

PROCESS FOR THE PRODUCTION OF VINYL ACETATE

The present invention relates to a process for the production of vinyl acetate.

Vinyl acetate is generally prepared on a commercial basis by contacting acetic acid and ethylene with molecular oxygen in the presence of a catalyst active for the production of vinyl acetate.

5 A catalyst suitable for use in the production of vinyl acetate may comprise a Group VIII metal, a catalyst promoter and an optional co-promoter. For example EP A-0672453 discloses a process for the production of vinyl acetate by the catalytic oxidation of ethylene in the presence of acetic acid wherein the catalyst is a supported palladium catalyst comprising a promoter and a co-promoter.

10 It has been found that when the catalyst is used in a fluid bed reactor and the acetic acid is introduced into the reactor in the liquid form, the catalyst particles can become sticky and join together, thus forming lumps especially over extended periods of operation. In extreme cases, fluidisation can be lost which may cause the reactor to be shut down.

15 European patent publication EP-0847982-A relates to a fluid bed process for the production of vinyl acetate in which liquid is introduced into the fluidised bed reactor for the purpose of removing heat. The liquid introduced into the fluidised bed may be a reactant including the acetic acid reactant. Promoter such as potassium acetate may be dissolved in the liquid feed to the bed. In the example described therein the catalyst had
20 a metal loading of 0.44 Pd, 0.36 Au and 2.5 K (weight %). This amount of potassium corresponds to 6.3 weight % potassium acetate. Although it is stated that the catalyst did not agglomerate and defluidise there is no indication of the scale of the experiment or

how long the experiment was performed.

We have found that the problem of stickiness can be avoided by limiting the amount of co-promoter material in the catalyst composition.

Accordingly, the present invention provides a process for the production of vinyl acetate which comprises feeding ethylene, liquid acetic acid and an oxygen-containing gas into a fluid bed reactor and reacting at elevated temperature in the fluid bed reactor the ethylene, acetic acid and oxygen in the presence of a fluid bed catalyst material, said catalyst material comprising a Group VIII metal, a promoter and a co-promoter, said co-promoter being present in the reactor in an amount of up to 6% by weight of the catalyst.

The present invention provides a process for the production of vinyl acetate which avoids the problem of catalyst stickiness and ultimate lump formation, especially over extended periods of operation (for example greater than 7 days).

The catalyst of the present invention is a fluid bed catalyst material, comprising a Group VIII metal, a promoter and a co-promoter. These compounds are suitably accommodated on a support.

With regards to the Group VIII metal, the preferred metal is palladium. Suitable sources of palladium include palladium (II) chloride, sodium or potassium tetrachloropalladate, (II), (Na_2PdCl_4 or K_2PdCl_4), palladium acetate, H_2PdCl_4 , palladium (II) nitrate or palladium (II) sulphate. The metal may be present in a concentration of greater than 0.2% by weight, preferably greater than 0.5% by weight, especially about 1% by weight based upon total weight of catalyst. The metal concentration may be as high as 10% by weight.

In addition to the Group VIII metal, the catalyst comprises a promoter. Suitable promoters include gold, copper, cadmium and/or nickel compounds. A preferred promoter is gold. Suitable sources of gold include gold chloride, tetrachloroauric acid (HAuCl_4), NaAuCl_4 , KAuCl_4 , dimethyl gold acetate, barium acetoaurate or gold acetate. The preferred gold compound is HAuCl_4 . The promoter metal may be present in an amount of from 0.1 to 10% by weight in the finished catalyst.

The catalyst composition comprises a co-promoter material present in a concentration of up to 6% by weight of the catalyst composition. Suitable co-promoters include Group I, Group II, lanthanide or transition metals, for example cadmium, barium, potassium, sodium, iron, manganese, nickel, antimony, and/or lanthanum, which are

present in the finished catalyst as salts, e.g. an acetate salt. The preferred salts are potassium or sodium acetate. The co-promoter is present in the catalyst composition in a concentration of up to 6% by weight of catalyst. Preferably, the concentration is from 3.5 to 5.5% by weight of catalyst, especially about 5% by weight.

