component II, catalyst component III (if used), an activator-support, an organoaluminum compound, and an olefin monomer (if used), can be precontacted in some aspects of this invention. When any precontacting occurs with an olefinic monomer, it is not necessary that the olefin monomer used in the precontacting step be the same as the olefin to be polymerized. Further, when a precontacting step among any combination of the catalyst components is employed for a first period of time, this precontacted mixture can be used in a subsequent postcontacting step between any other combination of catalyst components for a second period of time. For example, one or more metallocene compounds, the organoaluminum compound, and optionally 1-hexene can be used in a precontacting step for a first period of time, and this precontacted mixture then can be contacted with the activator-support to form a postcontacted mixture that can be contacted for a second period of time prior to initiating the polymerization reaction. For example, the first period of time for contact, the precontact time, between any combination of the metallocene compound(s), the olefinic monomer (if used), the activator-support, and the organoaluminum compound can be from about 1 minute to about 24 hours, from about 3 minutes to about 1 hour, or from about 10 minutes to about 30 minutes. The postcontacted mixture optionally can be allowed to remain in contact for a second period of time, the postcontact time, prior to initiating the polymerization process. According to one aspect of this invention, postcontact times between the precontacted mixture and any remaining catalyst components can be from about 1 minute to about 24 hours, or from about 5 minutes to about 1 hour.

POLYMERIZATION PROCESSES

Catalyst compositions of the present invention can be used to polymerize olefins to form homopolymers, copolymers, terpolymers, and the like. One such process for polymerizing olefins in the presence of a catalyst composition of the present invention can comprise contacting the catalyst composition with an olefin monomer and optionally an olefin comonomer (one or more) under polymerization conditions to produce an olefin polymer, wherein the catalyst composition can comprise catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator, and an optional co-catalyst. Catalyst components

I, II, and III are discussed herein. For instance, catalyst component I can comprise an unbridged metallocene compound having formula (I), catalyst component II can comprise a bridged metallocene compound having formula (II), and catalyst component III can comprise a half-metallocene compound having formula (IIIA) or
5 formula (IIIB).

In accordance with one aspect of the invention, the polymerization process can employ a catalyst composition comprising catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), and an activator, wherein the activator comprises an activator-support. Activator-supports
10 useful in the polymerization processes of the present invention are disclosed herein. The catalyst composition, optionally, can further comprise one or more than one organoaluminum compound or compounds (or other suitable co-catalyst). Thus, a process for polymerizing olefins in the presence of a catalyst composition can employ a catalyst composition comprising catalyst component I, catalyst component II (or
15 catalyst component I, catalyst component II, catalyst component III), an activator-support, and an organoaluminum compound. In some aspects, the activator-support can comprise (or consist essentially of, or consist of) fluorided alumina, chlorided alumina, bromided alumina, sulfated alumina, fluorided silica-alumina, chlorided silica-alumina, bromided silica-alumina, sulfated silica-alumina, fluorided silica-zirconia, chlorided
20 silica-zirconia, bromided silica-zirconia, sulfated silica-zirconia, fluorided silica-titania, fluorided silica-coated alumina, sulfated silica-coated alumina, phosphated silica-coated alumina, and the like, or combinations thereof; or alternatively a fluorided solid oxide and/or a sulfated solid oxide. In some aspects, the organoaluminum compound can comprise (or consist essentially of, or consist of) trimethylaluminum, triethylaluminum, tri-n-propylaluminum, tri-n-butylaluminum, triisobutylaluminum, tri-n-hexylaluminum, tri-n-octylaluminum, diisobutylaluminum hydride, diethylaluminum ethoxide, diethylaluminum chloride, and the like, or combinations thereof.
25

In accordance with another aspect of the invention, the polymerization process can employ a catalyst composition comprising catalyst component I, catalyst
30 component II (or catalyst component I, catalyst component II, catalyst component III), an activator-support, and an optional co-catalyst, wherein the co-catalyst can comprise an aluminoxane compound, an organoboron or organoborate compound, an ionizing

ionic compound, an organoaluminum compound, an organozinc compound, an organomagnesium compound, or an organolithium compound, or any combination thereof. Hence, aspects of this invention are directed to a process for polymerizing olefins in the presence of a catalyst composition, the processes comprising contacting a catalyst composition with an olefin monomer and optionally an olefin comonomer (one or more) under polymerization conditions to produce an olefin polymer, and the catalyst composition can comprise catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator-support, and an aluminoxane compound; alternatively, catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator-support, and an organoboron or organoborate compound; alternatively, catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator-support, and an ionizing ionic compound; alternatively, catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator-support, and an organoaluminum compound; alternatively, catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator-support, and an organozinc compound; alternatively, catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator-support, and an organomagnesium compound; or alternatively, catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator-support, and an organolithium compound. Furthermore, more than one co-catalyst can be employed, e.g., an organoaluminum compound and an aluminoxane compound, an organoaluminum compound and an ionizing ionic compound, etc.

In accordance with another aspect of the invention, the polymerization process can employ a catalyst composition comprising only one catalyst component I metallocene compound, only one catalyst component II metallocene compound, only one catalyst component III half-metallocene compound (if present), an activator-support, and an organoaluminum compound.

In accordance with yet another aspect of the invention, the polymerization process can employ a catalyst composition comprising catalyst component I, catalyst

component II (or catalyst component I, catalyst component II, catalyst component III), and an activator, wherein the activator comprises an aluminoxane compound, an organoboron or organoborate compound, an ionizing ionic compound, or combinations thereof.

5 The catalyst compositions of the present invention are intended for any olefin polymerization method using various types of polymerization reactor systems and reactors. The polymerization reactor system can include any polymerization reactor capable of polymerizing olefin monomers and comonomers (one or more than one comonomer) to produce homopolymers, copolymers, terpolymers, and the like. The
10 various types of reactors include those that can be referred to as a batch reactor, slurry reactor, gas-phase reactor, solution reactor, high pressure reactor, tubular reactor, autoclave reactor, and the like, or combinations thereof. Suitable polymerization conditions are used for the various reactor types. Gas phase reactors can comprise fluidized bed reactors or staged horizontal reactors. Slurry reactors can comprise
15 vertical or horizontal loops. High pressure reactors can comprise autoclave or tubular reactors. Reactor types can include batch or continuous processes. Continuous processes can use intermittent or continuous product discharge. Processes can also include partial or full direct recycle of unreacted monomer, unreacted comonomer, and/or diluent.

20 Polymerization reactor systems of the present invention can comprise one type of reactor in a system or multiple reactors of the same or different type (e.g., a single reactor, dual reactor, more than two reactors). Production of polymers in multiple reactors can include several stages in at least two separate polymerization reactors interconnected by a transfer device making it possible to transfer the polymers resulting
25 from the first polymerization reactor into the second reactor. The desired polymerization conditions in one of the reactors can be different from the operating conditions of the other reactor(s). Alternatively, polymerization in multiple reactors can include the manual transfer of polymer from one reactor to subsequent reactors for continued polymerization. Multiple reactor systems can include any combination
30 including, but not limited to, multiple loop reactors, multiple gas phase reactors, a combination of loop and gas phase reactors, multiple high pressure reactors, or a combination of high pressure with loop and/or gas phase reactors. The multiple

reactors can be operated in series, in parallel, or both. Accordingly, the present invention encompasses polymerization reactor systems comprising a single reactor, comprising two reactors, and comprising more than two reactors. The polymerization reactor system can comprise a slurry reactor, a gas-phase reactor, a solution reactor, in
5 certain aspects of this invention, as well as multi-reactor combinations thereof.

According to one aspect of the invention, the polymerization reactor system can comprise at least one loop slurry reactor comprising vertical or horizontal loops. Monomer, diluent, catalyst, and comonomer can be continuously fed to a loop reactor where polymerization occurs. Generally, continuous processes can comprise the
10 continuous introduction of monomer/comonomer, a catalyst, and a diluent into a polymerization reactor and the continuous removal from this reactor of a suspension comprising polymer particles and the diluent. Reactor effluent can be flashed to remove the solid polymer from the liquids that comprise the diluent, monomer and/or comonomer. Various technologies can be used for this separation step including, but
15 not limited to, flashing that can include any combination of heat addition and pressure reduction, separation by cyclonic action in either a cyclone or hydrocyclone, or separation by centrifugation.

A typical slurry polymerization process (also known as the particle form process) is disclosed, for example, in U.S. Patent Nos. 3,248,179, 4,501,885,
20 5,565,175, 5,575,979, 6,239,235, 6,262,191, and 6,833,415, each of which is incorporated herein by reference in its entirety.

Suitable diluents used in slurry polymerization include, but are not limited to, the monomer being polymerized and hydrocarbons that are liquids under polymerization conditions. Examples of suitable diluents include, but are not limited
25 to, hydrocarbons such as propane, cyclohexane, isobutane, n-butane, n-pentane, isopentane, neopentane, and n-hexane. Some loop polymerization reactions can occur under bulk conditions where no diluent is used. An example is polymerization of propylene monomer as disclosed in U.S. Patent Nos. 5,455,314, which is incorporated by reference herein in its entirety.

30 According to yet another aspect of this invention, the polymerization reactor system can comprise at least one gas phase reactor. Such systems can employ a continuous recycle stream containing one or more monomers continuously cycled

through a fluidized bed in the presence of the catalyst under polymerization conditions. A recycle stream can be withdrawn from the fluidized bed and recycled back into the reactor. Simultaneously, polymer product can be withdrawn from the reactor and new or fresh monomer can be added to replace the polymerized monomer. Such gas phase
5 reactors can comprise a process for multi-step gas-phase polymerization of olefins, in which olefins are polymerized in the gaseous phase in at least two independent gas-phase polymerization zones while feeding a catalyst-containing polymer formed in a first polymerization zone to a second polymerization zone. One type of gas phase reactor is disclosed in U.S. Patent Nos. 5,352,749, 4,588,790, and 5,436,304, each of
10 which is incorporated by reference in its entirety herein.

