

TITLE

CENTRIFUGAL CYCLONE SEPARATOR

BACKGROUND OF THE INVENTION

At least one embodiment of the invention is a centrifugal/ cyclone separator which separates particles, liquid droplets and or condensing mists (water based and or hydrocarbon based nature) from gases without using a filter element.

Generally, filters or some cyclone/ centrifugal separators having a coalescing filter element have at least one drawback. The coalescing filter element is choked quickly due to their small pore size and resulted in high maintenance.

A coalescing filter is used in conjunction with membrane filter to remove particles, liquid droplets and fine mists from gases. However, these filters are choked up quickly due to their small pore size and can only provide very short term service interval ranging from a few days to 2 weeks resulting in very high maintenance and replacement costs. Our separator is expected to operate maintenance-free since it does not make use of any filter element.

For example, cyclone/ centrifugal separators are used in high flow rate applications and not low flow rate applications. When this is used in conjunction with a coalescing filter, the filter element is choked up very quickly and requires very high

1 maintenance. Therefore, there is a need for a centrifugal cyclone separator which does
2 not have a coalescing filter element.

4 SUMMARY OF THE INVENTION

5
6 At least one embodiment of the invention relates to a centrifugal/ cyclone
7 separator which separates particles, liquid droplets and or condensing mists (water
8 based and or hydrocarbon based nature) from gases without using a filter element. With
9 at least one embodiment of the present invention, the centrifugal/ cyclone separator can
10 separate particles and or liquid droplets and condensing mists (water and or
11 hydrocarbon) from gases without using a filter element and can operate optimally on low
12 gas flow rate from 30 l/h up to 150 NI/h (Normal L/h). This embodiment is also able to
13 separate fine particles and condensing mists up to 5 to 10 micron size which is attributed
14 to the combined effect of the use of an inlet spiral tube, a first conical fin and a second
15 conical fin. In addition, it is also attributable to the cylindrical body and the extension of
16 the vortex finder below the second conical fin.

17
18 The separator is specially designed to work optimally on low pressure and low gas
19 flow rate from 30 l/h up to 150 NI/h and is able to separate fine particles/mists between 5
20 to 10 micron size. It is also designed to separate up to a maximum of 20 l/h of liquid flow
21 or 2000 NI/h gas flow or a maximum of 40l/h of liquid flow or 1000 NI/h of gas flow. The
22 separator can work at low pressure close to atmospheric pressure or up to 100 barg

1 (barg= pressure in bars above ambient or atmospheric pressure) pressure.

2
3 The present invention is an innovative break-through for applying cyclonic/
4 centrifugal separator under low gas flow rate from 30 NI/h to 500 NI/h. It does not require
5 a filter element and can separate particles droplets condensing mists between 5-10
6 micron or less than 1 micron with cooler or liquid injection. It provides a robust and
7 maintenance-free solution as compared to that of coalescing filter and membrane filters
8 which provides service interval of a few days to two (2) weeks due to chokage of the fine
9 pores. Many critical process gas analyzers which are used for quality and safety control
10 in the process plants are often destroyed or make unavailable due to carry-over or
11 chokage of the traditional coalescing filter and membrane filter.

12
13 One reason why the centrifugal/ cyclone separator of the present invention can
14 separate particles and or liquid droplets and condensing mists (water and or
15 hydrocarbon) from gases without using a filter element, and can operate optimally on low
16 gas flow rate from 30 l/h up to 150 NI/h and is able to separate fine particles and
17 condensing mists up to 5 to 10 micron size is attributed to the combined effect of one or
18 more of the components of the separator. These components can include one or more
19 of an inlet spiral tube, at least one conical fin, a step in the cylindrical body, and the
20 extension of the vortex finder below the conical fin.

BRIEF DESCRIPTION OF THE DRAWINGS

Other objects and features of the present invention will become apparent from the following detailed description considered in connection with the accompanying drawings which disclose at least one embodiment of the present invention. It should be understood, however, that the drawings are designed for the purpose of illustration only and not as a definition of the limits of the invention.

