

A process for stripping monomers and other volatile constituents from polymer melts

The invention relates to a process for stripping volatile
5 constituents such as solvents or monomers from polymer melts using an evaporator apparatus.

The removal of volatile constituents from polymer melts is generally one of the last process steps in the production
10 of polymers. The volatile constituents to be removed may be solvents which were used for the production of the polymers or residues of unreacted monomers after concluded transesterification or esterification or polymerisation reactions and elimination products from transesterification
15 or esterification reactions.

For the purposes of the present invention, volatile constituents are taken to mean any volatile impurities such as monomers, i.e. any starting materials, and volatile
20 components of all kinds such as for example solvents, low molecular weight reaction products, elimination products from the reaction, and decomposition and breakdown products which arise during the reaction, together with any secondary compounds introduced via the feedstocks. In
25 relation to the residual monomers, low molecular weight reaction products are hereinafter taken to mean those with a degree of polycondensation of up to 3.

The removal of such constituents is necessary because such
30 accompanying substances generally give rise to deficiencies in material properties such as thermal stability, processability, flow behaviour etc.. Such volatile constituents may also give rise to unwanted odour nuisances and/or be harmful to health.

Various apparatuses or processes are known depending on the viscosity of the polymer melts from which the volatile constituents are to be removed. Known apparatuses for this task in polymer melts are, for example, film evaporators or filmtruders, screw machines, strand evaporators or tubular evaporators.

Removal of volatile constituents by chemical means is described, for example, in EP 0 768 337 A1. Removal is effected by addition of CH-acidic organic compounds. The chemical conversion of residual monomers may possibly give rise to products with unwanted environmental impact, which distinctly complicates the use of the products in practical applications. Said process also cannot be used for removing residual solvents.

The process for reducing residual monomers with unsaturated fatty acids according to US 4,215,024 suffers from the same shortcomings.

Another known process describes the reduction of residual monomers by treating the moulding compositions with electron beam radiation, as described in DE 2 843 292 A1. The process is, however, much too costly on a full industrial scale. A process for the removal of residual volatiles by injection of supercritical solvents or gases into the polymer melt with subsequent depressurisation described in EP 0 798 314 A1 has also proved equally costly.

Conventional and usual processes are also based on the removal of volatile constituents by means of mechanically

assisted systems. Accordingly, extruders, such as for example in US 4,423,960, DE 2 721 848 C2, EP 0 411 510 B1 or in "Entgasen von Kunststoffen in mehrwelligen Schneckenmaschinen", Kunststoffe 71 (1981), pages 18-26, devolatilising centrifuges (US 4,940,472), friction compaction (EP 0 460 450 A2) or film evaporators (DE 1 925 063 A1 or EP 0 267 025 A1) are used. These processes conventionally have a short residence time of the order of a few minutes.

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All the above-stated mechanically assisted processes exhibit the disadvantage that heavy moving parts which move at high rotational speed and rotational frequencies are required in the apparatus. This results in costly apparatus or machinery which is susceptible to malfunctioning and wear. If adequate degassing efficiency is to be achieved, frequent circulation of the product is necessary. At the short residence times, elevated temperatures are, on the one hand, necessary in order to shift the diffusion coefficients and physical equilibria of the volatile components towards favourable values. On the other hand, such elevated temperatures are unavoidable because the frequent circulation of the product results in elevated input of energy. The person skilled in the art is aware that elevated temperatures strongly promote and accelerate unwanted reactions in polymers. Such reactions result in unwanted reductions in quality, such as for example discoloration and/or formation of gel particles, particles or specks and branched structures or even dissociation into monomers. The mechanical energy is usually produced from electrical energy, resulting in higher costs relative to the use of primary energy. Typical energy inputs of such

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processes are in the order of 0.05 to 0.2 kWh/kg of product.

"Static" degassing processes, which introduce mechanical energy only via pumps, usually gear pumps, are furthermore known to the person skilled in the art. These static processes operate in such a manner that a polymer melt, optionally with additives, is introduced into a degassing vessel, in which the volatile constituents evaporate and are drawn off in gaseous form. Such processes often have multiple stages.

One example of a static process is DE 10 031 766 A1, which describes a two-stage, continuous process for degassing styrene copolymers, in which, in a first stage, the concentration of polymer is adjusted to above 99.8 wt.% in a shell-and-tube heat exchanger with evaporation of volatile constituents and simultaneous input of energy and, in a second stage, the final concentration is obtained in a strand evaporator without intermediate superheating.

