

Description**Field of Invention**

- 5 The invention relates to a process for forming solid solutions and, in particular, to a process for making solid solutions in finely divided form.

Background of the Invention

- 10 Though the process of the invention has wide application for making virtually an infinite variety of solid solutions, it was developed initially for the purpose of providing a reliable and economic source of finely divided, uniformly sized particles of true solid solutions for use in making monolithic capacitors.

- Monolithic capacitors comprise a plurality of dielectric layers, at least two of which bear metallizations (electrodes) in desired patterns. Such capacitors are made by either the "green tape" process or by the thick multilayer process. In the former, multilayer capacitors are made from a green (unfired) tape of particles of dielectric materials held together with an organic binder by cutting pieces of tape from a sheet of tape, metallizing some of the tape pieces, stacking and laminating the pieces of tape, cutting the laminate to form individual capacitors and firing the resultant individual capacitors to drive off the organic binder and vehicles and to form a sintered (coherent) body. In the latter method, multilayer capacitors are made by printing and drying alternating layers of thick film conductor materials and dielectric material in a desired configuration on a rigid ceramic substrate such as Al_2O_3 . The sequence of steps is repeated until the desired number of capacitor layers is fabricated. The dried stack of capacitor layers is then fired in the same manner as the green tape to effect densification of the dielectric material.

- Metallizations useful in producing electrodes for capacitors usually consist of finely divided metal particles applied to the dielectric green tapes in the form of a dispersion of such particles in an inert liquid organic medium or vehicle. Selection of the composition of the metal particles is usually based on a compromise of cost and performance. Since base metals often are oxidized in air at elevated temperatures and/or in many cases react with the dielectric material during firing, noble metals are usually preferred because of their relative inertness during firing of the laminates to produce electrically continuous conductors. By far the most widely used monolithic capacitor electrode materials have been palladium and mixtures of finely divided palladium and silver powders which become alloyed during firing.

- In the fabrication of multilayer capacitors, the required solidus temperature of the electrode metal will ordinarily be determined by the sintering temperature of the dielectric material on which it is applied. In turn, the sintering temperature is determined by the physical and chemical characteristics of the dielectric material. Thus, to prevent excessive diffusion of the conductive metal into the dielectric layer during sintering, it is preferred to employ a metal or solid solution of metals having a solidus temperature higher than the firing temperature and preferably at least 50°C higher.

- Silver would most frequently be the noble metal electrode material of choice because it has both suitable conductive properties and the lowest cost of the noble metals. However, when used in capacitors, the electrode material is subjected to firing temperatures of 1100°C or even higher. These temperatures are necessary for most state-of-the-art dielectric materials to be sufficiently sintered to obtain suitable densification and dielectric properties. Because metallic silver melts at only about 961°C , silver metal alone would melt completely at 1100°C or higher and be of such low viscosity that it would too readily diffuse into the dielectric material and thus substantially degrade the capacitor properties of the sintered dielectric material. For this reason, it is preferred to employ a solid solution of palladium and silver which has a suitably high solidus temperature that it cannot migrate significantly into the dielectric material at normal firing temperatures. This solid solution or alloy is best provided as an already formed Pd/Ag alloy for the reason that any unalloyed silver would be available to migrate into the dielectric layer.

- As a result of the above considerations, for those X7R and NPO class capacitors which are fired at 1100° , a 30/70 Pd/Ag mixture is used. On the other hand, for a Z5U class capacitor which is fired at 1450°C , a 70/30 Pd/Ag or 100 Pd mixture is used as the noble metal component. In general, the ratio of palladium to silver is dependent upon the maximum firing temperature which is used to densify the dielectric material to a well sintered body.