In the drawings, wherein similar reference characters denote similar elements throughout the several views:

FIG. 1 is an open side view of a first embodiment of the invention;

FIG. 2 is a side view of the stopper plate for use in both the first and second embodiments of the invention; and

FIG. 3 is an open side view of a second embodiment of the invention;

FIG. 4 is a view of two separators in series; and

FIG. 5 is a side view of a cooler which can be optionally coupled to either an inlet of a first separator and/or an inlet of a second separator.

DETAILED DESCRIPTION OF PREFERRED EMBODIMENTS

Turning in detail to the drawings, FIG. 1 shows a first embodiment of a separator

10 which includes an inlet tube 1. Cyclonic/ centrifugal separators have been used widely for separation of particles, liquid droplets and or condensing mists from gases under high gas flow rate involving at least Nm^3/h gas flow rate in order to generate sufficient high centrifugal/ cyclone forces. The dirty/ wet gas enters the separator from the top via the inlet tube 1. This inlet tube 1 is coiled spirally downwards to create centrifugal/cyclone forces to separate the particles, liquid droplets and or condensing mists from the gas. This tube stops above the conical fin 3 which is located above the second conical fin 4.

Separator 10 has an inlet spiral tube 1 which has a small inner bore to generate high gas flow velocity leading to high centrifugal/ cyclonic forces inside the top cylindrical housing 2 for effective separation. The tube 1 also guides the gas, liquid droplets, and or condensing mists smoothly from the outside of the separator spirally downwards. This is an excellent key feature which meets the requirement of cyclone inlet geometry to provide a smooth flow with minimum turbulent and minimum erosion. It is vital that the cyclone separator inlet geometry separation minimizes turbulence in the gas flow which can create new liquid mists splashing or particles turbulent flow resulting in carry over to the clean and dry exist gas.

The other embodiment, that of separator 12 has an insert 1A having a threaded area forming a flow path which functions like a spiral tube. This insert can comprise a cylindrical block of material having a spiral path.

1
2 First and second conical fins 3 and 4 function to push the gas particles, liquid
3 droplets, and or condensing mists close to the cylindrical wall of the top housing 2. Upon
4 exiting the second conical fin 4 there is a step, ridge or protrusion 9 where the particles
5 liquid droplets and or mists enters cylindrical body 5 which is of bigger inner diameter
6 (see line d2) from that of the top cylindrical housing. The gas, particles, liquid droplets
7 and or mists continue to flow spirally downwards tangentially in the cylindrical body. The
8 tail end of the cyclonic gas flow rests on top of the vortex breaker 7 where the clean and
9 dry gas spirals axially upwards towards the vortex finder 6 and exit from the top right side
10 of the separator through gas outlet tube 15. The particles, liquid droplets and or
11 condensing mists continue to spiral beyond the vortex breaker and then their swirling
12 movement is stopped by the swirl stopper plates 8. The particles, liquid droplets mists
13 and or some gas then exit the separator from the bottom side 11.

14
15 First and second conical fins 3 and 4 force the gases, liquids droplets and mists
16 to coalesce/collide together to form larger size liquid droplets and larger size particles for
17 effective subsequent cyclonic/ centrifugal separation. The gaps between the first and
18 second conical fins 3 and 4 and the inner wall of 2 the top cylindrical housing can be
19 made relatively small. For example, this dimension can be any suitable dimension,
20 wherein different examples can include a range from 0.5 mm to 1 mm (millimeters) or
21 even up to 2 mm to enhance the compression and coalescing/collision effect. The edges
22 of the first and second conical fins 3 and 4 are sharp or substantially sharp or at least

1 sufficiently sharp to ensure clean dislodge of the gas, liquids and particles mixture and
2 also to ensure minimum restriction to gas flow.