According to still another aspect of the invention, a high pressure polymerization reactor can comprise a tubular reactor or an autoclave reactor. Tubular reactors can have several zones where fresh monomer, initiators, or catalysts are added. Monomer can be entrained in an inert gaseous stream and introduced at one
15 zone of the reactor. Initiators, catalysts, and/or catalyst components can be entrained in a gaseous stream and introduced at another zone of the reactor. The gas streams can be intermixed for polymerization. Heat and pressure can be employed appropriately to obtain optimal polymerization reaction conditions.

According to yet another aspect of the invention, the polymerization reactor
20 system can comprise a solution polymerization reactor wherein the monomer (and comonomer, if used) are contacted with the catalyst composition by suitable stirring or other means. A carrier comprising an inert organic diluent or excess monomer can be employed. If desired, the monomer/comonomer can be brought in the vapor phase into contact with the catalytic reaction product, in the presence or absence of liquid
25 material. The polymerization zone is maintained at temperatures and pressures that will result in the formation of a solution of the polymer in a reaction medium. Agitation can be employed to obtain better temperature control and to maintain uniform polymerization mixtures throughout the polymerization zone. Adequate means are utilized for dissipating the exothermic heat of polymerization.

30 Polymerization reactor systems suitable for the present invention can further comprise any combination of at least one raw material feed system, at least one feed system for catalyst or catalyst components, and/or at least one polymer recovery

system. Suitable reactor systems for the present invention can further comprise systems for feedstock purification, catalyst storage and preparation, extrusion, reactor cooling, polymer recovery, fractionation, recycle, storage, loadout, laboratory analysis, and process control.

5 Polymerization conditions that are controlled for efficiency and to provide desired polymer properties can include temperature, pressure, and the concentrations of various reactants. Polymerization temperature can affect catalyst productivity, polymer molecular weight, and molecular weight distribution. A suitable polymerization temperature can be any temperature below the de-polymerization temperature
10 according to the Gibbs Free energy equation. Typically, this includes from about 60 °C to about 280 °C, for example, or from about 60 °C to about 120 °C, depending upon the type of polymerization reactor(s). In some reactor systems, the polymerization temperature generally can fall within a range from about 70 °C to about 100 °C, or from about 75 °C to about 95 °C. Various polymerization conditions can be held
15 substantially constant, for example, for the production of a particular grade of olefin polymer.

Suitable pressures will also vary according to the reactor and polymerization type. The pressure for liquid phase polymerizations in a loop reactor is typically less than 1000 psig (6.9 MPa). Pressure for gas phase polymerization is usually at about
20 200 to 500 psig (1.4 MPa to 3.4 MPa). High pressure polymerization in tubular or autoclave reactors is generally run at about 20,000 to 75,000 psig (138 to 517 MPa). Polymerization reactors can also be operated in a supercritical region occurring at generally higher temperatures and pressures. Operation above the critical point of a pressure/temperature diagram (supercritical phase) may offer advantages.

25 Aspects of this invention are directed to olefin polymerization processes comprising contacting a catalyst composition with an olefin monomer and an optional olefin comonomer under polymerization conditions to produce an olefin polymer. The olefin polymer (e.g., ethylene copolymer) produced by the process can have any of the polymer properties disclosed herein, for example, a density from about 0.930 to about
30 0.948 g/cm³, and/or a zero-shear viscosity greater than about 5×10^5 Pa-sec (at 190 °C), and/or a CY-a parameter in a range from about 0.01 to about 0.40 (at 190 °C), and/or a peak molecular weight (Mp) in a range from about 30,000 to about 130,000 g/mol,

and/or a reverse comonomer distribution, and/or a single point notched constant tensile load (SP-NCTL) of at least 6,500 hours, and/or a natural draw ratio (NDR) of less than or equal to about 525 %, and/or a relationship between natural draw ratio (NDR, %) and density (g/cm^3) defined by the equation, $\text{NDR} < 7800(\text{density}) - 6800$, and/or a
5 relationship between natural draw ratio (NDR, %) and density (g/cm^3) defined by the equation, $\text{NDR} < 13404(\text{density}) - 12050$.

Aspects of this invention also are directed to olefin polymerization processes conducted in the absence of added hydrogen. An olefin polymerization process of this invention can comprise contacting a catalyst composition with an olefin monomer and
10 optionally an olefin comonomer in a polymerization reactor system under polymerization conditions to produce an olefin polymer, wherein the catalyst composition can comprise catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator, and an optional co-catalyst, and wherein the polymerization process is conducted in the
15 absence of added hydrogen (no hydrogen is added to the polymerization reactor system). As one of ordinary skill in the art would recognize, hydrogen can be generated in-situ by metallocene catalyst compositions in various olefin polymerization processes, and the amount generated can vary depending upon the specific catalyst composition and metallocene compound(s) employed, the type of polymerization
20 process used, the polymerization reaction conditions utilized, and so forth.

In other aspects, it may be desirable to conduct the polymerization process in the presence of a certain amount of added hydrogen. Accordingly, an olefin polymerization process of this invention can comprise contacting a catalyst composition with an olefin monomer and optionally an olefin comonomer in a
25 polymerization reactor system under polymerization conditions to produce an olefin polymer, wherein the catalyst composition comprises catalyst component I, catalyst component II (or catalyst component I, catalyst component II, catalyst component III), an activator, and an optional co-catalyst, and wherein the polymerization process is conducted in the presence of added hydrogen (hydrogen is added to the polymerization
30 reactor system). For example, the ratio of hydrogen to the olefin monomer in the polymerization process can be controlled, often by the feed ratio of hydrogen to the olefin monomer entering the reactor. The added hydrogen to olefin monomer ratio in

the process can be controlled at a weight ratio which falls within a range from about 25 ppm to about 1500 ppm, from about 50 to about 1000 ppm, or from about 100 ppm to about 750 ppm.

In some aspects of this invention, the feed or reactant ratio of hydrogen to olefin monomer can be maintained substantially constant during the polymerization run for a particular polymer grade. That is, the hydrogen:olefin monomer ratio can be selected at a particular ratio within a range from about 5 ppm up to about 1000 ppm or so, and maintained at the ratio to within about +/- 25% during the polymerization run. For instance, if the target ratio is 100 ppm, then maintaining the hydrogen:olefin monomer ratio substantially constant would entail maintaining the feed ratio between about 75 ppm and about 125 ppm. Further, the addition of comonomer (or comonomers) can be, and generally is, substantially constant throughout the polymerization run for a particular polymer grade.

However, in other aspects, it is contemplated that monomer, comonomer (or comonomers), and/or hydrogen can be periodically pulsed to the reactor, for instance, in a manner similar to that employed in U.S. Patent No. 5,739,220 and U.S. Patent Publication No. 2004/0059070, the disclosures of which are incorporated herein by reference in their entirety.

The concentration of the reactants entering the polymerization reactor system can be controlled to produce resins with certain physical and mechanical properties. The proposed end-use product that will be formed by the polymer resin and the method of forming that product ultimately can determine the desired polymer properties and attributes. Mechanical properties include tensile, flexural, impact, creep, stress relaxation, and hardness tests. Physical properties include density, molecular weight, molecular weight distribution, melting temperature, glass transition temperature, temperature melt of crystallization, density, stereoregularity, crack growth, long chain branching, and rheological measurements.

This invention is also directed to, and encompasses, the polymers produced by any of the polymerization processes disclosed herein. Articles of manufacture can be formed from, and/or can comprise, the polymers produced in accordance with this invention.

POLYMERS AND ARTICLES

Olefin polymers encompassed herein can include any polymer produced from any olefin monomer and comonomer(s) described herein. For example, the olefin polymer can comprise an ethylene homopolymer, a propylene homopolymer, an ethylene copolymer (e.g., ethylene/ α -olefin, ethylene/1-butene, ethylene/1-hexene, ethylene/1-octene, etc.), a propylene copolymer, an ethylene terpolymer, a propylene terpolymer, and the like, including combinations thereof. In one aspect, the olefin polymer can be an ethylene/1-butene copolymer, an ethylene/1-hexene copolymer, or an ethylene/1-octene copolymer, while in another aspect, the olefin polymer can be an ethylene/1-hexene copolymer.

If the resultant polymer produced in accordance with the present invention is, for example, an ethylene polymer, its properties can be characterized by various analytical techniques known and used in the polyolefin industry. Articles of manufacture can be formed from, and/or can comprise, the ethylene polymers of this invention, whose typical properties are provided below.

An illustrative and non-limiting example of an ethylene polymer of the present invention can have a density from about 0.930 to about 0.948 g/cm³, a zero-shear viscosity greater than about 5×10^5 Pa-sec (at 190 °C), a CY-a parameter in a range from about 0.01 to about 0.40 (at 190 °C), a peak molecular weight (Mp) in a range from about 30,000 to about 130,000 g/mol, and a reverse comonomer distribution. Another illustrative and non-limiting example of an ethylene polymer of the present invention can have a density from about 0.930 to about 0.948 g/cm³, a single point notched constant tensile load (SP-NCTL) of at least 6,500 hours, and a natural draw ratio (NDR) of less than or equal to about 525 %. Yet another illustrative and non-limiting example of an ethylene polymer of the present invention can have a density from about 0.930 to about 0.948 g/cm³, and a relationship between natural draw ratio (NDR, %) and density (g/cm³) defined by the equation, $NDR < 7800(\text{density}) - 6800$, and/or by the equation, $NDR < 13404(\text{density}) - 12050$. These illustrative and non-limiting examples of ethylene polymers consistent with the present invention also can have any of the polymer properties listed below and in any combination.

