

WASTE TREATMENT APPARATUS AND METHOD

Field

The present invention relates to waste treatment apparatus and methods, in particular apparatus and methods for treatment of waste from a range of sources, including commercial premises and domestic and multi-occupancy residences, by a process combining pyrolysis and combustion of waste.

Background

A combined pyrolysis and combustion process, and related apparatus, is known from WO 2007/104954. This efficiently destroys waste, reducing it to ash.

In operation of the process and apparatus, the inventors herein have devised developments to modify and improve upon the waste treatment achieved.

JP 2007-263534 describes a moving bed type gasification furnace. Operation of the furnace includes continuously blowing gas into the combustion zone directly from the gasifier side combined with stirring. This action is said to increase the uniformity of temperature distribution in the combustion zone. Similarly, it is known to fit an internal circulation fan into the chamber of WO 2007/104954 to promote even temperature distribution.

It is therefore an object of the invention to provide alternative, preferably improved, process and apparatus to treat waste on site on a domestic and/or large scale. It is an object of specific embodiments of the invention to do so for multi-occupancy residences and also individual domestic residences and commercial enterprises such as supermarkets and restaurants. A further object is to reduce and/or remove the need for the transport of waste and prevent waste ending up as landfill, allowing local authorities to meet the requirements of recycling directives. A still further object of the invention is to enable greater efficiency in collecting recyclable materials, improving public compliance by facilitating the recycling process.

Accordingly, the invention relates to a process for waste treatment and apparatus for carrying out waste treatment by a combination of (i) pyrolysis and (ii) combustion (also referred to as oxidation or gasification) steps, the process and apparatus incorporating one or more of the aspects of the invention described
5 herein.

Summary of Inventions

According to the invention there is a cyclic process for waste treatment, each cycle comprising:-

10 introducing waste into a chamber, heating the waste to an elevated temperature to effect pyrolysis of the waste, introducing oxygen into the chamber to effect gasification of the waste, and removing combusted waste from the chamber,
further comprising agitating the waste with gas to promote gasification.

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Also according to the invention there is apparatus for waste treatment is provided, suitable for carrying out the methods of invention, comprising:-

a sealable chamber,
a waste treatment zone in the chamber,
20 a port for introducing waste into the chamber,
a port for the exit of treated waste, and
a heating element,
the apparatus further comprising one or more air inlets in a wall of the chamber, a high pressure air source and one or more conduits to connect the air
25 inlets to the source of air at high pressure,
wherein the apparatus is adapted to agitate gasifying waste with the air to promote gasification.

Details of the Inventions

The invention provides processes for waste treatment comprising introducing waste into a chamber, heating the waste to an elevated temperature to effect pyrolysis of the waste, introducing oxygen into the chamber (typically using air) to effect combustion of the waste, and removing combusted waste from the chamber. Pyrolysis is carried out in the substantial absence of oxygen, meaning in practice a substantial absence of air. Typical operating temperatures are set out elsewhere herein. Waste may be thus destroyed by a combination of pyrolysis, combustion and combustion of that fraction of the waste that remains as char after pyrolysis.

The term combustion as used herein refers to the oxidative breakdown of waste materials using high temperatures and controlled oxygen input resulting in a substantially flame-free process phase. This phase of the process of the invention may also be termed gasification and/or oxidation.

Treated waste is generally mostly fine ash, but may also contain materials which remain untreated, such as metals and glass, which may be retained in the chamber, optionally separated from the ash. In an embodiment of the invention, the chamber has a grid with holes through which ash can pass but which retains larger items such as metal and glass. A grid is preferably located in the chamber forming a shelf or part of a shelf, and the method can comprise placing waste e.g. bags of waste, on the grid prior to treatment.

It has been noted that in operation of a known machine some items such as plastics decompose or evaporate during pyrolysis and are easily treated but other

items such as especially paper and textiles tend to accumulate in piles, with the middle of the pile insulated from temperature and combustion. At the end of the process, which for practical purposes is generally time limited, there may be charred remains that have not been fully treated. In other words, the waste treatment may be incomplete.

In a first aspect of the invention, a method of the invention comprises agitating waste during combustion. This can assist reducing the total time needed for the combustion step. It can assist increasing the amount of material combusted, leaving a reduced amount of untreated waste, preferably substantially no untreated waste, at the end of the process.

Pyrolysis and combustion apparatus of this aspect comprises a sealable chamber, a waste treatment zone in the chamber, a port for introducing waste into the chamber, a port for the exit of treated waste, a heating element, and an agitator.

The invention accordingly provides a cyclic process for waste treatment each cycle comprising:-

introducing waste into a chamber, heating the waste to an elevated temperature to effect pyrolysis of the waste, introducing oxygen into the chamber to effect gasification of the waste, and removing gasified waste from the chamber, further comprising agitating the waste to promote gasification.

The method comprises agitating the waste with gas, in particular by introducing gas at high pressure into the chamber so as to agitate the waste during combustion. In one method, a pile of combusting waste in the chamber is repeatedly agitated so as to promote combustion of waste within the pile. Waste is thus disrupted and for example sheets of paper in a pile or waste lying on top of and obscuring other uncombusted material is or are disrupted so that the hot, combusting atmosphere of the chamber has improved access to that otherwise hidden or obscured material.

Typically gas blasts are used of sufficient pressure and duration to disrupt an ash membrane formed on the surface of the waste pile during combustion. In embodiments of the invention the gas blasts are of sufficient pressure and duration to disrupt the waste pile. Preferably the disruption of the waste pile by gas blasts exposes uncombusted material from the interior of the waste pile to air (oxygen) in the chamber, promoting complete breakdown of all combustible material.