A strand evaporator operates by forming free-falling strands of melt in a cabinet, i.e. without supply of mechanical energy. In the cabinet, the strands are generally exposed to a vacuum at elevated temperatures. The heights of such apparatus are limited and thus so too is the residence time during which evaporation can occur. Another disadvantage of the process resides in the very large number of holes which are required for a good degassing result in the strand evaporator. The diameters of the holes are in the lower, single digit millimetre range, while, at throughput of a few tonnes per hour, the holes range in number from some thousands to a hundred thousand.

This is disadvantageous. Given the large number of holes, it is to be feared that specks and swollen solids may give rise to blockages and disruption to flow on exit from the hole. Finally, the efficiency of a strand evaporator
5 depends on the stability of the strands, which in turn depends in complex manner on product rheology, flow conditions in the gas space of the strand evaporator, the geometry and quality of the holes and temperature. It is accordingly difficult to establish and control constant
10 processing conditions.

Another example of a static process is US 4,699,976, which describes a two-stage, continuous process for degassing rubber-containing styrene polymers. This process uses two
15 degassing stages which are equipped with shell-and-tube heat exchangers. In the first stage, the polymer solution is concentrated to a residual content of volatile constituents of between 3% and 15%. In the second stage, evaporation is then performed to obtain the desired final
20 concentration. During this process, foaming occurs inside the tubes. This process cannot, however, be used if the concentration of volatile constituents is so low that the polymer melt does not foam because the volume of gas which arises is insufficient.

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"Neue Mischverfahren mit geringem Energiebedarf für Polymerherstellung und -aufbereitung", Chemische Industrie (1985) 37 (7), pages 473 to 476, describes a static process in which, prior to the final stage, an entraining agent is
30 mixed with the polymer before the product is introduced in the final stage into a degassing vessel. As is familiar to the person skilled in the art, the entraining agents used are primarily inert gases, such as for example nitrogen or

carbon dioxide or alternatively also water. In EP 0 027 700 A2, an inert entraining agent from the group comprising water, nitrogen, carbon dioxide or hydrocarbons with one to four carbon atoms is mixed with a polymer solution and
5 flashed in a chamber. Both the above-stated processes have disadvantages. Inert gases reduce the performance of the condensers in which the volatile constituents are to be condensed and increase the volume to be conveyed by the vacuum system, so increasing the cost of the process. The
10 use of water is disadvantageous because it entails restricting the temperature of the condensers to above 0°C in order to prevent freezing and this limits the performance of the condensing system, which must in turn be compensated by a larger and more costly vacuum
15 installation. Water may also react with various polymers, resulting in degradation of molecular weight and impairment of properties.

The concentration of residual volatiles is at thermodynamic
20 equilibrium, when, with ideal mass transfer and after an adequate residence time, the product is at equilibrium with the gas in the stripping apparatus at the selected temperature and the selected pressure, i.e. the concentration undergoes no further change. Changes of a
25 chemical nature due to thermal processes, such as dissociation, decomposition and the like, may severely restrict this statement and are not taken into account in the definition. This definition is familiar to the person skilled in the art. If degassing is to be possible at all
30 in an apparatus, the concentration of residual volatiles in the product must always be higher than corresponds to the thermodynamic equilibrium. A degassing apparatus is particularly advantageous if the concentrations of the

constituents to be stripped at the outlet thereof are as close as possible to the thermodynamic equilibrium, it being physically impossible for the concentrations to fall below this level.

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Static processes of the above-stated kind have the disadvantage that, for each stage, they permit and enable only one single degassing step in order to move towards the thermodynamic equilibrium before the product is again
10 discharged from the stage. If, for reasons of degassing efficiency, it is possible in the individual stage to reduce the concentration of a volatile component only by, for example, a factor of 3 relative to the input value, but the degassing task requires a reduction by a factor of 20
15 relative to the input value, a three-stage installation is required. Obviously, this is costly, highly complex and thus to be avoided if at all possible.

Without exception, the stated apparatuses have short
20 residence times. It is endeavoured to achieve short residence times in order to reduce the products' exposure to elevated temperatures because, as is familiar to the person skilled in the art, exposure to elevated temperatures results in unwanted quality impairment, such
25 as for example discoloration and/or in the formation of particles or specks due to secondary and decomposition reactions. The short residence times relate only to those states in which the product has a large surface area per unit mass in the stripping apparatus, i.e. not in "sumps"
30 in which the product is collected prior to discharge from the evaporation apparatus, where the surface area per unit mass is low.

