NO_x REDUCTION COMPOSITIONS FOR USE IN FCC PROCESSES

FIELD OF THE INVENTION

[0001] The present invention relates to NO_x reduction compositions and the method of use thereof to reduce NO_x emissions in refinery processes, and specifically in fluid catalytic cracking (FCC) processes. More particularly, the present invention relates to NO_x reduction compositions and their method of use to reduce the content of gas phase reduced nitrogen species in FCC regenerator off gases released from a fluid catalytic cracking unit (FCCU) regenerator operating in a partial or incomplete combustion mode.

BACKGROUND OF THE INVENTION

[0002] In recent years there has been an increased concern in the United States and elsewhere about air pollution from industrial emissions of noxious oxides of nitrogen, sulfur and carbon. In response to such concerns, government agencies have in some cases already placed limits on allowable emissions of one or more of the pollutants, and the trend is clearly in the direction of increasingly stringent restrictions.

[0003] NO_x, or oxides of nitrogen, in flue gas streams exiting from fluid catalytic cracking (FCC) regenerators is a pervasive problem. Fluid catalytic cracking units (FCCU) process heavy hydrocarbon feeds containing nitrogen compounds a portion of which is contained in the coke on the catalyst as it enters the regenerator. Some of this coke nitrogen is eventually converted into NO_x emissions, either in the FCC regenerator or in a downstream CO boiler. Thus all FCCUs processing nitrogen-containing feeds can have a NO_x emissions problem due to catalyst regeneration.

[0004] In an FCC process, catalyst particles (inventory) are repeatedly circulated between a catalytic cracking zone and a catalyst regeneration zone. During regeneration, coke from the cracking reaction deposits on the catalyst particles and is removed at elevated temperatures by oxidation with oxygen containing gases such as air. The removal of coke deposits restores the activity of the catalyst particles to the point where they can be reused in the cracking reaction. The coke removal step is performed over a wide range of oxygen conditions. At the minimum, there is typically at least enough oxygen to convert essentially all of the coke made to CO and

H_2O. At the maximum, the amount of oxygen available is equal to or greater than the amount necessary to oxidize essentially all of the coke to CO_2 and H_2O.

[0005] In an FCC unit operating with sufficient air to convert essentially all of the coke on the catalyst to CO_2 and H_2O, the gas effluent exiting the regenerator will contain "excess oxygen" (typically 0.5 to 4% of total off gas). This combustion mode of operation is usually called "full burn". When the FCCU regenerator is operating in full burn mode, the conditions in the regenerator are for the most part oxidizing. That is, there is at least enough oxygen to convert (burn) all reducing gas phase species (e.g., CO, ammonia, HCN) regardless of whether this actually happens during the residence time of these species in the regenerator. Under these conditions, essentially all of the nitrogen deposited with coke on the catalyst during the cracking process in the FCCU riser is eventually converted to molecular nitrogen or NO_x and exits the regenerator as such with the off gas. The amount of coke nitrogen converted to NO_x as opposed to molecular nitrogen depends on the design, conditions and operation of the FCCU, and especially of the regenerator, but typically the majority of coke nitrogen exits the regenerator as molecular nitrogen.

[0006] On the other hand, when the amount of air added to the FCCU regenerator is insufficient to fully oxidize the coke on the cracking catalyst to CO_2 and H_2O, some of the coke remains on the catalyst, while a significant portion of the burnt coke carbon is oxidized only to CO. In FCCUs operating in this fashion, oxygen may or may not be present in the regenerator off gas. However, should any oxygen be present in the regenerator off gas, it is typically not enough to convert all of the CO in a gas stream to CO_2 according to the chemical stoichiometry of

$$CO + \tfrac{1}{2} O_2 \rightarrow CO_2$$

This mode of operation is usually called "partial burn." When an FCC U regenerator is operating in partial burn mode, the CO produced, a known pollutant, cannot be discharged untreated to the atmosphere. To remove the CO from the regenerator off gas and realize the benefits of recovering the heat associated with burning it, refiners typically burn the CO in the regenerator off gas with the assistance of added fuel and

air in a burner usually referred to as "the CO boiler". The heat recovered by burning the CO is used to generate steam.

[0007] When the regenerator is operating in partial burn, the conditions in the regenerator, where the oxygen added with air has been depleted and CO concentration has built up, are overall reducing. That is, there is not enough oxygen to convert/burn all reducing species regardless if some oxygen is actually still present. Under these conditions some of the nitrogen in the coke is converted to so called "gas phase reduced nitrogen species ", examples of which are ammonia and HCN. Small amounts of NO_x may also be present in the partial burn regenerator off gas. When these gas phase reduced nitrogen species are burnt in the CO boiler with the rest of the regenerator off gas, they can be oxidized to NO_x, which is then emitted to the atmosphere. This NO_x along with any "thermal" NO_x formed in the CO boiler burner by oxidizing atmospheric N_2 constitute the total NO_x emissions of the FCCU unit operating in a partial or incomplete combustion mode.

[0008] FCCU regenerators may also be designed and operated in a "incomplete burn" mode intermediate between full burn and partial burn modes. An example of such an intermediate regime occurs when enough CO is generated in the FCCU regenerator to require the use of a CO boiler, but because the amounts of air added are large enough to bring the unit close to full burn operation mode, significant amounts of oxygen can be found in the off gas and large sections of the regenerator are actually operating under overall oxidizing conditions. In such case, while gas phase reduced nitrogen species can still be found in the off gas, significant amounts of NO_x are also present. In most cases a majority of this NO_x is not converted in the CO boiler and ends up being emitted to the atmosphere.

[0009] Yet another combustion mode of operating an FCCU is nominally in full burn with relatively low amounts of excess oxygen and/or inefficient mixing of air with coked catalyst. In this case, large sections of the regenerator may be under reducing conditions even if the overall regenerator is nominally oxidizing. Under these conditions reduced nitrogen species may be found in the regenerator off gas along with NO_x.

[0010] Various catalytic approaches have been proposed to control NO_x emissions in the flue gas exiting from the FCCU regenerator.

[0011] For example, recent patents, including U.S. Patents 6,280,607, 6,129,834 and 6,143,167, have proposed the use of NO_x removal compositions for reducing NO_x emissions from an FCCU regenerator. U.S. Patent 6,165,933 also discloses a NO_x reduction composition, which promotes CO combustion during an FCC catalyst regeneration process step while simultaneously reducing the level of NO_x emitted during the regeneration step. NO_x reduction compositions disclosed by these patents may be used as an additive, which is circulated along with the FCC catalyst inventory or incorporated as an integral part of the FCC catalyst.

[0012] In U.S. Patent 4,290,878, NO_x is controlled in the presence of a platinum-promoted CO oxidative promoter in a full burn combustion regenerator by the addition of iridium or rhodium on the combustion promoter in lesser amounts than the amount of platinum.

[0013] U.S. Patent 4,973,399, discloses copper-loaded zeolite additives useful for reducing emissions of NO_x from the regenerator of an FCCU unit operating in full CO-burning mode.

[0014] U.S. Patent 4,368,057, teaches the removal of NH_3 contaminants of gaseous fuel by reacting the NH_3 with a sufficient amount of NO.

