

A BARRIER MATERIAL COMPRISING A THERMOPLASTIC AND
A COMPATIBLE CYCLODEXTRIN DERIVATIVE

Field of the Invention

5 The invention relates to thermoplastic polymeric compositions used as packaging materials with barrier properties. The thermoplastic barrier material can take the form of a barrier coating, a flexible film, a semi-rigid or rigid sheet or a rigid structure. The
10 thermoplastic barrier materials can also take the form of a coating manufactured from an aqueous or solvent based solution or suspension of thermoplastic film forming components containing as one component, the barrier forming materials. Such a film sheet or coating
15 material can act as a barrier to a variety of permeants including water vapor; organics such as aliphatic and aromatic hydrocarbons, aliphatic and aromatic halides, heterocyclic hydrocarbons, alcohols, aldehydes, amines, carboxylic acids, ketones, ethers, esters, sulfides,
20 thiols, monomers, etc.; off flavors and off odors, etc. The thermoplastic barrier compositions of the invention can be extruded, laminated or molded into a variety of useful films, sheets, structures or shapes using conventional processing technology. Further, the
25 monolayer, bilayer or multilayer films can be coated, printed or embossed.

Background of the Invention

30 Much attention has been directed to the development of packaging materials in a film, a semi-rigid or rigid sheet and a rigid container made of a thermoplastic composition. In such applications, the polymeric composition preferably acts as a barrier to the passage of a variety of permeant compositions to prevent contact
35 between ,e.g., the contents of a package and the permeant. Improving barrier properties is an important goal for manufacturers of film and thermoplastic resins.

Barrier properties arise from both the structure

and the composition of the material. The order of the structure (i.e.), the crystallinity or the amorphous nature of the material, the existence of layers or coatings can affect barrier properties. The barrier property of many materials can be increased by using liquid crystal or self-ordering molecular technology, by axially orienting materials such as an ethylene vinyl alcohol film, or by biaxially orienting nylon films and by using other useful structures. Internal polymeric structure can be crystallized or ordered in a way to increase the resistance to permeation of a permeant. A material can be selected, for the thermoplastic or packaging coating, which prevents absorption of a permeant onto the barrier surface. The material can also be selected to prevent the transport of the permeant through the barrier. Permeation that corresponds to Fick's law and non-Fickian diffusion has been observed. Generally, permeation is concentration and temperature dependent regarding mode of transport.

The permeation process can be described as a multistep event. First, collision of the permeant molecule with the polymer is followed by sorption into the polymer. Next, migration through the polymer matrix by random hops occurs and finally the desorption of the penetrant from the polymer completes the process. The process occurs to eliminate an existing chemical concentration difference between the outside of the film and the inside of the package. Permeability of an organic molecule through a packaging film consists of two component parts, the diffusion rate and solubility of the molecule in the film. The diffusion rate measures how fast molecule transport occurs through the film. It affects the ease with which a permeant molecule moves within a polymer. Solubility is a measure of the concentration of the permeant molecule that will be in position to migrate through the film. Diffusion and solubility are important measurements of a

barrier film's performance. There are two types of mechanisms of mass transfer for organic vapors permeating through packaging films: capillary flow and activated diffusion. Capillary flow involves small molecules permeating through pinholes or highly porous media. This is of course an undesirable feature in a high barrier film. The second, called activated diffusion, consists of solubilization of the penetrants into an effectively non-porous film at the inflow surface, diffusion through the film under a concentration gradient (high concentration to low concentration), and release from the outflow surface at a lower concentration. In non-porous polymeric films, therefore, the mass transport of a penetrant includes three steps - sorption, diffusion, and desorption. Sorption and desorption depend upon the solubility of the penetrant in the film. The process of sorption of a vapor by a polymer can be considered to involve two stages: condensation of the vapor onto the polymer followed by solution of the condensed vapor into the polymer. For a thin-film polymer, permeation is the flow of a substance through a film under a permeant concentration gradient. The driving force for permeation is given as the pressure difference of the permeant across the film. Several factors determine the ability of a permeant molecule to permeate through a membrane: size, shape, and chemical nature of the permeant, physical and chemical properties of the polymer, and interactions between the permeant and the polymer.

A permeant for this application means a material that can exist in the atmosphere at a substantial detectable concentration and can be transmitted through a known polymer material. A large variety of permeants are known. Such permeants include water vapor, aromatic and aliphatic hydrocarbons, monomer compositions and residues, off odors, off flavors, perfumes, smoke,

pesticides, toxic materials, etc. A typical barrier material comprises a single layer of polymer, a two layer coextruded or laminated polymer film, a coated monolayer, bilayer or multilayer film having one or more
5 coatings on a surface or both surfaces of the film or sheet.

The two most widely used barrier polymers for food packaging are ethylene-vinyl alcohol copolymers (EVOH) ethylene vinyl acetate copolymers (EVA) and
10 polyvinylidene chloride (PVDC). Other useful thermoplastics include ethylene acrylic materials including ethylene acrylic acid, ethylene methacrylic acid, etc. Such polymers are available commercially and offer some resistance to permeation of gases, flavors,
15 aromas, solvents and most chemicals. PVDC is also an excellent barrier to moisture while EVOH offers very good processability and permits substantial use of regrind materials. EVOH copolymer resins are commonly used in a wide variety of grades having varying ethylene
20 concentrations. As the ethylene content is reduced, the barrier properties to gases, flavors and solvents increase. EVOH resins are commonly used in coextrusions with polyolefins, nylon or polyethylene terephthalate (PET) as a structural layer. Commercially, amorphous
25 nylon resins are being promoted for monolayer bottles and films. Moderate barrier polymer materials such as monolayer polyethylene terephthalate, polymethyl pentene or polyvinyl chloride films are available.

Substantial attention is now directed to a variety
30 of technologies for the improvement of barrier properties. The use of both physical barriers and active chemical barriers or traps in packaging materials are under active investigation. In particular, attention has focused on use of specific copolymer and
35 terpolymer materials; the use of specific polymer alloys, the use of improved coatings for barrier material such as silica metals, organometallics, and

other strategies.

Another important barrier technology involves the use of oxygen absorbers or scavengers that are used in polymeric coatings or in bulk polymer materials.

5 Metallic reducing agents such as ferrous compounds, powdered oxide or metallic platinum can be incorporated into barrier systems. These systems scavenge oxygen by converting it into a stable oxide within the film. Non-metallic oxygen scavengers have also been developed and
10 are intended to alleviate problems associated with metal or metallic tastes or odors. Such systems include compounds including ascorbic acid (vitamin C) and salts. A recent introduction involves organometallic molecules that have a natural affinity for oxygen. Such molecules
15 absorb oxygen molecules into the interior polymer chemical structure removing oxygen from the internal or enclosed space of packaging materials.

Packaging scientists are continuing to develop new polymeric films, coated films, polymeric alloys, etc.
20 using blends of materials to attain higher barrier properties. Many of these systems have attained some degree of utility but have failed to achieve substantial commercial success due to a variety of factors including obtaining barrier performance at low cost.

25 One problem that arises when searching for polymer blends or compounded polymeric materials, relates to the physical properties of the film. Films must retain substantial clarity, tensile strength, resistance to penetration, tear resistance, etc. to remain useful in
30 packaging materials. Blending unlike materials into a thermoplastic before film extrusion often results in a substantial reduction of film properties. Finding compatible polymer materials for polymer alloys, and compatible additives for polymeric materials typically
35 require empirical demonstration of compatibility and does not follow a clearly developed theory. However compatibility can be demonstrated by showing that the

compounded material obtains an improved barrier quality with little reduction in clarity, processability, or structural properties using conventional test methods. Accordingly, a substantial need exists for development of materials that can be incorporated into polymeric material to form a packaging thermoplastic having excellent barrier properties without any substantial reduction in structural properties.

10 **Brief Discussion of the Invention**

I have found that the barrier properties of a thermoplastic polymer can be improved, without any important reduction in clarity, processability or structural properties, by forming a barrier layer with a dispersed compatible cyclodextrin derivative in the polymer. I have developed two embodiments. The first comprises a barrier made using the thermoplastic technology containing the cyclodextrin derivative. The second, a coating made by casting a solution or suspension of a film forming polymer or polymer forming material combined with the cyclodextrin derivative to form a barrier layer. The cyclodextrin molecule without a compatible substituent group is not sufficiently compatible in the bulk material to result in a clear useful barrier layer or packaging material. The compatible cyclodextrin derivative is a compound substantially free of an inclusion complex. For this invention the term "substantially free of an inclusion complex" means that the quantity of the dispersed cyclodextrin derivative in the film contains a large fraction having cyclodextrin rings free of a permeant in the interior of the cyclodextrin molecule. The cyclodextrin compound will be added without complex, but some complexing can occur during manufacture from polymer degradation or from inks or coatings components. The internal cavity of the cyclodextrin remains unoccupied by any complexed molecule.

The cyclodextrin derivative has a substituent group bonded to the cyclodextrin molecule that is compatible with the polymeric material. Cyclodextrin is a cyclic dextran molecule having six or more glucose moieties in the molecule. Preferably, the cyclodextrin is an α -cyclodextrin (α CD), a β -cyclodextrin (β CD), a γ -cyclodextrin (γ CD) or mixtures thereof. We have found that the derivatization of the cyclodextrin molecule is essential for forming a cyclodextrin material that can be effectively blended into the thermoplastic bulk polymer material with no loss in clarity, processability or structural or packaging properties. The substituents on the cyclodextrin molecule are selected to possess a composition, structure and polarity to match that of the polymer to ensure that the cyclodextrin is sufficiently compatible in the polymer material. Further, a derivatized cyclodextrin is selected that can be blended into the thermoplastic polymer, formed into film, semirigid or rigid sheet or other rigid structural materials using conventional thermoplastic manufacturing techniques. Lastly, we have found that the cyclodextrin material can be used in forming such thermoplastic barrier structures without any substantial reduction in structural properties. The film can provide a trap or barrier to contaminant materials from the polymer matrix and from the product storage and use environment. Thermoplastic polymers used in manufacturing packaging film materials are typically products made by polymerizing monomers resulting from refinery processes. Any refinery stream used in polymerization chemistry, contains residual monomer, trace level refinery hydrocarbons, catalyst and catalyst by-products as impurities in the polymer matrix. Further, the environment in which materials are packaged after production, stored and used, often contain substantial proportions of contaminants that can permeate through a barrier film or sheet and can contaminate food or other

packaged items. Residual polymer volatiles are complexed by dispersing cyclodextrin into molten film polymer using an extruder. The residents time or mixing time of CD and molten polymer in the barrel of the extruder initiates the complexation of residual polymer volatiles. With environmental contaminants diffusing through the polymer, uncomplexed cyclodextrin dispersed in the polymer is believed to reside, not only between the polymer molecule chains, but in vaguely defined cavities between the polymer chains. As the permeant diffuses through the polymer on a tortuous path, the uncomplexed cyclodextrin is available to complex permeant molecules as they diffuse through the film. Some continual complexation and release of the same guest between cyclodextrin molecules in the film is possible. In other words, the cyclodextrin dispersed in the film is complexing and releasing. The diffusion rate may increase due to the number and size of the cavities caused by the presence of cyclodextrin. The modified cyclodextrin preferably has chemical properties that are compatible with the polymer and are of a size and shape that does not adversely affect the film's barrier property.

The beneficial effect of cyclodextrin over other high-barrier film technologies is twofold. First, cyclodextrin has the ability to complex residual organic volatile contaminants inherent in all polyethylene and polypropylene packaging films. Secondly, cyclodextrin offers the unique ability to complex permeants that may otherwise diffuse through the package film-improving product quality and safety.

Since all packaging films are permeable to organic vapors, measuring the amount that permeates through the film over time is an important performance measurement of a particular packaging film. The permeation process described above is fast for low-water-activity packaged food products (crackers, cookies, cereals). The process

of permeation can be faster or slower depending on the relative humidity outside the package and the product's storage temperature. As the relative humidity outside the package increase, the pressure differential between the outside and inside the package is greater. The greater the differential and/or the higher the temperature, the faster the organic permeants will diffuse through the film. The method used to test the film samples in this research used the worst case (60% relative humidity outside the package and 0.25 water activity inside the package) shelf-life storage conditions to accelerate the outcome of the testing. The organic permeant concentration used has been obtained from food products contaminated by inks used in printing on packaging materials, adhesive systems used in polymer or paper or foil laminations, or numerous environmental contaminants originating from gasoline, diesel fuel, paint solvent, cleaning materials, product fragrance, food products, etc. The relative humidity, water activity and permeant concentration have been used to test numerous high-barrier films presently used in the industry today. The testing has effectively demonstrated performance differences between various high-barrier films. Four test parameters are important in the performance of the high barrier film. First is the time it takes the permeant to begin diffusing through the package wall known as "lag-time", second, the rate the permeant diffuses through the film, third, the total amount of permeant that can pass through the film over a given time, and fourth, the effectiveness of the barrier to the permeant challenge.

Figure 1 is a graphical representation of the dimensions of the cyclodextrin molecule without derivatization. The α , β and γ cyclodextrins are shown.

Figure 2 is a schematic diagram of the extruder used to form the films set forth in Table I.

Figure 3 is a diagram of a test device used in measuring the permeability of the films of the inventions.

We have also found that inclusion of the
5 cyclodextrin derivatives in the thermoplastic materials of the invention can improve other properties of the film such as surface tension, static charge properties and other properties that improve the adaptability of this barrier material to coating and printing. The
10 cyclodextrin derivative materials can be included in a variety of a thermoplastic film and sheet.

Detailed Description of the Invention

15 Film

A film or a sheet is a flat unsupported section of a thermoplastic resin whose thickness is much smaller than its width or length. Films are generally regarded as being 0.25 millimeters (mm) or less, typically 0.01
20 to 20 mm thick. Sheet may range from about 0.25 mm to several centimeters (cm), typically 0.3 to 3 mm in thickness. Film or sheet can be used alone or in combination with other sheet, fabric or structural units through lamination, coextrusion or coating. For the
25 invention the term "web" includes film, sheet, semi-rigid and rigid sheet and formed rigid units. Important properties include tensile strength, elongation, stiffness, tear strength and resistance; optical properties including haze, transparency; chemical
30 resistance such as water absorption and transmission of a variety of permeant materials including water vapor and other permeants; electrical properties such as dielectric constant; and permanence properties including shrinkage, cracking, weatherability, etc.

35 Thermoplastic materials can be formed into barrier film using a variety of processes including blown thermoplastic extrusion, linear biaxially oriented film

extrusion and by casting from molten thermoplastic resin, monomer or polymer (aqueous or organic solvent) dispersion. These methods are well known manufacturing procedures. The characteristics in the polymer thermoplastics that lead to successful barrier film formation are as follows. Skilled artisans manufacturing thermoplastic polymers have learned to tailor the polymer material for thermoplastic processing and particular end use application by controlling molecular weight (the melt index has been selected by the thermoplastic industry as a measure of molecular weight -- melt index is inversely proportional to molecular weight, density and crystallinity). For blown thermoplastic extrusion polyolefins (LDPE, LLDPE, HDPE) are the most frequently used thermoplastic polymers, although polypropylene, nylon, nitriles, PETG and polycarbonate are sometimes used to make blown film. Polyolefins typically have a melt index from 0.2 to 3 grams/10 mins., a density of about 0.910 to about 0.940 grams/cc, and a molecular weight that can range from about 200,000 to 500,000. For biaxially oriented film extrusion the polymer most often used are olefin based - chiefly polyethylene and polypropylene (melt index from about 0.4 to 4 grams/10 mins. and a molecular weight of about 200,000 to 600,000). Polyesters and nylons can also be used. For casting, molten thermoplastic resin or monomer dispersion are typically produced from polyethylene or polypropylene. Occasionally, nylon, polyester and PVC are cast. For roll coating of aqueous based acrylic urethane and PVDC, etc. dispersions are polymerized to an optimum crystallinity and molecular weight before coating.

A variety of thermoplastic materials are used in making film and sheet products. Such materials include poly(acrylonitrile-co-butadiene-co-styrene) polymers, acrylic polymers such as the polymethylmethacrylate, poly-n-butyl acrylate, poly(ethylene-co-acrylic acid),

poly(ethylene-co-methacrylate), etc.; cellophane, cellulosics including cellulose acetate, cellulose acetate propionate, cellulose acetate butyrate and cellulose triacetate, etc.; fluoropolymers including
5 polytetrafluoroethylene (teflon), poly(ethylene-co-tetrafluoroethylene) copolymers, (tetrafluoroethylene-co-propylene) copolymers, polyvinyl fluoride polymers, etc., polyamides such as nylon 6, nylon 6,6, etc.; polycarbonates; polyesters such as poly(ethylene-co-
10 terephthalate), poly(ethylene-co-1,4-naphthalene dicarboxylate), poly(butylene-co-terephthalate); polyimide materials; polyethylene materials including low density polyethylene; linear low density polyethylene, high density polyethylene, high molecular
15 weight high density polyethylene, etc.; polypropylene, biaxially oriented polypropylene; polystyrene, biaxially oriented polystyrene; vinyl films including polyvinyl chloride, (vinyl chloride-co-vinyl acetate) copolymers, polyvinylidene chloride, polyvinyl alcohol, (vinyl
20 chloride-co-vinylidene dichloride) copolymers, specialty films including polysulfone, polyphenylene sulfide, polyphenylene oxide, liquid crystal polyesters, polyether ketones, polyvinylbutyrl, etc.

Film and sheet materials are commonly manufactured
25 using thermoplastic techniques including melt extrusion, calendaring, solution casting, and chemical regeneration processes. In many manufacturing steps an axial or a biaxial orientation step is used. The majority of film and sheet manufactured using melt extrusion techniques.
30 In melt extrusion, the material is heated above its melting point in an extruder typically having an introduction section 27, a melt region 28 and an extruder section 29. The melt is introduced to a slot die resulting in a thin flat profile that is rapidly
35 quenched to solid state and oriented. Typically the hot polymer film after extrusion is rapidly chilled on a roll or drum or using an air stream. Ultimately, a

quenching bath can be used. Thermoplastic materials can also be blown. The hot melt polymer is extruded in Fig. 2 in an annular die 22 in a tube form 21. The tube is inflated with air (see air inlet 26) to a diameter
5 determined by the desired film properties and by practical handling considerations. As the hot melt polymer emerges from the annular die, the extruded hot tube is expanded by air to 1.2 or four (4) times its initial die diameter. At the same time the cooling air
10 (see air flow 20) chills the web forming a solid extruded with a hollow circular cross section 21. The film tube is collapsed within a V-shaped frame 23 and is nipped at the end of the frame (nip rolls 24) to trap air within the thus formed bubble. Rolls 24 and 25 draw
15 the film from the die maintaining a continuous production of the extruded tube.