The waste may be agitated discontinuously. For example, a gas blast of duration less than 10 seconds or less than 5 seconds, preferably less than 3 seconds, more preferably 1 second or less may be followed by a period without gas blasts of at least 10 seconds or at least 20 seconds or at least 1 minute, preferably at least 2 minutes. Gas agitation may be used as and when needed according to the operator or as governed by control equipment.

The waste may be agitated at a frequency of from at least once every 20 seconds to at least once every 5 minutes. In use of the invention, we have agitated using bursts of air every 30 seconds and every 3 minutes, both found effective. Typically, air is used. Also typically, air is introduced at a pressure of 3 atmospheres (303.975 kPa) or greater, preferably 5 atmospheres (506.625 kPa) or greater. Hence, in specific embodiments, the method comprises periodically agitating combusting waste material with bursts of gas, preferably from different directions, so as to promote complete combustion of the waste.

In embodiments of the invention gas blasts may use inert gases such as nitrogen, argon, helium or mixtures thereof. The use of inert gases rather than air avoids intermittent input of additional oxygen to the system, which may be advantageous as combustion temperature within the apparatus is generally controlled by controlling air input to the chamber.

Gas bursts using air are typically used towards the end of the combustion phase of waste treatment as bursts of air during the pyrolysis phase may disrupt pyrolysis

and problems of incomplete combustion tend not to arise during the early stages of combustion. Gas bursts using inert gases may be initiated during combustion or pyrolysis phases of waste treatment.

5 The invention provides, in this aspect, apparatus for waste treatment according to a method of the invention comprising:-

- a sealable chamber,
- a waste treatment zone in the chamber,
- a port for introducing waste into the chamber,
- 10 a port for the exit of treated waste, and
- a heating element,

the apparatus further comprising one or more air inlets in a wall of the chamber, a high pressure air source and one or more conduits to connect the air inlets to the source of air at high pressure, wherein the apparatus is adapted to
15 agitate gasifying waste with the air to promote gasification.

There are preferably two or more air inlets. The one or more air inlets can be in the form of nozzles located in a wall portion, preferably a lower wall portion of the chamber, being at least half way down the wall, or in the bottom of the chamber.

20 They are hence suitably adapted in use to direct air at high pressure towards combusting material located towards the bottom of the chamber. One or more inlets in the sides of the chamber enable agitation from the sides, and one or more inlets in the bottom of the chamber enable agitation from below. A combination of disrupting bursts of air from different directions may produce a good result.

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An apparatus of the invention, described below in more detail, comprises a high pressure air source.

In embodiments of the invention, two or more inlets are arranged in the side walls
30 of the chamber. Preferably the inlets are arranged on opposite walls of the chamber so that bursts of gas can be input from alternating sides of the chamber. In preferred embodiments of the invention gas is injected through fan spray-heads, which spread the gas over a range of 65 to 180 degrees, preferably 90 to 120 degrees along a one dimensional plane (providing a broad, very "flat" spray,

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shaped like a fan). The inlets typically enter the chamber at a 90 degree angle in relation to the chamber wall and are then rotated about their axis such that the “fan shaped spray” of gas is orientated at about 45 degrees to the vertical.

- 5 A control unit is suitably included, adapted to introduce air into the chamber periodically via the one or more air inlets during the combustion phase of the process. In an example machine, made and tested, air was input from two jets located on opposite sides of the chamber, with air being input alternately from the two jets. Air was input under seven atmospheres (709.275 kPa) of pressure for a
10 duration of 0.4 seconds per blast – note also that a range of pressures will work. In this time, approximately 3 litres of air was injected into the chamber per burst. The frequency used was one burst every 30 seconds, though the method has worked satisfactorily with a frequency of one burst every 3 minutes.
- 15 This agitation method is independent of how the combusted material is removed from the chamber, whether mechanically using e.g. an auger or with water flushing or otherwise.

In typical use, a chamber fitted with such an air-blast system employs
20 discontinuous, high-pressure bursts whose purpose is to physically dismantle waste beds that have become compacted and covered in ash, and so do not allow the normal-pressure air flow to penetrate. Combustion of waste in general is improved. In particular, waste mixes with large amounts of paper are much more efficiently destroyed with the air blasts.

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A physical disruption of the waste bed through mechanical agitation means may partially achieve the same purpose, but the gas blasts of the invention have the advantages, inter alia, of (1) simpler construction of the chamber and (2) reduced sensitivity to hard bits of waste (cans, bottles, etc). An additional advantage of the
30 air agitation via jets rather than mechanically is hence that there are no additional internal components to the chamber – these internal components being liable to failure.

In preferred embodiments of the invention a software subroutine is used to control air blasts. Typically, at a set period into the combustion phase of waste treatment the software commences checking process parameters. These checks may be carried out from 30 up to 120 minutes into the combustion phase and are preferably carried out from 60 up to 100 minutes into the combustion phase. In preferred embodiments of the invention combustion checks are carried out about 70 or about 90 minutes into the combustion phase. The software checks that at least one of the following process parameters is met; the chamber is not hotter than a pre-determined maximum temperature, the exit of the catalyst reactor is not hotter than a predetermined temperature and air input during combustion has reached its maximum value. In embodiments of the invention at least two of these parameters must be satisfied and in preferred embodiments of the invention all of the set parameters must be satisfied. The parameter checks ensure that air blasts are input only when combustion is running under conditions which are not likely to be excessively disturbed by the air blasts. Once parameter checks have been satisfied the air blast subroutine can be activated.