[0015] However, aforementioned prior art has failed to appreciate an FCC process which minimizes the amount of NO_x and gas phase reduced nitrogen species, e.g. NH_3, HCN, in the flue gas of an FCCU regenerator operating in a partial or incomplete combustion mode.

[0016] Efforts to control ammonia released in an FCC regenerator operated in a partial or an incomplete mode of combustion have been known.

[0017] For example, U.S. Patent 5,021,144 discloses reducing ammonia in an FCC regenerator operating in a partial burn combustion mode by adding a significant excess of the amount of a carbon monoxide (CO) oxidative promoter sufficient to prevent afterburn combustion in the dilute phase of the regenerator.

[0018] U.S. Patent 4,755,282 discloses a process for reducing the content of ammonia in a regeneration zone off gas of an FCCU regenerator operating in a partial or incomplete combustion mode. The process requires passing a fine sized, i.e. 10 to 40 microns, ammonia decomposition catalyst to either the regeneration zone of an FCCU, or an admixture with the off gas from the regeneration zone of the FCCU, at a

predetermined make-up rate such that the residence time of the decomposition catalyst relative to the larger FCC catalyst particles will be short in the dense bed of the regenerator due to rapid elutriation of the fine sized ammonia decomposition catalyst particles. The fine sized elutriated decomposition catalyst particles are captured by a third stage cyclone separator and recycled to the regenerator of the FCCU. The decomposition catalyst may be a noble group metal dispersed on an inorganic support.

[0019] U.S. 4,744,962 is illustrative of a post-treatment process to reduce ammonia in the FCCU regenerator flue gas. The post-treatment involves treating the regenerator flue gas to lessen the ammonia content after the gas has exited the FCCU regenerator but before passage to the CO boiler.

[0020] There remains a need in the refining industry for improved compositions and processes which minimizes the content of gas phase reduced nitrogen species and NO_x emitted from a partial or incomplete combustion FCCU regenerator during an FCC process, which compositions are effective and simple to use.

SUMMARY OF THE INVENTION

[0021] The essence of the present invention resides in the discovery of particulate compositions which are capable of being circulated throughout a fluid catalytic cracking unit (FCCU) along with the cracking catalyst inventory to minimize the content of gas phase reduced nitrogen species, e.g. NH_3 and HCN, and NO_x present in the off gas of the FCCU regenerator when the FCCU regenerator is operated in a partial or incomplete burn mode. Advantageously, the compositions exhibit high efficiencies for the oxidation of gas phase reduced nitrogen species present in the regenerator off gas to molecular nitrogen prior to passage of the off gas to the CO boiler. This reduced content of gas phase reduced nitrogen species in the off gas provides for an overall reduction of NO_x emitted into the atmosphere from the FCCU due to a decrease in the amount of the nitrogen species being oxidized to NO_x in the CO boiler as CO is oxidized to CO_2.

[0022] Despite the reducing environment in an FCCU regenerator operated in a partial burn or incomplete burn mode, some NO_x may form in the regenerator. In addition to reducing the content of gas phase reduced nitrogen species, compositions

of the invention also enhance the removal of any NO_x formed in the partial or incomplete burn regenerator by catalyzing the reaction of NO_x with reductants typically found in the FCCU regenerator, e.g. CO, hydrocarbons, and gas phase reduced nitrogen species, to form molecular nitrogen. Advantageously, the compositions of the invention provide a reduction of NO_x formed in the regeneration prior to the NO_x exiting the regenerator and being passed unabated through the CO boiler into the environment.

[0023] In accordance with the present invention, compositions of the invention are comprised of a particulate composition which comprises (i) an acidic metal oxide which contains substantially no zeolite; (ii) an alkali metal, alkaline earth metal, and mixtures thereof, measured as the metal oxide, (iii) an oxygen storage component, and (iv) a noble metal component, preferably platinum, rhodium, iridium or mixtures thereof. In a preferred embodiment of the invention, compositions of the invention are used in the FCC process as separate additives particles circulated along with the circulating FCC catalyst inventory.

[0024] The present invention also provides a process for reducing the content of gas phase reduced nitrogen species released from the regenerator of an FCCU operated in a partial or incomplete mode of combustion. In accordance with the present invention, the process comprises contacting under FCC catalytic conditions the off gas of an FCCU regenerator operated in a partial or incomplete combustion mode with an amount of the compositions of the invention effective to oxidize the gas phase reduced nitrogen species to molecular nitrogen. The invention also provides a process for reducing NO_x emissions from an FCC process operated in a partial or incomplete combustion modes using the compositions of the invention.

[0025] Accordingly, it is an advantage of this invention to provide compositions which are useful to reduce the content of gas phase reduced nitrogen species released from an FCCU regenerator operating in partial or incomplete combustion modes during an FCC process.

[0026] It is also an advantage of this invention to provide compositions which are useful to reduce NO_x emissions from an FCCU regenerator operating in partial or incomplete combustion modes by minimizing the amount of reduced nitrogen species emitted from the regenerator during an FCC process.

[0027] Another advantage of the invention is to provide compositions which are effective to oxidize gas phase reduced nitrogen species released from an FCCU regenerator operating in partial or incomplete combustion modes to molecular nitrogen, thereby minimizing the conversion of the reduced nitrogen species to NO_x in the downstream CO boiler.

[0028] It is another advantage of this invention to provide compositions which are useful to reduce NO_x emissions from an FCCU regenerator operating in partial or incomplete combustion modes to molecular nitrogen by catalyzing the reaction of NO_x with CO and other reductants typically present in a partial or incomplete burn FCCU regenerator.

[0029] It is another advantage of this invention to provide a process for the reduction of the content of NO_x in the off gas of an FCCU regenerator operating in partial or incomplete combustion mode by reducing the content of gas phase reduced nitrogen species being emitted in the off gas released from the regenerator, prior to passage of the gas to a CO boiler, whereby as CO is oxidized to CO_2, a lesser amount of the gas phase reduced nitrogen species is oxidized to NO_x.

[0030] It is another advantage of this invention to provide a process for the reduction of gas phase reduced nitrogen species in an effluent gas stream passed from an FCC regenerator to a CO boiler, whereby as CO is oxidized to CO_2 a lesser amount of the reduced nitrogen species is oxidized to NO_x.

[0031] Another advantage of this invention is to provide a process for the reduction of the content of NO_x in the off gas of an FCCU regenerator operating in a partial or incomplete combustion mode by the reduction of NO_x being emitted in the off gas released from the regenerator, prior to passage of the gas to the CO boiler where the NO_x remains untreated and is eventually released into the environment.

[0032] Yet another advantage of this invention is to provide improved partial or incomplete combustion FCC processes using the compositions of the invention.

[0033] These and other aspects of the present invention are described in further detail below.

BRIEF DESCRIPTION OF THE DRAWINGS

[0034] FIG. 1 is a graphic representation of the comparison of ammonia reduction in an RTU where ammonia reacts with CO at various levels of oxygen in a reactor feed in the presence of Additives A, B and C, the cracking catalyst alone, and a commercial combustion promoter, CP-3®.