In order to achieve the aim of low residual contents of solvents or monomers, in known, mechanically assisted processes and apparatuses temperatures are raised, vigorous surface renewal is achieved, usually by elevated energy input, and it is endeavoured to achieve the best vacuums so that stripping may be performed efficiently, if possible within short residence times. In order to be able to operate with short residence times, the fullest possible use must be made of the effective parameters such as temperature, elevated mechanical energy input for rapid surface renewal and vacuum. The parameters diffusion and mass transfer, which are also highly significant, are product-specific, temperature-dependent physical variables and can only be influenced within this framework.

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However, as a consequence of elevated product temperatures, the processes known from the prior art frequently result in partial modification of the products. These modifications may, for example be manifested by discoloration and particle formation due to secondary and decomposition reactions. The formation of particles or also specks entails increased filtration efforts. Filtration units for viscous products are complex and, due to steep pressure gradients, difficult to operate. Temperatures are often increased in order to lower the melt viscosities of the products and so reduce the pressure gradient. However, the increase in temperature in turn has a disadvantageous impact on product quality.

30 The object accordingly arose of providing, on the basis of the prior art, an apparatus and a process which avoids the disadvantages stated in the prior art and gives rise to

good results in terms of stripping volatile constituents and of product quality.

It has now surprisingly been found that a process using an
5 apparatus of rotating perforated annular disks in a horizontally arranged cylindrical housing does not require a further increase in product temperature and stripping of the volatile constituents may proceed at a comparatively moderate temperature level. Surprisingly, despite the
10 longer residence times, the products produced in this apparatus exhibit good quality. It has also been found that it is advantageous and efficient for stripping if the polymer melt is exposed to the stripping conditions (temperature and vacuum) for a relatively extended period
15 and the melt is continuously taken up from the bottoms in the apparatus, so constantly forming new surfaces, and exposed to the vacuum and remixing of stripped polymer melt with as yet unstripped polymer melt is avoided. The longer residence times permit lower temperatures, which are very
20 gentle on the product. It has also been found to be particularly advantageous that, even at different throughputs, the movement of the melt may be determined and controlled externally by the rotational speed of the rotor, i.e. of the perforated annular disks. In many other
25 apparatuses, the flow profiles and residence times and thus the preconditions for uniform results change as throughput varies. In the apparatus according to the invention, a change in residence time due to a variation in throughput, which always has an impact on the stripping result, may
30 readily be corrected by adjusting filling level and rotational speed.

Particular advantages of the process according to the invention using the stripping apparatus are its cascading action, the extended residence times, which then also enable lower temperatures, the constantly renewed surfaces
5 due to rotation and consequent continuous film formation and stretching of the films as they run off the disks, the elevated throughputs per unit time which are possible in the stripping apparatus according to the invention and the independence from flow profiles, as occur in other
10 stripping installations. A cascading action is taken to mean that, as a result of the flow through the apparatus from the inlet to the outlet, the product running off the disks is conveyed with this flow towards the outlet and is not mixed with freshly inflowing product. Instead, the
15 melt, which has already in part moved towards equilibrium, is picked up again by the disks and degassed again. This results in the "cascading action", which may also be viewed as a division of the apparatus into several stages in a similar manner as in a column or in a series of stirred-
20 tank reactors. Due to the cascading, surface formation rates are vastly higher than in other stripping installations. It is furthermore advantageous to introduce the melts into the stripping apparatus at low delivery pressures; these pressures are incomparably higher for
25 example in strand evaporator installations due to the very large number of nozzles and the need to achieve a uniform distribution among all the nozzles. Another advantage is the low input of mechanical energy due to low rotational speeds, which rules out product stress due to elevated
30 temperatures and a severe shear field. Further processing of the monomer-reduced melts may be performed without further temperature correction, i.e. under mild conditions, without the melts having to be cooled for further

processing operations due to excessively high temperatures, for example downstream from extruders or film evaporators.

The extended residence time and good surface renewal of the
5 apparatus makes it possible in general to achieve the stripping performance of the apparatus without raising the temperature.

In particular, this apparatus does not have the
10 disadvantage of the static apparatuses that only one single stage is possible in order to approach thermodynamic equilibrium. Accordingly, at identical processing pressure, this apparatus is capable of achieving distinctly lower contents of residual volatiles than are static apparatuses.
15 The person skilled in the art would not have expected that excellent product quality may be obtained under conditions of extended residence time.

