

DescriptionDiscussion of the Background:

6 In many applications of gases, such as the manufacture of VLSI chips, high purity gases are needed during the manufacturing process to avoid, among others, the creation of defects during the various masking steps of the process. Avoiding such defects enhances the manufacture output of the process as well as the reliability of the chips. There is also a need for high purity gases in the optical, aerospace and pharmaceutical industries.

10 Various impurities such as particles or vapors may be present in compressed gases stored in a container such as a cylinder. It is known from the article entitled "A gas filtration system for concentrations of 10^{-5} particles/cm³" from G. Kasper and H.Y. Wen; published in Aerosol Science and Technology 5: 167-185 (1986), that "totally" particle-free process gases may be obtained. Particle analysis has been also carefully studied by the same authors and the results of this study has been published in the Proceedings -
 15 Institute of Environmental Sciences - May 6, 1987 - in an article entitled "Particle Analysis in cylinder gases".

Trace quantities of condensible vapors such as hydrocarbons or fluorinated hydrocarbons in gases are commonly detected and quantified by a variety of means such as chromatography in the gas phase, infrared (IR) absorption spectroscopy, mass spectrometry, total hydrocarbon detectors, etc.

20 Pressure reduction by critical orifice is commonly used in pressure regulators. For the purpose of sampling particles from compressed gases of pressure up to $34,5 \cdot 10^5$ Pa (500 psi), a pressure reducer, consisting of a clean orifice, a chamber into which the gas can expand, and a means to sample part of the expanding jet, can achieve "zero" particle shedding. Such a unit can be purchased from Liquid Air Corporation.

25 It is known that very high concentration of fine particles can be generated during the pressure reduction process if the upstream pressure exceeds a few hundred psi depending on the gas purity (J. Aerosol Sci., 19, 153, 1988). The particle concentration decreases with decreasing upstream pressure and drops to zero typically at pressures within the range of $20,7 \cdot 10^5$ Pa (300 psi) to $41,4 \cdot 10^5$ Pa (600 psi). It is documented that these particles are formed from condensation of trace amount of vapor impurities in the compressed
 30 gases.

The removal of vapor impurities (purification) is conventionally accomplished with the help of molecular sieve or activated carbon. This approach however may totally distort the original particle spectra and concentrations in the compressed gases.

35 Utilization of the differences in diffusion coefficients to remove unwanted nitric acid vapor from a gas stream to obtain true particulate nitrate is a common practice among air pollution researchers, where it is called "acid denuder". A basic coating is usually applied to the collection surfaces to retain the acid vapors, which may shed significant particles to upset the purpose of sampling particles from high-purity gases. The system is at ambient pressure. No temperature control is provided.

40 In view of the considerable demand for high purity gases and high purity gases containing particles there is therefore a strongly felt need for a method for separating condensible vapors from particles in a highly compressed gas. Such a method would ideally not affect the spectra or concentration of the particles in the compressed gas.

45 It is also known from EP-A-0312457 and EP-A-0312458 to generate droplets of condensible vapors in a carrier gas through a critical orifice and to discharge a carrier gas containing condensible vapors through a plurality of orifices without causing the condensation of the condensible vapors.

SUMMARY OF THE INVENTION

50 It is an object of this invention to provide a process for removing condensible vapors from a compressed gas containing particles, without affecting the spectra or concentration of these particles in the compressed gas.

The inventors have now discovered a process as defined in claim 1 which satisfies this object of this invention, and other objects which will become apparent from the description of the invention given hereinbelow.

55 The invention furthermore provides processes as defined in respectively claim 4 and claim 5.

In the process of the present invention, a starting compressed gas containing condensible vapors and particles is passed through a flow system. The flow system used comprises simple geometries and polished, clean surfaces. The flow rate of the compressed gas through the flow system and the flow system

geometry are selected such that particles having a diameter greater than 0.01 micrometers have a collision efficiency of less than 5% with the flow system surfaces and condensible vapor molecules have a collision efficiency of at least 98% with the flow system surfaces. The temperature of the flow system surfaces is then controlled to retain collided vapor molecules on the surfaces. This process produces a product
 5 compressed gas which is free of condensable vapors and contains the spectra and concentration of particles of the starting compressed gas.