[0035] FIG. 2 is a graphic representation of the comparison of ammonia conversion to NO in an RTU where ammonia reacts with CO at various levels of oxygen in a reactor feed in the presence of the Additives A, B and C, the cracking catalyst alone, and a commercial combustion promoter, CP-3®.

[0036] FIG. 3 is a graphic representation of the comparison of ammonia conversion in an RTU where ammonia reacts with NO_x at various levels of O_2 in a reactor feed in the presence of Additives A, B and C, the cracking catalyst alone, and a commercial combustion promoter, CP-3®.

[0037] FIG. 4 is a graphic representation of the comparison of NO_x conversion in an RTU where ammonia reacts with NO_x at various levels of O_2 in a reactor feed in the presence of Additives A, B and C, the cracking catalyst alone, and a commercial combustion promoter, CP-3®.

[0038] FIG. 5 is a graphic representation of the comparison of NO_x conversion in an RTU where NO_x reacts with CO at various levels of O_2 in a reactor feed in the presence of Additives A, B and C, the cracking catalyst alone, and a commercial combustion promoter, CP-3®.

DETAILED DESCRIPTION OF THE INVENTION

[0039] For purposes of this invention the term "NO_x" will be used herein to represent oxides of nitrogen, e.g. nitric oxide, (NO) and nitrogen dioxide (NO_2) the principal noxious oxides of nitrogen, as well as N_2O_4, N_2O_5, and mixtures thereof.

[0040] The term reduced "gas phase reduced nitrogen species" is used herein to indicate any gas phase species formed in the regenerator of a fluid catalytic cracking unit during a fluid catalytic cracking process which gas species contain a nitrogen having a nominal charge of less than zero. Examples of gas phase reduced nitrogen species include, but are not limited to, ammonia (NH_3), hydrogen cyanide (HCN), and the like.

[0041] The present invention encompasses the discovery that certain classes of compositions are very effective for the reduction of the overall NO_x emissions released from an FCCU when the FCCU regenerator is operated in a partial or incomplete burn combustion mode. The compositions of the invention are characterized in that they comprise (i) an acidic metal oxide component which contains substantially no zeolite; (ii) an alkali metal, alkaline earth metal and mixtures thereof; (iii) an oxygen storage component; and (iv) a noble metal component selected from the group consisting of platinum, iridium, rhodium, osmium, ruthenium, rhenium and mixtures thereof.

[0042] The acidic metal oxide useful in the compositions of the invention is any metal oxide component having sufficient acidity to adsorb a base, e.g. pyridine, and the like. In accordance with the present invention, the acidic metal oxide contains no or substantially no, i.e. less than 5 wt %, zeolite. Typically, the acidic metal oxide contains at least some alumina. Preferably, the acidic metal oxide contains at least 1 wt % alumina; more preferably, at least 25 wt % alumina; most preferably, at least 50 wt % alumina. It is also within the scope of the invention that the acidic metal oxide may contain other stabilizing metal oxides, such as for example, lanthana, zirconia, yttria, neodymia, samaria, europia, gadolinia and the like. In a preferred embodiment of the invention, the acidic metal oxide is selected from the group consisting of alumina, silica alumina, lanthana alumina and zirconia alumina.

[0043] The acidic metal oxide may be crystalline or amorphous. Amorphous silica aluminas are most preferred. Where an amorphous alumina silica is used, it will have an alumina to silica molar ratio of about 1 to 50:1, preferably about 2 to 20:1.

[0044] The amount of the acidic metal oxide component present in the composition of the invention will typically be at least 5 wt % of the total composition. Preferably, the amount of the acidic metal oxide component ranges from about 5 to about 98 wt %, more preferable from about 15 to about 95 wt % and even more preferable, from about 20 to about 90 wt % of the total composition.

[0045] Further, the acidic metal oxide has a sufficient surface area to promote the reduction of NO_x and gas phase reduced nitrogen species formed in the flue gas of an FCCU regenerator operated in a partial or incomplete combustion mode. Typically, the acidic metal oxide has a BET surface area of at least 5 m^2/g. Preferably, the acidic

metal oxide has a BET surface area of at 5 to 500 m^2/g, more preferably about 70-250 m^2/g.

[0046] Alkali metals useful to prepare the compositions of the invention include, but are not limited to, sodium, potassium, cesium, lithium and the like. Preferably, the alkali metal component is sodium. The amount of alkali metal present in the composition of the invention is typically at least 0.5 wt % (on a metal oxide basis). Preferably, the amount of alkali metal in the composition ranges from about 1 to about 20 wt %, most preferably, from about 1 to about 10 wt % (on a metal oxide basis) of the total composition.

[0047] Alkaline earth metals useful to prepare compositions in accordance with the present invention include, but are not limited to, magnesium, calcium, barium, strontium and the like. Preferably, the alkaline earth metal is magnesium. The amount of alkaline earth metal present in the composition of the invention is at least 0.5 wt % (on a metal oxide basis). Preferably, the amount of the alkaline earth metal ranges from about 0.5 to 60 wt %, most preferably 5 to 40wt %, (on a metal oxide basis) of the invention composition. It is within the scope of the invention to use the alkali and alkaline earth metals alone or in combination.

[0048] The oxygen storage component may be any metal oxide having oxygen storage capability. In a preferred embodiment of the invention, the oxygen storage component is a rare earth metal oxide or a transition metal oxide having oxygen storage capability. Suitable rare earth metal oxides include, but are not limited to, ceria, samaria, praseodymia, europia, terbia and mixtures thereof. Suitable transition metals include vanadia, manganese oxide, iron oxide, nickel oxide, copper oxide, cobalt oxide, chromia, titania, silver oxide, molybdenia, niobia, gold oxide, tungsten oxide, and mixtures thereof. In a most preferred embodiment of the invention at least a portion of the oxygen storage component is ceria. Even more preferred is that the oxygen storage metal oxide component consists essentially of ceria. It is also within the scope of the present invention that the oxygen storage metal oxide component may contain other stabilizing metal oxides such as, for example, zirconia and rare earth metal oxides typically not heretofore known in the art to have oxygen storage capability, e.g., lanthana, neodymia, gadolinia, yttria, scandia, hafnia, and mixtures thereof.

[0049] The oxygen storage metal oxide component is preferably present as a micro dispersed phase as opposed to large bulk oxide particles or ions located at exchange sites in the oxide support. The amount of the oxygen storage metal oxide present in the compositions of the invention may vary considerably relative to the amount of acidic metal oxide. Generally, the oxygen storage component is present in the amount of at least 0.1wt %; preferably from about 1 to 50 wt %; most preferably from about 5 to about 30 wt %, of the total composition.

[0050] In general, the noble metal component is any metal of the noble group metals including but not limited to, platinum, palladium, iridium, rhodium, osmium, or ruthenium, rhenium, and mixtures thereof. Preferably, the noble metal component is selected from the group consisting of platinum, iridium, rhodium, osmium, ruthenium, rhenium and mixtures thereof. Most preferably, the noble metal component is platinum, rhodium, iridium and mixtures thereof. Typically, the amount of the noble metal component useful in the present invention, calculated as the metal, is at least 0.1 parts per million, preferably at least 10 parts per million, most preferably at least 25 parts per million. In a preferred embodiment of the invention, the amount of the noble metal component ranges from about 0.1 to 5,000 parts per million, preferably from about 10 to 2500 parts per million, most preferably from about 25 to about 1500 parts per million.