We have found that in the preparation of biaxially oriented film and in the production of blown thermoplastic film that the melt temperature and the die
20 temperature are important in obtaining the permeability or permeant transmission rates preferred for films of the invention, to reduce melt fracture and to improve film uniformity (reduce surface defects). Referring to Figure 2, the temperature of the melt at the melt region
25 28 should range from about 390-420°F, preferably 395-415°F. The temperature of the extrusion die 29 should range from about 400-435°F, preferably 410-430°F. The extruded polymer can be cooled using ambient water baths or ambient air. The extruder can be operated at through
30 put such that production rates can be maintained but the polymer can be sufficiently heated to achieve the melt and die temperatures required. Production of the films of the invention at these temperatures ensures that the cyclodextrin material is fully compatible in the
35 thermoplastic melt, is not degraded by the high temperatures and a clear compatible useful barrier film is produced.



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REPLACED

Often two thermoplastic materials are joined in a coextrusion process to produce tailored film or sheet products adapted to a particular end use. One or more polymer types in two or more layers of melt are coextruded in a coextrusion die to have a film with versatile properties dried from both layers. Layers of the different polymers or resins are combined by either blending the materials in melt before extrusion or by parallel extrusion of the different thermoplastics. The melt flows laminarily through the die and onto a quenched drum. The film is processed conventionally and may be oriented after cooling. Films can contain a variety of additives such as antioxidants, heat stabilizers, UV stabilizers, slip agents, fillers, and anti-block agents.

The barrier layer of the invention can be made by casting an aqueous dispersion or solvent dispersion or solution of a film forming polymer and the cyclodextrin derivative. The aqueous or solvent based material can be formed by commonly available aqueous or solvent based processing of commercially available polymers, polymer dispersions, polymer solutions or both polymer and common aqueous or solvent processing technology. The cyclodextrin derivative material can be combined with such aqueous or solvent based dispersions or solutions to form a film forming or readily formed coating material. Such barrier layers or barrier coatings can be formed using commonly available coating technology including roller coating, doctor blade coating, spin coating, etc. While the coatings can be made and removed from a preparative surface, commonly coatings are formed on a thermoplastic or thermosetting polymer web, and remain in place to act as a barrier layer on a polymeric web used in a packaging. The typical coatings can be made from the same thermoplastic polymer materials used in film sheet or other structural layers using substantially similar loadings of the cyclodextrin

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derivative material. The barrier layer or barrier coatings formed using the film forming polymer and the cyclodextrin derivative can be used as a single coating layer or can be used in a multiple coating structure having a barrier layer or coating on one or both sides of a structural film or sheet which can be used with other coating layers including printing layers, clear coating layers and other layers conventional in packaging, food packaging, consumer product packaging, etc.

Cyclodextrin

The thermoplastic films of the invention contain a cyclodextrin having pendent moieties or substituents that render the cyclodextrin material compatible with the thermoplastic polymer. For this invention, compatible means that the cyclodextrin material can be uniformly dispersed into the melt polymer, can retain the ability to trap or complex permeant materials or polymer impurity, and can reside in the polymer without substantial reductions in polymer film characteristics. Compatibility can be determined by measuring polymer characteristics such as tensile strength, tear resistance, etc., permeability or transmission rates for permeants, surface smoothness, clarity, etc. Non-compatible derivatives will result in substantial reduced polymer properties, very high permeability or transmission rates and rough dull film. Qualitative compatibility screening can be obtained by preparing small batches (100 grams-one kilogram of thermoplastic and substituted cyclodextrin). The blended material is extruded at production temperatures as a linear strand extrudate having a diameter of about one to five mm. Incompatible cyclodextrin materials will not disperse uniformly in the melt and can be seen in the transparent melt polymer immediately upon extrusion from the extrusion head. We have found the incompatible



cyclodextrin can degrade at extrusion temperatures and produce a characteristic "burnt flour" odor in an extrusion. Further, we have found that incompatible cyclodextrin can cause substantial melt fracture in the extrudate which can be detected by visual inspection. Lastly, the extrudate can be cut into small pieces, cross-sectioned and examined using an optical microscope to find incompatible cyclodextrin clearly visible in the thermoplastic matrix. Cyclodextrin is a cyclic oligosaccharide consisting of at least six glucopyranose units joined by $\alpha(1\rightarrow4)$ linkages. Although cyclodextrin with up to twelve glucose residues are known, the three most common homologs (α cyclodextrin, β cyclodextrin and γ cyclodextrin) having 6, 7 and 8 residues have been used.

Cyclodextrin is produced by a highly selective enzymatic synthesis. They consist of six, seven, or eight glucose monomers arranged in a donut shaped ring, which are denoted α , β , or γ cyclodextrin respectively (See Figure 1). The specific coupling of the glucose monomers gives the cyclodextrin a rigid, truncated conical molecular structure with a hollow interior of a specific volume. This internal cavity, which is lipophilic (i.e.,) is attractive to hydrocarbon materials (in aqueous systems is hydrophobic) when compared to the exterior, is a key structural feature of the cyclodextrin, providing the ability to complex molecules (e.g., aromatics, alcohols, halides and hydrogen halides, carboxylic acids and their esters, etc.). The complexed molecule must satisfy the size criterion of fitting at least partially into the cyclodextrin internal cavity, resulting in an inclusion complex.

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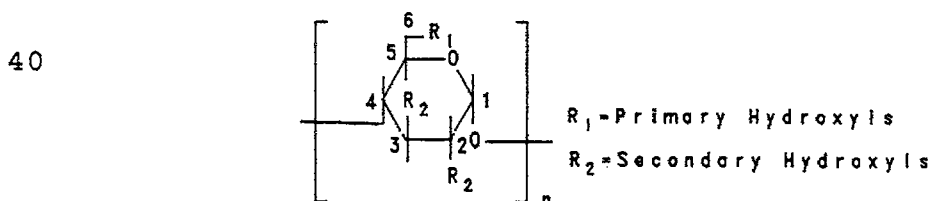
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CYCLODEXTRIN TYPICAL PROPERTIES

PROPERTIES	CD	α -CD	β -CD	γ -CD
5 Degree of Polymerization (n =)		6	7	8
Molecular Size (A°)				
10 inside diameter		5.7	7.8	9.5
outside diameter		13.7	15.3	16.9
height		7.0	7.0	7.0
15 Specific Rotation $[\alpha]_D^{25}$		+150.5	+162.5	+177.4
Color of iodine complex		Blue	Yellow	Yellowish Brown
20 Solubility in water (g/100 ml) 25°C				
25 Distilled Water		14.50	1.85	23.20

The oligosaccharide ring forms a torus, as a truncated cone, with primary hydroxyl groups of each glucose residue lying on a narrow end of the torus. The secondary glucopyranose hydroxyl groups are located on the wide end. The parent cyclodextrin molecule, and useful derivatives, can be represented by the following formula (the ring carbons show conventional numbering) in which the vacant bonds represent the balance of the cyclic molecule:



wherein R_1 and R_2 are primary or secondary hydroxyl as shown.

Cyclodextrin molecules have available for reaction with a chemical reagent the primary hydroxyl at the six position, of the glucose moiety, and at the secondary hydroxyl in the two and three position. Because of the geometry of the cyclodextrin molecule, and the chemistry of the ring substituents, all hydroxyl groups are not equal in reactivity. However, with care and effective reaction conditions, the cyclodextrin molecule can be reacted to obtain a derivatized molecule having all hydroxyl groups derivatized with a single substituent type. Such a derivative is a persubstituted cyclodextrin. Cyclodextrin with selected substituents (i.e.) substituted only on the primary hydroxyl or selectively substituted only at one or both the secondary hydroxyl groups can also be synthesized if desired. Further directed synthesis of a derivatized molecule with two different substituents or three different substituents is also possible. These substituents can be placed at random or directed to a specific hydroxyl. For the purposes of this invention, the cyclodextrin molecule needs to contain sufficient thermoplastic compatible substituent groups on the molecule to insure that the cyclodextrin material can be uniformly dispersed into the thermoplastic and when formed into a clear film, sheet or rigid structure, does not detract from the polymer physical properties.

Apart from the introduction of substituent groups on the CD hydroxyl other molecule modifications can be used. Other carbohydrate molecules can be incorporated into the cyclic backbone of the cyclodextrin molecule. The primary hydroxyl can be replaced using SN_2 displacement, oxidized dialdehyde or acid groups can be formed for further reaction with derivatizing groups, etc. The secondary hydroxyls can be reacted and removed leaving an unsaturated group to which can be added a

variety of known reagents that can add or cross a double bond to form a derivatized molecule.

Further, one or more ring oxygen of the glycan moiety can be opened to produce a reactive site. These
5 techniques and others can be used to introduce compatibilizing substituent groups on the cyclodextrin molecule.

The preferred preparatory scheme for producing a derivatized cyclodextrin material having a functional
10 group compatible with the thermoplastic polymer involves reactions at the primary or secondary hydroxyls of the cyclodextrin molecule. Broadly we have found that a broad range of pendant substituent moieties can be used on the molecule. These derivatized cyclodextrin
15 molecules can include acylated cyclodextrin, alkylated cyclodextrin, cyclodextrin esters such as tosylates, mesylate and other related sulfo derivatives, hydrocarbyl-amino cyclodextrin, alkyl phosphono and alkyl phosphato cyclodextrin, imidazolyl substituted
20 cyclodextrin, pyridine substituted cyclodextrin, hydrocarbyl sulphur containing functional group cyclodextrin, silicon-containing functional group substituted cyclodextrin, carbonate and carbonate substituted cyclodextrin, carboxylic acid and related
25 substituted cyclodextrin and others. The substituent moiety must include a region that provides compatibility to the derivatized material.

Acyl groups that can be used as compatibilizing functional groups include acetyl, propionyl, butyryl,
30 trifluoroacetyl, benzoyl, acryloyl and other well known groups. The formation of such groups on either the primary or secondary ring hydroxyls of the cyclodextrin molecule involve well known reactions. The acylation reaction can be conducted using the appropriate acid
35 anhydride, acid chloride, and well known synthetic protocols. Peracylated cyclodextrin can be made. Further, cyclodextrin having less than all of available

hydroxyls substituted with such groups can be made with one or more of the balance of the available hydroxyls substituted with other functional groups.

Cyclodextrin materials can also be reacted with alkylating agents to produce an alkylated cyclodextrin. Alkylating groups can be used to produce peralkylated cyclodextrin using sufficient reaction conditions exhaustively react available hydroxyl groups with the alkylating agent. Further, depending on the alkylating agent, the cyclodextrin molecule used in the reaction conditions, cyclodextrin substituted at less than all of the available hydroxyls can be produced. Typical examples of alkyl groups useful in forming the alkylated cyclodextrin include methyl, propyl, benzyl, isopropyl, tertiary butyl, allyl, trityl, alkyl-benzyl and other common alkyl groups. Such alkyl groups can be made using conventional preparatory methods, such as reacting the hydroxyl group under appropriate conditions with an alkyl halide, or with an alkylating alkyl sulfate reactant.

Tosyl (4-methylbenzene sulfonyl) mesyl (methane sulfonyl) or other related alkyl or aryl sulfonyl forming reagents can be used in manufacturing compatibilized cyclodextrin molecules for use in thermoplastic resins.

The primary -OH groups of the cyclodextrin molecules are more readily reacted than the secondary groups.

However, the molecule can be substituted on virtually any position to form useful compositions.

Such sulfonyl containing functional groups can be used to derivatize either of the secondary hydroxyl groups or the primary hydroxyl group of any of the glucose moieties in the cyclodextrin molecule. The reactions can be conducted using a sulfonyl chloride reactant that can effectively react with either primary or secondary hydroxyl. The sulfonyl chloride is used at appropriate mole ratios depending on the number of

target hydroxyl groups in the molecule requiring substitution. Both symmetrical (per substituted compounds with a single sulfonyl moiety) or unsymmetrical (the primary and secondary hydroxyls substituted with a mixture of groups including sulfonyl derivatives) can be prepared using known reaction conditions. Sulfonyl groups can be combined with acyl or alkyl groups generically as selected by the experimenter. Lastly, monosubstituted cyclodextrin can be made wherein a single glucose moiety in the ring contains between one and three sulfonyl substituents. The balance of the cyclodextrin molecule remaining unreacted.

Amino and other azido derivatives of cyclodextrin having pendent thermoplastic polymer containing moieties can be used in the sheet, film or container of the invention. The sulfonyl derivatized cyclodextrin molecule can be used to generate the amino derivative from the sulfonyl group substituted cyclodextrin molecule via nucleophilic displacement of the sulfonate group by an azide (N_3^-) ion. The azido derivatives are subsequently converted into substituted amino compounds by reduction. Large numbers of these azido or amino cyclodextrin derivatives have been manufactured. Such derivatives can be manufactured in symmetrical substituted amine groups (those derivatives with two or more amino or azido groups symmetrically disposed on the cyclodextrin skeleton or as a symmetrically substituted amine or azide derivatized cyclodextrin molecule. Due to the nucleophilic displacement reaction that produces the nitrogen containing groups, the primary hydroxyl group at the 6-carbon atom is the most likely site for introduction of a nitrogen containing group. Examples of nitrogen containing groups that can be useful in the invention include acetylamino groups (-NHAc), alkylamino including methylamino, ethylamino, butylamino, isobutylamino, isopropylamino, hexylamino, and other

alkylamino substituents. The amino or alkylamino substituents can further be reactive with other compounds that react with the nitrogen atom to further derivatize the amine group. Other possible nitrogen containing substituents include dialkylamino such as dimethylamino, diethylamino, piperidino, piperizino, quaternary substituted alkyl or aryl ammonium chloride substituents, halogen derivatives of cyclodextrins can be manufactured as a feed stock for the manufacture of a cyclodextrin molecule substituted with a compatibilizing derivative. In such compounds the primary or secondary hydroxyl groups are substituted with a halogen group such as fluoro, chloro, bromo, iodo or other substituents. The most likely position for halogen substitution is the primary hydroxyl at the 6-position.

Hydrocarbyl substituted phosphono or hydrocarbyl substituted phosphato groups can be used to introduce compatible derivatives onto the cyclodextrin. At the primary hydroxyl, the cyclodextrin molecule can be substituted with alkyl phosphato, aryl phosphato groups. The 2, and 3, secondary hydroxyls can be branched using an alkyl phosphato group.

The cyclodextrin molecule can be substituted with heterocyclic nuclei including pendent imidazole groups, histidine, imidazole groups, pyridino and substituted pyridino groups.

Cyclodextrin derivatives can be modified with sulfur containing functional groups to introduce compatibilizing substituents onto the cyclodextrin. Apart from the sulfonyl acylating groups found above, sulfur containing groups manufactured based on sulfhydryl chemistry can be used to derivatize cyclodextrin. Such sulfur containing groups include methylthio (-SMe), propylthio (-SPR), t-butylthio (-S-C(CH₃)₃), hydroxyethylthio (-S-CH₂CH₂OH), imidazolylmethylthio, phenylthio, substituted

phenylthio, aminoalkylthio and others. Based on the ether or thioether chemistry set forth above, cyclodextrin having substituents ending with a hydroxyl aldehyde ketone or carboxylic acid functionality can be prepared. Such groups include hydroxyethyl, 3-hydroxypropyl, methyloxyethyl and corresponding oxeme isomers, formyl methyl and its oxeme isomers, carbylmethoxy ($-O-CH_2-CO_2H$), carbylmethoxymethyl ester ($-O-CH_2CO_2-CH_3$). Cyclodextrin with derivatives formed using silicone chemistry can contain compatibilizing functional groups.

Cyclodextrin derivatives with functional groups containing silicone can be prepared. Silicone groups generally refer to groups with a single substituted silicon atom or a repeating silicone-oxygen backbone with substituent groups. Typically, a significantly proportion of silicone atoms in the silicone substituent bear hydrocarbyl (alkyl or aryl) substituents. Silicone substituted materials generally have increased thermal and oxidative stability and chemical inertness. Further, the silicone groups increase resistance to weathering, add dielectric strength and improve surface tension. The molecular structure of the silicone group can be varied because the silicone group can have a single silicon atom or two to twenty silicon atoms in the silicone moiety, can be linear or branched, have a large number of repeating silicone-oxygen groups and can be further substituted with a variety of functional groups. For the purposes of this invention the simple silicone containing substituent moieties are preferred including trimethylsilyl, mixed methyl-phenyl silyl groups, etc. We are aware that certain β CD and acetylated and hydroxy alkyl derivatives are available from American Maize-Products Co., Corn Processing Division, Hammond, IN.

Packages and Packed Items

The thermoplastic containing the compatible derivatized cyclodextrin can be used in a variety of packaging formats to package a variety of items. General packaging ideas can be used. For example, the

5 items can be packaged entirely in a film pouch, bag, etc. Further, the film can be used as a film closure on a rigid plastic container. Such containers can have a rectangular, circular, square or other shaped cross-section, a flat bottom and an open top. The container

10 and a thermoplastic film closure can be made of the thermoplastic materials of the invention. Further, the thermoplastics of the invention can be used in the formation of blister pack packaging, clam shell type enclosures, tub, tray, etc. Generally, two product

15 types require packaging in thermoplastic film of the invention having substantial barrier properties. In one product type, protecting the product from contamination from permeant sources outside the packaging material is important. Protecting food items from contamination by

20 aromatic and aliphatic hydrocarbons, fluorocarbons, ink and packaging residue, exhaust from transportation equivalent and other internal combustion engines, perfumes commonly used in a variety of consumer products such as scented paper products, bar soap, scented bath

25 products, cleaners, fabric softeners, detergents, dry bleaches, disinfectants, etc. All food items are the most common material requiring protection from outside contamination, other items can be sensitive to odors. Further, a variety of materials must be packaged in

30 barrier materials preventing the odor of the material from exiting the package. A large variety of food odors are readily transmitted by a variety of packaging materials. Such food odors can attract insect and rodent pests, can be objectionable to customers or

35 employees or can result in the substantial loss of important fragrance notes from packaged materials reducing product value. Important odors requiring

substantial barriers include odors derived from coffee, ready to eat cereal, frozen pizza, cocoa or other chocolate products, dry mix gravies and soups, snack foods (chips, crackers, popcorn, etc.), baked foods, dry
5 pet food (cat food, etc.), butter or butter-flavor notes, meat products, in particular butter or butter-flavor notes used in the manufacture of microwave popcorn in microwaveable paper containers, fruits and nuts, etc.