- The particles of the metal component of the metallization should be sufficiently small that the paste can be used even in conventional screen printing operations and that the particles can be readily sintered. Furthermore, in the production of capacitors from green dielectric sheets, the presence of coarse particles in the inner electrode prints must be avoided lest they cause puncturing of the green dielectric sheets. Generally, the metallizations are such that at least 90% of the noble metal particles are no greater than 8

micrometers in diameter; that is, in general their largest dimension should be no greater than 8 micrometers. However, when the thickness of the green dielectric layer is less than 1 mil, (25.4 micrometers) the particles must be correspondingly smaller.

The problem of making such particulate material as true solid solutions is illustrated quite graphically by reference to U.S. 3,390,981 to Hoffman. Based on a U.S. patent application filed in 1963, the patent purports to cover a process for producing solid solution particles of two noble metals by treating a solution of the metals with a reducing agent capable of simultaneously reducing the metal constituents to the corresponding metals. The process was carried out with at most mild agitation (rapid stirring, Example 1) and slow addition of reductant. By virtue of a particularly described melting point determination, it was concluded that the particles therefrom were solid solutions. However, modern x-ray diffraction studies of products made in accordance with the teaching of the reference show separate Ag and Pd peaks, which indicate a mixture of the two metals and not a true alloy or solid solution. It has since been shown that the melting points obtained as described in the reference were the result of formation of a solid solution during the melting point test itself (See col. 5, lines 17-23 of the reference).

Brief Description of the Invention

The invention is therefore directed to a process for forming a solid solution of two or more metals or metal oxides by ionic reaction and precipitation from the reaction medium comprising the steps of:

- A. In a high intensity mixing zone in which the energy dissipation rate is at least of 200 Joules/sec • liter, forming a reaction medium by mixing together an aqueous liquid solution of metal ions or metal oxide ions and at least a stoichiometric amount relative to the dissolved ions of a reactant fluid which is soluble in the aqueous solvent and which will react with the ions in the liquid phase to form metals or metal oxides therefrom and maintaining the pH of the reaction medium at a level of at least 9.5, maintaining the reaction of the metal ions at a rate faster than the rate of precipitation of metals or metal oxides from the reaction medium for a time sufficient, by which only solid solution particles of metals or metal oxides having the same ratio of metals as the aqueous liquid solution are simultaneously precipitated; and
- B. separating the solid solution particles from the reaction medium.

Detailed Description of the Invention

The process of the invention can be used to make almost any solid solution of metals or metal polymeric oxides so long as the following conditions can be met:

- (1) it must be possible to prepare aqueous solutions of the metal ions;
- (2) the ions of both metals must react with a common reactant system to form their respective precipitation species;
- (3) the kinetics of the reactions which produce the precipitating species must be similar. That is, the reaction rates must be roughly of the same order of magnitude;
- (4) both reactions must be sufficiently pH-sensitive that the reaction rate of each can be adjusted to be faster than the precipitation of each species. In other words, the precipitation must become the rate-controlling step for both reactions; and
- (5) the rate of both reactions must nevertheless be slower than the rate at which the microdispersion of the reactants is formed. This requirement, of course, influences the choice of the high intensity mixing apparatus for use in the invention.

Typical metallic solid solutions for which the invention is likely to be used include Pd/Ag, Rh/Ag, Pd/Cu, Pd/Pt, Pd/Ni, Cu/Ag and Pt/Au.

Among the other useful applications of the process of the invention is the preparation of polynary oxide compounds which are frequently used as the dielectric component of multilayer capacitors. These materials include pyrochlore-type compounds such as ruthenates of Bi and Pb. Such materials are usually made by firing an admixture of the metals and/or metal oxides. However, they can be made more reliably and economically by the process of the invention which requires no high temperature processing. Similarly, the complex bismuth iridates and ruthenates of U.S. 3,583,931 can also be made by the process of the invention. It will be recognized by those skilled in the art that the invention is limited to those proportions of metals and metal oxides which form at least solid solutions and/or compounds. It will be recognized that in most instances any water-soluble compound of the metals or metal oxides can be used such as halides, nitrates and the like. However, it should be noted that chlorides must not be used in making silver-containing alloys because they cause precipitation of the silver as an insoluble salt.