The object was surprisingly achieved by a process for
20 stripping volatile constituents from polymer melts using an apparatus which, under the action of gravity, constantly forms free films and has an elevated film formation rate. This is achieved by a horizontally arranged evaporator apparatus which comprises a cylindrical housing which
25 accommodates a rotor which is externally driven. The rotor consists of perforated disks in the form of circular rings which are connected together. This connection may consist of a central shaft, of external connecting elements, for example in the form of straight or angled plates or tubes,
30 or of a hollow shaft (hereinafter also denoted hollow cylinder), which may be perforated. The embodiment with a perforated hollow shaft is preferred.

The invention provides a process for stripping volatile constituents from polymer melts in an evaporator apparatus, characterised in that the horizontally arranged evaporator apparatus comprises a cylindrical housing in which, to
 5 provide constant surface renewal of the melt to be stripped, are arranged rotating perforated disks on a central shaft.

The perforated disks are circular rings which are in
 10 particular perforated in such a manner that the ratio of the total area of the circular ring to the area occupied by the webs between the holes is from 2.2-6.5, preferably from 2.5-5. It is particularly preferred to select the equivalent hole diameter in accordance with the formula

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$$A = x (\eta^2 / (kg^2 m^{-5} s^{-2}))^{1/3}.$$

The equivalent hole diameter A is here defined as the diameter of a circle of identical area. The dimensionless
 20 numerical factor x may vary between 0.002 and 0.030, preferably between 0.004 and 0.016. η is the kinematic melt viscosity in Pa.s.

The holes may assume various geometric shapes. The holes
 25 are preferably in the form of equilateral, rotationally symmetrical polygons which permit constant web widths of the surrounding metal surface, and rectangles.

It is possible to deviate from these shapes at the inner
 30 and outer edges of the annular disks so that the edge may be made circular. At elevated viscosities, the equivalent hole diameter is so large that spokes must be provided between the inner and outer edges, optionally with a

further division by a central ring. The boundaries of these holes are then the spokes and spoke sections and circular ring sections.

- 5 For degassing, it is advantageous for the size and shape of the holes of a perforated disk to be identical. It is furthermore advantageous for all the perforated disks of the evaporator apparatus to be identical with regard to the shape and size of the holes.

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All the metal surfaces or webs surrounding the holes are advantageously of a square or rectangular cross-section. Selection of the web widths makes it possible optimally to adapt the ratio of the melt-bearing area as the circular
15 ring disk emerges from the melt relative to the surrounding hole as a function of melt viscosity and other properties of the melt. In the case of a circular ring disk, it has proved favourable to select all the metal surfaces or webs surrounding the holes to be cross-sectionally constant and
20 identical in size.

The power input into such an apparatus may be very low, of the order of 0.01 kWh/kg. The increase in temperature to which the product is exposed in this apparatus is
25 accordingly slight. Since the internal surface of the apparatus which is available for heat transfer is very large relative to throughput, it is, however, also possible to heat or optionally cool the product by means of the wall temperature.

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The rotational speed of the rotor is favourably between 0.3 and 10 revolutions per minute, preferably between 0.5 and 5 revolutions per minute, particularly preferably between 0.8

and 3 revolutions per minute. The film formation rate is here greater than 5 and preferably greater than 10. It is defined as the ratio of the quantity of that material which is drawn up by the rotating disk and runs back down in the form of a free film to the total quantity of the throughput of the reactor.

According to the invention, the described apparatuses corresponding to the above-stated requirements may take various forms.

A preferred apparatus for performing the process according to the invention is described in "Polymerisieren im Ringscheibenreaktor", Kunststoffe 82 (1992) 1, pages 17-20 under the name VSR. The rotor here consists of various wheels which are connected with a central shaft via two (Figure 2) to four (Figures 3 and 4) spokes.

One particularly preferred apparatus for the stripping according to the invention of volatile constituents from polymer melts is a horizontally arranged cylindrical vessel with an agitator, as is described in DE 44 47 422 C2 (Karl Fischer Industrieanlagen GmbH) column 1, line 63 to column 7, line 39.

The external diameter of the rotor is preferably selected such that it fits into the cylindrical housing (hereinafter also denoted outer cylinder) of the evaporator apparatus, the length-to-diameter ratio of the outer cylinder preferably being between 0.6 and 2.5, particularly preferably between 0.8 and 2.