[0051] Additional materials optionally present in the compositions of the present invention include, but are not limited to, fillers, binders, etc., provided that said materials do not significantly adversely affect the performance of the compositions to reduce the content of gas phase nitrogen species and NO_x under partial or incomplete combustion conditions. It is preferred, however, that the compositions of the invention consist essentially of components (i) through (iv).

[0052] Compositions of the invention are in a particulate form and will typically have any particle size sufficient to permit the composition to be circulated throughout an FCCU simultaneously with the inventory of cracking catalyst during an FCC process. Typically the composition of the invention will have a mean particle size of greater than 45 μm. Preferably, the mean particle size is from about 50 to about 200 μm; most preferably from about 55 to about 150 μm, even more preferred from about 60 to 120 μm. The compositions of the invention typically have a Davison attrition

index (DI) value of about 0 to about 50, preferably from 0 to about 20; more preferably 0 to 15.

[0053] While the present invention is not limited to any particular process of preparation, typically compositions of the invention are prepared by impregnation of a microspheroidal particulate base material composition comprising components (i) - (iii) with a noble metal source. The base material composition may be prepared using any conventional method, see for example, U.S. Patents 6,280,607; 6,129,834 and 6,143,167, which patents teach preparing a base material composition comprising components (i) - (iii) by impregnation of a suitable acidic metal oxide support with precursors of components (ii)-(iii).

[0054] In one embodiment of the present invention, the base material composition may be prepared by mixing, preferably with agitation, an aqueous slurry containing an amount of a peptized acidic metal oxide, e.g. a peptized alumina, sufficient to provide at least 1.0 weight percent, preferably at least 25 wt %, most preferably at least 50 wt %, of the peptized acidic metal oxide in the final composition, and having from about 10 to about 30, preferably from about 20 to about 25, weight percent solids, with an oxygen storage transition metal and/or rare earth metal salt, e.g. a carbonate, nitrate, sulfate, chloride salts and the like, in an amount sufficient to provide at least 0.1 weight percent of an oxygen storage metal oxide, preferably ceria, in the final base material composition. Optionally, the oxygen storage transition metal and/or rare earth metal salt may also contain stabilizing amounts of a stabilizing metal, e.g. , zirconium and rare earth metals typically not heretofore known in the art to have oxygen storage capability, e.g., lanthanum, neodymium, gadolinium, yttrium, scandium, hafnium, and mixtures thereof. Preferably, the peptized acidic metal oxide containing slurry also contains an amount of an alkali metal and/or an alkaline earth metal sufficient to provide at least 0.5 wt % of alkali metal and/or alkaline earth metal in the final base material composition.

[0055] An additional acidic metal oxide source, e.g. sodium silicate as a silica source, may optionally be added, with agitation, to the oxygen storage metal containing slurry with agitation in an amount sufficient to provide at total of at least 5.0 weight percent, preferably from about 5 to about 98 weight percent, most preferably from about 15 to about 95 weight percent and even more preferable, from about 20 to about 90 weight

percent, of acidic metal oxide in the final composition. The oxygen storage metal oxide containing slurry is milled to reduce the particle size of the materials contained in the slurry to 10 microns or less, preferably 5 microns or less. The milled slurry is spray dried to obtain particles having a mean particle size of greater than 45 μm, preferably from about 50 to 200 μm, most preferably from about 55 to 150 μm, and calcined at a sufficient temperature and for a sufficient time to form the corresponding metal oxides, preferably from about 400°C to about 800°C for about thirty minutes to about 4 hours.

[0056] Optionally, the calcined metal oxide particles are treated with at least one aqueous alkali metal and/or alkaline earth metal salt solution in an amount sufficient to impregnate the particles and provide at least 0.5 weight percent alkali metal and/or alkaline earth metal in the final base material composition. Suitable salts for preparing the impregnating solutions include, but are not limited to, carbonates, bicarbonates, chlorides, nitrates, silicates and the like. The impregnated particles are thereafter dried and calcined at a temperature and for a time sufficient to form the corresponding metal oxide, e.g. from about 400°C to about 800° for about thirty minutes to about 4 hours.

[0057] The peptized acidic metal oxide containing slurry used to prepare the base material composition may be prepared by (i) forming an aqueous slurry containing an amount of at least one acidic metal oxide, preferably alumina, sufficient to provide at least 1.0 weight percent, preferably at least 25 wt %, most preferably at least 50 wt % , of the peptized acidic metal oxide in the final composition, and having from about 10 to about 30, preferably, 20 to about 25, weight percent solids and (ii) adding to the slurry an alkali base, e.g. sodium hydroxide, potassium hydroxide, sodium aluminate and the like, and/or an alkaline earth metal base, e.g. magnesium hydroxide, calcium hydroxide and the like, in an amount sufficient to peptize the acidic metal oxide and provide at least 0.5 weight percent alkali metal and/or alkaline earth metal in the final base material composition. In general the amount of alkali metal and/or alkaline earth metal base used ranges from about 0.01 to 1.0 mole of alkali base per mole of acidic metal oxide, preferably 0.4 to 0.7 mole of alkali base per mole of acidic metal oxide. Thereafter the slurry is aged, preferably with continuous agitation, at a temperature and for a time sufficient to permit complete peptization of the acidic metal oxide

contained in the slurry and obtain a high attrition resistant material having a Davison Index (DI) of 0 to about 50, preferably, from 0 to about 20, most preferably, from 0 to15. Preferably the slurry is aged from about room temperature to about 90°C for about 30 minutes to about 4 hours. Generally, the peptizable acidic metal oxide containing slurry is prepared by contacting an aqueous solution with a peptizable acidic metal oxide. It is within the scope of the invention that the peptizable acidic metal oxide contained in the slurry will also contain stabilizing amounts of stabilizing metal oxides, such as for example, lanthana, zirconia, yttria, neodymia, samaria, europia, gadolinia and the like. Optionally, the stabilizing metal oxides may be added in stabilizing amounts to the peptized acidic oxide containing slurry.

[0058] It is also within the scope of the invention to form the peptized acidic metal oxide containing slurry by peptization of the acidic metal oxide using an acid. In this case, a suitable acid, e.g. hydrochloric acid, formic acid, nitric acid, citric acid, sulfuric acid, phosphoric acid, acetic acid and the like, is added to the acidic metal oxide containing slurry in an amount sufficient to peptize the acidic metal oxide and obtain a high attrition resistant material as indicated by a DI of 0 to about 50, preferably from 0 to about 20, most preferably from 0 to 15. In general, the amount of acid used ranges from about 0.01 to 1.0, preferably from about 0.05 to 0.6, mole of acid per mole of acidic metal oxide. Thereafter the slurry is aged as herein described above.