Polymers of ethylene (copolymers, terpolymers, etc.) produced in accordance with some aspects of this invention generally can have a melt index (MI) from 0 to

about 10 g/10 min. Melt indices in the range from 0 to about 5 g/10 min, from 0 to about 2 g/10 min, or from 0 to about 1 g/10 min, are contemplated in other aspects of this invention. For example, a polymer of the present invention can have a melt index in a range from 0 to about 1.5, from 0 to about 0.5, from about 0.01 to about 5, from
5 about 0.01 to about 2, from about 0.05 to about 2, from about 0.05 to about 1, or from about 0.1 to about 1 g/10 min.

The densities of ethylene-based polymers produced using the catalyst systems and processes disclosed herein often are greater than or equal to about 0.930 g/cm³. In one aspect of this invention, the density of the ethylene polymer can be in a range from
10 about 0.930 to about 0.948 g/cm³. Yet, in another aspect, the density can be in a range from about 0.933 to about 0.948 g/cm³, such as, for example, from about 0.933 to about 0.946, from about 0.935 to about 0.947, from about 0.935 to about 0.946, from about 0.935 to about 0.944, or from about 0.936 to about 0.944 g/cm³.

Generally, polymers produced in aspects of the present invention have low
15 levels of long chain branching, with typically less than about 0.01 long chain branches (LCB) per 1000 total carbon atoms, but greater than zero, and similar in LCB content to polymers shown, for example, in U.S. Patent Nos. 7,517,939, 8,114,946, and 8,383,754, which are incorporated herein by reference in their entirety. In some aspects, the number of LCB per 1000 total carbon atoms can be less than about 0.008,
20 less than about 0.007, less than about 0.005, or less than about 0.003 LCB per 1000 total carbon atoms. Long chain branches (LCB) per 1000 total carbon atoms can be determined as described in U.S. Patent No. 8,114,946; "Diagnosing Long-Chain Branching in Polyethylenes," J. Mol. Struct. 485-486, 569-584 (1999); Y. Yu, D.C. Rohlffing, G.R. Hawley, and P.J. DesLauriers, *Polymer Preprint*, 44, 50, (2003); and J.
25 Phys. Chem. 1980, 84, 649; the disclosures of which are incorporated herein by reference in their entirety.

Consistent with aspects of this disclosure, ethylene polymers can have a single point notched constant tensile load (SP-NCTL) of at least 6,500 hours. Moreover, in some aspects, the ethylene polymers described herein can have a single point notched
30 constant tensile load (SP-NCTL) of at least 7,000 hours, at least 7,500 hours, at least 8,000 hours, at least 8,500 hours, at least 9,000 hours, or at least 10,000 hours, and often can range as high as 15,000 to 20,000 hours. The test is typically stopped after a

certain number of hours is reached, and given the long duration of the test, the upper limit of SP-NCTL (in hours) is generally not determined.

Often, the ethylene polymers can have a natural draw ratio (NDR) of less than or equal to about 525 %, less than or equal to about 520 %, less than or equal to about 510 %, or less than or equal to about 500 %. Representative non-limiting ranges include the following: from about 400 to about 525 %, from about 400 to about 515 %, from about 420 to about 520 %, from about 430 to about 515 %, and the like. In these and other aspects, ethylene polymers disclosed herein can have a relationship between natural draw ratio (NDR, %) and density (g/cm^3) defined by the equation, $\text{NDR} < 7800(\text{density}) - 6800$; alternatively, $\text{NDR} < 7800(\text{density}) - 6820$; alternatively, $\text{NDR} < 7800(\text{density}) - 6840$; alternatively, $\text{NDR} < 13404(\text{density}) - 12050$; alternatively, $\text{NDR} < 13404(\text{density}) - 12070$; or alternatively, $\text{NDR} < 13404(\text{density}) - 12090$.

In some aspects, the ethylene polymers of this invention can have a PSP2 value in a range from about 7.5 to about 15, or from about 8 to about 14. In other aspects, the PSP2 value can be in a range from about 8.5 to about 13, or from about 9 to about 12.5. PSP2 refers to the Primary Structure Parameter 2 as described and determined in U.S. Patent No. 8,048,679, the disclosure of which is incorporated herein by reference in its entirety.

Ethylene copolymers, for example, produced using the polymerization processes and catalyst systems described hereinabove can, in some aspects, have a reverse comonomer distribution, generally, the higher molecular weight components of the polymer have higher comonomer incorporation than the lower molecular weight components. Typically, there is increasing comonomer incorporation with increasing molecular weight. In one aspect, the number of short chain branches (SCB) per 1000 total carbon atoms of the polymer can be greater at Mw than at Mn. In another aspect, the number of SCB per 1000 total carbon atoms of the polymer can be greater at Mz than at Mw. In yet another aspect, the number of SCB per 1000 total carbon atoms of the polymer can be greater at Mz than at Mn. In still another aspect, the number of SCB per 1000 total carbon atoms of the polymer at a molecular weight of 10^6 can be greater than at a molecular weight of 10^5 .

Ethylene polymers, such as homopolymers, copolymers, etc., consistent with various aspects of the present invention generally can have a peak molecular weight

(Mp), for instance, in a range from about 30,000 to about 130,000, from about 35,000 to about 120,000, from about 35,000 to about 100,000, from about 40,000 to about 110,000, from about 40,000 to about 95,000, from about 50,000 to about 120,000, from about 50,000 to about 100,000, from about 30,000 to about 90,000, or from about 40,000 to about 80,000 g/mol.

In an aspect, ethylene polymers described herein can have a high load melt index (HLMI) in a range from about 1 to about 20, from about 2 to about 20, from about 4 to about 15, or from about 5 to about 18 g/10 min. In another aspect, ethylene polymers described herein can have a HLMI in a range from 0 to about 50, from 0 to about 40, from about 0.1 to about 45, or from about 5 to about 40 g/10 min.

In an aspect, ethylene polymers described herein can have a ratio of Mw/Mn, or the polydispersity index, in a range from about 5 to about 25, from about 7 to about 22, from about 7 to about 20, from about 8 to about 20, from about 8 to about 18, or from about 9 to about 18. In another aspect, ethylene polymers described herein can have a Mw/Mn in a range from about 10 to about 50, from about 11 to about 48, from about 10 to about 45, or from about 12 to about 30.

In an aspect, ethylene polymers described herein can have a ratio of Mz/Mw in a range from about 4.5 to about 7.5, from about 4.5 to about 6.5, from about 4.8 to about 7, from about 4.8 to about 6.2, from about 5 to about 6.5, or from about 5 to about 6. In another aspect, ethylene polymers described herein can have a Mz/Mw in a range from about 2.4 to about 8, from about 2.4 to about 7, from about 2.5 to about 7.5, or from about 2.5 to about 6.

In an aspect, ethylene polymers described herein can have a weight-average molecular weight (Mw) in a range from about 200,000 to about 500,000, from about 200,000 to about 425,000, from about 210,000 to about 475,000, from about 210,000 to about 400,000, from about 225,000 to about 450,000, or from about 225,000 to about 375,000 g/mol. In another aspect, ethylene polymers described herein can have a Mw in a range from about 150,000 to about 600,000, from about 150,000 to about 550,000, or from about 175,000 to about 375,000 g/mol.

In an aspect, ethylene polymers described herein can have a number-average molecular weight (Mn) in a range from about 8,000 to about 60,000, from about 8,000 to about 35,000, from about 15,000 to about 55,000, from about 15,000 to about

30,000, from about 18,000 to about 50,000, or from about 18,000 to about 28,000 g/mol. In another aspect, ethylene polymers described herein can have a Mn in a range from about 5,000 to about 30,000, from about 5,000 to about 25,000, from about 5,000 to about 17,000, from about 5,000 to about 15,000, or from about 6,000 to about 12,000 g/mol.

In an aspect, ethylene polymers described herein can have a z-average molecular weight (Mz) in a range from about 1,000,000 to about 5,000,000, from about 1,000,000 to about 3,000,000, from about 1,100,000 to about 4,000,000, from about 1,100,000 to about 2,500,000, from about 1,200,000 to about 3,000,000, or from about 1,200,000 to about 2,000,000 g/mol. In another aspect, ethylene polymers described herein can have a Mz in a range from about 450,000 to about 4,000,000, from about 450,000 to about 3,000,000, from about 520,000 to about 2,500,000, or from about 500,000 to about 800,000 g/mol.

In an aspect, ethylene polymers described herein can have a CY-a parameter at 190 °C in a range from about 0.01 to about 0.40, from about 0.03 to about 0.30, from about 0.05 to about 0.25, from about 0.08 to about 0.35, or from about 0.08 to about 0.28. In another aspect, ethylene polymers described herein can have a CY-a parameter in a range from about 0.40 to about 0.60, from about 0.45 to about 0.58, or from about 0.50 to about 0.56.

In an aspect, ethylene polymers described herein can have a zero-shear viscosity at 190 °C of greater than or equal to about 5×10^5 , greater than or equal to about 7.5×10^5 , greater than or equal to about 1×10^6 , in a range from about 5×10^5 to about 1×10^{12} , in a range from about 1×10^6 to about 1×10^9 , or in a range from about 1×10^6 to about 5×10^8 Pa-sec. In another aspect, ethylene polymers described herein can have a zero-shear viscosity in a range from about 1×10^4 to about 1×10^9 , from about 1×10^4 to about 1×10^8 , or from about 1×10^4 to about 5×10^6 Pa-sec.

Ethylene polymers consistent with certain aspects of the invention often can have a bimodal molecular weight distribution (as determined using gel permeation chromatography (GPC) or other recognized analytical technique). Often, in a bimodal molecular weight distribution, there is a valley between the peaks, and the peaks can be separated or deconvoluted. Typically, a bimodal molecular weight distribution can be

characterized as having an identifiable high molecular weight component (or distribution) and an identifiable low molecular weight component (or distribution).