10 The above explanation of the nature of the cyclodextrin derivatives, thermoplastic films, manufacturing detail regarding the production of film, and the processes of cyclodextrin to make compatible derivatives provides a basis for understanding
15 technology involving incorporating compatible cyclodextrin in thermoplastic film for barrier purposes. The following examples, film preparation and permeation data provide a further basis for understanding the invention and includes the best mode.

20 After our work in producing derivatives of cyclodextrins and compounding the cyclodextrins in thermoplastic films, we have found that the cyclodextrins can be readily derivatized using a variety of known chemical protocols. The cyclodextrin material
25 can be melt blended into thermoplastic materials smoothly resulting in clear extrudable thermoplastic materials with the cyclodextrin materials uniformly distributed throughout the thermoplastic. Further, we have found that the cyclodextrin derivatives can be
30 combined with a broad variety of thermoplastic films. The cyclodextrin materials can be incorporated into the films in a broad range of cyclodextrin concentrations. The cyclodextrin containing thermoplastic materials can be blown into films of varying thickness and can be
35 blown free of melt fracture or other film or sheet variation. We have found in our experimentation that the barrier properties, i.e. reduction in transmission

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rate of aromatic hydrocarbons, aliphatic hydrocarbons, ethanol and water vapor can be achieved using the cyclodextrin derivative technology. We have also found that the use of cyclodextrin materials improve the

5 surface properties of the film. The surface tension of the film surface and surface electrical properties were also improved. Such a result increases the utility of the films of the invention in coating, printing, laminating, handling, etc. In initial work we have also

10 found (1) several modified cyclodextrin candidates were found to be compatible with the LLDPE resin and provide good complexation of residual LLDPE volatile contaminants as well as reduce organic permeants diffusing through the film. (2) Unmodified β CD

15 adversely affects transparency, thermal stability, machinability, and barrier properties of the film. Conversely, selected modified β CD (acetylated and trimethylsilyl ether derivatives) have no affect on transparency and thermal stability. The machinability

20 of the extruded plastic material is effected somewhat causing some surface defects, thereby reducing the barrier properties of the film. (3) Films containing a modified β CD composition (1% by weight) reduce aromatic permeants by 35% at 72°F and 38% at 105°F; aliphatic

25 permeants were reduced by only 9% at 72°F. These results would improve significantly if worst case shelf-life testing conditions were not used to test the films. (4) Complexation rates were different for aromatic and aliphatic permeants. Films containing modified β CD had

30 better complexation rates for aromatics (gasoline-type compounds) than aliphatic (printing ink-type compounds). Conversely, film coating had significantly better complexation of aliphatic compound than aromatic compounds. (5) β CD containing acrylic coatings were the

35 star performers reducing aliphatic permeants from 46% to 88%, while aromatics were reduced by 29%.

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QUALITATIVE PREPARATION

Initially, we produced four experimental test films. Three of the films contained β -cyclodextrin β CD at loading of 1%, 3% and 5% (wt./wt.) while the fourth
5 was a control film made from the same batch of resin and additives but without β CD. The 5% loaded β CD film was tested for complexation of residual organic in the test film. Even though β CD was found to effectively complex residual organics in the linear low density polyethylene
10 (LLDPE) resin, it was incompatible with the resin and formed β CD particle agglomerations.

We have evaluated nine modified β cyclodextrins and a milled β -cyclodextrin (particle size 5 to 20 microns). The different cyclodextrin modifications were
15 acetylated, octanyl succinate, ethoxyhexyl glycidyl ether, quaternary amine, tertiary amine, carboxymethyl, succinylated, amphoteric and trimethylsilyl ether. Each experimental cyclodextrin (1% loading wt/wt) was mixed with low density polyethylene (LLDPE) using a Littleford
20 mixer and then extruded using a twin screw Brabender extruder.

The nine modified cyclodextrin and milled cyclodextrin LLDPE profiles were examined under an optical microscope at 50X and 200X magnification. The
25 microscopic examination was used to visually check for compatibility between LLDPE resin and cyclodextrin. Of the ten cyclodextrin candidates tested, three (acetylated, octanyl succinate and trimethylsilyl ether) were found visually to be compatible with the LLDPE
30 resin.

Complexed residual film volatiles were measured using cryotrapping procedure to test 5% β CD film sample and three extruded profiles containing 1% (wt/wt) acetylated β CD octanyl succinate β CD and trimethylsilyl
35 ether. The method consists of three separate steps; the first two are carried out simultaneously while the third, an instrumental technique for separating and

detecting volatile organic compounds, is conducted after one and two. In the first step, an inert pure, dry gas is used to strip volatiles from the sample. During the gas stripping step, the sample is heated at 120°C. The sample is spiked with a surrogate (benzene-d₆) immediately prior to the analysis. Benzene-d₆ serves as an internal QC surrogate to correct each set of test data for recovery. The second step concentrates the volatiles removed from the sample by freezing the compounds from the stripping gas in a headspace vial immersed in a liquid nitrogen trap. At the end of the gas-stripping step, an internal standard (toluene-d₈) is injected directly into the headspace vial and the vial is capped immediately. Method and system blanks are interspersed with samples and treated in the same manner as samples to monitor contamination. The concentrated organic components are then separated, identified and quantitated by heated headspace high resolution gas chromatography/mass spectrometry (HRGC/MS). The results of the residual volatile analyses are presented in the table below:

TABLE 1

25	<u>Sample Identification</u>	<u>% Volatile Complexation as Compared to Control</u>
	5% β CD Blown Film	80
30	1% Acylated β CD Profile	47
	1% Octanoyl Succinate β CD Profile	0
	1% Trimethylsilyl ether Profile	48
	1% β CD Milled Profile	29

35 In these preliminary screening tests, β CD derivatives were shown to effectively complex trace volatile organics inherent in low density polyethylene resin used to make experimental film. In 5% β CD loaded LLDPE film, approximately 80% of the organic volatiles were complexed. However, all β CD films (1% and 5%) had an off-color (light brown) and off-odor. The color and

odor problem is believed to be the result of direct decomposition of the CD or impurity in the CD. Two odor-active compounds (2-furaldehyde and 2-furanmethanol) were identified in the blown film samples.

Of the three modified compatible CD candidates (acetylated, octanyl succinate and trimethylsilyl ether), the acetylated and trimethylsilyl ether CD were shown to effectively complex trace volatile organics inherent in the LLDPE resin. One percent loadings of acetylated and trimethylsilyl ether (TMSE) β CD showed approximately 50% of the residual LPDE organic volatiles were complexed, while the octanyl succinate CD did not complex residual LLDPE resin volatiles. Milled β CD was found to be less effective (28%) than the acetylated and TMSE modified β CD's.

Plastic packaging materials all interact to some degree with the food product they protect. The main mode of interaction of plastic packaging of food is through the migration of organic molecules from the environment through the polymer film into the head space of the package where they are absorbed by the food product. Migration or transfer of organic molecules of the package to the food, during storage, is effected by environmental conditions such as temperature, storage time, and other environmental factors (e.g., humidity, type of organic molecules and concentration thereof). Migration can have both quality (consumer resistance) and toxicological influence. The objective of packaging film testing is to measure how specific barriers may influence the quality of packaged individual foods. To simulated accelerated shelf-life testing for low-water-activity food products, the testing was conducted at a temperature of 72°F and 105°F, and a relative humidity of 60%. These temperature and humidity conditions are probably similar to those found in uncontrolled warehouses, in transit, and in storage.



If a polymer is moisture sensitive, the relative humidity can affect the film's performance especially in low-water-activity food products. Because a packaging film during actual end-use conditions will be separating two moisture extremes, relative humidity in the permeation device was controlled on both sides of the film. The environment side, representing the outside of the package, was maintained at 60% relative humidity, and the sample side, representing the inside of a package containing a low-water-activity product, at 0.25.

A combination of permeants was used to measure the function and performance of the CD. A combination was used to be realistic, since gasoline (principally an aromatic hydrocarbon mixture) and printing ink solvents (principally an aliphatic hydrocarbon mixture) are not formed from a single compound but are a mixture of compounds.

The aromatic permeant contained ethanol (20 ppm), toluene (3 ppm), p-xylene (2 ppm), o-xylene (1 ppm), trimethyl-benzene (0.5 ppm) and naphthalene (0.5 ppm). The aliphatic permeant, a commercial paint solvent blend containing approximately twenty (20) individual compounds, was 20 ppm.

The permeation test device Figure 3 consists of two glass permeation cells or flasks with cavities of 1200 ml (environment cell or feed side) and 300 ml (sample cell or permeating side).

Experimental film performance was measured in the closed-volume permeation device. High-resolution gas chromatograph (HRGC) operated with a flame ionization detector (FID) was used to measure the change in the cumulative penetrant concentration as a function of time. Sample-side (food product side) compound concentrations are calculated from each compound's response factor. Concentrations are reported in parts per million (ppm) on a volume/volume basis. The

cumulative penetrant concentration on the sample-side of the film is plotted as a function of time.

We produced four experimental test films. Three of the films contained β CD at loading of 1%, 3% and 5% (wt/wt) while the fourth was a control film made from the same batch of resin and additives but without β CD.

A second experimental technique was also undertaken to determine whether β CD sandwiched between two control films will complex organic vapors permeating the film. The experiment was carried out by lightly dusting β CD between two control film sheets.

The testing showed the control film performed better than β CD loaded films. The permeation test results also demonstrated the higher the β CD loading the poorer the film performed as a barrier. The test results for sandwiching β CD between two control films showed β CD being twice as effective in reducing permeating vapors than the control samples without β CD. This experiment supported that CD does complex permeating organic vapors in the film if the film's barrier qualities are not changed during the manufacturing process making the film a less effective barrier.

The 1% TMSE β CD film was slightly better than the 1% acetylated β CD film (24% -vs- 26%) for removing aromatic permeants at 72°F adding more modified CD appeared to have no improvement.

For aromatic permeants at 105°F, both 1% TMSE β CD and 1% acetylated β CD are approximately 13% more effective removing aromatic permeants than 72°F. The 1% TMSE film was again slightly better than the 1% film (36% -vs- 31%) for removing aromatic permeants.

The 1% TMSE film was more effective initially removing aliphatic permeants than the 1% acetylated β CD film at 72°F. But for the duration of the test, 1% TMSE β CD was worse than the control while 1% acetylated β CD removed only 6% of the aliphatic permeants.



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We produced two experimental aqueous coating solutions. One solution contained hydroxyethyl β CD (35% by weight) and the other solution contained hydroxypropyl β CD (35 by weight). Both solutions contained 10% of an acrylic emulsion comprising a dispersion of polyacrylic acid having a molecular weight of about 150,000 (Polysciences, Inc.) (15% solids by weight) as a film forming adhesive. These solutions were used to hand-coat test film samples by laminating two LLDPE films together. Two different coating techniques were used. The first technique very slightly stretched two film samples flat, the coating was then applied using a hand roller, and then the films were laminated together while stretched flat. The Rev. 1 samples were not stretched during the lamination process. All coated samples were finally placed in a vacuum laminating press to remove air bubbles between the film sheets. Film coating thicknesses were approximately 0.0005 inches. These CD coated films and hydroxymethyl cellulose coated control films were subsequently tested.

A reduction in aromatic and aliphatic vapors by the hydroxyethyl β CD coating is greater in the first several hours of exposure to the vapor and then diminishes over the next 20 hours of testing. Higher removal of aliphatic vapors than aromatic vapors was achieved by the hydroxyethyl β CD coating; this is believed to be a function of the difference in their molecular size (i.e., aliphatic compounds are smaller than aromatic compounds). Aliphatic permeants were reduced by 46% as compared to the control over the 20 hour test period. Reduction of aromatic vapors was 29% as compared to the control over the 17 hour test period.

The Rev. 1 coated hydroxyethyl β CD reduced the aliphatic permeants by 87% as compared to the control over the 20 hour test period. It is not known if the method of coating the film was responsible for the



additional 41% reduction over the other hydroxyethyl β CD coated film.

The hydroxyethyl β CD coating was slightly better for removing aromatic permeants than the hydroxypropyl β CD coating (29% - 20%) at 72°F.

LARGE SCALE FILM EXPERIMENTAL
Preparation of Cyclodextrin Derivatives

10 Example I

An acetylated β -cyclodextrin was obtained that contained 3.4 acetyl groups per cyclodextrin on the primary -OH group.

Example II

15 Trimethyl Silyl Ether of β -cyclodextrin

Into a rotary evaporator equipped with a 4000 milliliter round bottom flask and a nitrogen atmosphere, introduced at a rate of 100 milliliters N_2 per minute, was placed three liters of dimethylformamide. Into the
20 dimethylformamide was placed 750 grams of β -cyclodextrin. The β -cyclodextrin was rotated and dissolved in dimethylformamide at 60°C. After dissolution, the flask was removed from the rotary evaporator and the contents were cooled to approximately
25 18°C. Into the flask, placed on a magnetic stirrer and equipped with a stir bar, was added 295 milliliters of hexamethyldisilylazine (HMDS- Pierce Chemical No. 84769), followed by the careful addition of 97
30 milliliters of trimethylchlorosilane (TMCS - Pierce Chemical No. 88531). The careful addition was achieved by a careful dropwise addition of an initial charge of 20 milliliters and after reaction subsides the careful dropwise addition of a subsequent 20 milliliter portions, etc. until addition is complete. After the
35 addition of the TMCS was complete, and after reaction subsides, the flask and its contents were placed on the rotary evaporator, heated to 60°C while maintaining an



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inert nitrogen atmosphere flow of 100 milliliters of N₂ per minute through the rotary evaporator. The reaction was continued for four hours followed by removal of solvent, leaving 308 grams of dry material. The material was removed from the flask by filtering, washing the filtrate with deionized water to remove the silylation products, vacuum oven drying (75°C at 0.3 inches of Hg) and stored as a powdered material and maintained for subsequent compounding with a thermoplastic material. Subsequent spectrographic inspection of the material showed the β -cyclodextrin to contain approximately 1.7 trimethylsilylether substituent per β -cyclodextrin molecule. The substitution appeared to be commonly on a primary 6-carbon atom.

Example III

An hydroxypropyl β -cyclodextrin was obtained with 1.5 hydroxypropyl groups per molecule on the primary 6-OH group of the β CD.

Example IV

An hydroxyethyl β -cyclodextrin was obtained with 1.5 hydroxyethyl groups per molecule on the primary 6-OH group of the β CD.

Preparation of Films

We prepared a series of films using a linear low density polyethylene resin, β CD and derivatized β CD such as the acetylated or the trimethylsilyl derivative of a β -cyclodextrin. The polymer particles were dry blended with the powdered β -cyclodextrin and β -cyclodextrin derivative material, a fluoropolymer lubricant (3M) and the antioxidant until uniform in the dry blend. The dry blend material was mixed and extruded in a pellet form in a Haake System 90, 3/4" conical extruder. The resulting pellets were collected for film preparation.

Table IA displays typical pelletizing extruder conditions. The films were blown in the apparatus of



Figure 2. Figure 2 shows extruded thermoplastic tube 21 exiting the die 22. The tube is collapsed by die 23 and layered by rollers 24 into the film 25. The extruded tube 21 is inflated using air under pressure blown through air inlet tube 26. The thermoplastic is melted in the extruder. The extruder temperature is taken at the mixing zone 27. The melt temperature is taken in the melt zone 28 while the die temperature is taken in the die 29. The extrudate is cooled using an air blown cooling stream from the cooling ring 20. The general schematic background of Figure 2 is representative of the Kiefel blown film extruder, 40 mm die diameter, used in the actual preparation of the blown film. The film is manufactured according to the above protocol and reported in Table IB. The film was tested for transmission rates at a variety of environmental conditions. Environmental test conditions are shown below in Table II.

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TABLE IA

0.5% TMSE Pelletizing 1-19-94

Run Time	0 min	Torque	4866 meter-gram	Rotor	198 rpm
13 sec		Tot. Torque	0.0 mkg-min	Aux.	0 %
Channels	--1--	--2--	--3--	--4--	--5--
Melt Temp	37	41	41	41	°C
Set Temp	150	160	160	170	°C
Deviation	0	0	0	0	°C
Cooling	Yes	Yes	Yes	Yes	
Pressure	0	0	2739	0	psi

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TABLE IB
Extruded Films (Exxon LL3201)
Made With Low Density Polyethylene

Roll No.	Sample ID	Fluoropolymer Additive	Extruder Temp. Zone 3 (F)	Melt Temp (F)	Die Temp. Zone 3 (F)	Lbs./Hr	RPM	Die Gap	Comments
1	Control	500 ppm	428	406	406	30.1	50	24	
2	1 % Ex. I	1000 ppm	441	415	420	29.7	50	35	
3	1 % Ex. I	1000 ppm	441	416	420	28.5	50	35	
4	1 % Ex. I	500 ppm	441	415	420	29.9	50	35	
5	1 % Ex. I	500 ppm	418	405	414	29.9	50	35	
6	1 % Ex. I	500 ppm	421	397	414	29.0	50	35	
7	0.5% Ex. I	500 ppm	421	403	415	29.0	50	35	Very slight melt fracture
8	2 % Ex. I	500 ppm	421	404	415	27.7	50	35	Particles in film.
9	1 % Ex. II	500 ppm	421	406	415	28.3	50	35	Particles in film.
10	1 % Ex. II	500 ppm	426	410	415	26.7	50	35	Particles in film.
11	1 % Ex. II	500 ppm	432	415	414	29.0	50	35	Particles in film.
12	1 % Ex. II	500 ppm	431	414	415	21.5	39	35	Particles in film.
13	0.5% Ex. II	500 ppm	431	415	415	27.7	50	35	Particles in film.
14	0.5% Ex. II	500 ppm	425	410	415	28.9	50	35	Particles in film.
15	2 % Ex. II	500 ppm	410	414	415	20.2	38	35	Particles in film.
16	2 % Ex. II	500 ppm	422	415	415	20.5	38	35	Particles in film.
17	2 % Ex. II	500 ppm	422	416	415	20.5	38	35	Particles in film.