A separate problem with a method using catalytic off-gas treatment, the subject of an earlier filed patent application by the same applicant now published as WO 2010/073008, is that during the pyrolysis phase there is a relatively small volume of pyrolysis off-gas generated in the chamber, and the gas may furthermore be generated sporadically, and may pass through the catalyst in bursts, due to uncontrolled and unpredictable expansions within the chamber during pyrolysis. Note that the pyrolysis process is fundamentally endothermic, in the substantial absence of oxygen. A problem is that the low and irregular flow of gas can mean that process control is difficult. There may be inadequate treatment by the catalyst as a result. In addition, the low amount of gas generated in the chamber can mean that temperature distribution in the chamber is not even.

Accordingly, a further embodiment of the invention provides a cyclic process for waste treatment, each cycle comprising:-

introducing waste into a chamber, heating the waste to an elevated temperature to effect pyrolysis of the waste, introducing oxygen into the chamber to effect combustion of the waste, and removing combusted waste from the chamber further comprising agitating the waste to promote gasification, and

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wherein the process comprises introducing a small amount of air, into the chamber during pyrolysis.

Preferably, the method comprises introducing gas, especially air, into the chamber during pyrolysis in an amount sufficient to provide a steady flow of off-gas from the chamber but sufficiently small (e.g. with sufficiently low oxygen content) that the pyrolysis remains endothermic. Introduction of air is not intended to effect significant combustion or oxidation of the waste, but is enough to flow gas smoothly out of the chamber. Air flow is related to chamber volume and waste load, though generally air can be introduced at a rate of up to 10 litres per minute per kg of waste, preferably at a rate of up to 7 litres per minute per kg of waste or at a rate of up to 4 litres per minute per kg of waste. Generally air is introduced at a rate of a least 0.5 litres per minute per kg of waste. In examples of operating this method, air has been introduced at a rate of approximately 10-20 litres per minute for a 8 Kg load of waste being processed in 3 hours. This compares with a typical air input rate of 100-150 litres per minute during the combustion phase for that process. Higher rates are used with bigger chambers and higher waste throughput. In a specific example, described in more detail below, 16 L/minute was input for an 8 Kg waste load, i.e. at 2 L/minute/kg of waste during the pyrolysis phase.

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The solution in this embodiment is thus to introduce a small amount of gas, conveniently air, into the chamber during the pyrolysis stage. Not enough is introduced to mean the phase is other than endothermic. The air is introduced so as to provide some flow of pyrolysis off-gas through the catalyst in a more controlled way. In addition, there is another advantage as the introduction of air

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enables circulation of the chamber contents to provide a more even temperature distribution.

5 It is a further option to use a pump to evacuate the chamber and draw off the pyrolysis off-gas.

Again, introduction of air during the pyrolysis phase is independent of how the ash is removed from the chamber.

10 In machines made to date which incorporate the pyrolysis / combustion method, a basket, grid or similar is used to provide a shelf onto which waste can be loaded in the chamber and to capture metal, glass and other items not treated by the process, which items either are removed after each cycle or which accumulate and are removed after several cycles. The tiny particles of ash fall through the grid but
15 the bigger metal and glass particles do not and are retained.

A problem is that ash may be produced as a “ghost” of the combusted waste and can retain some integrity, hence it will not easily disintegrate into tiny particles and fall through the grid; also, ash may accumulate on top of the non-treated
20 metal/glass or other material and so be prevented from falling through to the bottom of the chamber and the ash collection point, for example an auger or ash box.

A further embodiment of the invention provides a cyclic process for waste
25 treatment, each cycle comprising:-

introducing waste into a chamber, heating the waste to an elevated temperature to effect pyrolysis of the waste, introducing oxygen into the chamber to effect combustion of the waste, and removing combusted waste from the chamber, further comprising agitating the waste with gas to
30 promote gasification and further comprising agitating accumulated ash produced by the combustion so as to dislodge the ash and urge it towards an exit of the chamber.

In one such method, accumulated ash is agitated by injecting air into the chamber. This can be achieved by injecting air at high pressure from one or more outlets in a wall of the chamber. The ash is disrupted, for example the integrity of a "ghost" is broken up and particles of ash can now pass through the grid. Ash particles
5 lying on, say, a piece of metal are blown away and no longer prevented from falling towards the bottom of the chamber.

Air bursts suitable for this embodiment may have the same characteristics of those used to promote complete combustion as described elsewhere herein, and one set
10 of bursts may achieve both effects. Air bursts for this embodiment, to dislodge ash, may occur towards the end of the combustion phase. Air bursts to promote combustion may occur from earlier on, generally from the halfway point of combustion towards the end of combustion, though in practice the two phases may overlap. Air bursts to dislodge ash may also occur after combustion has
15 finished, for example as part of the chamber cycle or as part of a cleaning step.

Ash may also be dislodged, in another embodiment of the invention, by injecting water into the chamber, optionally in the form of steam. Steam bursts may have additional force and be effective at lower frequency than air bursts. Steam busts
20 may also be used after combustion has finished. The amount of water used is preferably sufficiently small that all is evaporated and exits the chamber as steam, none exiting as water. In this way, there is no need for a water drain to the chamber.

25 Apparatus for waste treatment according to a method of the invention can comprise air inlets for various purposes, combining more than one or all of the aspects of the invention. Accordingly, apparatus of the invention, for waste treatment in any of or in a combination of embodiments of the invention, is provided comprising:-

- 30 a sealable chamber,
 a waste treatment zone in the chamber,
 a port for introduction of waste into the chamber,
 a port for exit of treated waste,

a heating element,

the apparatus further comprising one or more air inlets in a wall of the chamber, a high pressure air source and one or more conduits to connect the air inlets to the source of air at high pressure, wherein the apparatus is adapted to agitate gasifying waste with the air to promote gasification, and one or more inlets located in a wall or floor of the chamber, said one or more inlets connected to an air supply via control equipment such that the or each of the one or more inlets can independently be used to introduce air into the chamber, and wherein the control equipment is programmed to operate in at least two of the following modes:-

(i) air is introduced into the chamber during pyrolysis of waste in the chamber;

(ii) air is introduced into the chamber in bursts during combustion of waste in the chamber to promote combustion of the waste; and

(iii) air is introduced into the chamber during and/or after combustion to dislodge accumulated ash.