As used herein, the term "solid solution" refers to a substitutional solid solution in which atoms of the solute metal (or oxide) become part of the space lattice of the solvent metal (or oxide), i.e., they take the place of some of the solvent atoms at lattice sites.

In some instances, the process of the invention may produce meta-stable solid solutions or glasses which can be stabilized by sintering to facilitate rearrangement of the atoms to a stable form. In general, the molar proportion of the metals or metal oxides in the process corresponds to their soluble proportions. It is not recommended to use an excess of any metal or metal oxide since it will be precipitated along with the desired alloy and act as an impurity in admixture with the desired solid solution. Therefore, it is preferred to employ the ionic solutions in approximately the same molar proportions as the solid solution which is sought. Thus, if a 70/30 Ag/Pd solid solution is sought, the molar proportions of the Ag and Pd ion solution should be substantially 70/30 also. The proportions of most metals that form solid solutions are readily available in the published literature.

Because the process of the invention is an ionic phenomenon, the preferred solvent for the ions is water. However, other water-compatible solvents can be used therewith, such as low molecular weight alkanols and glycols. Others will be apparent to those skilled in the art of ionic systems.

The ionic reactions which will be used in the process of the invention are pH sensitive. In particular, the reaction rate can be raised by increasing pH or lowered by decreasing pH. In general, it is preferred to use lower reaction rates which yield larger particles than those obtained at higher reaction rates. Nevertheless, the ionic reaction rate must still be sufficient that the precipitation of the solid solution is clearly the rate determining step.

Though heating the reaction system may increase the reaction rate somewhat, it is usually neither necessary nor preferred to heat the reactants or the reactor. Moreover, the heat of neutralization generated during the process is usually sufficient to raise the reaction temperature moderately to on the order of 70 - 80 °C.

To adjust the pH upward and therefore maintain the reaction rate sufficiently high, it is preferred to use a strong base because smaller volumes of base are required, thereby reducing the volume of fluids which must be mixed. It is preferred that the strong base have a pKa value of 11 and preferably 14. Preferred bases for this purpose are NaOH and KOH. Sodium carbonate can be used also; however it is not preferred because of its evolution of gas in the process. Ammonium hydroxide is not recommended in most instances because it is not strong enough and in some instances may form undesirable complexes and other by-products.

The reactant material which coreacts with the dissolved ions to form the insoluble species will vary widely depending upon the particular chemical reactions involved. However, it will frequently be a reductant material (reducing agent) or a combination of reductants. This is illustrated in the following table which lists several noble metal alloy systems and the reductant pairs which can be used to produce them in the process of the invention:

Table 1**REDUCTANT PAIRS FOR NOBLE
METAL SOLID SOLUTIONS**

Solid Solution Composition	Reductant Composition	
Pd/Au	For Pd Hypophosphorous Acid Sodium Hydro- sulfite	For Au Hydroquinone Hydrazine Sulfate Sulfurous Acid Sodium Sulfite Ferrous Sulfate
Pt/Au	For Pt Sodium borohydride Sodium hydro- sulfite	For Au Hydroquinone Hydrazine Sulfate Sulfurous Acid Sodium Sulfite Ferrous Sulfate
Pd/Ag	For Pd Sodium Boro- hydride Hypophosphorous Acid Hydroquinone	For Ag Sodium Formate Ammonium Formate Hydroxylamine Formic Acid Hydrazine Sulfate Tartaric Acid

As indicated in the above summary, it is necessary that the reactant liquids be mixed very rapidly to form a microdispersion and that the rate and size of the microdispersion must be sufficient to avoid any substantial precipitation of solids before the microdispersion is complete. Such microscale (diffusive) mixing must therefore be accomplished faster than the reaction rate of the reactant materials. The reaction time of ionic reactants of the type used in the invention are typically on the order of only a few milliseconds.