BRIEF DESCRIPTION OF THE FIGURES

10 A more complete appreciation of the invention and many of its attendant advantages will be readily obtained as the same becomes better understood by reference to the following detailed description when considered in connection with the accompanying figures, wherein:

FIGURE 1 illustrates background particle levels generated by condensation as a function of the cylinder (gas) pressure;

15 FIGURE 2 provides a schematic illustration of a design useful for particle sampling from high pressure gas cylinders;

FIGURE 3 provides a comparison of particle concentration below $41,4 \times 10^5$ Pa (600 psia) and above $41,4 \times 10^5$ Pa (600 psia), showing no particle loss due to the use of a cold trap in the system; and

FIGURE 4 provides particle concentration data in high pressure gas cylinders with different histories.

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

The invention provides a process for removing trace amount of condensible vapor impurities from highly compressed gases without disturbing the original particle size spectra and concentrations in the
 25 compressed gas. These condensible vapors can convert into particles under conditions of large temperature drop or pressure drop and totally distort the original particle information.

In accordance with the present invention, compressed gases are defined as comprising, among others, a carrier gas and condensible vapors. The compound gases may have pressures ranging from $6,9 \times 10^5$ Pa (100 psia) to $20,7 \times 10^6$ Pa (3000 psia). The carrier gas may be, e.g. nitrogen (N_2), argon, helium, carbon
 30 dioxide, carbon monoxide, hydrogen, methane, ethane, propane, etc.

Condensible vapors are defined for the present purposes as species which will condense to form droplets upon sufficient cooling of the carrier gas or upon contacting a sufficiently cool surface (*vide infra*), e.g. C_5-16 hydrocarbons or C_5-16 fluorinated hydrocarbons, etc., and higher hydrocarbons or fluorinated hydrocarbons which can include up to C_{30} hydrocarbons/fluorinated hydrocarbons under some circum-
 35 stances, such as when these vapors are present in a very low concentration. These condensible vapors are however present in their gaseous state before cooling and not as droplets.

The method of the invention thus distinguishes itself from other detection methods for preexisting particles and specifically from methods for the detection of preexisting oil droplets in gases which require the preexistence of such droplets. An example of such methods is given in U.S.-A-4794086

40 The present invention provides for the removal of either global amounts of condensible vapors or individual components within a "family" of such species (for example hydrocarbons).

One important application of the method of this invention, in conjunction with a critical orifice pressure reducer, is the analysis of particles present in highly compressed gases, e.g. cylinder gases. Such particle analysis is of critical importance to a variety of industrial processes that utilize ultra-pure, compressed
 45 gases and is a major topic of research on microcontamination. However, there is no current practical means for this particle analysis from compressed gases of pressure greater than $48,26 \times 10^5$ Pa (700 psi) because particles generated from condensible vapors during pressure reduction are usually orders of magnitude more numerous than the original particles (Figure 1).

Another important application of the present invention is that this method can be used for the purpose
 50 of purification of gases, especially during the cylinder filling process, to obtain ultra-clean gases. The present method is superior to conventional method in "zero" particle generation and low pressure drop.

The invention removes condensible vapors in a flow system of simple geometries and of polished, clean surfaces, such as art electro-polished round tube, an annular tube, or a rectangular slit. The term "simple" geometries" is used to indicate that these flow systems do not have sharp turns and/or dead
 55 spaces to trap particles.

It is well documented that particle loss can be significant in a flow system with complex geometry. The polished, clean surface of the flow systems used in this invention can prevent particle shedding or reentrainment, which is well recognized as a significant problem for rough surfaces.

The conventional vapor removing process (usually referred to as purification) utilizes complex flow systems with rough surfaces and porous pellets which can generate or trap substantial amount of particles. This conventional process is therefore not compatible with particle sampling and analysis.

The particles contained in the compound gases treated in this invention have diameters of at least 0.01 μm . The invention selectively removes condensable vapor molecules without affecting the particles in the gas stream.

It is well known that the diffusion coefficients for gas molecules are orders of magnitude larger than those of particles. For example, the diffusion coefficient for air molecules is $0.19 \text{ cm}^2.\text{s}^{-1}$ versus $0.00052 \text{ cm}^2.\text{s}^{-1}$ for particles of 0.01 μm diameter. (Note: 0.01 μm is currently the practical lower limit of detection by commonly used particle counters. The diffusion coefficient decreases further with increasing particle diameter.)