Polymers of ethylene, whether homopolymers, copolymers, and so forth, can be formed into various articles of manufacture. Articles which can comprise polymers of this invention include, but are not limited to, an agricultural film, an automobile part, a bottle, a drum, a fiber or fabric, a food packaging film or container, a food service article, a fuel tank, a geomembrane, a household container, a liner, a molded product, a medical device or material, a pipe, a sheet or tape, a toy, and the like. Various processes can be employed to form these articles. Non-limiting examples of these processes include injection molding, blow molding, rotational molding, film extrusion, sheet extrusion, profile extrusion, thermoforming, and the like. Additionally, additives and modifiers are often added to these polymers in order to provide beneficial polymer processing or end-use product attributes. Such processes and materials are described in *Modern Plastics Encyclopedia*, Mid-November 1995 Issue, Vol. 72, No. 12; and *Film Extrusion Manual – Process, Materials, Properties*, TAPPI Press, 1992; the disclosures of which are incorporated herein by reference in their entirety.

Applicants also contemplate a method for forming or preparing an article of manufacture comprising a polymer produced by any of the polymerization processes disclosed herein. For instance, a method can comprise (i) contacting a catalyst composition with an olefin monomer and an optional olefin comonomer under polymerization conditions in a polymerization reactor system to produce an olefin polymer, wherein the catalyst composition can comprise catalyst component I, catalyst component II, optional catalyst component III, an activator (e.g., an activator-support comprising a solid oxide treated with an electron-withdrawing anion), and an optional co-catalyst (e.g., an organoaluminum compound); and (ii) forming an article of manufacture comprising the olefin polymer. The forming step can comprise blending, melt processing, extruding, molding, or thermoforming, and the like, including combinations thereof.

EXAMPLES

The invention is further illustrated by the following examples, which are not to be construed in any way as imposing limitations to the scope of this invention. Various other aspects, embodiments, modifications, and equivalents thereof which, after reading

the description herein, may suggest themselves to one of ordinary skill in the art without departing from the spirit of the present invention or the scope of the appended claims.

Melt index (MI, g/10 min) was determined in accordance with ASTM D1238 at
5 190 °C with a 2,160 gram weight, and high load melt index (HLMI, g/10 min) was determined in accordance with ASTM D1238 at 190 °C with a 21,600 gram weight. Polymer density was determined in grams per cubic centimeter (g/cm³) on a compression molded sample, cooled at about 15 °C per hour, and conditioned for about 40 hours at room temperature in accordance with ASTM D1505 and ASTM D1928,
10 procedure C. Natural Draw Ratio (NDR, %) was determined in accordance with ASTM D638 (see also U.S. Patent No. 7,589,162, which is incorporated herein by reference in its entirety). Notched tensiles (Single point notched constant tensile load, SP-NCTL, hours), a measure of polymer stress crack resistance, were determined in accordance with ASTM D5397 at 30% yield.

15 Molecular weights and molecular weight distributions were obtained using a PL-GPC 220 (Polymer Labs, an Agilent Company) system equipped with a IR4 detector (Polymer Char, Spain) and three Styragel HMW-6E GPC columns (Waters, MA) running at 145 °C. The flow rate of the mobile phase 1,2,4-trichlorobenzene (TCB) containing 0.5 g/L 2,6-di-t-butyl-4-methylphenol (BHT) was set at 1 mL/min,
20 and polymer solution concentrations were in the range of 1.0-1.5 mg/mL, depending on the molecular weight. Sample preparation was conducted at 150 °C for nominally 4 hr with occasional and gentle agitation, before the solutions were transferred to sample vials for injection. The integral calibration method was used to deduce molecular weights and molecular weight distributions using a Chevron Phillips Chemicals
25 Company's HDPE polyethylene resin, MARLEX[®] BHB5003, as the broad standard. The integral table of the broad standard was pre-determined in a separate experiment with SEC-MALS. Mn is the number-average molecular weight, Mw is the weight-average molecular weight, Mz is the z-average molecular weight, Mv is the viscosity-average molecular weight, and Mp is the peak molecular weight.

30 Melt rheological characterizations were performed as follows. Small-strain (10%) oscillatory shear measurements were performed on a Rheometrics Scientific, Inc. ARES rheometer using parallel-plate geometry. All rheological tests were

performed at 190 °C. The complex viscosity $|\eta^*|$ versus frequency (ω) data were then curve fitted using the modified three parameter Carreau-Yasuda (CY) empirical model to obtain the zero shear viscosity – η_0 , characteristic viscous relaxation time – τ_η , and the breadth parameter – a . The simplified Carreau-Yasuda (CY) empirical model is as follows:

$$|\eta^*(\omega)| = \frac{\eta_0}{[1 + (\tau_\eta \omega)^a]^{(1-n)/a}},$$

wherein: $|\eta^*(\omega)|$ = magnitude of complex shear viscosity;
 η_0 = zero shear viscosity;
 τ_η = viscous relaxation time;
 a = “breadth” parameter (CY-a parameter);
 n = fixes the final power law slope, fixed at 2/11; and
 ω = angular frequency of oscillatory shearing deformation.

Details of the significance and interpretation of the CY model and derived parameters may be found in: C. A. Hieber and H. H. Chiang, *Rheol. Acta*, 28, 321 (1989); C.A. Hieber and H.H. Chiang, *Polym. Eng. Sci.*, 32, 931 (1992); and R. B. Bird, R. C. Armstrong and O. Hassager, *Dynamics of Polymeric Liquids, Volume 1, Fluid Mechanics*, 2nd Edition, John Wiley & Sons (1987); each of which is incorporated herein by reference in its entirety.

Short chain branch content and short chain branching distribution (SCBD) across the molecular weight distribution were determined via an IR5-detected GPC system (IR5-GPC), wherein the GPC system was a PL220 GPC/SEC system (Polymer Labs, an Agilent company) equipped with three Styragel HMW-6E columns (Waters, MA) for polymer separation. A thermoelectric-cooled IR5 MCT detector (IR5) (Polymer Char, Spain) was connected to the GPC columns via a hot-transfer line. Chromatographic data were obtained from two output ports of the IR5 detector. First, the analog signal goes from the analog output port to a digitizer before connecting to Computer “A” for molecular weight determinations via the Cirrus software (Polymer Labs, now an Agilent Company) and the integral calibration method using a broad MWD HDPE Marlex™ BHB5003 resin (Chevron Phillips Chemical) as the broad molecular weight standard. The digital signals, on the other hand, go via a USB cable

directly to Computer “B” where they are collected by a LabView data collection software provided by Polymer Char. Chromatographic conditions were set as follows: column oven temperature of 145 °C; flowrate of 1 mL/min; injection volume of 0.4 mL; and polymer concentration of about 2 mg/mL, depending on sample molecular weight. The temperatures for both the hot-transfer line and IR5 detector sample cell were set at 150 °C, while the temperature of the electronics of the IR5 detector was set at 60 °C. Short chain branching content was determined via an in-house method using the intensity ratio of CH₃ (I_{CH3}) to CH₂ (I_{CH2}) coupled with a calibration curve. The calibration curve was a plot of SCB content (x_{SCB}) as a function of the intensity ratio of I_{CH3}/I_{CH2}. To obtain a calibration curve, a group of polyethylene resins (no less than 5) of SCB level ranging from zero to ca. 32 SCB/1,000 total carbons (SCB Standards) were used. All these SCB Standards have known SCB levels and flat SCBD profiles pre-determined separately by NMR and the solvent-gradient fractionation coupled with NMR (SGF-NMR) methods. Using SCB calibration curves thus established, profiles of short chain branching distribution across the molecular weight distribution were obtained for resins fractionated by the IR5-GPC system under exactly the same chromatographic conditions as for these SCB standards. A relationship between the intensity ratio and the elution volume was converted into SCB distribution as a function of MWD using a predetermined SCB calibration curve (i.e., intensity ratio of I_{CH3}/I_{CH2} vs. SCB content) and MW calibration curve (i.e., molecular weight vs. elution time) to convert the intensity ratio of I_{CH3}/I_{CH2} and the elution time into SCB content and the molecular weight, respectively.

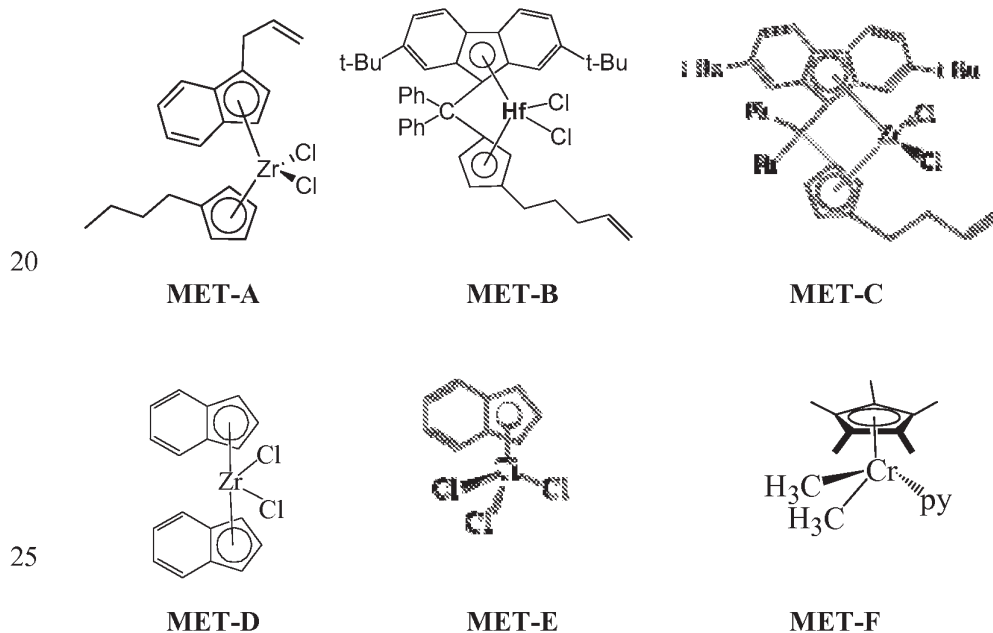
Fluorided silica-coated alumina activator-supports used in Examples 7-12 were prepared as follows. Bohemite was obtained from W.R. Grace & Company under the designation “Alumina A” and having a surface area of about 300 m²/g, a pore volume of about 1.3 mL/g, and an average particle size of about 100 microns. The alumina was first calcined in dry air at about 600 °C for approximately 6 hours, cooled to ambient temperature, and then contacted with tetraethylorthosilicate in isopropanol to equal 25 wt. % SiO₂. After drying, the silica-coated alumina was calcined at 600 °C for 3 hours. Fluorided silica-coated alumina (7 wt. % F) was prepared by impregnating the calcined silica-coated alumina with an ammonium bifluoride solution in methanol, drying, and then calcining for 3 hours at 600 °C in dry air. Afterward, the fluorided silica-coated

alumina was collected and stored under dry nitrogen, and was used without exposure to the atmosphere.