[0059] In a preferred embodiment of the invention, the base material composition is prepared by (1) preparing an aqueous acidic metal oxide slurry having from about 10 to about 30 percent solids, (2) adding to the slurry, preferably with agitation, a sufficient amount of an alkali base and/or an alkaline earth metal base in an amount sufficient to peptize the acidic metal oxide and provide at least 0.5 weight percent of alkali metal and/or alkaline earth metal, measured as the metal oxide in the final base material composition, (3) aging the base peptized acidic metal oxide containing slurry at a sufficient temperature and for a sufficient time to permit complete peptization of the acidic metal oxide in the slurry, (4) adding to the peptized slurry an oxygen storage metal salt in an amount sufficient to provide at least 0.1 weight percent of at least one oxygen storage metal oxide in the final base material composition, (5) optionally, adding to the slurry an additional acidic metal oxide source, e.g. sodium

silicate to provide silica, to provide an additional acidic metal oxide (6) diluting the resulting slurry with water to provide a solids concentration of about 5 to 25, preferably, from about 10 to about 20, weight % of the slurry, (7) milling the slurry to reduce the particle size of the materials contained in the slurry to 10 microns or less, preferably 5 microns or less, (8) spray-drying the milled slurry to obtain particles having a mean particle size of greater than 45 μm, preferably from about 50 to about 200 μm, more preferably from about 55 to 150 μm and most preferably from about 60 to 120 μm, (9) optionally drying the spray-dried particles at a sufficient temperature and for a sufficient time to remove volatiles, e.g. at about 100°C to about 250°C for about 1-4 hours, and (10) calcining the dried particles at a sufficient temperature and for sufficient time to form the corresponding metal oxides as described hereinabove. In the most preferred embodiment of the invention, the base material composition is prepared by sequentially performing steps (1) through (10) hereinabove.

[0060] Final compositions in accordance with the invention are prepared by impregnating the base material with an aqueous solution of at least one noble metal salt, e.g. nitrate, chloride, carbonates and sulfates salts, amine complexes, and the like, in an amount sufficient to provide at least 0.1 parts per million of noble metal, measured as the metal, in the final catalyst/additive composition and thereafter drying the impregnated particles to remove volatiles, e.g. typically at about 100°C to 250°C for 1 to 4 hours.

[0061] Compositions in accordance with the invention may be used as a component of a cracking catalyst in an FCC process to reduce gas phase reduced nitrogen species thereby reducing total NO_x emissions. In a preferred embodiment of the invention, the compositions are used in the form of a separate particle additive which is circulated along with the main cracking catalyst throughout the FCCU. Alternatively, the compositions of the invention are included as an additional component of the cracking catalyst to provide an integrated cracking/ NO_x reduction catalyst system.

[0062] Where the invention composition is used as a separate additive particulate, (as opposed to being integrated into the FCC catalyst particles themselves), the composition is used in an amount of at least 0.01 wt % of the FCC catalyst inventory. Preferably, the amount of the invention composition used ranges from about 0.01 to about 50 wt %, most preferably from about 0.1 to about 20 wt %, of the FCC catalyst

inventory. As separate particle additives, compositions of the invention may be added to the FCCU in the conventional manner, e.g. with make-up catalyst to the regenerator, or by any other convenient method.

[0063] Where compositions of the invention are integrated into the FCC catalyst particles themselves, any conventional FCC catalyst particle components may be used in combination with the compositions of the invention. If integrated into the FCC catalyst particles, the composition of the invention, typically represents at least about 0.01wt % of the FCC catalyst particle. Preferably, the amount of the invention compositions used ranges from about 0.01 to about 50 wt %, most preferably from about 0.1 to about 20 wt %, of the FCC catalyst particles.

[0064] Somewhat briefly, the FCC process involves the cracking of heavy hydrocarbon feedstocks to lighter products by contact of the feedstock in a cyclic catalyst recirculation cracking process with a circulating fluidizable catalytic cracking catalyst inventory consisting of particles having a size ranging from about 50 to about 150 μm, preferably from about 60 to about 120 μm. The catalytic cracking of these relatively high molecular weight hydrocarbon feedstocks result in the production of a hydrocarbon product of lower molecular weight. The significant steps in the cyclic FCC process are:

(i) the feed is catalytically cracked in a catalytic cracking zone, normally a riser cracking zone, operating at catalytic cracking conditions by contacting feed with a source of hot, regenerated cracking catalyst to produce an effluent comprising cracked products and spent catalyst containing coke and strippable hydrocarbons;

(ii) the effluent is discharged and separated, normally in one or more cyclones, into a vapor phase rich in cracked product and a solids rich phase comprising the spent catalyst;

(iii) the vapor phase is removed as product and fractionated in the FCC main column and its associated side columns to form gas and liquid cracking products including gasoline;

(iv) the spent catalyst is stripped, usually with steam, to remove occluded hydrocarbons from the catalyst, after which the stripped catalyst is oxidatively regenerated in a catalyst regeneration zone to produce hot, regenerated catalyst

which is then recycled to the cracking zone for cracking further quantities of feed.

[0065] Conventional FCC catalysts include, for example, zeolite based catalysts with a faujasite cracking component as described in the seminal review by Venuto and Habib, *Fluid Catalytic Cracking with Zeolite Catalysts*, Marcel Dekker, New York 1979, ISBN 0-8247-6870-1 as well as in numerous other sources such as Sadeghbeigi, *Fluid Catalytic Cracking Handbook*, Gulf Publ. Co. Houston, 1995, ISBN 0-88415-290-1. Typically, the FCC catalysts consist of a binder, usually silica, alumina, or silica alumina, a Y type zeolite acid site active component, one or more matrix aluminas and/or silica aluminas, and fillers such as kaolin clay. The Y zeolite may be present in one or more forms and may have been ultra stabilized and/or treated with stabilizing cations such as any of the rare earths.

[0066] Typical FCC processes are conducted at reaction temperatures of 480°C to 600°C with catalyst regeneration temperatures of 600°C to 800°C. As it is well known in the art, the catalyst regeneration zone may consist of a single or multiple reactor vessels. The compositions of the invention may be used in FCC processing of any typical hydrocarbon feedstock. The amount of the composition of the invention used may vary depending on the specific FCC process. Preferably, the amount of the compositions used is an amount sufficient to reduce the content of gas phase reduced nitrogen species in the flue gas of an FCCU regenerator operated in a partial or incomplete mode of combustion. Typically, the amount of the compositions used is at least 0.01 wt %, preferably from about 0.01 to about 50 wt %, most preferably from about 0.1 to 20 wt % of the cracking catalyst inventory.

[0067] In order to remove coke from the catalyst, oxygen or air is added to the regeneration zone. This is performed by a suitable sparging device in the bottom of the regeneration zone, or if desired, additional oxygen is added to the dilute phase of the regeneration zone. In the present invention an under-stoichiometric quantity of oxygen is provided to operate the regeneration zone in a partial or incomplete combustion mode.

[0068] The presence of the compositions in accordance with the invention during the catalyst regeneration step dramatically reduces the emissions of gas phase reduced

nitrogen species in the FCCU regenerator effluent. By removing the gas phase reduced nitrogen species from the effluent of the FCCU regenerator, significant reduction of NO_x emissions from the CO boiler is achieved. In some cases, NO_x reduction up to 90 % is readily achievable using the compositions and method of the invention.