Accordingly, the collision frequency with the tube walls is much higher for vapor molecules than for particles. For convenience, we define the collision efficiency (CE) as the fraction of the species of interest that collide with the walls.

By proper selection of flow rate, tube geometry, and tube length, it is possible to devise a system with negligible collision efficiency (e.g., 5%) for particles greater than 0.01 μm while having nearly 100% (e.g., >98%) collision efficiency for vapor molecules.

The collision efficiency in laminar flow can be calculated from

$$\begin{aligned} \text{CE} &= 5.50 K^{2/3} - 3.77 K \text{ for } K < 0.007 \\ \text{CE} &= 1 - 0.819 \exp(-11.5K) \text{ for } K > 0.007 \end{aligned}$$

where

$K = DL/Q$ for round tube

$K = DLW/QH$ for rectangular slit

where D is the diffusion coefficient, L the tube length, Q the flow rate, W the width of the slit, and H the height of the slit.

Tables 1 to 3 list the collision efficiency in a round tube for various tube lengths, flow rates, and diffusion coefficients. The range of diffusion coefficients covers most commonly encountered vapor species.

The last row of each table indicates the diffusion loss of 0.01 μm particles. The loss decreases with increasing particle size.

Table 1. L = 30 cm

6	Q (L/m) =	1	5	10	20
	D (cm ² /s)				
	0.2	0.987	0.642	0.459	0.334
10	0.1	0.897	0.459	0.334	0.268
	0.05	0.709	0.334	0.268	0.222
15	0.0005 (0.01 μ m)	0.048	0.017	0.011	0.007

Table 2. L = 60 cm

20	Q (L/m) =	1	5	10	20
	D (cm ² /s)				
25	0.2	1.000	0.844	0.642	0.459
	0.1	0.987	0.642	0.459	0.334
	0.05	0.897	0.459	0.334	0.268
30	0.0005 (0.01 μ m)	0.075	0.026	0.017	0.011

Table 3. L = 90 cm

40	Q (L/m) =	1	5	10	20
	D (cm ² /s)				
	0.2	1.000	0.932	0.763	0.560
45	0.1	0.998	0.763	0.560	0.400
	0.05	0.963	0.560	0.400	0.299
50	0.0005 (0.01 μ m)	0.097	0.034	0.022	0.014

The present process retains the collided vapor molecules on the tube walls by controlling the wall temperature. When vapor molecules collide with the wall, the molecules may stick or rebound depending upon the physical and chemical interactions occurring between the vapor and the collection surface. Conventional purification process rely on the adsorption properties of the collection surface to retain vapor molecules.

In the present invention the sticking probability of the colliding molecules is increased by decreasing the surface temperature. As the surface temperature decreases systematically, different species of trace vapors can be selectively removed. The temperature control can be obtained by a mechanical refrigerator or a reservoir of dry ice or liquid nitrogen. The suitable temperature ranges lie between the boiling point of the gas to be sampled and the lowest boiling point of the condensable vapors to be removed. In the present invention, at least a portion of the surface sufficient to trap the condensable vapors must be cooled.

The invention further provides a process for identifying the species of vapor impurities in cylinder gases. After trapping an adequate amount of vapor impurities, heated, clean gases can be directed through the tube to desorb the trapped vapors. Fourier transform infrared spectroscopy (FTIR), gas-chromatography (GC), or other instruments can be used on-line to identify the species of the trapped vapors.

Figure 2 shows the schematic design for the application of sampling particles from cylinder gases. The tube length and the temperature control method employed here only serve as an example. A 0,635 cm (1/4 inch) SSEP tubing of 1,22m (4 feet) long submerged in a dry ice-freon reservoir served as the vapor removing device (cold trap). The temperature of the cold trap was -78°C . The required tube length can be found in Table 1 to 3 for different applications. With this design, the background particle levels, generated from reentrainment and condensation, were controlled well.

The temperature control can be facilitated by a mechanical freezer, a jet-expansion device, or a reservoir filled with different liquefied gases.