Sulfated alumina activator-supports used in Examples 13-25 were prepared as follows. Bohemite was obtained from W.R. Grace & Company under the designation
5 “Alumina A” and having a surface area of about 300 m²/g and a pore volume of about 1.3 mL/g. This material was obtained as a powder having an average particle size of about 100 microns. This material was impregnated to incipient wetness with an aqueous solution of ammonium sulfate to equal about 15% sulfate. This mixture was then placed in a flat pan and allowed to dry under vacuum at approximately 110 °C for
10 about 16 hours. To calcine the resultant powdered mixture, the material was fluidized in a stream of dry air at about 550 °C for about 6 hours. Afterward, the sulfated alumina was collected and stored under dry nitrogen, and was used without exposure to the atmosphere.

EXAMPLES 1-25

15 Examples 1-6 utilized a commercially-available, nominal 0.937 density, ethylene/1-hexene copolymer (Chevron Phillips Chemical Company LP) produced using a chromium-based catalyst system. The following metallocene compounds were used in Examples 7-25 (Ph = phenyl, t-Bu = tert-butyl; py = pyridine):



The polymerization experiments of Examples 7-12 were conducted in a one-gallon stainless steel reactor. Isobutane (1.8-2.0 L) was used in all runs. Metallocene solutions were prepared at about 1 mg/mL in toluene. Approximately 0.6 mmol of alkyl aluminum (triisobutylaluminum, TIBA), 300 mg of fluorided silica-coated alumina, and the metallocene solutions were added in that order through a charge port while slowly venting isobutane vapor. The charge port was closed and isobutane was added. The contents of the reactor were stirred and heated to the desired run temperature of about 90 °C, and ethylene was then introduced into the reactor with 1-hexene and hydrogen at a specific ppm by weight of the ethylene. Ethylene and hydrogen were fed on demand at the specified weight ratio to maintain the target pressure of 390 psig pressure for the 30-60 minute length of the polymerization run (target was a nominal 400 g of polymer produced). The reactor was maintained at the desired run temperature throughout the run by an automated heating-cooling system. **Table I** summarizes certain information relating to the polymerization experiments of Examples 7-12.

Table I. Examples 7-12.

Example	MET-A (mg)	MET-B (mg)	1-hexene (g)	H ₂ (ppm)	PE produced (g)
7	1	1.5	10	150	403
8	1	1.5	15	150	416
9	0.9	1.5	15	150	399
10	0.9	1.5	20	150	412
11	0.8	1.5	15	175	337
12	1	1.7	30	150	406

Example 13 used the same general procedure as in Examples 7-12, except that sulfated alumina was used, a 25 wt. % solution of TIBA was used, and the hydrogen addition was measured as the pressure drop (ΔP) from an auxiliary vessel with a 700 psig starting pressure. For Example 13, 0.5 mL of TIBA, 0.15 g of sulfated alumina, 1 mL of MET-D solution, 0.4 mL of MET-C solution, and 42 g of 1-hexene were used. The reaction temperature was 78 °C, the reactor pressure was 345 psig, the reaction time was 30 min, and ΔP was 94 psig; 332 g of polymer were produced. Examples 14-

21 were conducted similarly to that of Example 13, with the differences noted as follows:

For Example 14, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 1 mL of MET-A solution, 0.25 mL of MET-C solution, and 42 g of 1-hexene were used. The reaction
5 temperature was 78 °C, the reactor pressure was 345 psig, the reaction time was 30 min, and ΔP was 63 psig; 273 g of polymer were produced.

For Example 15, 0.5 mL of TIBA, 0.15 g of sulfated alumina, 1 mL of MET-D solution, 0.4 mL of MET-C solution, and 42 g of 1-hexene were used. The reaction
10 temperature was 78 °C, the reactor pressure was 345 psig, the reaction time was 30 min, and ΔP was 63 psig; 309 g of polymer were produced.

For Example 16, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 1 mL of MET-A solution, 0.3 mL of MET-C solution, and 30 g of 1-hexene were used. The reaction
temperature was 78 °C, the reactor pressure was 345 psig, the reaction time was 30 min, and ΔP was 40 psig; 264 g of polymer were produced.

15 For Example 17, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 0.1 mL of MET-A solution, 1 mL of MET-C solution, 0.2 mL of MET-E solution, and 10 g of 1-hexene were used. The reaction temperature was 85 °C, the reactor pressure was 374 psig, the reaction time was 30 min, and ΔP was 63 psig; 346 g of polymer were produced.

For Example 18, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 0.2 mL of MET-A
20 solution, 1 mL of MET-C solution, 0.5 mL of MET-E solution, and 15 g of 1-hexene were used. The reaction temperature was 85 °C, the reactor pressure was 374 psig, the reaction time was 30 min, and ΔP was 63 psig; 376 g of polymer were produced.

For Example 19, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 0.2 mL of MET-A solution, 1 mL of MET-C solution, 1 mL of MET-E solution, and 20 g of 1-hexene
25 were used. The reaction temperature was 85 °C, the reactor pressure was 374 psig, the reaction time was 30 min, and ΔP was 63 psig; 328 g of polymer were produced.

For Example 20, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 0.5 mL of MET-A solution, 1 mL of MET-C solution, 0.2 mL of MET-F solution, and 10 g of 1-hexene
30 were used. The reaction temperature was 85 °C, the reactor pressure was 374 psig, the reaction time was 30 min, and ΔP was 24 psig; 229 g of polymer were produced.

For Example 21, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 0.5 mL of MET-A solution, 0.5 mL of MET-C solution, 0.5 mL of MET-F solution, and 40 g of 1-hexene

were used. The reaction temperature was 80 °C, the reactor pressure was 374 psig, the reaction time was 30 min, and ΔP was 95 psig; 249 g of polymer were produced.

For Example 22, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 0.4 mL of MET-C solution, 1 mL of MET-D solution, and 42 g of 1-hexene were used. The reaction
5 temperature was 78 °C, the reactor pressure was 345 psig, the reaction time was 30 min, and ΔP was 63 psig; 309 g of polymer were produced.

For Example 23, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 1 mL of MET-A solution, 0.2 mL of MET-C solution, 0.1 mL of MET-E solution, and 45 g of 1-hexene were used. The reaction temperature was 85 °C, the reactor pressure was 374 psig, the
10 reaction time was 30 min, and ΔP was 42 psig; 188 g of polymer were produced.

For Example 24, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 1 mL of MET-C solution, 0.2 mL of MET-E solution, and 20 g of 1-hexene were used. The reaction temperature was 85 °C, the reactor pressure was 374 psig, the reaction time was 30 min, and ΔP was 63 psig; 442 g of polymer were produced.

15 For Example 25, 0.5 mL of TIBA, 0.2 g of sulfated alumina, 0.2 mL of MET-C solution, 1 mL of MET-D solution, 0.3 mL of MET-E solution, and 45 g of 1-hexene were used. The reaction temperature was 85 °C, the reactor pressure was 374 psig, the reaction time was 30 min, and ΔP was 42 psig; 163 g of polymer were produced.

Table II summarizes certain polymer properties of Examples 1-25, while **FIGS.**
20 **1-3** illustrate the short chain branch distributions (comonomer distributions) of certain polymers, **FIGS. 4-8** illustrate the dynamic rheology properties at 190 °C for certain polymers, **FIGS. 9-13** illustrate the molecular weight distributions (amount of polymer versus the logarithm of molecular weight) of certain polymers, and **FIGS. 14-15** illustrate the natural draw ratio versus the density for certain polymers.

25 As shown in **FIGS. 2-3**, polymers produced using certain metallocene-based catalyst systems disclosed herein had a reverse comonomer distribution (e.g., relatively more short chain branches (SCB) at the higher molecular weights; assumes 2 methyl chain ends (CE)), as contrasted with the standard comonomer distribution resulting from a chromium-based catalyst system (see **FIG. 1**). For instance, in **FIGS. 2-3**, the
30 number of SCB per 1000 total carbon (TC) atoms of the polymer at M_z (or M_w) is greater than at M_n , while such is not the case in **FIG. 1**.

The rheology characteristics in **Table II** (e.g., zero-shear viscosity, CY-a parameter) and the viscosity curves of **FIGS. 4-8** illustrate a range of improved processability of polymers produced using certain metallocene-based catalyst systems disclosed herein, as compared to those produced from a chromium-based catalyst system. For instance, by comparing the shape of the viscosity curve and the zero-shear viscosity values, metallocene-based polymers, surprisingly, were produced which would likely have equivalent or superior melt strength to those of the chromium-based polymers; see e.g., **FIGS. 4-6** and Examples 1 and 7-12. Polymers with improved extrusion processability also were produced; see e.g., **FIGS. 7-8**.

10 Metallocene-based polymers were produced having similar or broader molecular weight distributions to chromium-based polymers, and a wide range of Mn, Mw, Mp, and Mz parameters; see e.g., **FIGS. 9-13** and Examples 1 and 7-25.