5 The catalyst material is a supported catalyst. Suitable catalyst supports include porous silica, alumina, silica/alumina, titania, silica/titania, zirconia or carbon. Preferably the support is silica. Suitably, the support may have a pore volume from 0.2 to 3.5 mL per gram of support, a surface area of 5 to 800 m² per gram of support and an apparent bulk density of 0.3 to 1.5 g/mL. The support may typically have a particle size
10 distribution such that at least 60% of the catalyst particles have a particle diameter of below 2×10^{-4} m (200 microns). Preferably at least 50%, more preferably, at least 80%, most preferably, at least 90% of the catalyst particles have a particle diameter less than 1.05×10^{-4} m (105 microns). Preferably no more than 40% of the catalyst particles have a diameter of less than 4×10^{-5} m (40 microns).

15 The catalyst may be prepared by any suitable method, such as that detailed in EP-A-0672453. Suitably, the first stage of the catalyst preparation process involves impregnation of the support material with a solution containing the required Group VIII metal and the promoter metal in the form of soluble salts. Examples of such salts are soluble halide derivatives. The impregnating solution is preferably an aqueous solution
20 and the volume of solution used is such that it corresponds to between 50 and 100% of the pore volume of the support, preferably 50 to 99% of the pore volume.

 The impregnated support is dried at ambient or reduced pressure and from ambient temperature to 150°C, preferably 60 to 130°C prior to metals reduction. To convert such materials into the metallic state, the impregnated support is treated with a
25 reducing agent such as ethylene, hydrazine, formaldehyde or hydrogen. If hydrogen is used, it will usually be necessary to heat the catalyst to 100 to 850°C in order to effect complete reduction.

 After the steps described above have been carried out, the reduced catalyst is washed with water and then dried. The dried carrier is then impregnated with the
30 required amount of co-promoter and thereafter dried. Alternatively, the wet, reduced, washed material is impregnated with co-promoter then dried.

 The method of catalyst preparation may be varied to optimise catalyst

performance based on maximising vinyl acetate yield and selectivity.

The process of the present invention comprises reacting ethylene, acetic acid and an oxygen-containing gas in the presence of the catalyst material. Ethylene may be used in substantially pure form or admixed with one or more of nitrogen, methane, ethane,
5 carbon dioxide and water in the form of steam or one or more of hydrogen, C_3/C_4 alkenes or alkanes. The ethylene in the combined feed to the reactor may be at least 60 mole%.

The oxygen-containing gas may suitably be air or a gas richer or poorer in molecular oxygen than air. Suitably, the gas may be oxygen diluted with a suitable
10 diluent, for example, nitrogen, argon or carbon dioxide. Preferably the gas is oxygen.

The acetic acid is introduced into the reactor in liquid form. Optionally, a portion of the acid may be introduced in the vapour form. The acetic acid is preferably crude acetic acid. Suitably, the liquid acetic acid may be introduced into the fluid bed reactor by any suitable injection means, for example a nozzle which may be a gas-induced
15 atomising nozzle or liquid-only spray-type nozzles. One or more nozzles may be used for this purpose. Additionally, recycled acetic acid may be introduced into the reactor. The recycled acetic acid may be pre-mixed with the crude acetic acid or may be introduced into the reactor using a separate injection means. The recycled acetic acid may suitably comprise water. Suitably, the water concentration in the recycle stream is
20 such that the water concentration being fed into the reactor is less than 6% by weight, preferably less than 4% more preferably, less than 3% of the total acid and water stream fed into the reactor. The usual precautions for introducing a liquid into a fluid bed should be taken, such as avoiding cold surfaces.

It is generally known in such catalytic processes that catalyst activity will
25 decrease with time for various reasons. In particular, due to the volatile nature of the co-promoter, the level of co-promoter in the catalyst material decreases with time. This results in loss of catalyst activity and a loss in selectivity. In order to maintain a constant concentration of co-promoter on the catalyst, the concentration being less than 6 wt%, fresh co-promoter may be added to the catalyst during the reaction. This may suitably be
30 carried out by adding the co-promoter material to the liquid acetic acid feed or to the liquid recycle acetic acid. Alternatively, the additional co-promoter may be introduced as a solution e.g. in water or in acid directly by spraying into the reactor through a suitable

injection means such as a nozzle. In each case, the co-promoter contacts the catalyst material.