Preferred apparatus, already made and tested, comprises two or more of said inlets. It is also preferred that the control equipment is programmed to operate in at least three of modes (i) to (iii).

In a further apparatus of the invention, air and water inputs are provided, hence said one or more inlets are connected to an air supply and to a water supply via the control equipment such that the or each of the one or more inlets can independently be used to introduce air or water into the chamber, and wherein the control equipment is also programmed to operate in mode (iv) wherein water is introduced into the chamber during and/or after combustion to dislodge accumulated ash.

The combustion phase of the process of the present invention tends to generate ash, which floats within the chamber and the concentration of ash can be increased following physical disruption of the waste, e.g. by high pressure gas bursts. This ash can damage the catalyst and is thus preferably filtered out of the gas exiting the chamber prior to contact of the gas with the catalyst. Metal or ceramic filters can be used but the inventors have thus far been unable to identify suitable metals or ceramics which can withstand the heat, temperature changes

and corrosive nature of the ash over repeated chamber cycles. A preferred option of the invention is therefore to filter the ash using an inertial separator such as a cyclone filter.

- 5 Accordingly, embodiments of the invention can provide a cyclic process for waste treatment, each cycle comprising:-

10 introducing waste into a chamber, heating the waste to an elevated temperature to effect pyrolysis of the waste, introducing oxygen into the chamber to effect gasification of the waste, and removing gasified waste from the chamber, further comprising agitating the waste with gas to promote gasification wherein pyrolysis of the waste generates off-gases which are passed through a catalyst to remove one or more noxious components thereof, and

15 wherein the off-gases are filtered using an inertial separator prior to contact of the off-gases with the catalyst.

Embodiments of the present invention also provide an apparatus for waste treatment, comprising:-

20 a sealable chamber,
a waste treatment zone in the chamber,
a port for introducing waste into the chamber,
a port for the exit of treated waste,
a heating element, and
a catalyst

25 the apparatus further comprising an inertial separator between the chamber and the catalyst.

30 The inertial separator of the present invention may be a settling chamber, baffle chamber or centrifugal collector. In preferred embodiments of the invention a centrifugal collector such as a cyclone separator is used. Suitable cyclone separators for use in the present invention include single-cyclone separators, multiple-cyclone separators and secondary air flow separators. In preferred embodiments of the invention a single-cyclone separator is used. Centrifugal separators such as cyclone separators have a particular advantage as they can be

used both to remove ash from the off gas and mix off-gas with air from a separate air supply to go into the catalyst. Apparatus of a particular embodiment of the invention, described in use below, comprises a cyclone that receives off gas from the chamber and receives an air supply for catalyst air and has an output to supply
5 filtered, mixed resultant gas to the catalyst.

In preferred embodiments of the invention filtration of off-gases using an inertial separator is carried out in combination with the use of high pressure gas bursts (as described above). An inertial separator may also be used when air is introduced
10 into the chamber during the pyrolysis phase of waste treatment.

This filtration method is independent of how the combusted material is removed from the chamber, whether mechanically using e.g. an auger or with water flushing or otherwise.
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Generally the process comprises introducing waste into a chamber, heating the waste to an elevated temperature to effect pyrolysis of the waste, introducing oxygen into the chamber to effect combustion of the waste, and removing combusted waste from the chamber, wherein the elevated temperature to effect
20 pyrolysis can be from 200-700°C or from 350-700°C and is typically from 400-700°C. Operating at these temperatures tends to avoid formation of some of the more noxious contaminants associated with standard pyrolysis units or form them to a lesser degree, whilst ensuring that substantially all waste, other than recyclable components, can be treated. Hence an advantage of the invention is
25 that treatment of off gases can be carried out with reduced on-site emissions. The pyrolysis temperature is preferably from 500-700°C, more preferably from 500-600°C. In a specific embodiment of the process, the system operates at about 550°C.

30 It is further preferred that combustion is carried out at elevated temperatures, typically 300°C or higher, 400°C or higher, preferably at least 450°C more

preferably at least 500°C. In typical operation of an apparatus of the invention, the chamber is heated to the pyrolysis temperature, pyrolysis is carried out and then combustion is carried out as the next step without specific separate heating or cooling of the chamber. Heat generated by combustion generally maintains an elevated temperature within the waste and depending upon its calorific content may slightly increase the temperature so chamber heaters are generally turned off during combustion. Heat can be removed from the chamber by passing off gases through a radiator or a heat exchanger and recovered heat can be used for other purposes. Chamber temperature can also be controlled by controlling flow of air into the chamber. Generally chamber temperature during combustion does not rise above 800°C and preferably not above 750°C or 700°C.

The duration of the pyrolysis phase can vary according to waste volume, in turn with a limit dictated by chamber volume. Apparatus of the invention are generally designed for use both in domestic and multi-occupancy residences and small commercial premises but also in larger, commercial settings.

Waste may enter the chamber at ambient temperature. The chamber is then sealed and the heaters are activated to heat the chamber to the operating temperature. Waste may enter the chamber at an elevated temperature, for example if there is little or no chamber cooling since its last operation. The chamber is then sealed and may already be at operational temperature; if needed, the heaters are activated to return the chamber to an operating temperature.