To form the required microdispersion of reactant liquids, it is necessary to use high intensity mixing apparatus. As used herein, the term high intensity mixing apparatus refers to those mixers which exhibit very high energy dissipation rates, such as on the order of 1000 HP per 1000 gallons (ca. 200 Joules/sec./liter) or higher. Typical mixers of this type are Waring® blenders, jet mixers, multiple jet mixers and side-T mixers. Others will be apparent to those skilled in the mixing art.

As mentioned above, it is also necessary that the microdispersion be maintained for a time sufficient to avoid any precipitation of separate metal species. Ordinarily this will be a matter of only a fraction of a second and therefore no separate operational step is required. Nevertheless, in situations where the precipitation step is quite slow, it may be necessary to adjust the rate of product offtake to allow sufficient residence time in the microdispersed state.

After removing the precipitated reaction product from the reactor, it is necessary to separate the solid solution particles from the reaction medium and by-products. Such solid-liquid separations can be accomplished quite easily by centrifugation and/or filtration methods which are well known in the unit operations arts. Drying of the separated particles can be accomplished by conventional means such as by solvent extraction and/or heating in air.

Depending on the particular metals being used in the process, the solid solution particles produced are quite small and have a surface area of 15-25 m²/g. Because the particles tend to be so small, they also tend to agglomerate and to result in dispersions which may vary in viscosity. It has been found, however, that the surface area of the particles can be reduced to on the order of 1-10 m²/g by heating them to 300-500°C for 1-16 hours. Higher temperatures can be used so long as the melting point of the solid solution is not exceeded. Thick film conductor pastes containing particles treated in this manner not only

have better viscosity stability but also thick film conductors made therefrom have better delamination resistance.

The process of the invention is likely to be most advantageous when carried out on a continuous basis. However, it can also be carried out on semicontinuous or even a batch basis.

The invention will be better understood by reference to the following examples. In the examples, particle size determinations were made by sedimentation techniques using the Sedigraph® 5000D particle size analyzer. Sedigraph is a tradename of the Micromeritics Instrument Corp., Northcross, GA, USA.

Comparative Example 1 - Prior Art Process

An attempt was made to synthesize a palladium silver alloy containing 1:1 weight ratio of palladium and silver via the method taught in U.S. 3,390,981. The procedure was as follows.

Fifty mL of concentrated commercial grade nitric acid was added to a 600 mL beaker containing 100 mL of deionized water. Twenty-five g of fine palladium powder and 0.5 g of NaNO_2 were added. The solution was stirred and heated to 50°C until all powder was dissolved. After all the powder is dissolved, the solution was transferred to a 4 L beaker equipped with a stirrer and an addition funnel. Four solutions were then prepared. Solution A was prepared by dissolving 256 g of ammonium nitrate in 280 mL of H_2O . Solution B was prepared by adding 39.4 g of silver nitrate in 150 mL of H_2O . Solution C was prepared by measuring out 125 mL of concentrated ammonium hydroxide and Solution D was prepared by measuring 130 mL of hypophosphorous acid into the addition funnel.

The palladium nitrate solution was neutralized in the beaker by adding ammonium hydroxide. The reaction was cooled to room temperature and then Solution A was added with stirring. After 1 minute, Solution B was added. After 2 minutes of elapsed time, Solution C was added. After 3 minutes of elapsed time, 5 mL of Solution D was added. Thereafter, the rest of Solution D was slowly added over the course of 30 minutes. The precipitate was then washed by decantation five times, filtered, and dried overnight at 60°C .

An x-ray diffraction pattern was taken of this material using $\text{CuK}\alpha_1$ radiation. Peaks were observed at 38.01° and 43.14° as well as 40.06° and 46.58° . These peaks are the ones expected for pure silver and pure palladium respectively. No peak was observed at either 39.05° or 44.86° , the expected peaks for a 50:50 solid solution of palladium and silver. Thus, it is evident that no solid solution was produced by the process taught by U.S. Patent 3,390,981.