15 The NDR data in **Table II** and **FIGS. 14-15** demonstrate superior NDR performance for the metallocene-based polymers, as compared to the chromium-based polymers: e.g., lower NDR values at an equivalent density, the same or lower NDR values at a higher density, etc. Lower NDR values typically correlate with improved stress crack resistance of the polymer.

20 Also unexpectedly, the metallocene-based polymers provided significantly improved stress crack resistance, as measured by the notched tensiles. Examples 1-6 failed the notched tensiles test at an average of 3,025 hours (and with an average 0.9377 density), while Examples 8-11 did not fail the notched tensile test at over 10,000 hours (in excess of 1 year of testing). Moreover, Examples 8-11 had a significantly higher average density of 0.9435 g/cc. Accordingly, polymers were produced that had a unique combination of chromium-like processability and melt strength, improved stress crack resistance (e.g., higher notched tensiles, lower NDR), and a higher density.

Table II. Polymer Properties of Examples 1-25.

Example	HLMl (g/10 min)	Density (g/cc)	NDR (%)	Mn (kg/mol)	Mw (kg/mol)	Mz (kg/mol)	Mv (kg/mol)	Mp (kg/mol)	Mw/Mn
1	12	0.937	525	16.5	197	1177	149	73	11.9
2	16	0.938							
3	17	0.938							
4	13	0.937	537						
5	14	0.938	533						
6	13	0.938	532						
7	12	0.9479	546	18.8	252	1384	181	50	13.4
8	15	0.9446	506	22.2	247	1334	177	47	11.1
9	12	0.9445	520	22.2	256	1373	185	49	11.5
10	14	0.9419	473	19.0	246	1318	177	43	12.9
11	7	0.9431	462	19.9	351	1828	250	47	17.7
12	11	0.9375	468	25.0	258	1533	187	62	10.3
13	42	0.9423	432	5.9	181	682	132	8	30.4
14	39	0.9422	425	10.3	191	808	140	19	18.6
15	32	0.9413	407	7.8	209	807	154	433	27.0
16	7	0.9386	401	8.3	235	748	184	384	28.2
17	21	0.9426	540	14.3	172	672	137	78	12.0
18	13	0.9367	453	13.6	195	703	158	89	14.4
19	17	0.9379	477	12.0	150	478	124	82	12.5
20	0.4	0.9397	406	11.2	541	2356	415	482	48.3
21	11	0.9420	510	8.0	358	2401	246	77	44.5
22	26	0.9400	503	9.2	198	798	147	16	21.7
23	2.6			7.8	206	546	170	271	26.3
24	4.4			9.1	221	571	185	261	24.3
25	2.5			8.6	198	522	164	264	23.1

Table II. Polymer Properties of Examples 1-25 (continued).

Example	SP-NCTL (hr)	η_0 (Pa-sec)	CY-a	τ_η (sec)	PSP2
1	6295	4.4E+06	0.15	1.9E+01	
2	1841				
3	3438				
4	2144				
5	1691				
6	2746				
7	3012	2.3E+07	0.12	9.9E+01	8.8
8	>10987	2.2E+07	0.13	2.3E+02	
9	>10987	7.4E+06	0.14	5.2E+01	8.8
10	>10987	3.2E+06	0.17	3.3E+01	10.1
11	>10987	2.6E+06	0.27	3.9E+01	
12	>8613	1.5E+08	0.09	2.2E+02	
13		7.4E+04			
14		7.2E+04			
15	>9547	1.1E+05	0.55	1.2E+00	12.4
16		1.2E+05			
17		4.3E+04			
18		4.1E+04	0.34	1.1E-01	
19		2.7E+04	0.35	6.3E-01	
20		5.7E+05	0.48	1.8E+00	
21		1.1E+06	0.23	8.4E+00	
22	>9692	1.1E+05	0.51	1.1E+00	11.9
23		7.7E+04	0.53	3.2E-01	
24		7.9E+04	0.53	3.0E-01	
25		6.8E+04	0.53	2.6E-01	

The invention is described above with reference to numerous aspects and embodiments, and specific examples. Many variations will suggest themselves to those skilled in the art in light of the above detailed description. All such obvious variations are within the full intended scope of the appended claims. Other embodiments of the invention can include, but are not limited to, the following (embodiments are described as “comprising” but, alternatively, can “consist essentially of” or “consist of”):

Embodiment 1. An ethylene polymer having a density from about 0.930 to about 0.948 g/cm³, a zero-shear viscosity greater than about 5×10^5 Pa-sec, a CY-a parameter in a range from about 0.01 to about 0.40, a peak molecular weight (Mp) in a range from about 30,000 to about 130,000 g/mol, and a reverse comonomer distribution.

Embodiment 2. An ethylene polymer having a density from about 0.930 to about 0.948 g/cm³, a single point notched constant tensile load (SP-NCTL) of at least 6,500 hours, and a natural draw ratio (NDR) of less than or equal to about 525 %.

Embodiment 3. An ethylene polymer having a density from about 0.930 to about 0.948 g/cm³, and a relationship between natural draw ratio (NDR, %) and density (g/cm³) defined by one or more of the following equations: $\text{NDR} < 7800(\text{density}) - 6800$, $\text{NDR} < 7800(\text{density}) - 6820$, $\text{NDR} < 7800(\text{density}) - 6840$, $\text{NDR} < 13404(\text{density}) - 12050$, $\text{NDR} < 13404(\text{density}) - 12070$, and/or $\text{NDR} < 13404(\text{density}) - 12090$.

Embodiment 4. The polymer defined in any one of embodiments 1-3, wherein the ethylene polymer has a melt index in any range disclosed herein, e.g., from 0 to about 2, from 0 to about 1, from 0 to about 0.5 g/10 min, etc.

Embodiment 5. The polymer defined in any one of embodiments 1-4, wherein the ethylene polymer has a density in any range disclosed herein, e.g., from about 0.933 to about 0.948, from about 0.933 to about 0.946, from about 0.935 to about 0.947, from about 0.935 to about 0.944, from about 0.936 to about 0.944 g/cm³, etc.

Embodiment 6. The polymer defined in any one of embodiments 1-5, wherein the ethylene polymer has less than about 0.008 long chain branches (LCB) per 1000 total carbon atoms, e.g., less than about 0.005 LCB, less than about 0.003 LCB, etc.

Embodiment 7. The polymer defined in any one of embodiments 1-6, wherein the ethylene polymer has a single point notched constant tensile load (SP-NCTL) in any

range disclosed herein, e.g., at least 7,000 hours, at least 7,500 hours, at least 8,000 hours, at least 8,500 hours, at least 9,000 hours, at least 10,000 hours, etc.

Embodiment 8. The polymer defined in any one of embodiments 1-7, wherein the ethylene polymer has a natural draw ratio (NDR) in any range disclosed herein, e.g., less than or equal to about 520 %, less than or equal to about 510 %, in a range from about 400 to about 525 %, in a range from about 420 to about 520 %, in a range from about 430 to about 515 %, etc.

Embodiment 9. The polymer defined in any one of embodiments 1-8, wherein the ethylene polymer has a PSP2 in any range disclosed herein, e.g., from about 7.5 to about 15, from about 8 to about 14, from about 8.5 to about 13, from about 9 to about 12.5, etc.

Embodiment 10. The polymer defined in any one of embodiments 1-9, wherein the ethylene polymer has a reverse comonomer distribution, e.g., the number of short chain branches (SCB) per 1000 total carbon atoms of the polymer at Mw is greater than at Mn, the number of short chain branches (SCB) per 1000 total carbon atoms of the polymer at Mz is greater than at Mw, the number of SCB per 1000 total carbon atoms of the polymer at Mz is greater than at Mn, the number of short chain branches (SCB) per 1000 total carbon atoms of the polymer at a molecular weight of 10^6 is greater than at a molecular weight of 10^5 , etc.

Embodiment 11. The polymer defined in any one of embodiments 1-10, wherein the ethylene polymer has a Mp in any range disclosed herein, e.g., from about 30,000 to about 130,000, from about 35,000 to about 120,000, from about 40,000 to about 110,000, from about 40,000 to about 80,000 g/mol, etc.

Embodiment 12. The polymer defined in any one of embodiments 1-11, wherein the ethylene polymer has a HLMI in any range disclosed herein, e.g., from about 1 to about 20, from about 2 to about 20, from about 5 to about 18 g/10 min, etc.

Embodiment 13. The polymer defined in any one of embodiments 1-12, wherein the ethylene polymer has a ratio of Mw/Mn in any range disclosed herein, e.g., from about 5 to about 25, from about 7 to about 20, from about 8 to about 18, etc.

Embodiment 14. The polymer defined in any one of embodiments 1-13, wherein the ethylene polymer has a ratio of Mz/Mw in any range disclosed herein, e.g., from about 4.5 to about 7.5, from about 4.8 to about 7, from about 5 to about 6, etc.

Embodiment 15. The polymer defined in any one of embodiments 1-14, wherein the ethylene polymer has a Mw in any range disclosed herein, e.g., from about 200,000 to about 500,000, from about 225,000 to about 450,000, from about 225,000 to about 375,000 g/mol, etc.

Embodiment 16. The polymer defined in any one of embodiments 1-15, wherein the ethylene polymer has a Mn in any range disclosed herein, e.g., from about 8,000 to about 60,000, from about 15,000 to about 30,000, from about 18,000 to about 50,000 g/mol, etc.

Embodiment 17. The polymer defined in any one of embodiments 1-16, wherein the ethylene polymer has a Mz in any range disclosed herein, e.g., from about 1,000,000 to about 5,000,000, from about 1,000,000 to about 3,000,000, from about 1,200,000 to about 2,000,000 g/mol, etc.

Embodiment 18. The polymer defined in any one of embodiments 1-17, wherein the ethylene polymer has a CY-a parameter in any range disclosed herein, e.g., from about 0.01 to about 0.40, from about 0.03 to about 0.30, from about 0.08 to about 0.35, etc.