In apparatus made and tested to date, this heating phase from ambient typically takes 2-20 minutes, preferably 5-10 minutes, being dependent on the operating temperature required, the chamber volume, and volume of waste in the chamber. In use, it is found that off-gases can evolve in fractions as the temperature increases and this is believed to result in reduced production of certain toxic components, notably dioxins and fluorins compared to industrial pyrolysis using higher temperatures, following rapid heating. Processes carried out in apparatus of the invention generally comprise holding the waste at the elevated temperature for

10-90 minutes, preferably for 20-60 minutes. In a specific embodiment of the process, the pyrolysis phase has a roughly 40 minute duration.

5 In some embodiments of the invention intelligent timing systems are used to control the length of the cycle. These systems can monitor the temperature of the off-gases being produced and adjust the cycle duration accordingly. Use of these systems improves the power efficiency of the process. In one example, a control system monitors the temperature of the off-gases or of the load, such as via a thermocouple located proximal to the waste in the chamber, and triggers
10 commencement of combustion once a predetermined temperature (say, about 450°C-500°C) is reached. In another example, a control system monitors the temperature of the off gases from the chamber and when the temperature has dropped to a pre-determined level (say 300°C-400°C) initiates the end of the combustion and, optionally, the beginning of cooling and cleaning of the chamber
15 by introduction of water (as superheated steam). Another option is to monitor the rate of cooling of the chamber, and once this reaches or approaches the natural cooling rate of the chamber, then initiate the end of the cycle. Another option is to monitor the oxygen content of gas leaving the chamber; a sufficiently high level of oxygen indicates combustion has stopped.

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In an example of the invention operating in situ, the apparatus is set up with a pre-programmed pyrolysis phase, based on the chamber volume and anticipated nature of the waste to be processed. The phase may be set up such that the elevated temperature is held for the duration of the pyrolysis phase and such that
25 50% or more of the waste is degraded, preferably 70% or more, more preferably 80% or more. In practice it is problematic and energy inefficient to ensure 100% treatment, especially when recyclable material is present such as metals and glass, which would not be degraded and which can be extracted for recycling. From expected waste volume and content the system may be set up for a given
30 property so that from 60% - 95% of waste by weight is pyrolysed.

In a typical operation of the apparatus, waste enters the destruction chamber and the lid is sealed, the chamber is then heated, to about 550°C. The off-gases produced during pyrolysis are monitored; as waste is destroyed the levels of these gases reduce, once they drop below a predetermined threshold the heaters are

- 5 switched off. During pyrolysis air is introduced into the chamber at a low rate, about 5-10 litres per minute to flow off-gas through the catalyst. After pyrolysis, substantially in the absence of oxygen, air is then passed through the heating coil and admitted into the chamber, this is at approximately 200-500°C on entry. Entry of the air initiates combustion of the residual waste within the destruction chamber.
- 10 No external heat is applied at this stage but the heat from the pyrolysis stage is retained. Regular agitation of the combusting waste is carried out with bursts of air towards the end of the combustion phase. Gas output is monitored during combustion, and while waste is present the chamber output exceeds the air input. Oxygen content can also be monitored for this purpose. During combustion, waste
- 15 is agitated as described herein to promote full combustion and reduce untreated waste at the end. When the gas output drops below, or oxygen content rises above (depending upon the monitoring adopted), a set threshold the airflow is shut off as combustion is considered finished for that cycle of operation. The residual waste, now largely ash can be agitated with air and/or water to help dislodge ash
- 20 so that it falls to the bottom of the chamber and is not retained on the grid. Ash is then removed from the chamber. This can be during combustion, e.g. using an auger or after combustion e.g. by hand auger or by flushing with water. Non-combusted material is retained by the metal grid, this can be removed for recycling or left in the machine for another cycle(s). Some pyrolyzable material may require
- 25 two or three cycles before it is completely destroyed.

Waste gases produced by pyrolysis and / or combustion are suitably treated to remove noxious components, depending upon the emissions standards required to be met in any given application.

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Gases can be passed through an oxidation catalyst, fed with air, preferably heated air, to destroy noxious components by oxidation.

Gases can be passed through an aqueous agitation system, to assist dissolution of gases. Gases can be bubbled through the solution, optionally containing softened water and optionally containing additives to promote dissolution of the
5 gases. Gases may also be passed through a water scrubber. Not all gases may be dissolved in the solution and it is preferred that gases are also filtered within a gas cleaning chamber. A catalyst can act as a gas cleaning chamber, and may be placed upstream or downstream of a scrubber. The method also may comprise discharging undissolved gases into the sewage system. Hence, in an embodiment,
10 filtered exhaust gases that have not been dissolved in solution or retained within the filter are discharged into the sewer. These gases then pass up the soil pipe to vent through venting stacks. The filtered exhaust produced is substantially colourless and odourless, principally consisting of carbon dioxide and carbon monoxide, though with a functioning catalyst the carbon monoxide content is
15 generally very low.

In embodiments of the invention comprising a catalyst it is preferred to filter off-gases using an inertial separator prior to contact of the off-gases with the catalyst.

20 In specific embodiments designed for domestic and such uses, all of the by-products of the process are disposed of into the sewer.

Combusted waste can be flushed from the chamber with water, wherein the water is introduced into the chamber as superheated steam. In use, the steam cools and
25 cleans the chamber and flushes away the ash residue of treated material. This is convenient and efficient. The chamber is left looking clean and hence more acceptable for users. There is reduced risk of residue in the chamber which is unsightly or has unpleasant odour. To carry out the flushing, water can be introduced into the chamber via piping in walls of the chamber, the water being
30 heated to form superheated steam as it passes through the piping. In this way the water is heated to the desired temperature by the chamber heat. Also, the chamber is cooled in readiness for a next cycle of use.