1 Also contains 500 ppm Irganox 1010 antioxidant and 1000 ppm IrgaFos 168.

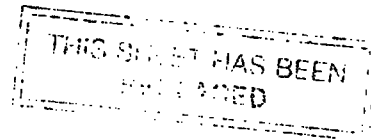


TABLE II
Test Conditions

Roll Sample ID Number	Temp. (F)	Sample Side	Environ. Side	Permeant
Roll #2	72	Rm & RH	Rm & RH	Aromatic/Alcohol
Roll #3				
Roll #5				
Roll #6				
Roll #5	72	Rm & RH	Rm & RH	Aromatic/Alcohol
Roll #8				
Roll #7	72	0.25 Aw	60 & RH	Aromatic/Alcohol
Roll #5				
Roll #3				
Roll #7	72	.60 Aw	30 & RH	Aromatic/Alcohol
Roll #5				
Roll #8				
Roll #2	105	Rm & RH	Rm & RH	Aromatic/Alcohol
Roll #3				
Roll #4				
Roll #5				
Roll #6				
Roll #8				
Roll #12				
Roll #7	105	0.25 Aw	15 & RH	Aromatic/Alcohol
Roll #5				
Roll #8				
Roll #13	72	Rm & RH	Rm & RH	Aromatic/Alcohol
Roll #14				
Roll #9				
Roll #11				
Roll #12				

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TABLE II. (Cont.)

Roll Sample ID Number	Test Conditions			Permeant ¹⁴
	Temp. (F)	Sample Side	Environ. Side	
Roll #15 Roll #16 Roll #17				
Roll #14	105	Rm & RH	Rm & RH	Aromatic/ Alcohol
Roll #15				
10% Ex. III in PVDC	72	0.25 Aw	60 % RH	Aromatic/ Alcohol
20% Ex. III in PVDC				
5% Ex. III/ Acrylic	72	Rm & RH	Rm & RH	Aromatic/ Alcohol
10% Ex. III/ Acrylic				
Roll #7 Roll #5 Roll #8	72	Rm & RH	Rm & RH	Naphtha
Roll #12 Roll #15	72	Rm & RH	Rm & RH	Naphtha

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3 7 ppm aromatic plus 20 ppm ETOH.

4 40 ppm Naphtha

The results of the testing show that the inclusion of a compatible cyclodextrin material in the thermoplastic films of the invention substantially improves the barrier properties by reducing transmission rate of a variety of
5 permeants. The data showing the improvement in transmission rate is shown below in the following data tables.

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Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDS Films

Sample Identification	Aromatic Transmission Rate*	Improvement Over Control	Temperature 72°F		Tot. Volatiles %
			Aromatics & Total Volatiles Transmission Rate*	Improvement Over Control	
Control Film	3.35E-04	0%	3.79E-04	0%	
1.0% CS-001 (Roll #2)	3.18E-04	5%	3.61E-04	5%	
1.0% CS-001 (Roll #3)	2.01E-04	40%	2.55E-04	33%	
1.0% CS-001 (Roll #5)	2.67E-04	20%	3.31E-04	13%	
1.0% CS-001 (Roll #6)	3.51E-04	-5%	3.82E-04	-1%	

Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Sample Identification	Aromatic Transmission Rate*	Temperature 72°F		Naphtha & Improvement Over Control
Control Film (Roll #1)	7.81E-03			0%
0.5% CS-001 (Roll #7)	7.67E-03			2%
1% CS-001 (Roll #5)	7.37E-03			6%
2% CS-001 (Roll #6)	6.53E-03			16%

100 in. $\pm$ 0.001 in.
24 hrs.

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Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 72°F

Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatic Transmission Rate*	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate*	T. Volatiles % Improvement Over Control
Control Film (Roll #1)	5.16E-04	0%	5.63E-04	0%
1.0% CS-001 (Roll #5)	4.01E-04	22%	5.17E-04	8%
2.0% CS-001 (Roll #8)	2.91E-04	44%	3.08E-04	45%

Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 72°F

Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatic Transmission Rate*	Naphtha % Improvement Over Control
Control Film (Roll #1)	7.81E-03	0%
0.5% CS-001 (Roll #7)	7.67E-03	2%
1% CS-001 (Roll #5)	7.37E-03	6%
2% CS-001 (Roll #8)	6.53E-03	16%

* $\frac{\text{gm} \cdot 0.001 \text{ in.}}{100 \text{ in}^2 \cdot 24 \text{ hrs.}}$

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Comparison of Transmission Rates in
Modified β -Cyclodextrin - LLDPE Films

Temperature 72°F

Sample Side: 0.25 Aw

Environment: 60% RH

Sample Identification	Aromatic Transmission Rate	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate	T. Volatiles % Improvement Over Control
Control Film (Roll #1)	3.76E-04	0%	3.75E-04	0%
0.5% CS-001 (Roll #7)	2.42E-04	36%	2.41E-04	36%
1% CS-001 (Roll #5)	3.39E-04	10%	3.38E-04	10%
2% CS-001 (Roll #8)	2.48E-04	34%	2.47E-04	34%

Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 105°F

Sample Side: Room % RH

Environment: Room % RH

Sample Identification	Aromatic Transmission Rate	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate	T. Volatiles % Improvement Over Control
Control Film (Roll #1)	1.03E-03	0%	1.13E-03	0%
1% CS-001	5.49E-04	47%	5.79E-04	49%
1% CS-001 (Roll #3)	4.74E-04	54%	5.00E-04	56%
1% CS-001 (Roll #4)	6.41E-04	38%	6.83E-04	40%
1% CS-001 (Roll #5)	5.22E-04	49%	5.54E-04	51%
1% CS-001 (Roll #6)	4.13E-04	60%	4.39E-04	61%
2% CS-001				

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45%
21%

6.18E-04
8.93E-04

42%
19%

5.95E-04
8.32E-04

(Roll #8)
1% TMSE
(Roll #12)

* $\frac{gm \cdot 0.001 \text{ in.}}{100 \text{ in}^2 \cdot 24 \text{ hrs}}$

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Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 105°F

Sample Side: Room % RH

Environment: Room % RH

Sample Identification	Aromatic Transmission Rate	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate	T. Volatiles % Improvement Over Control
Control Film (Roll #1)	4.34E-04	0%	4.67E-04	0%
0.5% CS-001 (Roll #7)	4.03E-04	7%	4.41E-04	6%
1.0% CS-001 (Roll #5)	5.00E-04	-15%	5.33E-04	-14%
2.0% CS-001 (Roll #8)	3.96E-04	9%	3.94E-04	16%

Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 72°F

Sample Side: Room % RH

Environment: Room % RH

Sample Identification	Aromatic Transmission Rate	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate	T. Volatiles % Improvement Over Control
Control Film 0.5% TMSE (Roll #13)	3.09E-04	0%	3.45E-04	0%
0.5% TMSE (Roll #14)	2.50E-04	19%	2.96E-04	14%
1% TMSE (Roll #9)	2.37E-04	23%	2.67E-04	33%
1% TMSE (Roll #10)	2.67E-04	14%	3.05E-04	12%
1% TMSE (Roll #11)	4.85E-04	-57%	5.27E-04	-53%
1% TMSE (Roll #12)	2.58E-04	17%	2.92E-04	15%
1% TMSE (Roll #12)	2.15E-04	31%	2.55E-04	26%

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2% TMSE (Roll #15)	2.54E-04	18%	3.04E-04	12%
2% TMSE (Roll #16)	2.79E-04	10%	3.21E-04	7%
2% TMSE (Roll #17)	2.81E-04	9%	3.24E-04	6%

* $\frac{gm \cdot 0.001 in.}{100 in^2 \cdot 24 hrs.}$

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Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 72°F

Sample Side: Room % RH

Environment: Room % RH

Sample Identification	Aromatic Transmission Rate*	Naphtha % Improvement Over Control
Control Film (Roll #1)	9.43E-03	0%
1% TMSE (Roll #12)	1.16E-02	-23%
2% TMSE (Roll #15)	1.56E-02	-65%

Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 72°F

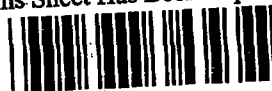
Sample Side: Room % RH

Environment: Room % RH

Sample Identification	Aromatic Transmission Rate*	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate*	T. Volatiles % Improvement Over Control
Control Film (Roll #1)	8.36E-04	0%	9.05E-04	0%
0.5% TMSE (Roll #14)	6.77E-04	19%	7.25E-04	20%
2% TMSE (Roll #15)	6.36E-04	24%	6.81E-04	25%

* $\frac{\text{gm} \cdot 0.001 \text{ in.}}{100 \text{ in}^2 \cdot 24 \text{ hrs.}}$

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Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 72°F
Sample Side: 0.25 Aw
Environment: 60% RH

Sample Identification	Aromatic Transmission Rate*	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate*	T. Volatiles % Improvement Over Control
PVdC Control	6.81E-05	0%	1.05E-04	0%
PVdC w/ 10% HP B-CyD	1.45E-05	79%	2.39E-05	77%
PVdC w/ 20% HP B-CyD	9.71E-05	-42%	1.12E-04	-7%

Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 72°F
Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatic Transmission Rate*	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate*	T. Volatiles % Improvement Over Control
Control Acrylic	2.07E-06	0%	2.10E-05	0%
5% HP B-CyD/ Acrylic	1.50E-06	27%	2.07E-05	1%
10% HP B-CyD/ Acrylic	4.13E-06	-100%	4.30E-05	-105%

* $\frac{\text{gm} \cdot 0.001 \text{ in.}}{100 \text{ in}^2 \cdot 24 \text{ hrs.}}$

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We prepared a series of aqueous coatings containing hydroxypropyl β CD. One of the coatings was prepared from a 10% acrylic emulsion (a polyacrylic acid polymer having a molecular weight of about 150,000 purchased from Polysciences, Inc.). The 10% acrylic emulsion contained hydroxypropyl β CD at a 5% and 10% by weight loading. These solutions were used to hand-coat test film samples by laminating two films. The coatings were applied to linear low density polyethylene film sheet containing 0.5% acetylated β CD (Roll No. 7) and to a second film sheet containing 2% acetylated β CD (Roll No. 8) using a hand roller and then laminating the films. The films were not stretched during lamination. All coated samples were placed in a vacuum laminating press to remove air bubbles between the film sheets. The acrylic coating thickness was about 0.0002 inch. An acrylic coated control was prepared in an identical manner containing no hydroxypropyl β CD. The multilayer structure was tested with the 0.5% acetylated β CD film facing the environmental flask side of the test cell (Fig. 3).

A second coating was prepared from a vinylidene chloride latex (PVDC, 60 wt-% solids) purchased from Dagax Laboratories, Inc. The PVDC latex coating was prepared with two levels of hydroxypropyl β CD - 10% and 20% by weight of the derivatized cyclodextrin. These solutions were used to hand-coat linear low density polyethylene test film samples by laminating the two films together. The coatings were applied to two control film sheets (rolled into one) using a hand roller and laminated together. The films were not stretched during lamination process. All coated samples were placed in a vacuum laminating press to remove air bubbles between the film sheets. The PVDC coating thickness was approximately 0.0004 inch. A PVDC coated control was prepared in an identical manner but without hydroxypropyl β CD.



The data following the preparatory examples showing improvement in transmission rate was obtained using the following general test method.

Method Summary

5 This method involves experimental techniques designed to measure the permeability of selected organic molecules through food packaging films, using a static concentration gradient. The test methodology simulates accelerated shelf-life testing conditions by
 10 implementing various storage humidities, product water activities and temperature conditions and using organic molecule concentrations found in previously tested food products to simulate outside-the-package organic vapors in the permeation test cell. This procedure allows for
 15 the determination of the following compounds: ethanol, toluene, p-xylene, o-xylene, 1,2,4-trimethyl benzene, naphthalene, naphtha solvent blend, etc.

20	Environmental <u>Test Compounds</u>	Threshold	
		Odor Conc. <u>ul/L ppm</u>	Cell Conc. <u>ul/L ppm</u>
25	Ethanol	5 - 5000	20
	Toluene	0.10- 20	3
	p-Xylene	0.5	2
	o-Xylene	0.03- 12	1
	1,2,3-Trimethyl Benzene	NA	0.5
30	Naphthalene	0.001- 0.03	0.5
	Naphtha Solvent Blend	NA	40

Table 1. Permeant Test Compounds

35 In a typical permeation experiment, three steps are involved. They are (a) the instrument sensitivity calibration, (b) film testing to measure transmission and diffusion rates, and (c) the quality control of the permeation experiment.

40 Film samples are tested in a closed-volume permeation device. High-resolution gas chromatograph (HRGC) operated with a flame ionization detector (FID)

is used to measure the change in the cumulative penetrant concentration as a function of time.

Sample-side and environment-side test compound concentrations are calculated from each compound's response factor or calibration curve. Concentrations are then volume-corrected for each specific set of permeation cells if permeant mass is desired.

The cumulative penetrant concentration is plotted as a function of time on both the upstream (environment) and downstream (sample) side of the film. The diffusion rate and transmission rate of the permeant are calculated from the permeation curve data.

1.0 Equipment and Reagents

2.1 Equipment

Gas chromatograph (HP 5880) equipped with flame ionization detector, a six-port heated sampling valve with 1 ml sampling loop and data integrator

J&W capillary column. DB-5, 30M X 0.250mm ID, 1.0 umdf.

Glass permeation test cells or flasks. Two glass flasks with cavities of approximately 1200 ml (environment cell or feed side) and 300 ml (sample flask or permeating side) (Fig. 3).

Permeation cell clamping rings (2).

Permeation cell aluminum seal rings (2).

Natural Rubber Septa. 8 mm OD standard-wall or 9 mm OD (Aldrich Chemical Company, Milwaukee, WI).

Assorted laboratory glass ware and syringes.

Assorted laboratory supplies.

2.2 Reagents

Reagent water. Water in which interferences are not observed at the MDL of the chemical analytes of interest. A water purification system is used to generate reagent water which has been boiled to 80% volume, capped, and allowed to cool to room temperature before use.

Stock Ethanol/Aromatic Standard solution. Ethanol

(0.6030 gram), toluene (0.1722 gram), p-xylene (0.1327 gram), o-xylene (0.0666 gram), trimethylbenzene (0.0375 gram) and naphthalene (0.0400 gram) package in 1 ml sealed glass ampules. Naphtha blends standard is a commercial paint solvent blend containing approximately twenty (20) individual aliphatic hydrocarbon compounds obtained from Sunnyside Corporation, Consumer Products Division, Wheeling, IL.

Triton X-100. Nonylphenol nonionic surface active agent (Rohm and Hass).

2.0 Standards Preparation

2.2 Permeation Working Standard

A stock permeant test standard solution is used. These standards are prepared by weight from neat certified reference compounds, actual weight and weight percent are shown.

The working ethanol/aromatic standard is prepared by injecting 250 ul of the stock standard solution into 100 ml of reagent water containing 0.1 gram of surfactant (Triton X-100). It is important that the Triton X-100 is completely dissolved in the reagent water prior to adding the permeant stock standard. This will insure dispersing the test compounds in the water. In addition, the working standard should be mixed thoroughly each time an aliquot is dispensed. It is advisable to transfer the working standard to crimp-top vials with no headspace to minimize losses due to the large headspace in the volumetric flask used to prepare the standard.

A working naphtha blend standard is prepared by injecting 800 μ L of the "neat" naphtha solvent blend into 100 milliliters of reagent water containing 0.2 gram of surfactant (Triton X-100).

An opened stock standard solution should be transferred from the glass snap-cap vial to a crimp-top vial for short-term storage. The vials may be stored in an explosion-proof refrigerator or freezer.

2.1 Calibration Standards

Calibration standards are prepared at a minimum of three concentration levels by adding volumes of the working standard to a volumetric flask and diluting to
5 volume with reagent water. One of the standards is prepared at a concentration near, but above, the method detection limit. The other concentrations correspond to the expected range of concentrations found in the environment and sample side cells.

10 3.0 Sample Preparation

3.1 Film Sample Preparation

The environment flask Figure 3 and sample flask are washed before use in soapy water, thoroughly rinsed with deionized water, and oven-dried. Following cleaning,
15 each flask is fitted with a rubber septum.

The film test specimen is cut to the inside diameter of the aluminum seal ring using a template. The film test specimen diameter is important to prevent diffusion losses along the cut edge circumference. The
20 film sample, aluminum seals, and flasks are assembled as shown in Figure 3, but the clamping ring nuts are not tightened.

The test cell (Fig. 3) is prepared. First the sample flask 32 and environment flask 31 are flushed
25 with dry compressed air to remove humidity in the sample and environment flasks. This is done by puncturing the sample system 33 and environment septum 34 with a needle and tubing assembly which permits a controlled flow of dry air through both flasks simultaneously. The clamp
30 rings 35 are loosely fitted to the flasks to eliminate pressure buildup on either side of the film 30. After flushing both flasks for approximately 10 minutes, the needles are removed and the clamp rings tightened, sealing the film 30 between the two flasks. Rubber
35 faced aluminum spacers 36a, 36b are used to ensure a gas tight fit.

The sample side is injected with 2 μ L of water per

300 ml flask volume. Since the sample flasks vary in volume, the water is varied to correspond to the volume variations. The 2 μ L of water in the 300 ml flask volume is comparable to a 0.25 water activity product at 72°F. Next, 40 μ L, the permeation ethanol/aromatic working standard or 40 μ L of the naphtha blend working standard prepared according to section 2.2, is injected into the environmental flask. Either of these working standards will produce a 60% relative humidity at 72°F with a permeant concentration (parts per million-volume/volume) in the 1200 ml volume flask indicated in Table I. Other humidities or permeant concentrations may be employed in the test method by using psychrometric chart to determine humidity and using the gas loss to calculate permeant concentration. The time is recorded and the permeation cell placed into a thermostatically controlled oven. Samples may be staggered to accommodate GC run time. Three identical permeation devices are prepared. Triplicate analyses are used for QC purposes.