Examples 1-3

An organic liquid solution of palladium nitrate was prepared by dissolving 350 g of palladium metal in 500 mL of commercially available concentrated nitric acid. The reaction was stirred overnight and any unreacted metal was removed by filtration. The solution was then standardized. The palladium concentration was determined by weighing a 1 mL aliquot of solution and then firing the aliquot at 1000°C for 15 minutes. After cooling, the residual metal was weighed and the per cent metal of the solution was determined as well as the molarity. The hydrogen ion concentration was determined by complexing the palladium ions with an added 5 g of sodium chloride to a 1 mL aliquot of solution. The hydrogen ions were then titrated with 0.1 molar solution of sodium hydroxide using a pH meter to indicate the endpoint. In a typical experiment, the palladium concentration was about 3.5 molar and the acid concentration was about 1 to 2 molar.

An aqueous silver nitrate solution was prepared by dissolving silver bullion in commercially available concentrated nitric acid. The solution was typically 6-7 molar in silver nitrate and 0.5 molar in nitric acid.

Using the above-described stock solution of palladium nitrate, a sufficient amount of stock was used to precipitate 1 kg of an alloy containing 30 weight per cent palladium. In a typical experiment, 841 mL of a stock solution containing 3.35 moles of palladium per liter of solution was combined with 991 mL of a 6.488 molar solution of silver nitrate. The resulting solution was then made up to a volume of 4 L using deionized water.

A second solution was prepared by diluting 474 mL of commercially available 13.5 molar formaldehyde solution to 4 L. This gave a solution that was 6.357/4 molar in formaldehyde. This represents a 5% molar excess of formaldehyde relative to the amount of metal to be reduced.

A third solution containing sodium hydroxide was prepared by dissolving 580 g of sodium hydroxide in 4 L of water. This is a sufficient amount to neutralize the residual acid in the metal solution, neutralize the protons released during the reaction and provide a 5% excess relative to the amount of metal to be reduced in the reaction.

The three solutions were placed in flasks. The solutions were then pumped to a reactor using peristaltic pumps. Flow meters on each of the solution lines were used to insure that the flow rates were maintained at 100 mL per minute. The lines from the metal solution and the line containing the formaldehyde were joined in a simple T connection before the reactor. The sodium hydroxide and the metal and formaldehyde solutions were then pumped to the reactor. A Waring blender was used as the reaction chamber. A third line connected to the reactor removed the reacted solution from the reactor with both intake and offtake lines being located just above the mixer impeller. This solution was pumped to a holding tank. After the reaction was complete, the solution was filtered and the powder was washed on the filter until the filtrate coring through the powder was at a pH of 8 or less. The filter cake was then dried using a freeze-dryer. Composition, yields and properties of three batches of Pd/Ag alloy made by the above-described process are given in Table 2 below:

Table 2
PREPARATION OF Pd/Ag ALLOYS

EXAMPLE NO.	<u>1</u>	<u>2</u>	<u>3</u>
Composition, % wt.			
Ag	69.3	69.4	69.4
Pd	29.0	28.7	29.0
Yield, %	99.4	95.7	98.5
Properties			
Surface Area, m ² /g	17.1	19.0	18.8
Particle Size, 50% point μ m	2.63	1.54	1.58
X-ray Diffraction Peaks, Degrees (CuK α_1)	38.7	38.9	38.9
	45.0	45.1	45.0

Examples 4-9

A series of Pd/Ag alloys was made by the method of Example 1 in which the amount of Pd was varied from 1.3 to 34.0 wt. % and the amount of reducing agent was increased accordingly. The resultant alloy compositions, yields and properties of the powders are given in Table 3 below:

Table 3

PREPARATION OF Pd/Ag ALLOYS
EFFECT OF INCREASING Pd CONCENTRATION

EXAMPLE NO.	<u>4</u>	<u>5</u>	<u>6</u>
Composition, % wt.			
Ag	97.9	96.7	94.6
Pd	1.3	2.3	4.2
Yield, %	>98	>98	>98
Properties			
Surface Area, m ² /g	6.0	-	5.7
Particle Size, 50% point μm	1.43	1.00	2.84
EXAMPLE NO.	<u>7</u>	<u>8</u>	<u>9</u>
Composition, % wt.			
Ag	87.5	78.4	64.6
Pd	11.5	20.1	34.0
Yield, %	>98	>98	>98
Properties			
Surface Area, m ² /g	6.9	14.1	18.5
Particle Size, 50% point μm	2.79	1.78	1.49

The foregoing data show that the alloys having higher levels of Pd in the alloy tended to have higher surface areas. It is interesting to note that between about 4 and 12% Pd, the alloy particles had larger particle sizes.

Examples 10-12

A further series of Pd/Cu alloys was made in the manner of Examples 1-3 except that a stoichiometric amount of hydrazine sulfate was used as the reducing agent and the amount of Cu was varied from 8.8 to 30.4%. Composition and volume of the reactant solutions were as follows:

1.0 liter aqueous solution of 164 g PdCl₂ and 52 g CuNO₃·2.5 H₂O

1.1 liter aqueous solution of 117 g hydrazine sulfate (H₂N₂)₂SO₄)

1.1 liter aqueous solution of NaOH.

Each of the procedures produced alloyed (solid solution) particles. It was interesting to note that the Pd/Cu alloy exhibited particle surface areas 2.5 to 3 times as high as the Pd/Ag alloys. The composition and surface area of the alloys from this series are given in Table 4 below:

Table 4

PREPARATION OF Pd/Cu ALLOYS

EXAMPLE NO.	<u>10</u>	<u>11</u>	<u>12</u>
Alloy Composition, % wt.			
Cu	30.4	24.3	8.8
Pd	69.6	75.7	85.9
Properties			
Surface Area, M ² /g	50.0	51.7	31.1

Example 13

A still further powdered alloy was prepared by the procedure of Examples 1-3 in which Rh was alloyed with Ag. In this example, Rh₂O₃ was dissolved in an excess of aqueous HNO₃ and combined with the AgNO₃ solution and the amount of base added was sufficient to neutralize the additional acid in the RhNO₃/AgNO₃ solution. The resultant alloy contained 99.5% Ag and 0.5% Rh. The surface area of the particle was 4.3 m²/g and the particle size 50% point was 1.36 μm. This alloy would be quite suitable for low conductivity Ag conductor compositions.

In all the foregoing Examples 1-13, the particulate products exhibited two x-ray diffraction peaks which were well removed from the known location of the peaks for the individual metals. Thus, it is clear that the powders produced by the process of the invention are true solid solutions.

Examples 14-18 and Comparative Example 2

A series of five 30/70 Pd/Ag alloy powders was prepared in the manner of Examples 1-3 in which the pH of reaction solutions was varied. As shown by the data in Table 5 below, more finely divided particles were produced at pH values above pH 9 and especially pH 9.5 and higher.

Table 5

PREPARATION OF Pd/Ag ALLOYS EFFECT OF pH ON PARTICLE SIZE		
Example No.	Reaction Solution pH	Particle Size μm
Comparative 2	9.0	9.8
14	9.5	2.6
15	10.0	1.7
16	10.5	1.4
17	11.0	1.2

Claims

1. A process for forming a solid solution of two or more metals or metal oxides by ionic reaction and precipitation from an aqueous reaction medium comprising the steps of:

A. In a high intensity mixing zone in which the energy dissipation rate is at least of 200 Joules/sec/liter, forming a reaction medium by mixing together an aqueous liquid solution of metal ions or metal oxide ions and at least a stoichiometric amount relative to the dissolved ions of a reactant fluid which is soluble in the aqueous solvent and which will react with the ions in the liquid phase to form metals or metal oxides therefrom and maintaining the pH of the reaction medium at a level of at least 9.5, maintaining the reaction of the metal ions at a rate faster than the rate of precipitation of metals or metal oxides from the reaction medium for a time sufficient, by which only solid solution particles of metals or metal oxides having the same ratio of metals as the aqueous

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liquid solution are simultaneously precipitated; and
B. separating the solid solution particles from the reaction medium.