An oxygen supply (generally as air) is preferably linked by piping to the chamber and arranged such that in use oxygen is supplied to the chamber via the piping. Water, if supplied to the chamber, can be supplied to the chamber via the same piping. Flow rates vary with factors including chamber size. Air input during pyrolysis can be as low as 5 litres per minutes. Air input during combustion of a large load may be from 50 to 1000 litres per minute. We have operated embodiments with air flow rates of from 25 – 200 litres/min.

- For all aspects of the invention, the chamber volume may vary; suitable chambers volumes are in the range from $0.01 - 5.00\text{m}^3$, preferably from $0.01 - 3.00\text{m}^3$, for domestic type units more preferably in the range from $0.02 - 0.30\text{m}^3$, especially from $0.03 - 0.20\text{m}^3$ or from $0.04 - 0.10\text{m}^3$. Chambers with volumes of about 0.06m^3 and about 0.14m^3 have been successfully tested to date.

The invention is now illustrated in the following specific embodiment with reference to the accompanying drawing in which:-

Fig. 1 shows a schematic diagram of apparatus of the invention

Example 1

Waste is processed by pyrolysis and combustion in a sealable chamber shown schematically in Fig. 1 having a lid, heated using panel heaters and having a gas exit port, a catalyst for off-gas treatment, a heater to heat air for the catalyst, a gas scrubber and a heat exchanger to heat air entering the chamber with heat extracted from exhaust gas. Water input for cleaning and emptying the chamber is optional.

The lid of the processing chamber is opened and a waste load of approximately 8 Kg enters the chamber (which is at ambient temperature) and is placed on a grid towards the bottom of the chamber. The lid is then closed and the chamber is sealed.

The chamber panel heaters are activated and the interior temperature is raised to between 500-550°C. Air is input to the chamber from the start at a rate of approximately 16 L/minutes to flow off-gases smoothly from the chamber and to promote even temperature distribution within the chamber, the catalyst bed is heated with air from the blower to about 550-600°C and the emitted gases are passed through the catalyst.

Air input to the catalyst is initially about 200 L/minute, rising to 800 L/minute during the process, and the pyrolysis phase lasts for approximately 40 minutes.

After the pyrolysis phase has completed the external panel heaters are turned off and air input to the chamber is increased up to about 150 L/minute for the oxidation / combustion phase.

With the introduction of air, the waste begins to glow. The volume of the waste decreases further, typically reaching around 5% of its original volume. The waste is converted to a very fine ash. Smoke and particulate levels in the system increase during the air injection phase. All gaseous exhausts are passed through the catalyst.

During the combustion phase, the combusting mass of waste is agitated by high pressure blasts of air, alternately from opposite sides of the chamber, air being injected every minute in 0.4 second blasts at 7 bar (7 atmospheres (709.275 kPa)), the amount of air injected being approximately 3 L per blast. This agitates the mass and promotes full combustion. Towards the end of the combustion phase, similar agitation is used to dislodge ash that had piled up on the grid or accumulated on top of untreated metal or glass, so the ash drops to the bottom of the chamber.

When the combustion phase has completed the air injection is turned off, the gas exhaust valve is closed and ash is removed from the chamber whilst the chamber is still hot using an auger. The system is ready for the next cycle.

5 **Example 2**

- Waste is processed as per example 1. At the end of the combustion phase, the liquid exhaust valve is opened and water flows through the same tubes as the air, around the outside of the chamber and is injected as superheated steam. The steam is initially injected in a series of pulses, then as a constant stream. The pulses are of duration 150 – 300 milliseconds, then 500 – 1000 milliseconds every 30 seconds then continuously on for 3 minutes, when the water is injected at approximately 2 l/min.
- The initial steam blasts dislodge ash, urging it towards the chamber exit. At this stage all steam can exit the chamber as a gas, there being no water output. Subsequent steam both flushes the ash out through to the exhaust, and cleans the internal faces of the chamber. The steam has a cooling effect on the chamber, and after approximately 1 minute the internal temperature of the chamber drops to below 100°C. After the steam injection has completed the lid opens and the system is ready for its next cycle. Any incompatible waste that has not been decomposed by the cycle is held in a drawer, and can be removed and recycled.

Example 3

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- Waste is processed by pyrolysis and combustion in a sealable chamber shown schematically in Fig. 1 having a lid, heated using panel heaters and having a gas exit port, a catalyst for off-gas treatment, a heater to heat air for the catalyst, a gas scrubber and a heat exchanger to heat air entering the chamber with heat extracted from exhaust gas. Water input for cleaning and emptying the chamber is optional.
- 30

The lid of the processing chamber is opened and a waste load of approximately 8 Kg enters the chamber (which is at ambient temperature) and is placed on a grid towards the bottom of the chamber. The lid is then closed and the chamber is sealed.

5

The chamber panel heaters are activated and the interior temperature is raised to between 500-550°C. Air is input to the chamber from the start at a rate of approximately 16 L/minutes to flow off-gases smoothly from the chamber and to promote even temperature distribution within the chamber, the catalyst bed is heated with air from the blower to about 550-600°C and the emitted gases are passed through the catalyst.

Air input to the catalyst is initially about 200 L/minute, rising to 800 L/minute during the process, and the pyrolysis phase lasts for approximately 40 minutes.

15

After the pyrolysis phase has completed the external panel heaters are turned off and air input to the chamber is increased up to about 150 L/minute for the oxidation / combustion phase.