At the end of each time interval, a sample from the group is removed from the oven. The environmental flask is analyzed first, using a heated six-port sampling valve fitted with a 1 ml loop. The loop is flushed with a 1 ml volume of the environment-side or sample-side air. The loop is injected onto the capillary column. The GC/FID system is started manually following the injection. Up to eight 1 ml sample injections may be taken from the sample and environment side of a single permeation experiment.

Sample side and environment side test compound concentrations are calculated from each compound's calibration curve or response factor (equation 1 or 3). Concentrations are then volume-corrected for each specific set of permeation flasks if permeant mass is desired.

4.0 Sample Analysis



4.1 Instrument Parameters

Standards and samples are analyzed by gas chromatography using the following method parameters:

Column: J&W column, DB-5, 30 M, 0.25 mm ID, 1 umdf
5 Carrier: Hydrogen
Split Vent: 9.4 ml/min
Injection Port Temp: 105°C
Flame Detector Temp: 200°C
Oven Temp 1: 75°C
10 Program Rate 1: 15°C
Oven Temp 2: 125°C
Rate 2: 20°C
Final Oven Temp: 200°C
Final Hold Time: 2 Min
15 The six-port sampling valve temperature is set to 105°C.

4.2 Calibration

A three point calibration is prepared using standards in the range of the following test compounds:

20

		Calibration Curve Range	
<u>Test Compounds</u>		<u>ppm (μL)</u>	
25	Ethanol	2	20
	Toluene	0.3	3
	p-Xylene	0.2	2
	o-Xylene	0.1	1
	1,2,4-Trimethyl Benzene	0.05	0.5
30	Naphthalene	0.05	0.5
	Naphtha Solvent Blend	4.0	40

To prepare a calibration standard, add an appropriate volume of the working standard solution to
35 an aliquot of reagent water in a volumetric flask.

4.2.1 Secondary Dilutions of Working Standard for Calibration Curve

5 to 1 dilution: Place 5 ml of working standard into a 25-ml volumetric flask, stopper, then mix by
40 inverting flask.

2.5 to 1 dilution: Place 10 ml of working standard

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into a 25-ml volumetric flask, stopper, then mix by inverting flask.

Analyze each calibration standard and tabulate compound peak area response versus the concentration of the test compound in the environment side cell. The results are used to prepare a calibration curve for each compound. The naphtha solvent blend is a commercial paint solvent containing approximately twenty (20) individual aliphatic hydrocarbon compounds. The response versus concentration is determined by totaling the area under each of the twenty individual peaks. Method of least squares is used to fit a straight line to the calibration curve. The slope of each test compound's calibration curve is then calculated for determining the unknown concentration. The average response factor may be used in place of the calibration curve.

The working calibration curve or response factor must be verified on each working day by measurement of one or more calibration standards. If the response of any compound varies more than 20%, the test must be repeated using a fresh calibration standard. If the results still do not agree, generate a new calibration curve.

25 4.3 Analysis of Calibration Curve and Method
Detection Level Samples

Recommended chromatographic conditions are summarized above.

Calibrate the system daily as described above.

30 Check and adjust split vent rate and check rate with soap film flow meter.

To generate accurate data, samples, calibration standards and method detection level samples must be analyzed under identical conditions.

35 Calibration standards and method detection samples are prepared in the environment flask only. This is accomplished by using a 1/2 inch plastic disk and

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aluminum sheet disk the diameter of the environment
flange in place of the sample flask. A single sealing
ring is placed onto the environmental glass flange
followed by an aluminum sheet, and then the plastic
5 disk.

The environment flask is flushed with dry
compressed air to remove humidity in the sample and
environment flask. This is done by puncturing the
environment septa with a needle and tubing assembly
10 which permits a controlled flow of dry air through the
flask. The clamp rings are loosely fitted to the flask
to eliminate pressure buildup. After flushing both
flasks for approximately 10 minutes, the needle is
removed and the clamp rings tightened, sealing the
15 aluminum sheet against the seal ring.

Next, 40 μ l of the permeation ethanol/aromatic
working standard or secondary dilutions of the working
standard is injected into the environment flask.
Alternatively, 40 μ L of the naphtha solvent blend or
20 secondary dilutions of the working standard is injected
into the environmental flask. The time is recorded and
the flask is placed into a thermostatically controlled
oven.

At the end of 30 minutes, the environment flask is
25 removed from the oven. The environmental flask is
analyzed using a heated six-port sampling valve fitted
with a 1 ml loop. The loop is flushed with a 1 ml
volume of the environment-side or sample-side air. The
loop is injected onto the capillary column. The GC/FID
30 system is started manually following the injection.

4.4 Calculation of Results

4.4.1 Test Compound Response Factor

Sample-side and environment-side test compound
concentrations are calculated for each compound's
35 calibration curve slope or response factor (RF).
Concentrations are then volume-corrected for each
specific set of permeation cells if permeant mass is



desired.

$$\text{Concentration of Compound in ppm} = \frac{\text{Peak Area}}{\text{Calibration Curve Slope}} \quad (1)$$

$$\text{Compound Specific RF} = \frac{\text{Concentration of Compound in ppm}}{\text{Peak Area}} \quad (2)$$

$$\text{Concentration of Compound in ppm} = \text{Peak Area} \times \text{RF} \quad (3)$$

10

The cumulative penetrant mass is plotted as a function of time on both the upstream (environment) and downstream (sample) side of the film. The diffusion rate and transmission rate of the permeant area calculated from the transmission curve data.

4.4.2 Transmission Rate

When a permeant does not interact with the polymer, the permeability coefficient, R , is usually characteristic for the permeant-polymer system. This is the case with the permeation of many gases, such as hydrogen, nitrogen, oxygen, and carbon dioxide, through many polymers. If a permeant interacts with polymer molecules, as is the case with the permeant test compounds used in this method, P is no longer constant and may depend on the pressure, film thickness, and other conditions. In such cases, a single value of P does not represent the characteristic permeability of the polymer membrane and it is necessary to know the dependency of P on all possible variables in order to obtain the complete profile of the permeability of the polymer. In these cases, the transmission rate, Q , is often used for practical purposes, when the saturated vapor pressure of the permeant at a specified temperature is applied across the film. Permeability of films to water and organic compounds is often expressed this way.

$$P = \frac{(\text{Amount of Permeant})(\text{Film Thickness})}{(\text{Area})(\text{Time})(\text{Pressure-drop Across the Film})} \quad (4)$$

$$Q = \frac{(\text{Amount of Permeant})(\text{Film Thickness})}{(\text{Area})(\text{Time})} \quad (5)$$

In this application, Q is represented in units of

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gm-0.001 inches
100 in²-day.

One of the major variables in determining the permeation coefficient is the pressure drop across the film. Since the transmission rate Q includes neither pressure nor concentration of the permeant in its dimensions, it is necessary to know either vapor pressure or the concentration of permeant under the conditions of the measurement in order to correlate Q to P .

The pressure-drop across the film from environment side to sample side is principally due to water vapor pressure. The water concentration or humidity does not remain constant and is not measured during the time intervals the organic compounds are analyzed, and therefore the pressure across the membrane is not determined.

The above examples of thermoplastic films containing a variety of compatible cyclodextrin derivatives shows that the invention can be embodied in a variety of different thermoplastic films. Further, a variety of different compatible derivatized cyclodextrin materials can be used in the invention. Lastly, the films can be manufactured using a variety of film manufacturing techniques including extrusion and aqueous dispersion coating to produce useful barriers.

The above specification, examples of substituted cyclodextrin, extruded thermoplastic films and test data provide a basis for understanding the technical aspects of

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the invention. Since the invention can be made with a variety of embodiments, the invention resides in the claims hereinafter appended.

WE CLAIM:

1. A thermoplastic film composition, having improved barrier properties, the film composition comprising:
 - (a) a thermoplastic polymer web; and
 - (b) uniformly dispersed in the web, an effective permeant absorbing amount of a polymer compatible cyclodextrin derivative;wherein the cyclodextrin is substantially free of an inclusion complex compound.
2. The film of claim 1 wherein the thermoplastic polymer comprises a vinyl polymer comprising an α -olefin.
3. The film of claim 1 wherein the thermoplastic polymer comprises a chlorine containing vinyl polymer comprising vinyl chloride or vinylidene dichloride.
4. The film of claim 3 wherein the thermoplastic polymer comprises a poly(vinyl chloride-co-vinyl acetate) or a poly(vinyl chloride-co-vinylidene dichloride).
5. A film of claim 2 wherein the thermoplastic polymer comprises a polyvinylalcohol, a poly(ethylene-co-vinyl alcohol), a poly(ethylene-co-acrylic acid) or a poly(ethylene-co-methyl acrylate).
6. The film of claim 1 wherein the cyclodextrin derivative comprises a β -cyclodextrin derivative.
7. The film of claim 6 wherein the cyclodextrin derivative contains at least one substituent on a cyclodextrin primary carbon atom.
8. The film of claim 1 wherein the cyclodextrin



comprises α -cyclodextrin, β -cyclodextrin, γ -cyclodextrin or mixtures thereof.

9. The film of claim 1 wherein the thermoplastic
5 web contains about 0.1 to 5 wt-% of the polymer compatible cyclodextrin derivative.

10. A packaged food comprising at least one food item and a package substantially surrounding the item,
10 the package comprising a thermoplastic film composition, having improved barrier properties, the film composition comprising:

(a) a thermoplastic polymer web; and
(b) uniformly dispersed in the web, an
15 effective permeant absorbing amount of a polymer compatible cyclodextrin derivative;
wherein the cyclodextrin is substantially free of an inclusion complex compound.

20 11. The food of claim 10 wherein the thermoplastic polymer comprises a vinyl polymer comprising an alpha-olefin.

12. The food of claim 10 wherein the thermoplastic
25 polymer comprises a chlorine containing vinyl polymer comprising vinyl chloride or vinylidene dichloride.

13. The food of claim 12 wherein the thermoplastic polymer comprises a poly(vinyl chloride-co-vinyl
30 acetate) or a poly(vinyl chloride-co-vinylidene dichloride).

14. The food of claim 11 wherein the thermoplastic polymer comprises a polyvinylalcohol, poly(ethylene-co-
35 vinyl alcohol), a poly(ethylene-co-methyl acrylate).

15. The food of claim 10 wherein the cyclodextrin



derivative comprises a β -cyclodextrin derivative.

16. The food of claim 10 wherein the cyclodextrin derivative contains at least one substituent on a
5 cyclodextrin primary carbon atom.

17. The food of claim 10 wherein the cyclodextrin comprises α -cyclodextrin, β -cyclodextrin, γ -cyclodextrin or mixtures thereof.

10

18. The food of claim 10 wherein the thermoplastic web contains about 0.1 to 5 wt-% of the polymer compatible cyclodextrin derivative.

15 19. A method to prevent moisture vapor transmission to an item which method comprises separating the item from a source of moisture by imposing a thermoplastic film barrier between the source of moisture and the item, the film barrier comprising:

20 (a) a thermoplastic polymer web; and
(b) uniformly dispersed in the web, an effective permeant absorbing amount of a polymer compatible derivative cyclodextrin;
wherein the cyclodextrin is free of an inclusion complex
25 compound.

20. The method of claim 19 wherein the thermoplastic polymer comprises a vinyl polymer comprising an alpha-olefin.

30

21. The method of claim 19 wherein the thermoplastic polymer comprises a chlorine containing vinyl polymer comprising vinyl chloride or vinylidene dichloride.

35

22. The method of claim 21 wherein the thermoplastic polymer comprises a poly(vinyl chloride-



* C L M S *



co-vinyl acetate) or a poly(vinyl chloride-co-vinylidene dichloride).

23. The method of claim 20 wherein the
5 thermoplastic polymer comprises a polyvinylalcohol, poly(ethylene-co-vinyl alcohol), a polyethylene-co-methyl acrylate).

24. The method of claim 19 wherein the
10 cyclodextrin derivative comprises a β -cyclodextrin derivative.

25. The method of claim 19 wherein the
cyclodextrin derivative contains at least one
15 substituent on a cyclodextrin primary carbon atom.

26. The method of claim 19 wherein the
cyclodextrin comprises α -cyclodextrin, β -cyclodextrin, γ -cyclodextrin or mixtures thereof.
20

27. The method of claim 19 wherein the
thermoplastic web contains about 0.1 to 5 wt-% of the
polymer compatible cyclodextrin derivative.

25 28. A method to prevent contamination of a food item by a hydrocarbon vapor which method comprises separating the food item from a source of the hydrocarbon by imposing a thermoplastic film barrier between the source of hydrocarbon and the food item, the
30 film barrier comprising:

- (a) a thermoplastic polymer web; and
 - (b) uniformly dispersed in the web, an effective permeant absorbing amount of a polymer compatible cyclodextrin derivative;
- 35 wherein the cyclodextrin is free of an inclusion complex compound.



29. The method of claim 28 wherein the thermoplastic polymer comprises a vinyl polymer comprising an alpha-olefin.

5 30. The method of claim 28 wherein the thermoplastic polymer comprises a chlorine containing vinyl polymer comprising vinyl chloride or vinylidene dichloride.

10 31. The method of claim 30 wherein the thermoplastic polymer comprises a poly(vinyl chloride-co-vinyl acetate) or a poly(vinyl chloride-co-vinylidene dichloride).

15 32. The method of claim 29 wherein the thermoplastic polymer comprises a polyvinylalcohol, poly(ethylene-co-vinyl alcohol) or a polyethylene-co-methyl acrylate).

20 33. The method of claim 28 wherein the cyclodextrin derivative comprises a β -cyclodextrin derivative.

25 34. The method of claim 28 wherein the cyclodextrin derivative contains at least one substituent on a cyclodextrin primary carbon atom.

30 35. The method of claim 28 wherein the cyclodextrin comprises α -cyclodextrin, β -cyclodextrin, γ -cyclodextrin or mixtures thereof.

35 36. The method of claim 28 wherein the thermoplastic web contains about 0.1 to 5 wt-% of the polymer compatible cyclodextrin derivative.

37. A thermoplastic film composition, having improved barrier properties, the film composition



comprising:

(a) a thermoplastic polyethylene having a melt index of 0.1 to 4 and a molecular weight greater than 200,000; and

5 (b) uniformly dispersed in the web, an about 0.1 to 5 wt-% of a permeant absorbing amount of a polymer compatible cyclodextrin derivative; wherein the cyclodextrin is free of an inclusion complex compound.

10

38. The composition of claim 37 wherein the thermoplastic polyethylene comprises a linear polyethylene.

15

39. The composition of claim 38 wherein the thermoplastic polyethylene comprises a linear low density polyethylene.

20

40. The composition of claim 37 wherein the polyethylene has a melt index of about 0.2 to 3.

25

41. The composition of claim 37 wherein the cyclodextrin derivative comprises an acetyl derivative of the cyclodextrin.

42. The composition of claim 37 wherein the cyclodextrin derivative comprises a trimethylsilyl derivative of the cyclodextrin.

30

43. The composition of claim 37 wherein the cyclodextrin comprises a β -cyclodextrin.

35

44. The composition of claim 37 wherein the cyclodextrin derivative is formed on at least one primary carbon of the cyclodextrin.

45. The composition of claim 37 wherein the



cyclodextrin comprises an α -cyclodextrin, a β -cyclodextrin, a γ -cyclodextrin or mixtures thereof.

46. The composition of claim 37 wherein the
5 cyclodextrin is present at a concentration of about 0.1 to 2 wt-%.

47. The composition of claim 37 wherein the
thermoplastic polyethylene comprises a web.

10

48. A thermoplastic film composition, having improved barrier properties, the film composition comprising:

(a) a thermoplastic polymer comprising a
15 chlorine containing vinyl polymer; and

(b) uniformly dispersed in the web, permeant absorbing amount of a polymer compatible cyclodextrin derivative;

wherein the cyclodextrin is free of an inclusion complex
20 compound.

49. The film composition of claim 48 wherein the thermoplastic web comprises a polyvinyl chloride homopolymer.

25

50. The film composition of claim 48 wherein the thermoplastic web comprises a polyvinylidene dichloride homopolymer.

30 51. The film composition of claim 48 wherein the thermoplastic web comprises a poly(vinyl chloride-co-vinylidene dichloride) polymer.

52. The film composition of claim 48 wherein the
35 thermoplastic web comprises a poly(vinyl chloride-co-vinyl acetate).



53. The film composition of claim 48 wherein the cyclodextrin derivative comprises an acetylated cyclodextrin.

5 54. The film composition of claim 48 wherein the cyclodextrin derivative comprises a trimethylsilyl derivative of cyclodextrin.

55. The film composition of claim 48 wherein the
10 cyclodextrin comprises an α -cyclodextrin, a β -cyclodextrin, a γ -cyclodextrin or mixtures thereof.

56. The composition of claim 48 wherein the cyclodextrin derivative is present in the thermoplastic
15 web at a concentration of about 0.5 to 2 wt-%.

57. A method to prevent contamination of a food item by a fragrance, which method comprises separating the food item from a source of the fragrance by imposing
20 a thermoplastic film barrier between the food item and the source of fragrance, the film barrier comprising:
(a) a thermoplastic polymer web; and
(b) a uniformly dispersed in the web, an effective fragrance permeant absorbing amount of a
25 polymer compatible cyclodextrin derivative;
wherein the cyclodextrin is free of an inclusion complex compound.

58. The method of claim 57 wherein the
30 thermoplastic polymer comprises a vinyl polymer comprising an alpha-olefin.

59. The method of claim 57 wherein the thermoplastic polymer comprises a chlorine containing
35 vinyl polymer comprising vinyl chloride or vinylidene dichloride.



60. The method of claim 59 wherein the thermoplastic polymer comprises a poly(vinyl chloride-co-vinyl acetate) or a poly(vinyl chloride-co-vinylidene dichloride).

5

61. The method of claim 58 wherein the thermoplastic polymer comprises a polyvinylalcohol, poly(ethylene-co-vinyl alcohol), a poly(ethylene-co-methyl acrylate).

10

62. The method of claim 57 wherein the cyclodextrin comprises a β -cyclodextrin.

63. The method of claim 57 wherein the cyclodextrin contains at least one substituent on a cyclodextrin primary carbon atom.