The detected background particle concentration with an absolute filter in-line but by-passing the cold trap is given in Figure 1, which illustrates background particle levels, generated by condensation, as a function of cylinder (gas) pressure. Figure 1 illustrates that particle concentration increases with cylinder Pressure. The CNC counts are two orders of magnitude higher than the LAS-X counts. The detected background particle concentration with the cold trap is given in Table 4. The background level can be further reduced by employing a lower flow rate, a longer tube in the cold trap or a lower reservoir temperature.

Figure 3 shows that the use of a cold trap does not cause extra particle loss. Figure 3 provides particle concentration data for a turbulently filled cylinder. The concentration of the particles remains the same with and without the cold trap at pressures less than $41,4 \times 10^5$ Pa (600 psi), where no condensation occurs.

Figure 4 shows examples of measuring true particle concentration in turbulent-filled and aged cylinders by employing the present method. Figure 4 provides particle concentrations for high pressure gases in cylinders with different histories.

As this graph illustrates, the concentration of particles can be different by two orders of magnitude depending on the history of the high pressure gas in the cylinder. Notably, with well-aged high pressure gases in cylinders (i.e. with gases which have been stored under high pressure in cylinders and undisturbed for at least one month), the concentration of particles is relatively low. As seen from a comparison of the two curves provided in Figure 4 for particle concentrations in well-aged high pressure gas cylinders, without the present invention, it is not possible to measure the Particle content of a gas obtained from a well-aged cylinder at pressures greater than $68,95 \times 10^5$ (1,000 psia) (see Figure 1).

Table 4

Achievable Particle Background With a Filter and a Cold Trap					
Test Pressure (PSIA) 10^5 Pa		CNC $>0.01 \mu\text{m}$ Particles/scf	LAS-X		
			$>0.2 \mu\text{m}$ Particles/scf	$>0.3 \mu\text{m}$ Particles/scf	$>0.5 \mu\text{m}$ Particles/scf
500	34,475	3.2	0	0	0
1000	68,95	4.8	2.4	2.4	0
1500	103,93	16	4.0	1.3	0
1800	124,11	90	25	14	3.1
2000	137,9	209	46	25	9.2

**Claims**

1. A process for removing condensible vapors from a compressed gas containing condensible vapors and particles without affecting the spectra or concentration of said particles in said compressed gas, said process comprising:
- 5 (i) passing a starting compressed gas containing condensible vapors and particles through a flow apparatus without sharp turns and/or dead spaces to trap particles, preferably an electro-polished round tube, an annular tube or a rectangular slit, the flow apparatus comprising polished clean surfaces;
- 10 (ii) selecting (iia) a compressed gas flow rate through said flow apparatus and (iib) a flow apparatus length and geometry, such that particles having a diameter greater than 0.01 μm have a collision efficiency of less than 5% with said flow apparatus surfaces and condensible vapor molecules have a collision efficiency of at least 98% with said flow apparatus surfaces;
- 15 (iii) controlling the temperature of at least a portion of the surfaces of said flow apparatus to retain collided vapor molecules on said portion of the surfaces; and
- (iv) obtaining a product compressed gas free of condensible vapors and containing the spectra and concentration of particles of said starting compound gas.
2. The process of Claim 1, wherein said condensible vapors comprise a hydrocarbon or a fluorinated hydrocarbon.
3. The process of Claim 1 or 2, comprising charging a cylinder with said product compressed gas.
4. A process for identifying the species of condensible vapor impurities in a compressed gas, comprising:
- 25 (i) passing a starting compressed gas containing condensible vapors through a flow apparatus length and geometry, such that particles having a diameter greater than 0.01 μm have a collision efficiency of less than 5% with said flow apparatus surfaces and condensible vapor molecules have a collision efficiency of at least 98% with said flow apparatus surfaces, said flow apparatus being comprised of simple geometrics without sharp turns and/or dead spaces, preferably an electro-polished round tube or a rectangular slit, and being comprised of polished, clean surfaces;
- 30 (ii) selecting (iia) a compressed gas flow rate through said flow apparatus and (iib) a flow apparatus length and geometry, such that particles in said gas having a diameter greater than 0.01 μm have a collision efficiency of less than 5% with said flow apparatus surfaces and said condensible vapor molecules have a collision efficiency of at least 98% with said flow apparatus surfaces;
- 35 (iii) controlling the temperature of at least a portion of the surfaces of said flow apparatus to retain collided vapor molecules on said portion of the surfaces;
- (iv) replacing said starting compressed gas passing through said flow apparatus with a clean gas and desorbing said retained vapor molecules;
- 40 (v) identifying the vapor molecules.
5. A process for the analysis of particles present in a compressed gas, comprising:
- (i) passing a starting compressed gas containing condensible vapors and particles through a flow apparatus length and geometry, such that particles having a diameter greater than 0.01 μm have a collision efficiency of less than 5% with said flow apparatus surfaces and condensible vapor molecules have a collision efficiency of at least 98% with said flow apparatus surfaces, said flow apparatus being comprised of simple geometrics without sharp turns and/or dead spaces, preferably an electro-polished round tube, an annular tube or a rectangular slit, and being comprised of polished, clean surfaces;
- 45 (ii) selecting (iia) a compressed gas flow rate through said flow apparatus and (iib) a flow apparatus length and geometry such that particles having a diameter greater than 0.01 μm have a collision efficiency of less than 5% with said flow apparatus surfaces and condensible vapor molecules have a collision efficiency of at least 98% with said flow apparatus surfaces;
- 50 (iii) controlling the temperature of at least a portion of the surfaces of said flow system to retain collided vapor molecules on said portion of the surfaces;
- 55 (iv) obtaining a product compressed gas free of condensible vapors and containing the spectra and concentration of particles of said starting compressed gas;
- (v) analyzing the particles present in said product compressed gas.