[0069] To further illustrate the present invention and the advantages thereof, the following specific examples are given. The examples are given as specific illustrations of the claimed invention. It should be understood, however, that the invention is not limited to the specific details set forth in the examples.

[0070] All parts and percentages in the examples as well as the remainder of the specification which refers to solid compositions or concentrations are by weight unless otherwise specified. However, all parts and percentages in the examples as well as the remainder of the specification referring to gas compositions are molar or by volume unless otherwise specified.

[0071] Further, any range of numbers recited in the specification or claims, such as that representing a particular set of properties, units of measure, conditions, physical states or percentages, is intended to literally incorporate expressly herein by reference or otherwise, any number falling within such range, including any subset of numbers within any range so recited.

EXAMPLES

[0072] The efficiency of the compositions of the invention to reduce NO_x and/or gas phase reduced nitrogen species from an FCCU regenerator operating in a partial or incomplete burn mode was evaluated in the Examples using a Regenerator Test Unit (RTU) and model reactions. The RTU is an apparatus specifically designed to simulate the operation of an FCCU regenerator. The RTU is described in detail in G. Yaluris and A.W. Peters "Studying the Chemistry of the FCCU Regenerator Under Realistic Conditions," Designing Transportation Fuels for a Cleaner Environment, J.G. Reynolds and M.R. Khan, eds., p. 151, Taylor & Francis, 1999, ISBN: 1-56032-813-4, which description is herein incorporated by reference.

[0073] The model reaction for determining the ability of the compositions of the invention to reduce gas phase reduced nitrogen species without converting the species to NO_x in the RTU was the reaction of NH_3 over a cracking catalyst inventory containing the additive tested in the presence of CO and various amounts of O_2. In this experiment NH_3 represents the gas phase reduced nitrogen species, and CO and O_2 represent the other reductants and oxidizers typically found in an FCC unit regenerator operating in partial burn. As the O_2 level in the reactor changes, the various reducing/oxidizing conditions that can be encountered from regenerator to regenerator or inside the same regenerator can be simulated. The key measurement in this experiment in addition to NH_3 conversion, is how much of the NH_3 is converted to NO_x if any. It is desirable that the latter conversion is as low as possible for the widest range of O_2 amounts in the reactor.

[0074] The ability of compositions of the invention to convert NO_x in a FCCU regenerator operated in a partial or incomplete burn mode was determined in the RTU by measuring the activity of the composition to catalyze the reaction of NO_x with CO. The key performance measurement in this test is the NO_x conversion. It is desirable to have high NO_x conversion to nitrogen for a wide range of O_2 amounts.

[0075] Gas phase reduced nitrogen species are reductants for reducing NO_x after it is formed. The ability of compositions of the invention to catalyze this reaction while simultaneously converting the reduced nitrogen species to molecular nitrogen was

determined by measuring in the RTU the activity of the compositions for converting NH_3 with NO_x under various O_2 levels, simulating the reducing/oxidizing conditions possible in a regenerator operating in partial burn. It is desirable in this experiment to have high NO_x conversion to nitrogen.

EXAMPLE 1

[0076] A silica-alumina slurry was prepared by adding 30 pounds of SRSII silica-alumina powder to 57 pounds of water that have been heated to 38 °C. (SRSII sold by Grace Davison, a Business Unit of W.R. Grace & Co.-Conn., in Columbia, MD, silica-alumina powder contained 6% SiO_2 , 94% Al_2O_3 and had a moisture content of 33%.) The slurry was prepared in a steam-jacketed stainless steel tank fitted with an electric powered agitator. Six pounds of an aqueous hydrochloric acid solution (35% HCl) and 6.7 pounds of an aqueous aluminum chlorohydrol solution (22% Al_2O_3) were added to the silica-alumina slurry. The mixture was heated to 55 °C and allowed to age at this temperature for 4 hours with continuous agitation. After the age period, 15.3 pounds of cerium carbonate crystals (obtained from Rhone Poulenc, Inc., 96% CeO_2, 4% La_2O_3, 50% moisture) was added to the tank and 30 pounds of water were added to the tank to reduce the solid content of the slurry to 20 wt%.

[0077] The mixture was milled in a Draiswerke horizontal media mill of ca. 12L working volume, filled to about 80% of the volume with 1.2 mm diameter glass beads. The slurry was pumped at a rate of about 2.3 liters per minute. This milling reduced the average particle size of the materials contained in the slurry to less than 10 microns.

[0078] The milled slurry was fed to a 10 ft. diameter Bowen Engineering spray drier fitted with a rotary atomizer. The spray drier was operated at 315 °C inlet air temperature and 138 °C outlet air temperature. The slurry feed rate was used to control the outlet air temperature. The rotational speed of the atomizer was adjusted until ~ 50% of the product microspheres were retained on a No. 200 screen.

[0079] The spray dried product was loaded into stainless steel trays and heat treated for 2 hours at 675 °C. Only enough material was loaded in each tray so as to obtain a thin layer (~ ¼ inch) of catalyst on the bottom of each tray.

[0080] A one-third portion of the material was then charge into a small Eirich mixer and sprayed with a aqueous solution of sodium carbonate to obtain about 5% Na_2O in the final product. The amount of solution was adjusted not to exceed the water pore volume of the powder. The impregnated material was dried in an oven at 120 °C overnight and calcined for 2 hours at 675 °C. The final composition had the following analysis: 66.2% Al_2O_3, 3.9% SiO_2, 23.9% CeO_2, 1% La_2O_3, 5% Na_2O.

EXAMPLE 2

[0081] An aqueous slurry of peptizable alumina was prepared by combining 27.8 pounds of Versal-700 alumina powder (obtained from LaRoche Industries, Inc., 99% Al_2O_3, 30% moisture) with 52 pounds of water at room temperature in a well agitated tank. While mixing, 2.7 pounds of a sodium hydroxide solution were slowly added to the slurry and the mixture was aged for 20 minutes at room temperature. At the end of the age period, 4.5 pounds of a sodium silicate solution (27.3% SiO_2, 5.7% Na_2O) and 13.6 pounds of cerium carbonate crystals were added to the slurry. Additional water was added to the slurry to bring the solids concentration to 12%. The material was milled, spray dried and calcined using the methods described in Example 1. The final composition had the following analysis: 67.4% Al_2O_3, 4.3% SiO_2, 22.9% CeO_2, 0.9% La_2O_3 and 4.5% Na_2O.

EXAMPLE 3

[0082] An aqueous solution was prepared consisting of 3 pounds of Lignosite-823 surfactant (obtained from Georgia-Pacific West, Inc.) in 180 pounds of water at room temperature. Twenty six pounds of Versal-700 alumina powder (obtained from LaRoche Industries, Inc., 99% Al_2O_3, 30% moisture) and 29.3 pounds of an aqueous formic acid solution (45% CH_2O_2) were added to the Lignosite solution. The slurry was allowed to age for 10 minutes with continuous agitation and then 12 pounds of cerium carbonate crystals were slowly added with continuous agitation. The slurry was milled, spray dried and calcined as described in Example 1 above.