2. The process of claim 1 in which one component of the solid solution is silver metal and in step A, the liquid ionic solution is free of halides and the reactant fluid is a reductant and the pH is maintained at a level of at least 11 by the addition of an hydroxide of an alkali or alkaline earth metal.
3. The process of claim 2 in which the solid solution is an alloy of silver and palladium.
4. The process of claim 2 in which the reductant is formaldehyde.
5. The process of claim 1 in which one component of the solid solution is RuO_2 and another component is selected from the group consisting of bismuth oxide, lead oxide and mixtures thereof, and the solid solution is a ruthenate of bismuth and/or lead having a pyrochlore-type structure.
6. The process of claim 1 in which one component of the solid solution is palladium metal and in step A, the reactant fluid is a reductant and the pH is maintained at a level of at least 11 by the addition of an hydroxide of an alkali or alkaline earth metal.
7. The process of claim 6 in which the solid solution is an alloy of palladium and copper.
8. The process of claim 7 in which the reductant is hydrazine.
9. The process of claim 1 in which the recovered particles are heated to at least 300°C but below the melting point of the solid solution to effect reduction of the surface area of the particles.

Patentansprüche

1. Verfahren zur Bildung einer Feststofflösung zweier oder mehrerer Metalle oder Metalloxide durch Ionenreaktion und Fällung aus einem wäßrigen Reaktionsmedium, umfassend die Schritte:
A. Bildung eines Reaktionsmediums in einer Zone sehr intensiver Vermischung, in der die Energie-dissipationsgeschwindigkeit wenigstens $200\text{ J/s}\cdot\text{l}$ ist, durch Zusammenmischen einer wäßrigen flüssigen Lösung von Metall-Ionen oder Metalloxyd-Ionen und wenigstens einer stöchiometrischen Menge, bezogen auf die gelösten Ionen, eines Fluid-Reaktionspartners, der in dem wäßrigen Lösungsmittel löslich ist und der mit den Ionen in der flüssigen Phase reagiert, um daraus Metalle oder Metalloxide zu bilden, und Halten des pH des Reaktionsmediums bei einem Wert von wenigstens 9,5; Halten der Reaktion der Metall-Ionen bei einer Geschwindigkeit, die höher ist als die Fällungsgeschwindigkeit der Metalle oder Metalloxide aus der Reaktionsmischung für eine genügend lange Zeit, wodurch nur Feststofflösungsteilchen der Metalle oder Metalloxide mit dem gleichen Verhältnis an Metallen wie die wäßrige flüssige Lösung gleichzeitig ausgefällt werden; und
B. Abtrennen der Feststofflösungsteilchen vom Reaktionsmedium.
2. Verfahren nach Anspruch 1, wobei eine Komponente der Feststofflösung metallisches Silber ist und die flüssige ionische Lösung bei Schritt A frei von Halogeniden ist und der Fluidreaktionspartner ein Reduktionsmittel ist und der pH durch Zugabe eines Alkali- oder Erdalkalimetallhydroxids auf einem Wert von wenigstens 11 gehalten wird.
3. Verfahren nach Anspruch 2, wobei die Feststofflösung eine Legierung aus Silber und Palladium ist.
4. Verfahren nach Anspruch 2, wobei das Reduktionsmittel Formaldehyd ist.
5. Verfahren nach Anspruch 1, wobei eine Komponente der Feststofflösung RuO_2 ist, und eine weitere Komponente ausgewählt ist aus der Gruppe bestehend aus Bismutoxyd, Bleioxyd und deren Mischungen, und die Feststofflösung ein Ruthenat von Bismut und/oder Blei mit einer Struktur vom Pyrochlore-Typ ist.
6. Verfahren nach Anspruch 1, wobei eine Komponente der Feststofflösung metallisches Palladium ist und der Fluidreaktionspartner bei Schritt A ein Reduktionsmittel ist und der pH durch Zugabe eines Alkali-



oder Erdalkalimetallhydroxids auf einem Wert von wenigstens 11 gehalten wird.