**Patentansprüche**

1. Verfahren zum Entfernen kondensierbarer Dämpfe aus einem komprimierten Gas, das kondensierbare Dämpfe und Partikel enthält, ohne die Spektren oder die Konzentration dieser Partikel in dem komprimierten Gas zu beeinträchtigen, wobei das Verfahren umfaßt:

(i) Leiten eines kondensierbare Dämpfe und Partikel enthaltenden komprimierten Startgases durch eine Durchlaufvorrichtung ohne scharfe Windungen und/oder Toträume, in denen sich Partikel absetzen, bevorzugt ein elektropoliertes rundes Rohr, ein ringförmiges Rohr oder einen rechteckigen Schlitz, wobei die Durchlaufvorrichtung polierte saubere Oberflächen umfaßt;

(ii) Auswählen (iia) eines Durchflusses des komprimierten Gases durch die Durchlaufvorrichtung und (iib) einer Länge und Geometrie der Durchlaufvorrichtung derart, daß Partikel mit einem Durchmesser größer als $0,01\mu\text{m}$ einen Kollisionswirkungsgrad von weniger als 5% mit den Oberflächen der Durchlaufvorrichtung und kondensierte Dampfmoleküle einen Kollisionswirkungsgrad von mindestens 98% mit den Oberflächen der Durchlaufvorrichtung haben;

(iii) Steuern der Temperatur von zumindest einem Bereich der Oberflächen der Durchlaufvorrichtung zum Zurückhalten kollidierter Dampfmoleküle auf diesem Bereich der Oberflächen; und

(iv) Gewinnen eines komprimierten Produktgases, das frei von kondensierten Dämpfen ist und die Spektren und die Konzentration der Teilchen des komprimierten Startgases hat.

2. Verfahren nach Anspruch 1, wobei die kondensierbaren Dämpfe Kohlenwasserstoff oder fluorierten Kohlenwasserstoff umfassen.

3. Verfahren nach Anspruch 1 oder 2, umfassend das Befüllen eines Zylinders mit dem komprimierten Produktgas.

4. Verfahren zum Identifizieren der Art kondensierbarer Dampfverunreinigungen in einem komprimierten Gas, umfassend:

(i) Leiten eines kondensierbare Dämpfe enthaltenden komprimierten Startgases durch eine Durchlaufvorrichtung mit einer Länge und Geometrie derart, daß Partikel mit einem größeren Durchmesser als $0,01\mu\text{m}$ einen Kollisionswirkungsgrad von weniger als 5 % mit den Oberflächen der Durchlaufvorrichtung und kondensierbare Dampfmoleküle einen Kollisionswirkungsgrad von zumindest 98% mit den Oberflächen der Durchlaufvorrichtung haben, wobei die Durchlaufvorrichtung eine einfache Geometrie ohne scharfe Windungen und/oder Toträume, bevorzugt einem elektropolierten runden Rohr, einem ringförmigen Rohr oder einem rechteckigen Schlitz hat und polierte, saubere Oberflächen umfaßt;