Embodiment 19. The polymer defined in any one of embodiments 1-18, wherein the ethylene polymer has a zero-shear viscosity in any range disclosed herein, e.g., greater than about 5×10^5 , greater than about 7.5×10^5 , greater than about 1×10^6 , in a range from about 1×10^6 to about 1×10^9 Pa-sec, etc.

Embodiment 20. The polymer defined in any one of embodiments 1-11, wherein the ethylene polymer has a HLMI in any range disclosed herein, e.g., from 0 to about 50, from about 0.1 to about 45, from about 5 to about 40 g/10 min, etc.

Embodiment 21. The polymer defined in any one of embodiments 1-11 and 20, wherein the ethylene polymer has a ratio of Mw/Mn in any range disclosed herein, e.g., from about 10 to about 50, from about 11 to about 48, from about 12 to about 30, etc.

Embodiment 22. The polymer defined in any one of embodiments 1-11 and 20-21, wherein the ethylene polymer has a ratio of Mz/Mw in any range disclosed herein, e.g., from about 2.4 to about 8, from about 2.4 to about 7, from about 2.5 to about 6, etc.

Embodiment 23. The polymer defined in any one of embodiments 1-11 and 20-22, wherein the ethylene polymer has a Mw in any range disclosed herein, e.g., from

about 150,000 to about 600,000, from about 150,000 to about 550,000, from about 175,000 to about 375,000 g/mol, etc.

Embodiment 24. The polymer defined in any one of embodiments 1-11 and 20-23, wherein the ethylene polymer has a M_n in any range disclosed herein, e.g., from about 5,000 to about 17,000, from about 5,000 to about 15,000, from about 6,000 to about 12,000 g/mol, etc.

Embodiment 25. The polymer defined in any one of embodiments 1-11 and 20-24, wherein the ethylene polymer has a M_z in any range disclosed herein, e.g., from about 450,000 to about 3,000,000, from about 520,000 to about 2,500,000, from about 500,000 to about 800,000 g/mol, etc.

Embodiment 26. The polymer defined in any one of embodiments 2-11 and 20-25, wherein the ethylene polymer has a CY-a parameter in any range disclosed herein, e.g., from about 0.40 to about 0.60, from about 0.45 to about 0.58, from about 0.50 to about 0.56, etc.

Embodiment 27. The polymer defined in any one of embodiments 2-11 and 20-26, wherein the ethylene polymer has a zero-shear viscosity in any range disclosed herein, e.g., from about 1×10^4 to about 1×10^9 , from about 1×10^4 to about 1×10^8 , from about 1×10^4 to about 5×10^6 Pa-sec, etc.

Embodiment 28. The polymer defined in any one of embodiments 1-27, wherein the ethylene polymer is an ethylene/ α -olefin copolymer.

Embodiment 29. The polymer defined in any one of embodiments 1-28, wherein the ethylene polymer is an ethylene/1-butene copolymer, an ethylene/1-hexene copolymer, or an ethylene/1-octene copolymer.

Embodiment 30. The polymer defined in any one of embodiments 1-29, wherein the ethylene polymer is an ethylene/1-hexene copolymer.

Embodiment 31. An article comprising the ethylene polymer defined in any one of embodiments 1-30.

Embodiment 32. An article comprising the ethylene polymer defined in any one of embodiments 1-30, wherein the article is an agricultural film, an automobile part, a bottle, a drum, a fiber or fabric, a food packaging film or container, a food service article, a fuel tank, a geomembrane, a household container, a liner, a molded product, a medical device or material, a pipe, a sheet or tape, or a toy.

Embodiment 33. A catalyst composition comprising: catalyst component I comprising any unbridged metallocene compound disclosed herein, catalyst component II comprising any bridged metallocene compound disclosed herein, any activator disclosed herein, and optionally, any co-catalyst disclosed herein.

Embodiment 34. The composition defined in embodiment 33, wherein catalyst component II comprises a bridged zirconium or hafnium based metallocene compound.

Embodiment 35. The composition defined in embodiment 33, wherein catalyst component II comprises a bridged zirconium or hafnium based metallocene compound with an alkenyl substituent.

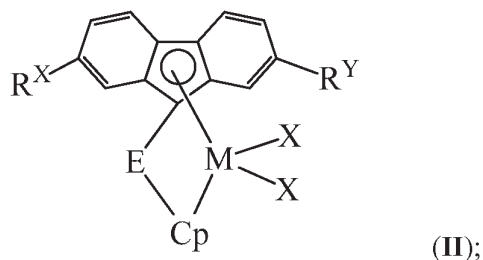
Embodiment 36. The composition defined in embodiment 33, wherein catalyst component II comprises a bridged zirconium or hafnium based metallocene compound with an alkenyl substituent and a fluorenyl group.

Embodiment 37. The composition defined in embodiment 33, wherein catalyst component II comprises a bridged zirconium or hafnium based metallocene compound with a cyclopentadienyl group and a fluorenyl group, and with an alkenyl substituent on the bridging group and/or on the cyclopentadienyl group.

Embodiment 38. The composition defined in embodiment 33, wherein catalyst component II comprises a bridged metallocene compound having an aryl group substituent on the bridging group.

Embodiment 39. The composition defined in embodiment 33, wherein catalyst component II comprises a dinuclear bridged metallocene compound with an alkenyl linking group.

Embodiment 40. The composition defined in embodiment 33, wherein catalyst component II comprises a bridged metallocene compound having formula (II):



wherein M is any Group IV transition metal disclosed herein, Cp is any cyclopentadienyl, indenyl, or fluorenyl group disclosed herein, each X independently is

any monoanionic ligand disclosed herein, R^X and R^Y independently are any substituent disclosed herein, and E is any bridging group disclosed herein.

Embodiment 41. The composition defined in any one of embodiments 33-40, wherein catalyst component I comprises an unbridged zirconium or hafnium based metallocene compound containing two cyclopentadienyl groups, two indenyl groups, or a cyclopentadienyl and an indenyl group.

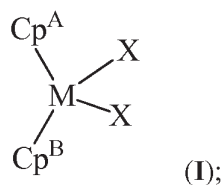
Embodiment 42. The composition defined in any one of embodiments 33-40, wherein catalyst component I comprises an unbridged zirconium or hafnium based metallocene compound containing two cyclopentadienyl groups.

Embodiment 43. The composition defined in any one of embodiments 33-40, wherein catalyst component I comprises an unbridged zirconium or hafnium based metallocene compound containing two indenyl groups.

Embodiment 44. The composition defined in any one of embodiments 33-40, wherein catalyst component I comprises an unbridged zirconium or hafnium based metallocene compound containing a cyclopentadienyl and an indenyl group.

Embodiment 45. The composition defined in any one of embodiments 33-40, wherein catalyst component I comprises a dinuclear unbridged metallocene compound with an alkenyl linking group.

Embodiment 46. The composition defined in any one of embodiments 33-40, wherein catalyst component I comprises an unbridged metallocene compound having formula (I):



wherein M is any Group IV transition metal disclosed herein, Cp^{A} and Cp^{B} independently are any cyclopentadienyl or indenyl group disclosed herein, and each X independently is any monoanionic ligand disclosed herein.

Embodiment 47. The composition defined in any one of embodiments 33-46, wherein the activator comprises an activator-support, an aluminoxane compound, an organoboron or organoborate compound, an ionizing ionic compound, or any combination thereof.

Embodiment 48. The composition defined in any one of embodiments 33-47, wherein the activator comprises an activator-support, the activator-support comprising any solid oxide treated with any electron-withdrawing anion disclosed herein.

Embodiment 49. The composition defined in any one of embodiments 33-48, wherein the activator comprises fluorided alumina, chlorided alumina, bromided alumina, sulfated alumina, fluorided silica-alumina, chlorided silica-alumina, bromided silica-alumina, sulfated silica-alumina, fluorided silica-zirconia, chlorided silica-zirconia, bromided silica-zirconia, sulfated silica-zirconia, fluorided silica-titania, fluorided silica-coated alumina, sulfated silica-coated alumina, phosphated silica-coated alumina, or any combination thereof.

Embodiment 50. The composition defined in any one of embodiments 33-48, wherein the activator comprises a fluorided solid oxide and/or a sulfated solid oxide.

Embodiment 51. The composition defined in any one of embodiments 33-47, wherein the activator comprises an aluminoxane compound.

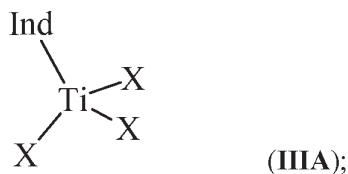
Embodiment 52. The composition defined in any one of embodiments 33-51, wherein the catalyst composition comprises a co-catalyst, e.g., any co-catalyst disclosed herein.

Embodiment 53. The composition defined in any one of embodiments 33-52, wherein the co-catalyst comprises any organoaluminum compound disclosed herein.

Embodiment 54. The composition defined in any one of embodiments 33-53, wherein a weight ratio of catalyst component I to catalyst component II in the catalyst composition is in any range disclosed herein, e.g., from about 10:1 to about 1:10, from about 5:1 to about 1:5, from about 2:1 to about 1:2, etc.

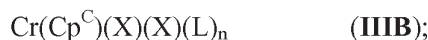
Embodiment 55. The composition defined in any one of embodiments 33-54, wherein the catalyst composition further comprises catalyst component III comprising any half-metallocene compound disclosed herein.

Embodiment 56. The composition defined in embodiment 55, wherein catalyst component III comprises a half-metallocene compound having formula (IIIA):



wherein Ind is any indenyl group disclosed herein, and each X independently is any monoanionic ligand disclosed herein.

Embodiment 57. The composition defined in embodiment 55, wherein catalyst component III comprises a half-metallocene compound having formula (IIIB):



wherein Cp^{C} is any cyclopentadienyl, indenyl, or fluorenyl group disclosed herein, each X independently is any monoanionic ligand disclosed herein, each L is any neutral ligand disclosed herein, and integer n is 0, 1 or 2.