3
4 Step, ridge or protrusion 9 is disposed at the joint between the top cylindrical
5 housing 2 and the cylindrical body 5. Step 9 ensures that liquid droplets, particles and
6 or condensing mists dislodge cleanly and outwardly from the second conical fin 4 to
7 avoid re-entrainment or creep flow around to the vortex finder 6 resulting in carry over
8 with the existing clean and dry gas. The vortex finder 6 also extends below second
9 conical fin 4 for the same purpose.

10
11 Lastly, two separators can be used in series to provide coarse and fine separation
12 to avoid overloading the first separator. With this design, the gaps between first conical
13 fin 3 and second conical fin 4 and the inner wall of the top cylindrical housing 2 of the first
14 separator is usually bigger than that of the second separator. This configuration is
15 shown in FIG. 4 which shows two separators 10a and 10b shown aligned in series with
16 each other so that the material can make a pass through two different separators. With
17 this design, the first separator 10a in the series would have the larger gap between the
18 first conical fin 3, the second conical fin 4 and the inner wall shown here as 20 in
19 separator 10a than the gap 21 between conical fin 3, and second conical fin 4 and wall
20 2b in separator 10b. As shown in this diagram, the processed gasses exit from exit port
21 15 and enter into port 16 on separator 10b. In this way, the gasses are processed twice
22 so that there is sufficient separation of particles from the gasses.

1
2 To enhance separation efficiency, two separators can be used in series to
3 guarantee separation performance where the first separator can be used for coarse
4 separation while the second separator for fine separation without overloading the first
5 separator. For separation of very fine mists or particles of less than 5 or smaller micron
6 size in a very dry gas, a cooler shall be used in conjunction with the separator to create
7 small amount of liquid condensate which forms liquid droplets or liquid film which can
8 allow fine particles, mists to stick onto due to adhesion.

9
10 For separation of very fine mists or particles of less than 1 micron, the device can
11 include a cooler 30 made up of a tube coil where fine mists can be adhered onto the
12 liquid film due to centrifugal forces inside the tube coil and allows other mists/particles to
13 adhere to. As shown in FIG. 5, the cooler 30 has an inlet 31 and an outlet 32 that can
14 be connected to inlet spiral tube 14 of first separator or inlet spiral tube 16 of the 2nd
15 separator. The cooler 30 serves to form liquid condensation which will create a liquid
16 film for fine mists/fine particles to adhere onto before the separator. In at least one
17 embodiment, the cooler is separate from the separator because the flow velocity in the
18 separator is too fast and the residence time is too short to create the desired results.

19
20 The reason why the centrifugal/ cyclone separator can separate particles liquid
21 droplets condensing mists (water based and or hydrocarbon based nature} from gases
22 without using a filter element, and can operate optimally at low gas flow rate from 30 1/h

1 up to 150 NI/h, and is able to separate fine particles condensing mists up to 5 to 10
2 micron size is attributed to the combined effect of the components listed above. For
3 example, with the first embodiment, the design relies on the use of the inlet spiral tube 1,
4 the first conical fin 3 and the second conical fin 4, and the step 9 on the cylindrical body
5 and the extension of the vortex finder below second conical fin 4. With the second
6 embodiment, the design differs in that it relies on the insert 1A with threaded area
7 forming a flow path like spiral tube, while relying on the same or similar components as
8 with the first embodiment listed above.

9
10 The combined effect of these key components is an excellent separator geometry
11 which ensures very smooth non-turbulent, high velocity flow rate which generates high
12 centrifugal/ cyclonic action for separation. There is also low restriction to low gas flow.
13 excellent compression and collision/ coalescing of fine condensing mists and particles
14 with liquid droplets and large particles to create larger size droplets/ particles for effective
15 separation by the first and second conical fins 3 and 4. Finally, the sharp edges of the
16 first and second conical fins 3 and 4, the step 9 at the joint between the top cylindrical
17 housing and the cylindrical body and the extension of the vortex finder below the second
18 conical fin 4 all ensure clean dislodge and outwardly separation of particles liquid
19 droplets and condensing mists and gas to prevent carry-over to the existing clean and
20 dry gas.

21
22 The length of cylindrical body 5 can be shortened to improve residence time

1 inside the separator without affecting the separation efficiency.