(ii) Auswählen (iia) eines Durchflusses des komprimierten Gases durch die Durchlaufvorrichtung und (iib) einer Länge und Geometrie der Durchlaufvorrichtung derart, daß Partikel mit einem Durchmesser größer als $0,01\mu\text{m}$ in diesem Gas einen Kollisionswirkungsgrad von weniger als 5% mit den Oberflächen der Durchlaufvorrichtung und kondensierte Dampfmoleküle einen Kollisionswirkungsgrad von mindestens 98% mit den Oberflächen der Durchlaufvorrichtung haben;

(iii) Steuern der Temperatur von zumindest einem Bereich der Oberflächen der Durchlaufvorrichtung zum Zurückhalten kollidierter Dampfmoleküle auf diesem Bereich der Oberflächen;

(iv) Ersetzen des die Durchlaufvorrichtung durchsetzenden komprimierten Startgases durch ein sauberes Gas und Desorbieren der zurückgehaltenen Dampfmoleküle;

(v) Identifizieren der Dampfmoleküle.

5. Verfahren zur Analyse von in einem komprimierten Gas vorhandenen Partikeln, umfassend:

(i) Leiten eines kondensierbare Dämpfe und Partikel enthaltenden komprimierten Startgases durch eine Durchlaufvorrichtung mit einer Länge und Geometrie derart, daß Partikel mit einem größeren Durchmesser als $0,01\mu\text{m}$ einen Kollisionswirkungsgrad von weniger als 5 % mit den Oberflächen der Durchlaufvorrichtung und kondensierbare Dampfmoleküle einen Kollisionswirkungsgrad von zumindest 98% mit den Oberflächen der Durchlaufvorrichtung haben, wobei die Durchlaufvorrichtung eine einfache Geometrie ohne scharfe Windungen und/oder Toträume, bevorzugt einem elektropolierten runden Rohr, einem ringförmigen Rohr oder einem rechteckigen Schlitz hat und polierte, saubere Oberflächen umfaßt;

(ii) Auswählen (iia) eines Durchflusses des komprimierten Gases durch die Durchlaufvorrichtung und (iib) einer Länge und Geometrie der Durchlaufvorrichtung derart, daß Partikel mit einem Durchmesser größer als $0,01\mu\text{m}$ einen Kollisionswirkungsgrad von weniger als 5% mit den Oberflächen der



Durchlaufvorrichtung und kondensierte Dampfmoleküle einen Kollisionswirkungsgrad von mindestens 98% mit den Oberflächen der Durchlaufvorrichtung haben;

(iii) Steuern der Temperatur von zumindest einem Bereich der Oberflächen der Durchlaufvorrichtung zum Festhalten kollidierter Dampfmoleküle auf diesem Bereich der Oberflächen;

5 (iv) Gewinnen eines komprimierten Produktgases, das frei von kondensierten Dämpfen ist und die Spektren und die Konzentration der Teilchen des komprimierten Startgases hat;

(v) Analysieren der im komprimierten Produktgas vorhandenen Partikel.

Revendications

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1. Procédé d'enlèvement des vapeurs condensables d'un gaz comprimé renfermant des vapeurs condensables et des particules, sans affecter les spectres ou la concentration desdites particules dans ledit gaz comprimé, ledit procédé comprenant:

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(i) faire passer un gaz comprimé de départ renfermant des vapeurs condensables et des particules dans un dispositif de débit sans courbes raides et/ou des espaces sans issu pouvant retenir les particules, de préférence une tubulure ronde électro-polie, une tubulure annulaire ou une fente rectangulaire, le dispositif de débit comprenant des surfaces polies et propres;

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(ii) choisir (iia) un taux de débit de gaz comprimé à travers ledit dispositif de débit et (iib) une longueur et une géométrie du dispositif de débit, faisant en sorte que les particules ayant un diamètre supérieur à 0,01 μm ont une efficacité de collision inférieure à 5% avec lesdites surfaces du dispositif de débit et les molécules de vapeur condensables possèdent une efficacité de collision d'au moins 98% avec lesdites surfaces dudit dispositif de débit;

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(iii) régler la température d'au moins une portion desdites surfaces dudit dispositif de débit pour retenir les molécules de vapeur entrant en collision sur ladite portion des surfaces; et

(iv) obtenir un produit gazeux comprimé libre de vapeur condensable et contenant les spectres et une concentration de particules dudit composé gazeux de départ.