[0083] The calcined product was loaded into an Eirich mixer and sprayed with a aqueous solution of sodium silicate containing 9.2% SiO_2 and 1.92% Na_2O. The

impregnated material was dried in an oven at 120 °C overnight and calcined for 2 hours at 675 °C. The product was impregnated again with an aqueous solution of sodium carbonate containing 7.0% Na_2O, followed by drying and calcining as described in Example 1 above.

EXAMPLE 4

[0084] A microspheriodal particulate support material was prepared as a base material for the preparation of a NO_x composition of the invention. A slurry was prepared from an aqueous slurry having 20% solids of a peptizable alumina (Versal 700 alumina prowder obtained from La Roche Industries Inc., 99% Al_2O_3, 30% moisture). The alumina slurry was prepared using 31.6 lbs of the alumina. To the alumina slurry 3.87 lbs of an aqueous sodium hydroxide solution (50% NaOH) was added. Next, 10.4 lbs of cerium carbonate crystals (obtained from Rhone Poulenc, Inc., 96% CeO_2, 4% $La2O_3$, 50% moisture) was added to the slurry. The slurry was diluted in with a sufficient amount of water to bring the solids concentration of the slurry to 12%. Finally, 3.38 lbs of exchanged silica sol of Nalco 1140 (obtained from Nalco Chemicals Co.) was added to the slurry. The mixture was agitated to assure good mixing and then milled in a stirred media mill to reduce agglomerates to substantially less than 10 microns. The milled mixture was then spray dried as described in Example 1 to form approximately 70 micron microspheres and thereafter calcined at approximately 650 °C to remove volatiles. The resulting material had the following analysis: 2.3% total volatiles, and approximately 4.5% SiO_2, 5% Na_2O, 16.8% CeO_2 and 73% Al_2O_3, and BET surface area of 140 m^2/g.

EXAMPLE 5

[0085] A composition, Additive A, was prepared in accordance with the present invention using the base material prepared in Example 4. 80.0g of the base material was placed in an inclined beaker on a mechanical rotator. A platinum impregnation solution was prepared by weighing out 0.1715g of an aqueous platinum tetramine dihydroxide solution (22.79% platinum) and diluting with DI water to 100g total. The

base material was then impregnated by gradually spraying with 50g of the dilute Pt solution through an air mist spray nozzle system. The wet impregnated base material was dried in an oven at 120 °C overnight. The dried cake was in the form of large chunks and was first ground in a blender and screened before calcining at 650 °C for two hours to decompose the nitrates and remove volatiles. The resulting material contained: 72.5% Al_2O_3, 4.4% SiO_2, 5% Na_2O, 18.8% CeO_2, 331ppm Pt and had a BET surface area of 135 m^2/g.

EXAMPLE 6

[0086] A composition, Additive B, was prepared in accordance with the present invention using the base material prepared in Example 4. 80.0 g of the base material was placed in an inclined beaker on a mechanical rotator. A master Rh solution was prepared by diluting 1.0098g of an aqueous rhodium nitrate salt solution (10% Rh) to 77.48 g of DI water. The base material was then impregnated by gradually spraying with 60g of the dilute Rh solution through an air mist spray nozzle system. The wet impregnated material was dried in an oven at 120 °C overnight. The dried cake was in the form of large chunks and was first ground in a blender and screened before calcining at 650 °C for two hours to decompose the nitrates and remove volatiles. The resulting material contained: 73.2 % Al_2O_3, 4.5% SiO_2, 5.1% Na_2O, 17.5% CeO_2, 1005 ppm Rh and had a BET surface area of 127 m^2/g.

EXAMPLE 7

[0087] A composition, Additive C, was prepared in accordance with the present invention using the base material prepared in Example 4. 80.0 g of the base material was placed in an inclined beaker on a mechanical rotator. A master Rh solution was prepared by diluting 1.0098g of an aqueous rhodium nitrate salt solution (10% Rh) to 77.48 g of DI water. A further dilution was prepared by removing 5.83g of the previously made master dilution and adding DI water to 60g total weight. The base material was then impregnated by gradually spraying with 60g of the latter dilute Rh solution through an air mist spray nozzle system. The wet impregnated material was

dried in an oven at 120 °C over night. The dried cake was in the form of large chunks and was first ground in a blender and screened. The dried cake containing ~100 ppm Rh was placed in an inclined beaker on a mechanical rotator. A platinum impregnation solution was prepared by weighing out 0.1715g of an aqueous platinum tetramine dihydroxide solution (22.79% Pt) and diluting with DI water to 100g total. 50g of said solution was then impregnated onto the dried rhodium containing powder by gradually spraying through an air mist spray nozzle system. The wet impregnated material was dried in an oven at 120 °C overnight. The dried cake was in the form of large chunks and was first ground in a blender and screened before calcining at 650 °C for two hours to decompose the nitrates and remove volatiles. The resulting material contained: 72.5 % Al_2O_3, 4.3% SiO_2, 5.1% Na_2O, 16.9% CeO_2, 90 ppm Rh, 355 ppm Pt, and had a BET surface area or 134 m^2/g.

EXAMPLE 8

[0088] The activity of Additives A, B and C to reduce NH_3 in an FCC unit regenerator operating in partial burn or incomplete combustion was compared to the activity of the cracking catalyst alone and a commercially available CO combustion promoter, CP-3® (platinum on alumina) (sold by Grace Davison, a business unit of W.R. Grace & Co.-Conn., Columbia, MD). The experiments were conducted by reacting in the RTU reactor NH_3 with CO at various levels of O_2, simulating partial burn. After calcination for 2 hours at 595 °C, the additive was blended at 0.5% level with FCC catalyst, which had been deactivated for 4 hours at 816 °C in a fluidized bed reactor with 100% stream. CP-3® was blended at 0.25% with the cracking catalyst. The cracking catalyst alone, and the platinum-based CO combustion promoter Grace Davison CP-3® or the additive/cracking catalyst blend were separately fed to the RTU reactor operating at 700 °C. The gas feed to the RTU was a mixture of NH_3 and CO containing approximately 600 ppm NH_3, 5000-5500 ppm CO, various amounts of O_2 added as 4% O_2 in N_2, with the balance being nitrogen. The total gas feed rate excluding the O_2 containing gas feed was 1000-1100 sccm. The results are recorded in FIG. 1 and FIG. 2 below.

[0089] As shown in FIGS. 1 and 2, Additives A, B and C are very effective in minimizing NH_3 and preventing its conversion to NO_x. No other nitrogen oxides (e.g., NO_2 or N_2O) were detected, indicating the conversion of NH_3 to molecular nitrogen. Additives B and C are the most effective of the three additives. The activity of additives A, B, and C for reducing NH_3 under partial burn conditions was far superior to that of the conventional combustion promoter, like the commercially available CP®-3.

EXAMPLE 9

[0090] The activity of Additives A, B and C for reducing NH_3 and NO_x present in an FCC unit regenerator operating in partial burn or incomplete combustion was also compared to the activity of the cracking catalyst alone and a commercially available CO combustion promoter, CP-3®, using the reaction of NH_3 with NO_x under partial burn conditions. The experiments were conducted as in example 8 except that the gas mixture fed to the RTU reactor contained approximately 1000 ppm NH_3 and 500-550 ppm NO_x as well as various amounts of oxygen with the balance nitrogen. The results are recorded in FIG. 3 and FIG. 4 below.