64. The method of claim 57 wherein the cyclodextrin comprises α -cyclodextrin, β -cyclodextrin, γ -cyclodextrin, or mixtures thereof.

65. The method of claim 57 wherein the thermoplastic web contains about 0.1 to about 5 wt-% of the polymer compatible cyclodextrin derivative.

25

66. A method for preventing release of a pest attracting aroma from a food item comprising a meat product or a food product containing a cocoa derivative which method comprises imposing a barrier between the food item and the environment effective to prevent the release of a pest attracting aroma, said barrier comprising:

- (a) a thermoplastic polymer web; and
- (b) uniformly dispersed in the web, an effective aroma permeant absorbing amount of the polymer compatible derivative of a cyclodextrin; wherein the cyclodextrin is free of an inclusion complex

35



compound.

67. The method of claim 66 wherein the thermoplastic polymer comprises a vinyl polymer
5 comprising an alpha-olefin.

68. The method of claim 66 wherein the thermoplastic polymer comprises a chlorine containing vinyl polymer comprising vinyl chloride or vinylidene
10 dichloride.

69. The method of claim 68 wherein the thermoplastic polymer comprises a poly(vinyl chloride-co-vinyl acetate) or a poly(vinyl chloride-co-vinylidene
15 dichloride).

70. The method of claim 67 wherein the thermoplastic polymer comprises a polyvinylalcohol, poly(ethylene-co-vinyl alcohol), a poly(ethylene-co-methyl acrylate).
20

71. The method of claim 66 wherein the cyclodextrin comprises a β -cyclodextrin.

25 72. The method of claim 66 wherein the cyclodextrin contains at least one substituent on a cyclodextrin primary carbon atom.

73. The method of claim 66 wherein the
30 cyclodextrin comprises α -cyclodextrin, β -cyclodextrin, γ -cyclodextrin, or mixtures thereof.

74. The method of claim 66 wherein the thermoplastic web contains about 0.1 to about 5 wt-% of
35 the polymer compatible cyclodextrin derivative.

75. A method of manufacturing a thermoplastic



polymer barrier composition, said method comprises:

- (a) introducing a blend of an extrudable thermoplastic and a thermoplastic polymer compatible cyclodextrin derivative into a melt zone producing a compatible blend of the thermoplastic polymer and the polymer compatible cyclodextrin derivative having a temperature of about 390 to 410°F;
- (b) extruding the compatible melt blend in an extrusion die producing an extrudate having a temperature of about 400 to 425°F; and
- (c) cooling the extrudate to form a film.

76. The process of claim 75 wherein the extrusion die comprises a linear extrusion die followed by a biaxially orientation step.

77. The method of claim 75 wherein the extrusion die comprises a circular extrusion die.

78. The method of claim 75 wherein the thermoplastic comprises a vinyl polymer comprising a α -olefin having a molecular weight of greater than 200,000 and a melt index of about 0.1 to 4.

79. The method of claim 75 wherein the thermoplastic polymer comprises a chlorine containing vinyl polymer comprising vinyl chloride or vinylidene dichloride.

80. The method of claim 79 wherein the thermoplastic polymer comprises a polyvinyl chloride co-vinyl acetate or a polyvinyl chloride co-vinylidene dichloride.

81. The method of claim 78 wherein the thermoplastic polymer comprises a polyvinylalcohol,



poly(ethylene-co-vinyl alcohol) or a poly(ethylene-co-methyl acrylate).

82. The method of claim 75 wherein the
5 cyclodextrin comprises a β -cyclodextrin.

83. The method of claim 75 wherein the
cyclodextrin comprises α -cyclodextrin, β -cyclodextrin,
 γ -cyclodextrin or mixtures thereof.
10

84. The method of claim 78 wherein the polymer is
linear low density polyethylene.

85. A thermoplastic film composition, having
15 improved barrier properties, the film composition
comprising:

(a) a web comprising a thermoplastic
polypropylene web having a melt index of 0.1 to 4
and a molecular weight greater than 200,000; and
20 (b) uniformly dispersed in the web, and about
0.1 to 5 wt-% of a permeant absorbing amount of a
polymer compatible cyclodextrin derivative;
wherein the cyclodextrin is free of an inclusion complex
compound.

25

86. The composition of claim 85 wherein the
polymer molecular weight is greater than 250,000.

87. The composition of claim 85 wherein the
30 polypropylene has a melt index of about 0.2 to 3.

88. The composition of claim 85 wherein the
cyclodextrin derivative comprises an acetyl derivative
of the cyclodextrin.

35

89. The composition of claim 85 wherein the
cyclodextrin derivative comprises a trimethylsilyl



derivative of the cyclodextrin.

90. The composition of claim 85 wherein the cyclodextrin comprises a β -cyclodextrin.

5

91. The composition of claim 85 wherein the cyclodextrin derivative is formed on at least one primary carbon of the cyclodextrin.

10

92. The composition of claim 85 wherein the cyclodextrin comprises an α -cyclodextrin, a β -cyclodextrin, a γ -cyclodextrin or mixtures thereof.

15

93. The composition of claim 85 wherein the cyclodextrin is present at a concentration of about 0.1 to 2 wt-%.

20

94. The composition of claim 85 wherein the thermoplastic polypropylene comprises a web.

95. A thermoplastic film composition, having improved barrier properties, the film composition comprising:

25

- (a) a polymer web; and
- (b) a coating on the web comprising at least one layer of a film forming polymer and uniformly dispersed in the layer, an effective permeant absorbing amount of a polymer compatible cyclodextrin derivative;

30

wherein the cyclodextrin is substantially free of an inclusion complex compound.

35

96. The film of claim 95 wherein the film forming polymer comprises a vinyl polymer comprising an alpha-olefin.

97. The film of claim 96 wherein the film forming



polymer comprises a polyethelene or a polypropylene.

98. The film of claim 95 wherein the film forming polymer comprises a chlorine containing polymer.

5

99. The film of claim 98 wherein the chlorine containing vinyl polymer comprising vinyl chloride or vinylidene dichloride.

10 100. The film of claim 98 wherein the film forming polymer comprises a poly(vinyl chloride-co-vinyl acetate) or a poly(vinyl chloride-co-vinylidene dichloride).

15 101. A film of claim 95 wherein the film forming polymer comprises a polyvinylalcohol, poly(ethylene-co-vinyl alcohol), a poly(ethylene-co-acrylic acid) or a poly(ethylene-co-methyl acrylate).

20 102. The film of claim 95 wherein the cyclodextrin derivative comprises a β -cyclodextrin derivative.

25 103. The film of claim 95 wherein the cyclodextrin derivative contains at least one substituent on a cyclodextrin primary carbon atom.

104. The film of claim 95 wherein the cyclodextrin comprises α -cyclodextrin, β -cyclodextrin, γ -cyclodextrin or mixtures thereof.

30

105. The film of claim 95 wherein the coating contains about 0.1 to 10 wt-% of the polymer compatible cyclodextrin derivative.

35 106. A laminate comprising at least two films, at least one film comprising the film of claim 1.

1/3

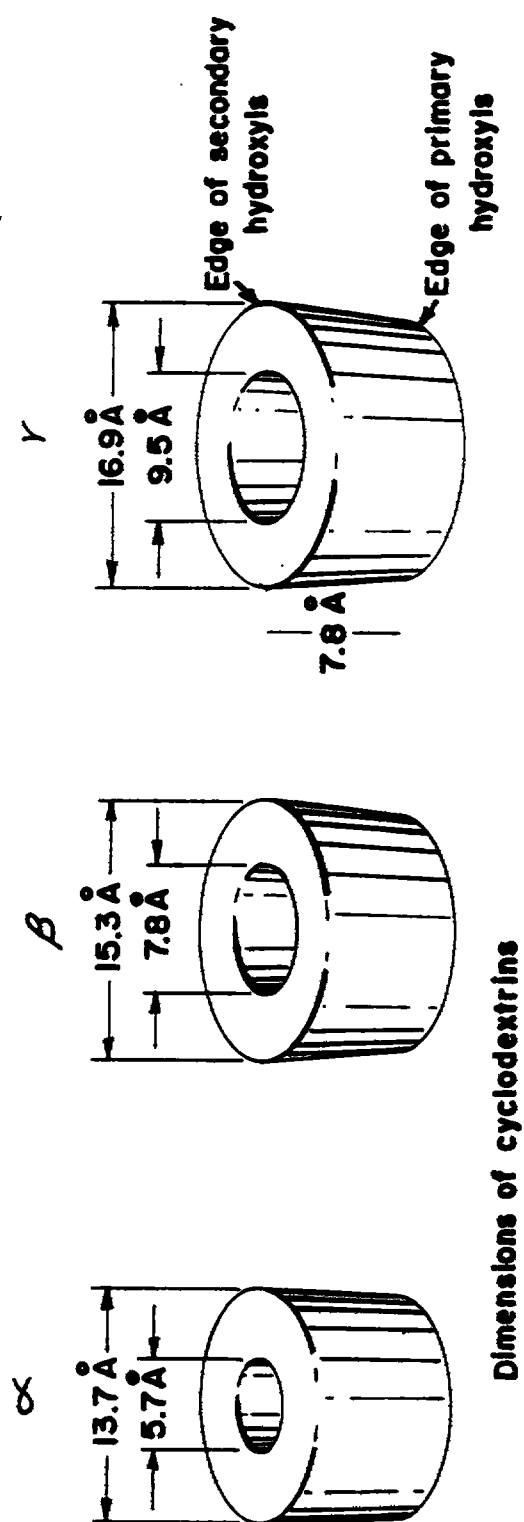


FIG.1

FIG. 2

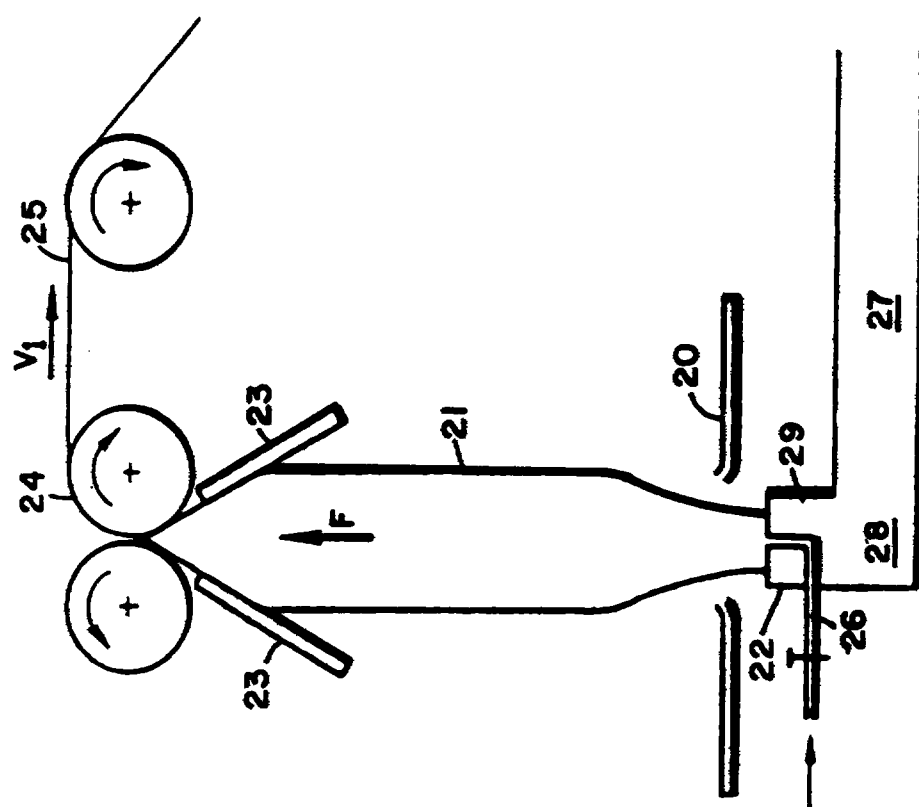
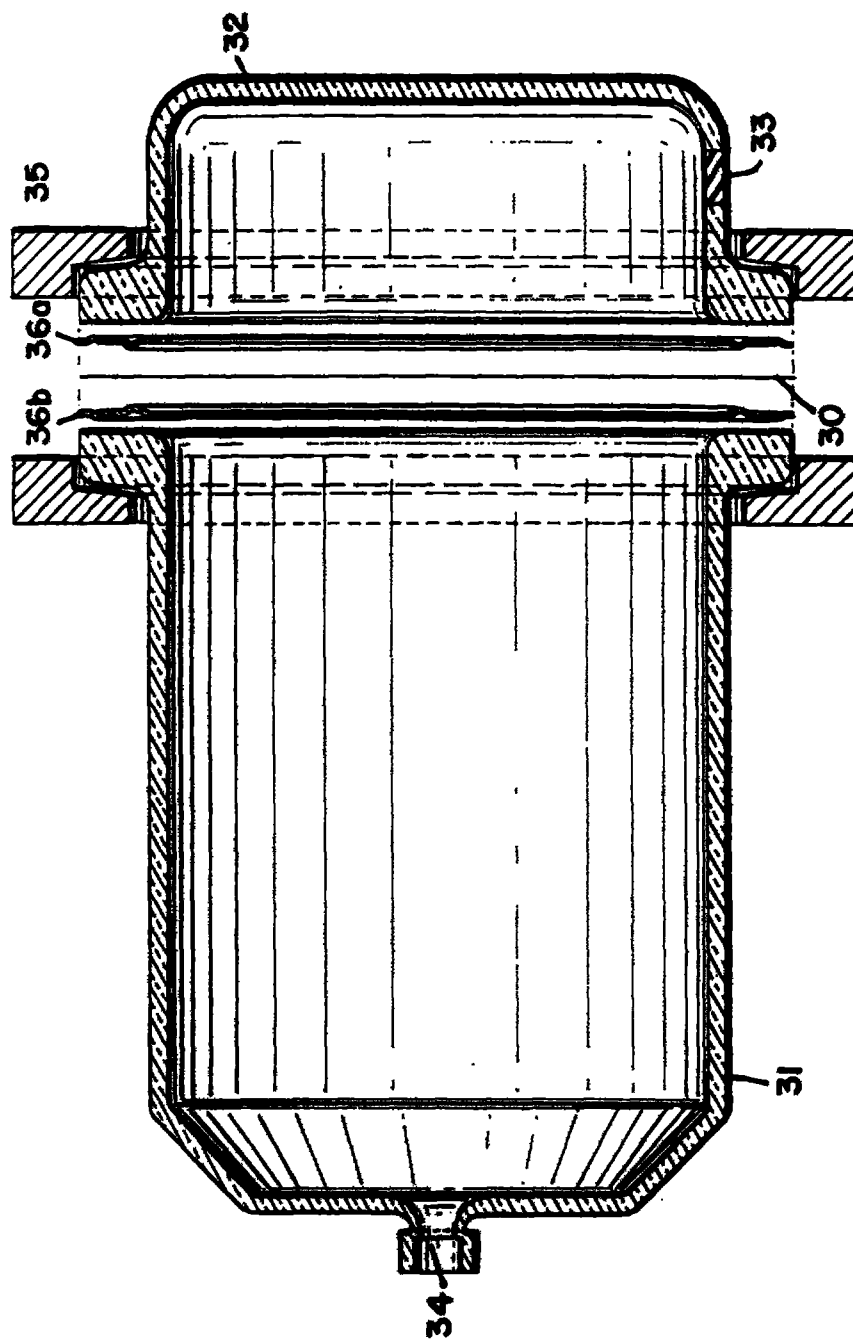


FIG. 3



quenching bath can be used. Thermoplastic materials can also be blown. The hot melt polymer is extruded in Fig. 2 in an annular die 22 in a tube form 21. The tube is inflated with air (see air inlet 26) to a diameter
5 determined by the desired film properties and by practical handling considerations. As the hot melt polymer emerges from the annular die, the extruded hot tube is expanded by air to 1.2 or four (4) times its initial die diameter. At the same time the cooling air
10 (see air flow 20) chills the web forming a solid extruded with a hollow circular cross section 21. The film tube is collapsed within a V-shaped frame 23 and is nipped at the end of the frame (nip rolls 24) to trap air within the thus formed bubble. Rolls 24 and 25 draw
15 the film from the die maintaining a continuous production of the extruded tube.

We have found that in the preparation of biaxially oriented film and in the production of blown thermoplastic film that the melt temperature and the die
20 temperature are important in obtaining the permeability or permeant transmission rates preferred for films of the invention, to reduce melt fracture and to improve film uniformity (reduce surface defects). Referring to Figure 2, the temperature of the melt at the melt region
25 28 should range from about 390-420°F (198-216°C), preferably 395-415°F (202-213°C). The temperature of the extrusion die 29 should range from about 400-435°F (204-224°C), preferably 410-430°F (210-221°C). The extruded polymer can be cooled using ambient water baths
30 or ambient air. The extruder can be operated at through put such that production rates can be maintained but the polymer can be sufficiently heated to achieve the melt and die temperatures required. Production of the films of the invention at these temperatures ensures that the
35 cyclodextrin material is fully compatible in the thermoplastic melt, is not degraded by the high temperatures and a clear compatible useful barrier film

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is produced.

Often two thermoplastic materials are joined in a coextrusion process to produce tailored film or sheet products adapted to a particular end use. One or more
5 polymer types in two or more layers of melt are coextruded in a coextrusion die to have a film with versatile properties dried from both layers. Layers of the different polymers or resins are combined by either blending the materials in melt before extrusion or by
10 parallel extrusion of the different thermoplastics. The melt flows laminarly through the die and onto a quenched drum. The film is processed conventionally and may be oriented after cooling. Films can contain a variety of additives such as antioxidants, heat stabilizers, UV
15 stabilizers, slip agents, fillers, and anti-block agents.