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2. Procédé selon la revendication 1, où lesdites vapeurs condensables comprennent un hydrocarbure ou un hydrocarbure fluoré.

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3. Procédé selon la revendication 1 ou 2, comprenant le chargement d'un cylindre avec ledit produit gazeux comprimé.

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4. Procédé d'identification des espèces d'impuretés des vapeurs condensables dans un gaz comprimé, comprenant:

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(i) faire passer un gaz comprimé de départ renfermant des vapeurs condensables sur la longueur et la géométrie d'un dispositif de débit, de façon à ce que les particules ayant un diamètre supérieur à 0,01 μm possèdent une efficacité de collision inférieure à 5% avec lesdites surfaces du dispositif de débit et les molécules de vapeur condensable possèdent une efficacité de collision d'au moins 98% avec lesdites surfaces du dispositif de débit, ledit dispositif de débit comprenant des surfaces à géométrie simple, polies et propres;

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(ii) choisir (iia) un taux de débit de gaz comprimé à travers ledit dispositif de débit et (iib) lequel comporte une longueur ayant une géométrie, en sorte que les particules dans ledit gaz ayant un diamètre supérieur 0,01 μm possèdent une efficacité de collision inférieure à 5% avec lesdites surfaces du dispositif de débit et lesdites molécules de vapeur condensable possèdent une efficacité de collision d'au moins 98% avec lesdites surfaces du dispositif de débit, ledit dispositif de débit comprenant des surfaces à géométries simples, sans courbes raides et/ou espaces sans issus, de préférence une tubulure ronde électro-polie ou une fente rectangulaire, et comprenant des surfaces polies, et propres;

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(iii) régler la température d'au moins une portion des surfaces dudit dispositif de débit pour retenir les molécules de vapeur en collision sur ladite portion des surfaces;

(iv) remplacer ledit gaz comprimé de départ passant dans ledit dispositif de débit avec un gaz propre et effectuer la désorption desdites molécules de vapeur qui y sont retenues;

(v) identifier les molécules de vapeur.

5. Procédé d'analyse des particules présentes dans un gaz comprimé, comprenant:

(i) faire passer un gaz comprimé de départ renfermant des vapeurs condensables sur la longueur et la géométrie d'un dispositif de débit, de façon à ce que les particules ayant un diamètre supérieur à



0.01 μm possèdent une efficacité de collision inférieure à 5% avec lesdites surfaces dudit dispositif de débit et les molécules de vapeur condensables possèdent une efficacité de collision d'au moins 98% avec lesdites surfaces du dispositif de débit, ledit dispositif de débit comprenant des géométries simples, sans courbes raides et/ou des espaces sans issu, de préférence une tubulure ronde électro-polie, une tubulure annulaire ou une fente rectangulaire, et comprenant des surfaces polies et propres;

(ii) choisir (iia) un taux de débit de gaz comprimé dans ledit dispositif de débit et (iib) une longueur et une géométrie du dispositif de débit faisant en sorte que les particules possédant un diamètre supérieur à 0,01 μm ont une efficacité de collision inférieure à 5% avec lesdites surfaces du dispositif de débit et les molécules de vapeur condensable possèdent une efficacité de collision d'au moins 98% avec lesdites surfaces du dispositif de débit;

(iii) régler la température d'au moins une portion des surfaces dudit système de débit pour retenir les molécules de vapeur en collision sur ladite portion des surfaces;

(iv) obtenir un produit gazeux comprimé libre de vapeur condensable et contenant les spectres et une concentration de particule dudit gaz comprimé de départ;

(v) analyser les particules présentes dans ledit produit gazeux comprimé.