20 With the introduction of air, the waste begins to glow. The volume of the waste decreases further, typically reaching around 5% of its original volume. The waste is converted to a very fine ash. Smoke and particulate levels in the system increase during the air injection phase. All gaseous exhausts pass through a cyclone where they are filtered and mixed with air for the catalyst before being passed through the catalyst.

25

70 minutes into the combustion phase a software subroutine checks that the following process parameters are met:-

30

the chamber is not hotter than 600°
the exit of the catalyst reactor is not hotter than 680°C
air input to the chamber is at 150 L/minute.

Once all process parameters are satisfied the air blast subroutine is activated and the following steps are carried out:-

- 5 air input to the chamber is reduced by two thirds,
 air flow to the cyclone is increased to maximum,
 a compressed air pump is activated for 14 seconds, pumping air into a 0.7L
 tank connected to air injection points within the chamber,
 air pressure in the tank reaches about 7 bar,
- 10 a valve connected to an air injection point is opened for 400 milliseconds
 then closed,
 after 4 seconds the valve is opened again for 400 milliseconds,
 this is repeated five times with the same valve and the air tank is emptied,
 the air tank is then recompressed as above and the process is repeated for
- 15 the opposite air valve.

Air input to the chamber is gradually increased back up to 150L/min. The software again checks the process parameters and once these are met the air blast subroutine is again activated as above.

- 20 Towards the end of the combustion phase, air agitation is used to dislodge ash
 that has piled up on the grid or accumulated on top of untreated metal or glass, so
 the ash drops to the bottom of the chamber.

- 25 When the combustion phase has completed the air injection is turned off, the gas
 exhaust valve is closed and ash is removed from the chamber whilst the chamber
 is still hot using an auger. The system is ready for the next cycle.

Example 4

- 30 Apparatus of the invention was loaded with catalogues having gloss paper sheets.
 The catalogues were placed in the exact centre of the chamber grid and had A4

dimensions, forming a pile of 96mm in height and had a weight of 4kg. The grid was formed by a mesh basket which was suspended within the chamber. The chamber of the apparatus used was approximately 43cm in internal diameter, and approximately 75cm in internal depth.

5

The waste treatment process was computer software controlled and proceeded in the following manner:-

- 10 - Upon starting the run, the catalyst was first heated by a flow of hot air, and the chamber was heated up to a maximum of 120°C as measured by the air temperature in the top section of the chamber.

Pyrolysis Stage

- 15 - After approximately 30min, as the catalyst bed had reached 380°C, the chamber temperature set point was increased to 350°C, and air was injected from the chamber bottom to a flow of approximately 25L/min (the air trickle air flow).
- These conditions were maintained for 30min.

20

Gasification Stage

- 25 - The temperature set-point was increased to 480°C, and the main air pump was switched on, gradually increasing its air flow by 20% every 20s until its maximum of approximately 150L/min was reached.
- This condition remained unchanged for 70min (during which there was constant air flow).
- After 70min: (1) the temperature set point of the chamber was increased to 550°C and (2) the air blasts sequence started.
- 30 - The air blasts sequence operated as described in example 3, with the following exceptions:

1. the compression time was set to 18s (having an initial pressure of 7bar)
 2. the main air pump was cyclically reduced to around 30% of maximum (by closing an air valve) and, in principle, increased by 20% every 20s. Whenever the air flow reached maximum, it was reduced again to 30% and the air blast sequence started. That resulted in about one double sequence (that is, once from each side) approximately every 3 minutes.
- 100 min after the start of the air blasts (170min since the start of the gasification stage), the process automatically timed out and all the heaters and air pumps (but not the air blower into the catalyst) were switched off.

Cooling

- Normally, as the chamber temperature naturally reached 440°C, active cooling with water injection would have started but this was stopped manually to allow checking of the load.
- It took approximately 100min for the temperature to cool enough for the chamber to be opened – in the 250 – 300°C range.
- The basket was then lifted out and the contents that remained in it – that is, load remains that did not simply fall through the bottom of the basket during the run – were weighed and compared.

Following waste treatment the remains on the basket had a weight of 0.69kg, that is, a reduction in mass of 83%. Also, the “catalogue shape” of the pile was significantly disturbed with only a small charred core of each sheet.

Comparative Example 1

- Apparatus of the invention was loaded with catalogues having gloss paper sheets. The catalogues were placed in the exact centre of the chamber grid and had A4 dimensions, forming a pile of 96mm in height and had a weight of 4kg. The grid

was formed by a mesh basket which was suspended within the chamber. The chamber of the apparatus used was approximately 43cm in internal diameter, and approximately 75cm in internal depth.

- 5 The waste treatment process was computer software controlled and proceeded as per example 4, however, the air compressor was mechanically disabled for this run and no air blasts occurred.

- The weight of the load remaining in the basket after treatment was reduced from
- 10 4.0kg to 1.1kg – a reduction in mass of 73%. Also, the catalogue pile essentially retained its shape, with individual sheets recognizable, but having turn completely white on the outside, due to a fine layer of ash. The catalogue pile had additionally “swollen” (that is with spaces between individual sheets), and, when opened, the core of each sheet consisted of black charred material. The outside of each sheet
 - 15 consisted of very fragile ash which collapsed upon touch.

The invention hence provides treatment of waste by pyrolysis and combustion, and apparatus for doing so.