The process is carried out in a fluid bed reactor and may suitably be operated at a temperature from 100 to 400°C, preferably 140 to 210°C and a pressure of 10^5 to 2×10^6 Pa gauge (1 to 20 barg), preferably 6×10^5 to 1.5×10^6 Pa gauge (6 to 15 barg), especially 7×10^5 to 1.2×10^6 Pa gauge (7 to 12 barg).

The present invention will now be illustrated with reference to Figure 1 and the following Examples in which Figure 1 is a schematic representation of a reactor system for use in the present invention.

The examples were carried out on a full recycle pilot plant which was operated at steady state. The apparatus is as shown in Figure 1 and includes a feed system, reactor gas/liquid separation, gas recycle, product recovery and liquid recycle. With reference to Figure 1, fresh acetic acid from storage (1) and recycle acetic acid are pumped together with some recycle gas (3) to twin fluid nozzle within the fluid bed (2). The remainder of the recycle gas feed (3), fresh ethylene (4) and oxygen (5) enter the plenum and through a sintered plate into the reactor. Fresh oxygen (6) may be fed directly into the fluid bed. A freeboard section is provided for disengaging the catalyst (7). The gaseous products exit the reactor through exit (8) through sintered filter elements (not shown). The reactor temperature is controlled using a pumped system where hot heat transfer fluid is passed through three jackets (not shown) attached to the reactor wall. All equipment is constructed out of 316L stainless steel.

Example 1 is an example according to the present invention. Comparative Example A is not according to the invention wherein the process uses a catalyst not according to the present invention in that it contains more than 6% by weight co-promoter.

Example 1

(a) Preparation of Catalyst Support

The support was prepared by spray drying a mixture of silica sol 1060 (obtained from Nalco Chemical Company) and Aerosil® silica (obtained from Degussa Chemical Company). In the dried support 80% of the silica sol came from the sol and 20% of the silica came from the Aerosil. The spray dried microspheres were calcined in air at 640°C for 4 hours. The particle size distribution of the support which was used for the catalyst

preparation is as follows:

	<u>Particle size (microns)</u>	<u>%</u>
	$>3 \times 10^{-4} \text{ m } (>300)$	2
5	$4.4 \times 10^{-5} \text{ m} - 3 \times 10^{-4} \text{ m} (44-300)$	68
	$<4.4 \times 10^{-5} (<44)$	30

It should be understood that the particle size distribution given above is not intended to be limiting and that variations in this distribution are contemplated depending upon reactor size and operating conditions.

10 (b) Preparation of Catalyst

The silica support (54.4kg) obtained from step (a) above was impregnated with a solution of $\text{Na}_2\text{PdCl}_4 \cdot x\text{H}_2\text{O}$ (containing 1000g Pd) and $\text{AuCl}_4 \cdot x\text{H}_2\text{O}$ (containing 400g Au) in distilled water by incipient wetness. The resulting mixture was mixed thoroughly, left to stand for 1 hour and dried overnight.

15 The impregnated material was then added slowly to a 5% solution of N_2H_4 in distilled water and the mixture allowed to stand with occasional stirring. Thereafter, the mixture was filtered and washed with 4 x 400 litres of distilled water. The resulting solid was dried overnight.

20 The material was impregnated with a solution of potassium acetate (2.8kg) by incipient wetness. The resulting mixture was mixed thoroughly, left to stand for 1 hour and dried overnight. The catalyst was then screened to remove particles having a particle size greater than 106 microns.

The resulting catalyst comprised 1.45 wt% palladium, 0.65 wt% gold and 4.3 wt% potassium acetate.

25 (c) Production of Vinyl Acetate

4.5kg of catalyst prepared according to step (b) above was loaded into the reactor. The reactor was operated at 8×10^5 Pa gauge (8 barg) with a bed temperature profile of : bottom 145°C, middle 152.5°C, top 155°C. The total feed composition in mole percent entering the catalyst bed was ethylene:oxygen:acetic acid:inerts
30 58.9:4.9:11:25.2 respectively at a total reactor inlet velocity of 13.2 cm/sec at process conditions with a twin fluid nozzle liquid to gas weight ratio of 2.05:1. The process was operated under these conditions in excess of 28 days with no operational upset.

Example A (Comparative Example)

(a) Preparation of Catalyst Support.

The support was prepared as detailed in Example 1, above.