[0091] As shown in FIG. 3 and FIG. 4, compositions of the invention, i.e. Additives A, B and C, showed enhanced conversion of NH_3 and NO_x to molecular nitrogen. No other nitrogen oxides, like N_2O or NO_2, were detected during these experiments, indicating the conversion of NH_3 to molecular nitrogen.

EXAMPLE 10

[0092] The activity of Additives A, B and C to reduce NO_x formed in an partial burn or incomplete burn FCCU was compared to that of the cracking catalyst alone and a commercially-available, platinum-containing combustion promoter, CP-3®, by measuring the activity of the materials to covert NO_x to molecular nitrogen in the presence of CO at various levels of oxygen. The experiments were conducted as in Example 8 except that the gas feed to the reactor was a mixture containing 5000-5500

ppm CO, 500-550 ppm NO_x, various amounts of oxygen added as 4% O_2/N_2, and the balance nitrogen. The results are recorded in FIG. 5 below.

[0092] FIG. 5 show that Additives A, B and C are very effective for converting NO_x under partial burn conditions. They are also more effective than the combustion promoter at low levels of oxygen simulating partial burn. No other nitrogen oxides like N_2O or NO_2 were detected.

WHAT IS CLAIMED IS:

1. A composition for reducing the content of NO_x and gas phase reduced nitrogen species during catalyst regeneration in a fluid catalytic cracking (FCC) process, said composition comprising particles having a mean particle size of about 50 to about 200 μm and comprising (i) at least about 5.0 wt % of acidic metal oxide containing substantially no zeolite; (ii) a metal component selected from the group consisting of alkali metal, alkaline earth metal, and mixtures thereof; (iii) at least 0.1 wt %, measured as metal oxide, of an oxygen storage metal oxide; and (iv) at least 0.1 ppm of a noble metal component selected from the group consisting of platinum, iridium, sodium, osmium, ruthenium, rhenium and mixtures thereof, said metal component (ii) being present in amount of at least 0.5 wt %, measured as metal oxide, of the composition.

2. The composition of Claim 1 wherein the acidic metal oxide is selected from the group consisting of alumina, silica alumina, lanthana alumina and zirconia alumina.

3. The composition of Claim 2 wherein the said acidic metal oxide is silica alumina.

4. The composition of Claim 1 wherein the acidic metal oxide further comprises at least one stabilizing metal oxide.

5. The composition of Claim 4 wherein the stabilizing metal oxide is selected from the group consisting of yttria, neodymia, samaria, europia, gadolinia and mixtures thereof.

6. The composition of Claim 1 wherein the component (ii) is alkali metal.

7. The composition of Claim 6 wherein said alkali metal is selected from the group consisting of sodium, potassium, cesium, lithium and mixtures thereof.

8. The composition of Claim 7 wherein the alkali metal is sodium or potassium.

9. The composition of Claim 8 wherein the alkali metal is sodium.

10. The composition of Claim 1 wherein component (ii) contains an alkaline earth metal.

11. The composition of Claim 10 wherein the alkaline earth metal is selected from the group consisting of magnesium, calcium barium, strontium and mixtures thereof.

12. The composition of Claim 11 wherein the alkaline earth metal is magnesium.

13. The composition of Claim 1 wherein the oxygen storage component (iii) is a rare earth metal oxide having oxygen storage capability, a transition metal oxide having oxygen storage capability, and mixtures thereof.

14. The composition of Claim 13 wherein the oxygen storage component (iii) is a rare earth metal oxide having oxygen storage capability.

15. The composition of Claim 14 wherein the rare earth metal oxide is selected from the group of ceria, samaria, praseodymia, europia, terbia and mixtures thereof.

16. The composition of Claim 13 wherein the oxygen storage component (iii) is a transition metal oxide having oxygen storage capability.

17. The composition of the above Claim 16 wherein the transition metal oxide is selected from the group consisting of vanadium, manganese oxide, iron oxide, nickel

oxide, copper oxide, cobalt oxide, chromia, titania, silver oxide, molybdenia, niobia, gold oxide, tungsten oxide, and mixtures thereof.

18. The composition of Claim 15 wherein at least a portion of the rare earth metal oxide comprise ceria.

19. The composition of Claim 18 wherein the rare earth metal oxide consists essentially of ceria.

20. The composition of Claim 13 wherein the oxygen storage metal oxide component (iii) further comprises at least one stabilizing metal oxide.

21. The composition of Claim 21 wherein the stabilizing metal oxide is selected from the group consisting of zirconia, lanthana, neodymia, gadolinia, yttria, scandia, hafnia, and mixtures thereof.

22. The composition of Claim 1 wherein the noble metal component is selected from the group consisting of platinum, iridium, rhodium, osmium, ruthenium, rhenium and mixtures thereof.

23. The composition of Claim 22 wherein the noble metal component is selected from the group consisting of platinum, rhodium, iridium and mixtures thereof.

24. A fluid cracking catalyst comprising (a) a cracking component suitable for catalyzing the cracking of hydrocarbons, and (b) the composition of claim 1.

25. The cracking catalyst of Claim 24 wherein said cracking catalyst comprises an admixture of components (a) and (b).

26. The cracking catalyst of Claim 24 wherein said catalyst comprises integral particles which contain both components (a) and (b).

27. The cracking catalyst of Claim 24 wherein component (b) comprises at least 0.01 wt % of the cracking catalyst.

28. A method of reducing gas phase reduced nitrogen species emissions from the regeneration zone during fluid catalytic cracking of a hydrocarbon feedstock into lower molecular weight components, said method comprising contacting a hydrocarbon feedstock with a cracking catalyst at elevated temperature whereby lower molecular weight hydrocarbon components are formed, said cracking catalyst comprising (a) a cracking component suitable for catalyzing the cracking of hydrocarbons, and (b) the composition of claim 1.

29. The method of Claim 28 further comprising recovering the cracking catalyst from said contacting step and treating the used catalyst in a regeneration zone to regenerate said catalyst.

30. The method of Claim 29 wherein the regeneration zone is operated in a partial mode of combustion.

31. The method of Claim 28 wherein components (a) and component (b) are fluidized during contacting said hydrocarbon feedstock.

32. The method of Claim 29 wherein the regeneration zone is operated in incomplete mode combustion.

33. A method of reducing NO_x emissions from the regeneration zone during fluid catalytic cracking of a hydrocarbon feedstock into lower molecular weight components, said method comprising contacting a hydrocarbon feedstock with a cracking catalyst at elevated temperature whereby lower molecular weight hydrocarbon components are formed, said cracking catalyst comprising (a) a cracking

component suitable for catalyzing the cracking of hydrocarbons, and (b) the composition of claim 1.

34. The method of Claim 33 further comprising recovering the cracking catalyst from said contacting step and treating the used catalyst in a regeneration zone to regenerate said catalyst.

35. The method of Claim 34 wherein the regeneration zone is operated in a partial mode of combustion.

36. The method of Claim 33 wherein components (a) and component (b) are fluidized during contacting said hydrocarbon feedstock.

37. The method of Claim 34 wherein the regeneration zone is operated in an incomplete mode of combustion.