The barrier layer of the invention can be made by casting an aqueous dispersion or solvent dispersion or solution of a film forming polymer and the cyclodextrin
20 derivative. The aqueous or solvent based material can be formed by commonly available aqueous or solvent based processing of commercially available polymers, polymer dispersions, polymer solutions or both polymer and common aqueous or solvent processing technology. The
25 cyclodextrin derivative material can be combined with such aqueous or solvent based dispersions or solutions to form a film forming or readily formed coating material. Such barrier layers or barrier coatings can be formed using commonly available coating technology
30 including roller coating, doctor blade coating, spin coating, etc. While the coatings can be made and removed from a preparative surface, commonly coatings are formed on a thermoplastic or thermosetting polymer web, and remain in place to act as a barrier layer on a
35 polymeric web used in a packaging. The typical coatings can be made from the same thermoplastic polymer materials used in film sheet or other structural layers

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using substantially similar loadings of the cyclodextrin derivative material. The barrier layer or barrier coatings formed using the film forming polymer and the cyclodextrin derivative can be used as a single coating layer or can be used in a multiple coating structure having a barrier layer or coating on one or both sides of a structural film or sheet which can be used with other coating layers including printing layers, clear coating layers and other layers conventional in packaging, food packaging, consumer product packaging, etc.

Cyclodextrin

The thermoplastic films of the invention contain a cyclodextrin having pendent moieties or substituents that render the cyclodextrin material compatible with the thermoplastic polymer. For this invention, compatible means that the cyclodextrin material can be uniformly dispersed into the melt polymer, can retain the ability to trap or complex permeant materials or polymer impurity, and can reside in the polymer without substantial reductions in polymer film characteristics. Compatibility can be determined by measuring polymer characteristics such as tensile strength, tear resistance, etc., permeability or transmission rates for permeants, surface smoothness, clarity, etc. Non-compatible derivatives will result in substantial reduced polymer properties, very high permeability or transmission rates and rough dull film. Qualitative compatibility screening can be obtained by preparing small batches (100 grams-one kilogram of thermoplastic and substituted cyclodextrin). The blended material is extruded at production temperatures as a linear strand extrudate having a diameter of about one to five mm. Incompatible cyclodextrin materials will not disperse uniformly in the melt and can be seen in the transparent melt polymer immediately upon extrusion from the

extrusion head. We have found the incompatible cyclodextrin can degrade at extrusion temperatures and produce a characteristic "burnt flour" odor in an extrusion. Further, we have found that incompatible
5 cyclodextrin can cause substantial melt fracture in the extrudate which can be detected by visual inspection. Lastly, the extrudate can be cut into small pieces, cross-sectioned and examined using an optical microscope to find incompatible
10 cyclodextrin clearly visible in the thermoplastic matrix. Cyclodextrin is a cyclic oligosaccharide consisting of at least six glucopyranose units joined by $\alpha(1\rightarrow4)$ linkages. Although cyclodextrin with up to twelve glucose residues are known, the three most common
15 homologs (α cyclodextrin, β cyclodextrin and γ cyclodextrin) having 6, 7 and 8 residues have been used.

Cyclodextrin is produced by a highly selective enzymatic synthesis. They consist of six, seven, or
20 eight glucose monomers arranged in a donut shaped ring, which are denoted α , β , or γ cyclodextrin respectively (See Figure 1). The specific coupling of the glucose monomers gives the cyclodextrin a rigid, truncated conical molecular structure with a hollow interior of a
25 specific volume. This internal cavity, which is lipophilic (i.e.,) is attractive to hydrocarbon materials (in aqueous systems is hydrophobic) when compared to the exterior, is a key structural feature of the cyclodextrin, providing the ability to complex
30 molecules (e.g., aromatics, alcohols, halides and hydrogen halides, carboxylic acids and their esters, etc.). The complexed molecule must satisfy the size criterion of fitting at least partially into the cyclodextrin internal cavity, resulting in an inclusion
35 complex.

rate of aromatic hydrocarbons, aliphatic hydrocarbons, ethanol and water vapor can be achieved using the cyclodextrin derivative technology. We have also found that the use of cyclodextrin materials improve the

5 surface properties of the film. The surface tension of the film surface and surface electrical properties were also improved. Such a result increases the utility of the films of the invention in coating, printing, laminating, handling, etc. In initial work we have also

10 found (1) several modified cyclodextrin candidates were found to be compatible with the LLDPE resin and provide good complexation of residual LLDPE volatile contaminants as well as reduce organic permeants diffusing through the film. (2) Unmodified β CD

15 adversely affects transparency, thermal stability, machinability, and barrier properties of the film. Conversely, selected modified β CD (acetylated and trimethylsilyl ether derivatives) have no affect on transparency and thermal stability. The machinability

20 of the extruded plastic material is effected somewhat causing some surface defects, thereby reducing the barrier properties of the film. (3) Films containing a modified β CD composition (1% by weight) reduce aromatic permeants by 35% at 72°F and 38% at 105°F (40.5°C);

25 aliphatic permeants were reduced by only 9% at 72°F (22°C). These results would improve significantly if worst case shelf-life testing conditions were not used to test the films. (4) Complexation rates were different for aromatic and aliphatic permeants. Films

30 containing modified β CD had better complexation rates for aromatics (gasoline-type compounds) than aliphatic (printing ink-type compounds). Conversely, film coating had significantly better complexation of aliphatic compound than aromatic compounds. (5) β CD containing

35 acrylic coatings were the star performers reducing aliphatic permeants from 46% to 88%, while aromatics were reduced by 29%.

odor problem is believed to be the result of direct decomposition of the CD or impurity in the CD. Two odor-active compounds (2-furaldehyde and 2-furanmethanol) were identified in the blown film samples.

Of the three modified compatible CD candidates (acetylated, octanyl succinate and trimethylsilyl ether), the acetylated and trimethylsilyl ether CD were shown to effectively complex trace volatile organics inherent in the LLDPE resin. One percent loadings of acetylated and trimethylsilyl ether (TMSE) β CD showed approximately 50% of the residual LPDE organic volatiles were complexed, while the octanyl succinate CD did not complex residual LLDPE resin volatiles. Milled β CD was found to be less effective (28%) than the acetylated and TMSE modified β CD's.

Plastic packaging materials all interact to some degree with the food product they protect. The main mode of interaction of plastic packaging of food is through the migration of organic molecules from the environment through the polymer film into the head space of the package where they are absorbed by the food product. Migration or transfer of organic molecules of the package to the food, during storage, is effected by environmental conditions such as temperature, storage time, and other environmental factors (e.g., humidity, type of organic molecules and concentration thereof). Migration can have both quality (consumer resistance) and toxicological influence. The objective of packaging film testing is to measure how specific barriers may influence the quality of packaged individual foods. To simulated accelerated shelf-life testing for low-water-activity food products, the testing was conducted at a temperature of 72°F (22°C) and 105°F (40.5°C), and a relative humidity of 60%. These temperature and humidity conditions are probably similar to those found in uncontrolled warehouses, in transit, and in storage.

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cumulative penetrant concentration on the sample-side of the film is plotted as a function of time.

We produced four experimental test films. Three of the films contained β CD at loading of 1%, 3% and 5% (wt/wt) while the fourth was a control film made from the same batch of resin and additives but without β CD.

A second experimental technique was also undertaken to determine whether β CD sandwiched between two control films will complex organic vapors permeating the film. The experiment was carried out by lightly dusting β CD between two control film sheets.

The testing showed the control film performed better than β CD loaded films. The permeation test results also demonstrated the higher the β CD loading the poorer the film performed as a barrier. The test results for sandwiching β CD between two control films showed β CD being twice as effective in reducing permeating vapors than the control samples without β CD. This experiment supported that CD does complex permeating organic vapors in the film if the film's barrier qualities are not changed during the manufacturing process making the film a less effective barrier.

The 1% TMSE β CD film was slightly better than the 1% acetylated β CD film (24% -vs- 26%) for removing aromatic permeants at 72°F (22°C) adding more modified CD appeared to have no improvement.

For aromatic permeants at 105°F (40.5°C), both 1% TMSE β CD and 1% acetylated β CD are approximately 13% more effective removing aromatic permeants than 72°F (22°C). The 1% TMSE film was again slightly better than the 1% film (36% -vs- 31%) for removing aromatic permeants.

The 1% TMSE film was more effective initially removing aliphatic permeants than the 1% acetylated β CD film at 72°F (22°C). But for the duration of the test, 1% TMSE β CD was worse than the control while 1%

acetylated β CD removed only 6% of the aliphatic permeants.

We produced two experimental aqueous coating solutions. One solution contained hydroxyethyl β CD (35% by weight) and the other solution contained hydroxypropyl β CD (35 by weight). Both solutions contained 10% of an acrylic emulsion comprising a dispersion of polyacrylic acid having a molecular weight of about 150,000 (Polysciences, Inc.) (15% solids by weight) as a film forming adhesive. These solutions were used to hand-coat test film samples by laminating two LLDPE films together. Two different coating techniques were used. The first technique very slightly stretched two film samples flat, the coating was then applied using a hand roller, and then the films were laminated together while stretched flat. The Rev. 1 samples were not stretched during the lamination process. All coated samples were finally placed in a vacuum laminating press to remove air bubbles between the film sheets. Film coating thicknesses were approximately 0.0005 inches (0.013 mm). These CD coated films and hydroxymethyl cellulose coated control films were subsequently tested.

A reduction in aromatic and aliphatic vapors by the hydroxyethyl β CD coating is greater in the first several hours of exposure to the vapor and then diminishes over the next 20 hours of testing. Higher removal of aliphatic vapors than aromatic vapors was achieved by the hydroxyethyl β CD coating; this is believed to be a function of the difference in their molecular size (i.e., aliphatic compounds are smaller than aromatic compounds). Aliphatic permeants were reduced by 46% as compared to the control over the 20 hour test period. Reduction of aromatic vapors was 29% as compared to the control over the 17 hour test period.

The Rev. 1 coated hydroxyethyl β CD reduced the aliphatic permeants by 87% as compared to the control

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over the 20 hour test period. It is not known if the method of coating the film was responsible for the additional 41% reduction over the other hydroxyethyl β CD coated film.

- 5 The hydroxyethyl β CD coating was slightly better for removing aromatic permeants than the hydroxypropyl β CD coating (29% -vs- 20%) at 72°F (22°C).

LARGE SCALE FILM EXPERIMENTAL

10 Preparation of Cyclodextrin Derivatives

Example I

- An acetylated β -cyclodextrin was obtained that contained 3.4 acetyl groups per cyclodextrin on the
15 primary -OH group.

Example II

 Trimethyl Silyl Ether of β -cyclodextrin

- Into a rotary evaporator equipped with a 4000 milliliter round bottom flask and a nitrogen atmosphere,
20 introduced at a rate of 100 milliliters N_2 per minute, was placed three liters of dimethylformamide. Into the dimethylformamide was placed 750 grams of β -cyclodextrin. The β -cyclodextrin was rotated and dissolved in dimethylformamide at 60°C. After
25 dissolution, the flask was removed from the rotary evaporator and the contents were cooled to approximately 18°C. Into the flask, placed on a magnetic stirrer and equipped with a stir bar, was added 295 milliliters of hexamethyldisilylazine (HMDS- Pierce Chemical No.
30 84769), followed by the careful addition of 97 milliliters of trimethylchlorosilane (TMCS - Pierce Chemical No. 88531). The careful addition was achieved by a careful dropwise addition of an initial charge of 20 milliliters and after reaction subsides the careful
35 dropwise addition of a subsequent 20 milliliter portions, etc. until addition is complete. After the addition of the TMCS was complete, and after reaction

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subsides, the flask and its contents were placed on the rotary evaporator, heated to 60°C while maintaining an inert nitrogen atmosphere flow of 100 milliliters of N₂ per minute through the rotary evaporator. The reaction
5 was continued for four hours followed by removal of solvent, leaving 308 grams of dry material. The material was removed from the flask by filtering, washing the filtrate with deionized water to remove the silylation products, vacuum oven drying (75°C at 0.3
10 inches of Hg [10kPa]) and stored as a powdered material and maintained for subsequent compounding with a thermoplastic material. Subsequent spectrographic inspection of the material showed the β -cyclodextrin to contain approximately 1.7 trimethylsilylether
15 substituent per β -cyclodextrin molecule. The substitution appeared to be commonly on a primary 6-carbon atom.

Example III

20 An hydroxypropyl β -cyclodextrin was obtained with 1.5 hydroxypropyl groups per molecule on the primary 6-OH group of the β CD.

Example IV

25 An hydroxyethyl β -cyclodextrin was obtained with 1.5 hydroxyethyl groups per molecule on the primary 6-OH group of the β CD.

Preparation of Films

We prepared a series of films using a linear low density polyethylene resin, β CD and derivatized β CD such as the acetylated or the trimethylsilyl derivative of a β -cyclodextrin. The polymer particles were dry blended with
5 the powdered β -cyclodextrin and β -cyclodextrin derivative material, a fluoropolymer lubricant (3M) and the antioxidant until uniform in the dry blend. The dry blend material was mixed and extruded in a pellet form in a Haake System 90, 3/4" conical extruder. The resulting pellets
10 were collected for film preparation.

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Table IA displays typical pelletizing extruder conditions. The films were blown in the apparatus of Figure 2. Figure 2 shows extruded thermoplastic tube 21 exiting the die 22. The tube is collapsed by die 23 and
5 layered by rollers 24 into the film 25. The extruded tube 21 is inflated using air under pressure blown through air inlet tube 26. The thermoplastic is melted in the extruder. The extruder temperature is taken at the mixing zone 27. The melt temperature is taken in the melt zone 28
10 while the die temperature is taken in the die 29. The extrudate is cooled using an air blown cooling stream from the cooling ring 20. The general schematic background of Figure 2 is representative of the Kiefel blown film extruder, 40 mm die diameter, used in the actual
15 preparation of the blown film. The film is manufactured according to the above protocol and reported in Table IB. The film was tested for transmission rates at a variety of environmental conditions. Environmental test conditions are shown below in Table II.

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TABLE IA

0.5% TMSF Pelletizing 1-19-94

Run Time	0 min	Torque	4866 meter-gram	Rotor	198 rpm
	13 sec	Tot. Torque	0.0 mkg-min	Aux.	0 %
Channels	-1-	-2-	-3-	-4-	-5-
Melt Temp	37	41	41	41	°C
Set Temp	150	160	160	170	°C
Deviation	0	0	0	0	°C
Cooling	Yes	Yes	Yes	Yes	
Pressure	0	0	2739	0	psi
			(18.9 mpa)		

TABLE IB
Extruded Films (Bxton M3201)
Made With Low Density Polyethylene

Roll No.	Sample ID	Fluoropolymer Additive	Extruder Temp. Zone 3 (°F)	Melt Temp (°F)	Die Temp. Zone 3 (°F)	Lbs./Hr (g/s)	RPM	Die Gap	Comments
1	Control	500 ppm	426 (220°C)	406 (208°C)	406 (208°C)	30.1 (3.81)	50	24	
2	1 % Ex. I	1000 ppm	441 (227°C)	415 (213°C)	420 (216°C)	29.7 (3.74)	50	35	
3	1 % Ex. I	1000 ppm	441 (227°C)	416 (213.3°C)	420 (216°C)	28.5 (3.59)	50	35	
4	1 % Ex. I	500 ppm	441 (227°C)	415 (213°C)	420 (216°C)	29.9 (3.77)	50	35	
5	1 % Ex. I	500 ppm	421 (216°C)	405 (207°C)	414 (212°C)	29.0 (3.65)	50	35	
6	1 % Ex. I	500 ppm	421 (216°C)	397 (203°C)	415 (213°C)	29.0 (3.65)	50	35	
7	0.5% Ex. I	500 ppm	421 (216°C)	401 (206°C)	415 (213°C)	27.7 (3.49)	50	35	Very slight melt fracture
8	2 % Ex. I	500 ppm	421 (216°C)	404 (207°C)	415 (213°C)	26.3 (3.36)	50	35	Particles in film.
9	1 % Ex. II	500 ppm	426 (219°C)	410 (210°C)	415 (213°C)	26.7 (3.36)	50	35	Particles in film.
10	1 % Ex. II	500 ppm	432 (222°C)	415 (213°C)	414 (212°C)	29.0 (3.65)	50	35	Particles in film.
11	1 % Ex. II	500 ppm	431 (221.6°C)	414 (213°C)	415 (213°C)	21.5 (2.71)	39	35	Very slight yellowing to film.
12	1 % Ex. II	500 ppm	431 (221.6°C)	415 (213°C)	415 (213°C)	27.7 (3.49)	35	35	Particles in film.
13	0.5% Ex. II	500 ppm	425 (218°C)	410 (210°C)	415 (213°C)	28.9 (3.64)	50	35	Particles in film.
14	0.5% Ex. II	500 ppm	410 (210°C)	414 (212°C)	415 (213°C)	20.2 (2.55)	38	35	Particles in film.
15	2 % Ex. II	500 ppm	422 (217°C)	415 (213°C)	415 (213°C)	20.5 (2.58)	38	35	Very slight yellowing to film.
16	2 % Ex. II	500 ppm	422 (217°C)	415 (213°C)	415 (213°C)	20.5 (2.58)	38	35	Particles in film.
17	2 % Ex. II	500 ppm	422 (217°C)	416 (213.3°C)	415 (213°C)	20.5 (2.58)	38	35	Very slight yellowing to film.

Also contains 500 ppm Irganox 1010 antioxidant and 1000 ppm Irgafos 168.

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TABLE II
Test Conditions

Roll Sample ID Number	Temp. (°F)	Sample Side	Revol. Side	Permeant ^a
Roll #2 Roll #3 Roll #5 Roll #6	72 (22°C)	Rm & RH	Rm & RH	Aromatic/Alcohol
Roll #5 Roll #8	72 (22°C)	Rm & RH	Rm & RH	Aromatic/Alcohol
Roll #7 Roll #5 Roll #8	72 (22°C)	0.25 Aw	60 & RH	Aromatic/Alcohol
Roll #7 Roll #5 Roll #8	72 (22°C)	.60 Aw	10 & RH	Aromatic/Alcohol
Roll #2 Roll #3 Roll #4 Roll #5 Roll #6 Roll #8 Roll #12	105 (40.5°C)	Rm & RH	Rm & RH	Aromatic/Alcohol
Roll #7 Roll #5 Roll #8	105 (40.5°C)	0.25 Aw	15 & RH	Aromatic/Alcohol
Roll #13 Roll #14 Roll #9 Roll #11 Roll #12	72 (22°C)	Rm & RH	Rm & RH	Aromatic/Alcohol

TABLE II (cont.)