It is also advantageous to arrange the rotor eccentrically in the outer cylinder, such that the vapours formed may be discharged via an enlarged slot in the upper part of the apparatus. This measure brings about a major reduction in
5 entrainment of polymer particles into the vapour line and vacuum installation.

A particular advantage of the particularly preferred embodiment is the extremely rigid construction and form of
10 the hollow shaft bearing the perforated disks. The hollow shaft is provided with orifices or holes, such that the resultant vapours may flow away unimpeded. The manner in which the rotor is mounted makes it possible to operate the reactor with different temperatures in the bottoms zone and
15 in the vapour zone. The design furthermore makes it possible to limit the entrainment of relatively high viscosity melts as the rotor rotates by the incorporation of stators which project between the disks. Especially in the case of relatively high viscosity melts, this measure
20 optimises the ratio of melt surface area to melt volume on the disk.

However, for optimum and thus very particularly preferred use of the apparatus presented in DE 4 447 422 C2 for
25 stripping polymer melts, it is convenient to make still further modifications to the designs presented in DE 4 447 422 C2.

If melt viscosities are excessively low, typically below 20
30 Pa.s, it may thus happen that wetting of the rotating circular disk is inadequate. It has proved advantageous in this connection to arrange lifting elements on the outer periphery of the annular disks in such a manner that, as

the lifting elements rise, the circular disk is continuously rinsed with melt.

When stripping relatively high viscosity polymer melts,
5 typically of above 200 Pa·s, lifting of excessive quantities of product by the rotating circular disk may result in unwanted conditions, such as for example disruption of film formation. A method for preventing this phenomenon, which is improved relative to DE 4 447 422 C2,
10 is to provide horizontal doctor bars on the stators at the bottoms filling level. Any coalescence of melt behind this bar in the direction of rotation of the rotor is thus avoided. These bars may be mounted directly on the housing or be supported by optional additional bars which are
15 likewise fastened to the evaporator wall. The doctor bars and/or supporting bars may here be designed, as described in DE 44 47 422 C2, in such a manner as to promote material conveyance. This is particularly significant and advantageous to assist conveyance of the melt to the
20 evaporator outlet.

It may be advantageous to heat the vapour or gas zone differently from the underlying melt or bottoms zone of the cylindrical evaporator. It is accordingly advantageous to
25 heat the upper gas zone to a lower level, i.e. to temperatures which are 5 to 20°C lower, than the melt zone therebelow. Any polymer films on the walls in the gas zone of the evaporator have a long residence time and suffer less damage due to lower temperatures. This measure ensures
30 longer evaporator service periods, reduced formation of specks due to cracked products and better colours of the final products.

Different degassing process temperatures must be selected for different polymers. They are substantially dependent on the thermal stability of the polymer to be processed.

Another vital factor is also the desired residual content
5 of constituents to be stripped. Pressures are adjusted between 0.01 and 15 mbar, preferably 0.05 to 10 mbar and the average residence times amount to 10 to 240 minutes, preferably 15 to 180 minutes and particularly preferably between 20 and 60 minutes.

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If the temperatures of the polymer melts introduced into the evaporator apparatus are appreciably, i.e. of the order of 20 to 50°C, below the desired operating temperatures, which conventionally amount to 200 to 350 K, of the
15 evaporator apparatus, it may be advantageous to heat the melt before introduction with heat exchangers suitable for polymer melts. In this manner, it is possible to reduce the temperature differences between the heating medium and the product in the evaporator in order to avoid product damage
20 on the walls.

The product is preferably introduced into the evaporator via a valve with automatic pressure control in such a manner that direct depressurisation into the product space
25 occurs at the input end of the evaporator. Due to the elevated thermal potential of the immediate surroundings, cooling effects are avoided, which may be disadvantageous with regard to particle contents, for example of a crystalline nature. To this end, the product inlet valve is
30 for example arranged in the end face of the reactor.

It is advantageous to offset the vapour outlets arranged on the top of the evaporator by 15° to 60° relative to the

perpendicular in the direction of rotation of the rotor, in order to reduce melt reflux.

The invention also provides an evaporator apparatus
5 comprising a horizontally arranged, cylindrical housing, a rotor comprising circular perforated disks which are arranged on a central shaft, the length-to-diameter ratio of the cylindrical housing being between 0.6 and 2.5.