7. Verfahren nach Anspruch 6, wobei die Feststofflösung eine Legierung aus Palladium und Kupfer ist.
8. Verfahren nach Anspruch 7, wobei das Reduktionsmittel Hydrazin ist.
9. Verfahren nach Anspruch 1, wobei die gewonnenen Teilchen auf wenigstens 300° C, aber unterhalb des Schmelzpunkts der Feststofflösung erhitzt werden, um Reduktion des Oberflächenbereichs der Teilchen zu bewirken.

Revendications

1. Un procédé de formation d'une solution solide d'au moins deux métaux ou oxydes métalliques par réaction ionique et précipitation à partir d'un milieu réactionnel aqueux, comprenant les étapes suivantes:

A. dans une zone de mélange à intensité élevée, dans laquelle le taux de dissipation de l'énergie est au moins égal à 200 Joules/seconde/litre, on forme un milieu réactionnel en mélangeant une solution liquide aqueuse d'ions métalliques ou d'ions d'oxydes métalliques avec au moins une quantité stoechiométrique, par rapport aux ions dissous, d'un fluide réactif qui est soluble dans le solvant aqueux et qui peut réagir avec les ions en phase liquide pour former des métaux ou oxydes métalliques à partir de ceux-ci, le pH du milieu réactionnel étant maintenu au moins à 9,5, et l'on maintient la vitesse de réaction des ions métalliques à une valeur supérieure à la vitesse de précipitation des métaux ou des oxydes métalliques à partir du milieu réactionnel pendant un temps suffisant, de façon à ce que, seules des particules de solution solide de métaux ou d'oxydes métalliques offrant le même rapport de métaux que la solution liquide aqueuse soient simultanément précipitées;

B. on sépare les particules de solution solide du milieu réactionnel.

2. Le procédé selon la revendication 1, caractérisé en ce que l'un des composants de la solution solide est de l'argent métallique et que, dans l'étape A, la solution ionique liquide est exempte d'halogénure, le fluide réactif est un agent réducteur et le pH est maintenu à une valeur au moins égale à 11 par addition de l'hydroxyde d'un métal alcalin ou d'un métal alcalino-terreux.
3. Le procédé selon la revendication 2, caractérisé en ce que la solution solide est un alliage d'argent et de palladium.
4. Le procédé selon la revendication 2, caractérisé en ce que l'agent réducteur est le formaldéhyde.
5. Le procédé selon la revendication 1, caractérisé en ce que l'un des composants de la solution solide est le RuO₂, un autre composant est choisi dans le groupe constitué par: oxyde de bismuth, oxyde de plomb et leurs mélanges, et la solution solide est un ruthénate de bismuth et/ou de plomb présentant une structure de type pyrochlore.
6. Le procédé selon la revendication 1, caractérisé en ce que l'un des composants de la solution solide est du palladium métallique et que, dans l'étape A, le fluide réactif est un agent réducteur et le pH est maintenu à une valeur au moins égale à 11 par addition de l'hydroxyde d'un métal alcalin ou d'un métal alcalino-terreux.
7. Le procédé selon la revendication 6, caractérisé en ce que la solution solide est un alliage de palladium et de cuivre.
8. Le procédé selon la revendication 7, caractérisé en ce que l'agent réducteur est l'hydrazine.
9. Le procédé selon la revendication 1, caractérisé en ce que les particules récupérées sont chauffées à une température au moins égale à 300° C, mais qui est inférieure au point de fusion de la solution solide, pour effectuer une réduction de l'aire surfacique des particules.