Claims

1. A cyclic process for waste treatment each cycle comprising:-
introducing waste into a chamber, heating the waste to an elevated temperature to effect pyrolysis of the waste, introducing oxygen into the chamber
5 to effect gasification of the waste, and removing treated waste from the chamber,
further comprising agitating the waste with gas to promote gasification.
2. A process according to claim 1, comprising introducing gas into the chamber at a pressure of 3 atmospheres (303.975 kPa) or greater so as to agitate
10 the waste during gasification.
3. A process according to claim 1 or 2, comprising repeatedly agitating a pile of gasifying waste in the chamber so as to promote gasification of waste within the pile.
15
4. A process according to any of claims 1-3, comprising agitating the waste at a frequency from at least once every 20 seconds to at least once every 5 minutes.
5. A process according to any of claims 1-4, wherein the gas comprises air.
20
6. A process according to any preceding claim, comprising introducing gas into the chamber at a pressure of 5 atmospheres (506.625 kPa) or greater so as to agitate the waste during gasification.
- 25 7. A process according to any previous claim, comprising periodically disrupting gasifying waste material with bursts of air so as to promote gasification of the waste.
8. A process according to claim 7, comprising periodically agitating gasifying
30 waste material with bursts of gas from different directions.

9. Apparatus for waste treatment, for carrying out the method of any of claims 1 to 8, comprising:-
- a sealable chamber,
 - a waste treatment zone in the chamber,
 - 5 a port for introducing waste into the chamber,
 - a port for the exit of treated waste, and
 - a heating element,
- the apparatus further comprising one or more air inlets in a wall of the chamber, a high pressure air source and one or more conduits to connect the air
- 10 inlets to the source of air at high pressure,
- wherein the apparatus is adapted to agitate gasifying waste with the air to promote gasification.
10. Apparatus according to claim 9, comprising two or more air inlets.
- 15
11. Apparatus according to claim 9 or 10, wherein the one or more air inlets are in the form of nozzles located in a lower wall portion of the chamber, being at least half way down the wall, or in the bottom of the chamber.
- 20
12. Apparatus according to any of claims 9-11, wherein the one or more air inlets are adapted in use to direct air at high pressure towards gasifying material located towards the bottom of the chamber.
- 25
13. Apparatus according to any of claims 9-12, comprising a control unit adapted to introduce air into the chamber periodically via the one or more air inlets.
- 30
14. Apparatus according to any of claims 9-14, wherein in use air is introduced into the chamber at a pressure of at least 3 atmospheres.
15. Apparatus according to any of claims 9-14, wherein in use air is introduced into the chamber at a pressure of at least 5 atmospheres.

16. A process according to any of claims 1 to 8, further comprising introducing a small amount of air into the chamber during pyrolysis.
- 5 17. A process according to claim 16, comprising introducing air into the chamber during pyrolysis in an amount sufficient to promote smooth flow of off-gas from the chamber but sufficiently small that the pyrolysis remains endothermic.
18. A process according to claim 16 or 17, comprising introducing air at a rate
10 of up to 10 litres per minute per kg of waste.
19. A process according to claim 18, comprising introducing air at a rate of up to 4 litres per minute per kg of waste.
- 15 20. A process according to claim 18 or 19, comprising introducing air at a rate of a least 0.5 litres per minute per kg of waste.
21. A process according to any of claims 1 to 8 and 16 to 20, further comprising agitating accumulated ash produced by the gasification so as to dislodge the
20 accumulated ash and urge it towards an exit of the chamber.
22. A process according to claim 21, comprising agitating the accumulated ash by injecting air into the chamber at the accumulated ash.
- 25 23. A process according to claim 22, comprising injecting air at high pressure from one or more outlets in a wall of the chamber.
24. A process according to claim 21, comprising agitating the ash by injecting water into the chamber at the ash, optionally in the form of steam.
- 30 25. A process according to claim 24, wherein the amount of water is sufficiently small that all is evaporated and exits the chamber as steam, none exiting as water.

26. A process according to any of claims 1 to 8 and 16 to 25, wherein the temperature to effect pyrolysis is from 400-700°C.

5 27. A process according to any of claims 1 to 8 and 16 to 26, comprising carrying out gasification at a temperature of at least 400°C.

28. Apparatus for waste treatment according to any of claims 9 to 15, comprising one or more inlets located in a wall or floor of the chamber, said one or
10 more inlets connected to an air supply via control equipment such that the inlet can, or each of the inlets can independently, be used to introduce air into the chamber, and wherein the control equipment is programmed to operate in at least two of the following modes:-

(i) air is introduced into the chamber during pyrolysis of waste in the
15 chamber to dilute off-gas exiting the chamber;

(ii) air is introduced into the chamber in bursts during gasification of waste in the chamber to promote gasification of the waste; and

(iii) air is introduced into the chamber during gasification to dislodge accumulated ash.

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29. Apparatus according to claim 28, comprising two or more of said inlets.

30. Apparatus according to claim 28 or 29, wherein the control equipment is programmed to operate in all least three of modes (i) to (iii).

25

31. Apparatus according to any of claims 28 to 30, wherein said one or more inlets are connected to an air supply and to a water supply via the control equipment such that the or each of the one or more inlets can independently be used to introduce air or water into the chamber, and wherein the control equipment
30 is also programmed to operate in mode (iv) wherein water is introduced into the chamber during gasification to dislodge accumulated ash.

32. A process for waste treatment according to any of claims 1 to 8 and 16 to 27, comprising:-

5 introducing waste into a chamber, heating the waste to an elevated temperature to effect pyrolysis of the waste, introducing oxygen into the chamber to effect gasification of the waste, and removing gasified waste from the chamber, wherein pyrolysis of the waste generates off-gases which are passed through a catalyst to remove one or more noxious components thereof, and

10 wherein the off-gases are filtered using an inertial separator prior to contact of the off-gases with the catalyst.

33. An apparatus for waste treatment according to any of claims 9 to 15 and 28 to 31, further comprising a catalyst and an inertial separator between the chamber and the catalyst.