(b) Preparation of Catalyst

5 The silica support (54.4kg) obtained from (a) above was impregnated with a solution of $\text{Na}_2\text{PdCl}_4 \cdot x\text{H}_2\text{O}$ (containing 1850g Palladium) and $\text{AuCl}_4 \cdot x\text{H}_2\text{O}$ (containing 740g Au) in distilled water by incipient wetness. The resulting mixture was mixed thoroughly, left to stand for 1 hour and dried overnight.

10 A portion of the impregnated material (18 kg) was added slowly to a 10% solution of N_2H_4 in distilled water and the mixture allowed to stand overnight with occasional stirring. Thereafter, the mixture was filtered and washed with 4 x 200 litres of distilled water. The solid was then dried overnight.

15 The material was impregnated with an aqueous solution of potassium acetate (1.4kg) by incipient wetness. The resulting mixture was mixed thoroughly, left to stand 1 hour and dried overnight.

The resulting catalyst comprised 3.1 wt% palladium, 1.26 wt % gold and 6.3 wt% potassium acetate.

(c) Production of Vinyl Acetate

20 3.45 kg of catalyst prepared according to step (b) above containing 6.3 wt% potassium acetate was loaded to the reactor. The reactor was operated at 8×10^5 Pa gauge (8 barg) with a bed temperature profile of: bottom 150°C, middle 155°C, top 155°C. The total feed composition in mole percent entering the catalyst bed was ethylene:oxygen:acetic acid:inerts 47:3:22:28 respectively at a total reactor inlet velocity of 6.7 cm/sec at process conditions with a twin fluid nozzle liquid to gas weight ratio of 2.14:1. After 7 days of operation, the oxygen detected at the reactor exit suddenly increased with a fall in production rate to near zero. This suggested that the catalyst bed was not fluidising adequately and had probably become "sticky" so not mixing adequately with the gas feed. The process was shut down and the catalyst dried at 150°C for 12 hours. Upon discharging the catalyst from the reactor both free flowing catalyst and lumps were recovered. The free flowing catalyst analysed for 2.1 wt% potassium, the lumps analysed for 4.8 wt% potassium. These results suggest migration had occurred when the bed became "sticky" and poorly fluidised.

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Claims:

1. A process for the production of vinyl acetate which comprises feeding ethylene, liquid acetic acid and an oxygen-containing gas into a fluid bed reactor and reacting at elevated temperature in the fluid bed reactor the ethylene, acetic acid and oxygen in the presence of a fluid bed catalyst material, said catalyst material comprising a Group VIII
5 metal, a promoter and a co-promoter, said co-promoter being present in the reactor in an amount of up to 6% by weight of the catalyst.
2. A process as claimed in claim 1 in which the Group VIII metal is palladium.
3. A process as claimed in claim 1 or claim 2 in which the Group VIII metal is present in a concentration of greater than 0.2 % by weight of the total weight of the
10 catalyst and up to 10 % by weight of the weight of the catalyst.
4. A process as claimed in any one of the preceding claims in which the promoter is selected from the group consisting of gold, copper, cadmium, nickel and mixtures thereof.
5. A process as claimed in any one of the preceding claims in which the promoter is
15 present in an amount of from 0.1 to 10 % by weight as metal in the catalyst material.
6. A process as claimed in any one of the preceding claims in which the co-promoter is selected from the group consisting of salts of Group I, Group II, lanthanides and transition metals.
7. A process as claimed in claim 6 in which the co-promoter is selected from the
20 group consisting of salts of cadmium, barium, potassium, sodium, iron, manganese, nickel, antimony, lanthanum and mixtures thereof.
8. A process as claimed in any one of the preceding claims in which the co-promoter



is present in a concentration from 3.5 to 5.5 % by weight of the catalyst, preferably about 5 % by weight.

9. A process as claimed in any one of the preceding claims in which co-promoter is added to the catalyst during the reaction.

5 10. A process as claimed in claim 9 in which said added co-promoter is added to the liquid acetic acid feed or to a liquid recycle acetic acid.

11. A process as claimed in claim 9 in which said added co-promoter is added as a solution sprayed into the reactor through injection means.

12. A process as claimed in claim 11 in which said added co-promoter is added as a
10 solution in water or in acid.

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