2
3 The gaps between the conical fins 3 and 4 and the inner diameter of top
4 cylindrical housing 2 can be increased up to 2 mm if the size of the largest particle is
5 expected to be around 1 + mm for coarse separation such as shown in the embodiment
6 10A in FIG. 4. The overall diameter and dimension of the separator can be increased
7 proportionally to maintain steps and thickness of the top cylindrical housing and the
8 cylindrical body. The thickness of the top cylindrical housing 2 and cylindrical body can
9 be increased to cope with higher pressure and temperature as required for mechanical
10 strength. However, the internal dimensions of the mentioned key features shall not be
11 reduced. The length of the spiral coil can be increased or decreased slightly without
12 affecting the separation efficiency.

13
14 The first embodiment of the separator comprises an inlet spiral tube 1 which has a
15 small inner bore to generate high gas flow velocity leading to high centrifugal/ cyclonic
16 forces inside the top cylindrical housing 2 for effective separation. It is also designed to
17 separate up to a maximum of 20 l/h of liquid flow from 2000 NI/h gas flow or maximum of
18 40l/h from 1000 NI/h gas flow.

19
20 At least one embodiment uses a step 9 positioned at the joint between the top
21 cylindrical housing 2 or first section or first body to the second portion of the housing or
22 second cylindrical body 5 to ensure that liquid droplets, particles and or mists dislodge

1 cleanly and outwardly from the second conical fin 4 to avoid re-entrainment or surface
2 flow around to the vortex finder 6 resulting in carry over with the existing clean and dry
3 gas. The vortex finder 6 also extends 5mm below the second conical fin 4 for the same
4 purpose.

5
6 Lastly, small amount of water or hydrocarbon liquid spray can also be added with
7 the inlet dry and dirty gas to create liquid droplets or films for the fine mist and fine
8 particles to adhere onto.

9
10 The materials listed above, particularly the first body section 2, and the second
11 body section 5 of the housing, the spiral tube 1, the insert 1A, the conical fin 3, the
12 conical fin 4, the vortex finder 6, the vortex breaker 7, the swirl stopper plate 8, and the
13 step 9, can be made from any suitable material such as but not limited to Stainless Steel,
14 corrosion resistant metal or alloys, PTFE, Polycarbonate or other hard plastic that is
15 mechanically strong to withstand the operating pressure and chemically resistant.

16
17 In all, the design allows for a filterless separator or a separator having no
18 coalescing filter using the geometry of the components listed above. This creates a
19 device that does not need to be serviced as much and does not need numerous filter
20 replacements as well. Thus, the components as described above create a cyclone in
21 the gas using a spiral feed mechanism or spiral mechanism such as tube 1 or
22 component 1A to create a separating cyclonic effect in the gas. The more dense

1 particles are pushed towards the edge of the housing where they condense. The
2 separator elements or fins 3 and 4 are configured to push these components towards the
3 wall of the housing where they will coalesce or condense. These condensed particles
4 then drop towards the outlet 11 while the remaining uncondensed portion of the gas is
5 driven against the vortex breaker 7 and sent up into the vortex finder 6 wherein the
6 remaining gas is passed up and out of the separator out from outlet port 15. In this way
7 gasses are separated from liquid or solid material without the need for a filter that would
8 otherwise need to be replaced.

9
10 Accordingly, while at least one embodiment of the present invention have been
11 shown and described, it is to be understood that many changes and modifications may
12 be made thereunto without departing from the spirit and scope of the invention as
13 defined in the appended claims.

CLAIMS**WHAT IS CLAIMED IS:**

1. A separator for use with a gas or a liquid comprising:
 - a) at least one housing comprising at least one inlet and at least one outlet;
 - b) at least one spiral mechanism configured to cause the gas or the liquid to spiral within said housing;
 - c) at least one separator element disposed adjacent to said at least one spiral mechanism and configured to further separate particles from the gas or the liquid.
2. The separator as in claim 1, wherein said housing comprises a cylinder having a substantially hollow inner region.
3. The separator as in claim 1, wherein said spiral mechanism comprises at least one spiral tube.
4. The separator as in claim 1, wherein said spiral mechanism comprises at least one insert having a threaded area forming a flow path.
5. The separator as in claim 1, wherein said spiral mechanism comprises an insert comprising a substantially cylindrical block of material having a spiral path.