Test Conditions

Roll Sample ID Number	Temp. (F)	Sample Side	Environment Side	Test Material
Roll #15 Roll #16 Roll #17	105 (40.5°C)	Rm & RH	Rm & RH	Aromatic/Alcohol
Roll #14 Roll #15				
10% Rx. III in PVDC	72 (22°C)	0.25 Aw	60 & RH	Aromatic/Alcohol
20% Rx. III in PVDC				
5% Rx. III/ Ac. IIIc	72 (22°C)	Rm & RH	Rm & RH	Aromatic/Alcohol
10% Rx. III/ Acrylic				
Roll #7 Roll #5 Roll #8	72 (22°C)	Rm & RH	Rm & RH	Naphtha
Roll #12 Roll #15	72 (22°C)	Rm & RH	Rm & RH	Naphtha

3 7 ppm aromatic plus 20 ppm EtOH.

4 40 ppm Naphtha

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Comparison of Transmission Rates in
Modified β -Cyclodextrin - I/PDE Films

Temperature: 72°F (22°C)
Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatics %		Tot. Volatiles %	
	Aromatic Transmission Rate*	Improvement Over Control	Total Volatiles Transmission Rate*	Improvement Over Control
Control Film	3.35E-04	0%	3.79E-04	0%
1.0% CS-001 (Roll #2)	3.18E-04	5%	3.61E-04	5%
1.0% CS-001 (Roll #3)	2.01E-04	40%	2.55E-04	33%
1.0% CS-001 (Roll #5)	2.67E-04	20%	3.31E-04	13%
1.0% CS-001 (Roll #6)	3.51E-04	-5%	3.82E-04	-1%

Comparison of Transmission Rates in
Modified β -Cyclodextrin - I/PDE Films

Temperature: 72°F (22°C)
Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatic		Naphtha %	
	Transmission Rate*	Improvement Over Control	Transmission Rate*	Improvement Over Control
Control Film (Roll #1)	7.81E-03	0%		
0.5% CS-001 (Roll #7)	7.67E-03	2%		
1% CS-001 (Roll #5)	7.37E-03	6%		
2% CS-001 (Roll #8)	6.53E-03	16%		

* $9\text{m} \times 0.001\text{ in.} (0.025\text{ mm})$
 $100\text{ in}^2 (0.0645\text{ m}^2) \times 24\text{ hrs.}$

Temperature: 72°F (22°C)
Sample Side: Room & Rill
Environment: Room & Rill

<u>Sample</u> <u>Identification</u>	<u>Aromatic</u> <u>Transmission Rate</u>	<u>Aromatics %</u> <u>Improvement</u> <u>Over Control</u>	<u>Total Volatiles</u> <u>Transmission Rate</u>	<u>T. Volatiles %</u> <u>Improvement</u> <u>Over Control</u>
Control Film (Roll #1)	5.16E-04	0%	5.63E-04	0%
1.0% CS-001 (Roll #5)	4.01E-04	22%	5.17E-04	8%
2.0% CS-001 (Roll #8)	2.91E-04	44%	3.08E-04	45%

Comparison of Transmission Rates in Modified β -Cyclodextrin - LPDE Films

Temperature 72°F (22°C)
Sample Side: Room 5 RH
Environment: Room 5 RH

Sample Identification	Aromatic Transmission Rate*	Naphtha % Improvement Over Control
Control Film (Roll #1)	7.81E-03	0%
0.5% CS-001 (Roll #7)	7.67E-03	2%
1% CS-001 (Roll #5)	7.37E-03	6%
2% CS-001 (Roll #8)	6.53E-03	16%

$$\frac{\text{gm} \cdot 0.001 \text{ in.} (0.025 \text{ mm})}{100 \text{ in}^2 (0.0645 \text{ m}^2) \cdot 24 \text{ hrs.}}$$

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Comparison of Transmission Rates in
Modified β -Cyclodextrin - LADPE Films

Temperature 72°F (22°C)
Sample Side: 0.25 Aw
Environment: 60% RH

Sample Identification	Aromatic Transmission Rate*	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate*	T. Volatiles % Improvement Over Control
Control Film (Roll #1)	3.76E-04	0%	3.75E-04	0%
0.5% CS-001 (Roll #7)	2.42E-04	36%	2.41E-04	36%
1% CS-001 (Roll #5)	3.39E-04	10%	3.38E-04	10%
2% CS-001 (Roll #8)	2.48E-04	34%	2.47E-04	34%

Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 105°F (40.5°C)
Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatic Transmission Rate*	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate*	T. Volatiles % Improvement Over Control
Control Film (Roll #1)	1.03E-03	0%	1.13E-03	0%
1% CS-001 (Roll #2)	5.49E-04	47%	5.79E-04	49%
1% CS-001 (Roll #3)	4.74E-04	54%	5.00E-04	56%
1% CS-001 (Roll #4)	6.41E-04	38%	6.83E-04	40%
1% CS-001 (Roll #5)	5.22E-04	49%	5.54E-04	51%
1% CS-001 (Roll #6)	4.13E-04	60%	4.39E-04	61%
2% CS-001				

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(ROI #8)	5.95E-04	4.2%	6.18E-04	4.5%
1% TMSR				
(ROI #12)	8.32E-04	1.9%	8.93E-04	2.1%
* $\frac{\text{gm} \cdot 0.001 \text{ in.} \cdot (0.025 \text{ mm})}{100 \text{ in}^2 (0.0645 \text{ m}^2) \cdot 24 \text{ hrs}}$				

(Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature: 105°F (40.5°C)
Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatic Transmission Rate*	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate*	T. Volatiles % Improvement Over Control
Control Film (Roll #1)	4.34E-04	0%	4.67E-04	0%
0.5% CS-001 (Roll #7)	4.03E-04	7%	4.41E-04	6%
1.0% CS-001 (Roll #5)	5.00E-04	-15%	5.33E-04	-14%
2.0% CS-001 (Roll #8)	3.96E-04	9%	3.94E-04	16%

(Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature: 72°F (22°C)
Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatic Transmission Rate*	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate*	T. Volatiles % Improvement Over Control
Control Film 0.5% TMSE (Roll #13)	3.09E-04	0%	3.45E-04	0%
0.5% TMSE (Roll #14)	2.50E-04	19%	2.96E-04	14%
1% TMSE (Roll #9)	2.37E-04	23%	2.67E-04	33%
1% TMSE (Roll #10)	2.67E-04	14%	3.05E-04	12%
1% TMSE (Roll #11)	4.85E-04	-57%	5.27E-04	-53%
1% TMSE (Roll #12)	2.58E-04	17%	2.92E-04	15%
	2.15E-04	31%	2.55E-04	26%

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2% TMSB (Roll #15)	2.54E-04	18%	3.04E-04	12%
2% TMSB (Roll #16)	2.79E-04	10%	3.21E-04	7%
2% TMSB (Roll #17)	2.81E-04	9%	3.24E-04	6%
* $\frac{gm \cdot 0.001 in. (0.025 mm)}{100 in^2 (0.0645 m^2)} \cdot 24 hrs.$				

Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPPDE Films

Temperature 72°F (22°C)
Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatic Transmission Rate*	Naphtha % Improvement Over Control
Control Film (Roll #1)	9.43E-03	0%
1% TMSE (Roll #12)	1.16E-02	-23%
2% TMSE (Roll #15)	1.56E-02	-65%

Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPPDE Films

Temperature 72°F (22°C)
Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatic Transmission Rate*	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate*	T. Volatiles % Improvement Over Control
Control Film (Roll #1)	8.36E-04	0%	9.05E-04	0%
0.5% TMSE (Roll #14)	6.77E-04	19%	7.25E-04	20%
2% TMSE (Roll #15)	6.36E-04	24%	6.81E-04	25%

* $\frac{\text{gm} \cdot 0.001 \text{ in.} (0.025 \text{ mm})}{100 \text{ in}^2 (0.0645 \text{ m}^2) \cdot 24 \text{ hrs.}}$

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Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 72°F (22°C)
Sample Side: 0.25 Aw
Environment: 60% RH

Sample Identification	Aromatic Transmission Rate	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate	T. Volatiles % Improvement Over Control
PVdC Control	6.81E-05	0%	1.05E-04	0%
PVdC w/ 10% HP B-CyD	1.45E-05	79%	2.39E-05	77%
PVdC w/ 20% HP B-CyD	9.71E-05	-42%	1.12E-04	-7%

Comparison of Transmission Rates in
Modified β -Cyclodextrin - LPDE Films

Temperature 72°F (22°C)
Sample Side: Room % RH
Environment: Room % RH

Sample Identification	Aromatic Transmission Rate	Aromatics % Improvement Over Control	Total Volatiles Transmission Rate	T. Volatiles % Improvement Over Control
Control Acrylic	2.07E-06	0%	2.10E-05	0%
5% HP B-CyD/ Acrylic	1.50E-06	27%	2.07E-05	1%
10% HP B-CyD/ Acrylic	4.13E-06	-100%	4.30E-05	-105%

* $9m \times 0.001 in. (0.025 mm)$
 $100 in^2 (0.0645 m^2) \cdot 24 hrs.$

We prepared a series of aqueous coatings containing hydroxypropyl β CD. One of the coatings was prepared from a 10% acrylic emulsion (a polyacrylic acid polymer having a molecular weight of about 150,000 purchased from Polysciences, Inc.). The 10% acrylic emulsion contained hydroxypropyl β CD at a 5% and 10% by weight loading. These solutions were used to hand-coat test film samples by laminating two films. The coatings were applied to linear low density polyethylene film sheet containing 0.5% acetylated β CD (Roll No. 7) and to a second film sheet containing 2% acetylated β CD (Roll No. 8) using a hand roller and then laminating the films. The films were not stretched during lamination. All coated samples were placed in a vacuum laminating press to remove air bubbles between the film sheets. The acrylic coating thickness was about 0.0002 inch (0.005mm). An acrylic coated control was prepared in an identical manner containing no hydroxypropyl β CD. The multilayer structure was tested with the 0.5% acetylated β CD film facing the environmental flask side of the test cell (Fig. 3).

A second coating was prepared from a vinylidene chloride latex (PVDC, 60 wt-% solids) purchased from Dagax Laboratories, Inc. The PVDC latex coating was prepared with two levels of hydroxypropyl β CD - 10% and 20% by weight of the derivatized cyclodextrin. These solutions were used to hand-coat linear low density polyethylene test film samples by laminating the two films together. The coatings were applied to two control film sheets (rolled into one) using a hand roller and laminated together. The films were not stretched during lamination process. All coated samples were placed in a vacuum laminating press to remove air bubbles between the film sheets. The PVDC coating thickness was approximately 0.0004 inch (0.01mm). A PVDC coated control was prepared in an identical manner but without hydroxypropyl β CD.

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300 ml flask volume. Since the sample flasks vary in volume, the water is varied to correspond to the volume variations. The 2 μ L of water in the 300 ml flask volume is comparable to a 0.25 water activity product at 72°F (22°C). Next, 40 μ L, the permeation ethanol/aromatic working standard or 40 μ L of the naphtha blend working standard prepared according to section 2.2, is injected into the environmental flask. Either of these working standards will produce a 60% relative humidity at 72°F with a permeant concentration (parts per million-volume/volume) in the 1200 ml volume flask indicated in Table I. Other humidities or permeant concentrations may be employed in the test method by using psychrometric chart to determine humidity and using the gas loss to calculate permeant concentration. The time is recorded and the permeation cell placed into a thermostatically controlled oven. Samples may be staggered to accommodate GC run time. Three identical permeation devices are prepared. Triplicate analyses are used for QC purposes.

At the end of each time interval, a sample from the group is removed from the oven. The environmental flask is analyzed first, using a heated six-port sampling valve fitted with a 1 ml loop. The loop is flushed with a 1 ml volume of the environment-side or sample-side air. The loop is injected onto the capillary column. The GC/FID system is started manually following the injection. Up to eight 1 ml sample injections may be taken from the sample and environment side of a single permeation experiment.

Sample side and environment side test compound concentrations are calculated from each compound's calibration curve or response factor (equation 1 or 3). Concentrations are then volume-corrected for each specific set of permeation flasks if permeant mass is desired.

4.0 Sample Analysis

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into a 25-ml volumetric flask, stopper, then mix by inverting flask.

Analyze each calibration standard and tabulate compound peak area response versus the concentration of the test compound in the environment side cell. The results are used to prepare a calibration curve for each compound. The naphtha solvent blend is a commercial paint solvent containing approximately twenty (20) individual aliphatic hydrocarbon compounds. The response versus concentration is determined by totaling the area under each of the twenty individual peaks. Method of least squares is used to fit a straight line to the calibration curve. The slope of each test compound's calibration curve is then calculated for determining the unknown concentration. The average response factor may be used in place of the calibration curve.

The working calibration curve or response factor must be verified on each working day by measurement of one or more calibration standards. If the response of any compound varies more than 20%, the test must be repeated using a fresh calibration standard. If the results still do not agree, generate a new calibration curve.

25 4.3 Analysis of Calibration Curve and Method Detection Level Samples

Recommended chromatographic conditions are summarized above.

Calibrate the system daily as described above.

30 Check and adjust split vent rate and check rate with soap film flow meter.

To generate accurate data, samples, calibration standards and method detection level samples must be analyzed under identical conditions.

35 Calibration standards and method detection samples are prepared in the environment flask only. This is accomplished by using a 1/2 inch (1.27 cm) plastic disk

and aluminum sheet disk the diameter of the environment
flange in place of the sample flask. A single sealing
ring is placed onto the environmental glass flange
followed by an aluminum sheet, and then the plastic
5 disk.

The environment flask is flushed with dry
compressed air to remove humidity in the sample and
environment flask. This is done by puncturing the
environment septa with a needle and tubing assembly
10 which permits a controlled flow of dry air through the
flask. The clamp rings are loosely fitted to the flask
to eliminate pressure buildup. After flushing both
flasks for approximately 10 minutes, the needle is
removed and the clamp rings tightened, sealing the
15 aluminum sheet against the seal ring.

Next, 40 μ l of the permeation ethanol/aromatic
working standard or secondary dilutions of the working
standard is injected into the environment flask.
Alternatively, 40 μ L of the naphtha solvent blend or
20 secondary dilutions of the working standard is injected
into the environmental flask. The time is recorded and
the flask is placed into a thermostatically controlled
oven.

At the end of 30 minutes, the environment flask is
25 removed from the oven. The environmental flask is
analyzed using a heated six-port sampling valve fitted
with a 1 ml loop. The loop is flushed with a 1 ml
volume of the environment-side or sample-side air. The
loop is injected onto the capillary column. The GC/FID
30 system is started manually following the injection.

4.4 Calculation of Results

4.4.1 Test Compound Response Factor

Sample-side and environment-side test compound
concentrations are calculated for each compound's
35 calibration curve slope or response factor (RF).
Concentrations are then volume-corrected for each
specific set of permeation cells if permeant mass is

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$$\frac{\text{gm}-0.001 \text{ inches } (0.025 \text{ mm})}{100 \text{ in}^2 (0.0645\text{m}^2) \text{-day.}}$$

One of the major variables in determining the
5 permeation coefficient is the pressure drop across the
film. Since the transmission rate Q includes neither
pressure nor concentration of the permeant in its
dimensions, it is necessary to know either vapor
pressure or the concentration of permeant under the
10 conditions of the measurement in order to correlate Q to
 P .

The pressure-drop across the film from environment
side to sample side is principally due to water vapor
pressure. The water concentration or humidity does not
15 remain constant and is not measured during the time
intervals the organic compounds are analyzed, and
therefore the pressure across the membrane is not
determined.

The above examples of thermoplastic films
20 containing a variety of compatible cyclodextrin
derivatives shows that the invention can be embodied in
a variety of different thermoplastic films. Further, a
variety of different compatible derivatized cyclodextrin
materials can be used in the invention. Lastly, the
25 films can be manufactured using a variety of film
manufacturing techniques including extrusion and aqueous
dispersion coating to produce useful barriers.

The above specification, examples of substituted
cyclodextrin, extruded thermoplastic films and test data
30 provide a basis for understanding the technical aspects
of

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(21) International Application Number: PCT/US95/05999 (22) International Filing Date: 16 May 1995 (16.05.95) (30) Priority Data: 08/264,771 23 June 1994 (23.06.94) US (71) Applicant: ASPEN RESEARCH CORPORATION [US/US]; 436 West County Road D, New Brighton, MN 55112-3522 (US). (72) Inventors: WOOD, Willard, E.; 3470 Siems Court, Arden Hills, MN 55112 (US). BEAVERSON, Neil, J.; 5809 147th Street North, Hugo, MN 55038 (US). (74) Agent: DAIGNAULT, Ronald, A.; Merchant, Gould, Smith, Edell, Welter & Schmidt, P.A., 1000 Norwest Center, 55 E. Fifth Street, St. Paul, MN 55101 (US).		(81) Designated States: AM, AT, AU, BB, BG, BR, BY, CA, CH, CN, CZ, DE, DK, EE, ES, FI, GB, GE, HU, IS, JP, KE, KG, KP, KR, KZ, LK, LR, LT, LU, LV, MD, MG, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, <u>SG</u> , SI, SK, TJ, TM, TT, UA, UG, UZ, VN, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG), ARIPO patent (KE, MW, SD, SZ, UG). Published <i>With international search report.</i>
(54) Title: A BARRIER MATERIAL COMPRISING A THERMOPLASTIC AND A COMPATIBLE CYCLODEXTRIN DERIVATIVE		
(57) Abstract A barrier film composition can comprise a thermoplastic web comprising a thermoplastic polymer and a dispersed cyclodextrin composition having substituents that compatibilize the cyclodextrin in the film. The thermoplastic/cyclodextrin film obtains substantial barrier properties from the interaction between the substituted cyclodextrin in the film material with a permeant. The substituents on the cyclodextrin molecule cause the cyclodextrin to be dispersible and stable in the film material resulting in an extrudable thermoplastic. Such materials can be used as a single layer film material, a multilayer film material which can be coated or uncoated and can be used in structural materials wherein the thermoplastic is of substantial thickness resulting in structural stiffness. The cooperation between the cyclodextrin and the thermoplastic polymer provides barrier properties to a web wherein a permeant can be complexed or entrapped by the cyclodextrin compound and held within the film preventing the permeant from passing through the film into the interior of a film, an enclosure or container. The permeant can comprise a variety of well known materials such as moisture, aliphatic or aromatic hydrocarbons, monomer materials, off flavors, toxic compounds, etc.		