Embodiment 58. The composition defined in any one of embodiments 55-57, wherein the weight percentage of catalyst component III is in any range disclosed herein, e.g., from about 5 to about 50%, from about 10 to about 45%, etc., based on the total weight of catalyst components I, II, and III.

Embodiment 59. An olefin polymerization process, the process comprising contacting the catalyst composition defined in any one of embodiments 33-58 with an olefin monomer and optionally an olefin comonomer in a polymerization reactor system under polymerization conditions to produce an olefin polymer.

Embodiment 60. The process defined in embodiment 59, wherein the polymerization reactor system comprises a batch reactor, a slurry reactor, a gas-phase reactor, a solution reactor, a high pressure reactor, a tubular reactor, an autoclave reactor, or a combination thereof.

Embodiment 61. The process defined in any one of embodiments 59-60, wherein the polymerization reactor system comprises a slurry reactor, a gas-phase reactor, a solution reactor, or a combination thereof.

Embodiment 62. The process defined in any one of embodiments 59-61, wherein the polymerization reactor system comprises a loop slurry reactor.

Embodiment 63. The process defined in any one of embodiments 59-62, wherein the polymerization reactor system comprises a single reactor.

Embodiment 64. The process defined in any one of embodiments 59-62, wherein the polymerization reactor system comprises 2 reactors.

Embodiment 65. The process defined in any one of embodiments 59-62, wherein the polymerization reactor system comprises more than 2 reactors.

Embodiment 66. The process defined in any one of embodiments 59-65, wherein the olefin monomer comprises any olefin monomer disclosed herein, e.g., any C_2 - C_{20} olefin.

Embodiment 67. The process defined in any one of embodiments 59-66, wherein the olefin monomer and the optional olefin comonomer independently comprise a C_2 - C_{20} alpha-olefin.

Embodiment 68. The process defined in any one of embodiments 59-67, wherein the olefin monomer comprises ethylene.

Embodiment 69. The process defined in any one of embodiments 59-68, wherein the catalyst composition is contacted with ethylene and an olefin comonomer comprising a C_3 - C_{10} alpha-olefin.

Embodiment 70. The process defined in any one of embodiments 59-69, wherein the catalyst composition is contacted with ethylene and an olefin comonomer comprising 1-butene, 1-hexene, 1-octene, or a mixture thereof.

Embodiment 71. The process defined in any one of embodiments 59-70, wherein the olefin polymer produced is defined in any one of embodiments 1-30.

Embodiment 72. An olefin polymer produced by the process defined in any one of embodiments 59-70.

Embodiment 73. An ethylene polymer defined in any one of embodiments 1-30 produced by the process defined in any one of embodiments 59-70.

Embodiment 74. An article comprising the polymer defined in embodiment 72 or 73.

Embodiment 75. A method of forming or preparing an article of manufacture comprising a polymer, the method comprising (i) performing the olefin polymerization process defined in any one of embodiments 59-70 to produce the polymer defined in any one of embodiments 1-30, and (ii) forming the article of manufacture comprising the polymer, e.g., utilizing any technique disclosed herein.

CLAIMS

1. An ethylene polymer having a density from about 0.930 to about 0.948 g/cm³, a zero-shear viscosity greater than about 5×10^5 Pa-sec, a CY-a parameter in a range from about 0.01 to about 0.40, a peak molecular weight (Mp) in a range from about 30,000 to about 130,000 g/mol, and a reverse comonomer distribution.
2. The polymer of claim 1, wherein the ethylene polymer has a density in a range from about 0.933 to about 0.946 g/cm³.
3. The polymer of claim 1, wherein the ethylene polymer has:
a natural draw ratio (NDR) in a range from about 400 to about 525 %; and
a single point notched constant tensile load (SP-NCTL) of at least 8,000 hours.
4. The polymer of claim 1, wherein the ethylene polymer has:
a HLMI in a range from about 1 to about 20 g/10 min;
a ratio of Mw/Mn in a range from about 5 to about 25;
a ratio of Mz/Mw in a range from about 4.5 to about 7.5; and
a Mn in a range from about 8,000 to about 60,000 g/mol.
5. The polymer of claim 1, wherein the ethylene polymer has:
a density in a range from about 0.935 to about 0.946 g/cm³;
a zero-shear viscosity in a range from about 7.5×10^5 to about 1×10^9 Pa-sec;
a CY-a parameter in a range from about 0.08 to about 0.35; and
a Mp in a range from about 35,000 to about 120,000 g/mol.
6. The polymer of claim 1, wherein a relationship between natural draw ratio (NDR, %) and density (g/cm³) of the ethylene polymer is defined by the equation:

$$\text{NDR} < 7800(\text{density}) - 6800.$$

7. The polymer of claim 1, wherein the ethylene polymer is an ethylene/1-butene copolymer, an ethylene/1-hexene copolymer, or an ethylene/1-octene copolymer.
8. An article comprising the ethylene polymer of claim 1.
9. An ethylene polymer having a density from about 0.930 to about 0.948 g/cm³, a single point notched constant tensile load (SP-NCTL) of at least 6,500 hours, and a natural draw ratio (NDR) of less than or equal to about 525 %.

10. The polymer of claim 9, wherein the ethylene polymer has:
a density in a range from about 0.933 to about 0.946 g/cm³;
a natural draw ratio (NDR) in a range from about 400 to about 525 %; and
a single point notched constant tensile load (SP-NCTL) of at least 9,000 hours.
11. The polymer of claim 9, wherein the ethylene polymer has:
a HLMI in a range from 0 to about 50 g/10 min;
a ratio of Mw/Mn in a range from about 10 to about 50;
a ratio of Mz/Mw in a range from about 2.4 to about 8; and
a Mn in a range from about 5,000 to about 25,000 g/mol.
12. The polymer of claim 9, wherein a relationship between natural draw ratio (NDR, %) and density (g/cm³) of the ethylene polymer is defined by the equation:

$$\text{NDR} < 13404(\text{density}) - 12050.$$

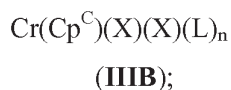
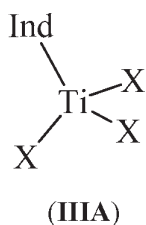
13. The polymer of claim 9, wherein the ethylene polymer is an ethylene/1-butene copolymer, an ethylene/1-hexene copolymer, or an ethylene/1-octene copolymer.
14. An article comprising the ethylene polymer of claim 9.
15. A catalyst composition comprising:
catalyst component I comprising an unbridged Group IV transition metal based metallocene compound;
catalyst component II comprising a bridged Group IV transition metal based metallocene compound with a fluorenyl group;
catalyst component III comprising a titanium or chromium half-metallocene compound;
an activator; and
optionally, a co-catalyst.
16. The composition of claim 15, wherein the activator comprises an aluminoxane compound, an organoboron or organoborate compound, an ionizing ionic compound, or any combination thereof.
17. An olefin polymerization process, the process comprising contacting the catalyst composition of claim 15 with an olefin monomer and an optional olefin

comonomer in a polymerization reactor system under polymerization conditions to produce an olefin polymer, wherein the catalyst composition comprises:

an unbridged metallocene compound containing two cyclopentadienyl groups, two indenyl groups, or a cyclopentadienyl and an indenyl group;

a bridged metallocene compound with a cyclopentadienyl group and fluorenyl group, and an alkenyl substituent on the cyclopentadienyl group and/or on the bridging group;

a half-metallocene compound having formula (IIIA) or formula (IIIB):



wherein:

Ind is an indenyl group;

Cp^{C} is a cyclopentadienyl, indenyl, or fluorenyl group;

each X independently is a monoanionic ligand; and

each L is a neutral ligand, and integer n is 0, 1 or 2;

an activator-support comprising a solid oxide treated with an electron-withdrawing anion; and

an organoaluminum compound.

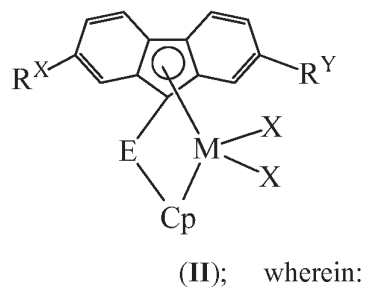
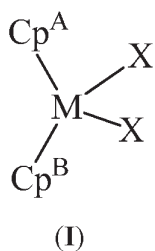
18. The process of claim 17, wherein:

the activator-support comprises a fluorided solid oxide and/or a sulfated solid oxide;

the organoaluminum compound comprises trimethylaluminum, triethylaluminum, tri-n-propylaluminum, tri-n-butylaluminum, triisobutylaluminum, tri-n-hexylaluminum, tri-n-octylaluminum, diisobutylaluminum hydride, diethylaluminum ethoxide, diethylaluminum chloride, or any combination thereof;

catalyst component I comprises an unbridged metallocene compound having formula (I) and catalyst component II comprises a bridged metallocene compound having formula (II):

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each M independently is Zr or Hf;

Cp^A and Cp^B independently are a cyclopentadienyl or indenyl group;

Cp is a cyclopentadienyl group;

each X independently is a monoanionic ligand;

R^X and R^Y independently are H, a halide, a C₁ to C₃₆ hydrocarbyl group, a C₁ to C₃₆ halogenated hydrocarbyl group, a C₁ to C₃₆ hydrocarboxy group, or a C₁ to C₃₆ hydrocarbylsilyl group; and

E is a bridging group.

19. The process of claim 17, wherein the polymerization reactor system comprises a slurry reactor, gas-phase reactor, solution reactor, or a combination thereof.

20. The process of claim 17, wherein the catalyst composition is contacted with ethylene and an olefin comonomer comprising 1-butene, 1-hexene, 1-octene, or a mixture thereof.