1
2
3 6. The separator as in claim 1, wherein said at least one separator element
4 comprises a substantially conical fin.
5

6 7. The separator as in claim 1, wherein said at least one separator element
7 comprises a first conical fin, and a second conical fin disposed adjacent to said
8 first conical fin.
9

10 8. The separator as in claim 1, wherein said housing comprises a first body
11 section and a second body section, said inlet being coupled to said first body
12 section, and said outlet being coupled to said second body section.
13
14

15 9. The separator as in claim 8, wherein said first body section is narrower than
16 said second body section.
17

18 10. The separator as in claim 9, further comprising a step, coupled to said
19 housing, said step formed in a region where said first body section meets said
20 second body section.
21
22

23 11. The separator as in claim 9, wherein said step is positioned adjacent to said
24 first body section and adjacent to said at least one separator element.

1
2 12. The separator as in claim 8, further comprising a vortex finder extending from
3 said first body section to said second body section.

4
5
6 13. The separator as in claim 12, further comprising a vortex breaker positioned
7 downstream from said vortex finder, in said second body section.

8
9 14. The separator as in claim 13, further comprising a swirl stopper plate
10 configured to interrupt a swirling flow of fluid and/or gasses inside the housing.

11
12
13 15. The separator as in claim 14, wherein said swirl stopper plate is positioned
14 adjacent to said outlet in said second body section.

15
16 16. The separator as in claim 7, wherein said housing has an inner wall and
17 wherein said first conical fin and said second conical fin is spaced from said inner
18 wall of said housing by .5 mm to 2 mm.

19
20 17. The separator as in claim 1, wherein said separator is configured to separate
21 at a rate of up to 20 l/h for fluid flow rate or 2000 NI/h for gas flow rate.

22
23 18. The separator as in claim 1, wherein said separator is configured to separate
24 particles in a condensing mist of up to 10 microns in size.

1 19. The separator as in claim 1, further comprising a cooler having an outlet
2 coupled to said inlet of said separator and configured to cool the input of gasses or
3 liquid into the separator.
4

5 20. A separator assembly comprising:

6 a first separator comprising:

7
8 a) at least one housing comprising at least one inlet and at least one outlet;

9 b) at least one spiral mechanism configured to cause gas or liquid to spiral
10 within said housing;

11 c) at least one separator element disposed adjacent to said at least one spiral
12 mechanism and configured to further separate particles.

13 a second separator comprising:

14
15 a) at least one housing comprising at least one inlet and at least one outlet;

16 b) at least one spiral mechanism configured to cause gas or liquid to spiral
17 within said housing;

18 c) at least one separator element disposed adjacent to said at least one spiral
19 mechanism and configured to further separate particles.

20 wherein said separator element of said second separator is spaced from said
21 housing at a distance smaller than a distance that said separator element of said
22 first separator is spaced from said housing of said first separator.
23

24 21. A process for separating material comprising a gas and at least one of a solid

1 and/or a liquid comprising;

2 a) introducing the material to be separated into a separator;

3 b) passing the material to be separated into at least one spiral
4 mechanism to create a cyclonic effect;

5 c) passing said material to be separated through a separator element
6 comprising a plurality of fins which are configured to create a
7 collision effect to condense particles of the material to be separated
8 into at non-gaseous form;

9 d) passing said material past a step inside of said housing so that said
10 material to be separated in non gaseous form separate from said
11 separator element;

12 e) removing at least some of said material to be separated in non
13 gaseous form from at least some of a remaining gas;

14 f) expelling at least some of said non gaseous material to be
15 separated from the separator from a first outlet port; and

16 g) expelling at least some of said gaseous material to be separated
17 from a second outlet port.