10 Any conventional materials which do not cause direct damage to the product may be used for the production and manufacture of the evaporator apparatus used according to the invention. Particularly suitable materials for the treatment of polycarbonates are non-rusting steels of type
15 CrNi(Mo) 18/10, such as for example 1.4571 or 1.4541 (steel classification 2001, publisher: Stahlschlüssel Wegst GmbH, Th-Heuss-Straße 36, D-71672 Marbach) and Ni-based alloys of type C, such as for example 2.4605 or 2.4610 (steel classification 2001, publisher: Stahlschlüssel Wegst GmbH,
20 Th-Heuss-Straße 36, D-71672 Marbach). The non-rusting steels are used at process temperatures of up to approx. 290°C and the Ni-based alloys at process temperatures of above approx. 290°C. When treating styrene polymers and styrene copolymers, for example comprising acrylonitrile, a
25 stainless steel typical for chemical applications, for example 1.4571 to DIN or 316 SS to ASME, is advantageous for product quality.

The apparatus used in the process according to the
30 invention is shown schematically in Figure 1 and described below: the polymer melt is introduced via the product inlet 1 of the housing 10 by means of a pipe with control valve into the end face of the evaporator. The product outlet 2

of the melt is effected by means of a gear pump at the opposite end to the product inlet 1 on the underside of the housing 10 of the cylindrical evaporator. The evaporated volatile constituents are drawn off from the evaporator at the top via the vapour port 3. The rotor with the annular disks 5 mounted thereon is set in rotation with a shaft 4. The annular disks 5 are connected together via a hollow shaft 9. The stators 6 fastened to the internal wall 8 of the cylindrical housing 10 spread the polymer melt on the annular disks 5 and, at elevated viscosities, prevent bridging between the annular disks 5. The level of the bottoms is adjusted with an overflow weir, which may be a metal sheet 7, for example a metal sheet without or also with openings. In the embodiment shown in Figure 1, the central shaft is arranged centrally in the outer cylinder, i.e. the evaporator housing.

The necessary vacuum is preferably generated using jet or vapour pumps which are ideally operated with substances inherent to the system and process. It is, however, also possible to use the generally conventional liquid ring pumps in combination with Roots vacuum pumps to generate the vacuum. It is advantageous to operate the liquid ring pumps with a substance from the process.

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The process according to the invention for the removal of volatile components from polymer melts, is in particular suitable for melts of engineering thermoplastics such as polycarbonate, polyester, polyester carbonates, polyamides, polymethyl methacrylate, and blends of these polymers, particularly preferably polycarbonate, polyester, polyester carbonates, and blends of these polymers, very particularly preferably polycarbonate.

The process according to the invention may for example be used in processes for the production of polymers, in particular of engineering thermoplastics such as

5 polycarbonate, polyester, polyester carbonates, polyamides, polymethyl methacrylate, polystyrene, copolymers of styrene and acrylic monomers such as acrylonitrile and/or methyl methacrylate, and blends of these polymers, particularly preferably polycarbonate, polyester, polyester carbonates
10 and copolymers of styrene and acrylonitrile, and blends of these polymers, very particularly preferably polycarbonate.

The polymer melts to be stripped using the process according to the invention may originate from various
15 processes such as two-phase interfacial condensation reactions, melt transesterification reactions, solid phase condensation reactions, emulsion polymerisation reactions, bulk polymerisation reactions and the like or be produced by melting existing polymeric material. Such processes are
20 sufficiently well known from the prior art. There are no limitations or restrictions with regard to the manner of polymer production, the installation used or the production process which is performed.

25 The polymer melts to be stripped may be combined with inhibitors before being stripped according to the invention. Inhibitors are taken to mean any compounds which have a decisive inhibitory effect on chemical reaction kinetics, such that quality-impairing modification of the
30 polymer is avoided. Addition thereof is, for example, necessary after the production of polymers which still contain monomers and reaction products after completion of

the reaction in order to reduce the contents of low molecular weight compounds by thermal processes.

Suitable inhibitors for polycarbonate which has been
5 produced by the transesterification process are acid components such as Lewis or Brønsted acids or esters of strong acids. The pKa value of the acid should be no greater than 5, preferably less than 3. The acid components or the esters thereof are added in order to deactivate the
10 reaction mixture, i.e. ideally to bring the reaction to a complete standstill.

Examples of suitable acid components are: orthophosphoric acid, phosphorous acid, pyrophosphoric acid, hypophosphoric
15 acid, polyphosphoric acids, benzenephosphonic acid, sodium dihydrogenphosphate, boric acid, arylboronic acids, hydrochloric acid (hydrogen chloride), sulfuric acid, ascorbic acid, oxalic acid, benzoic acid, salicylic acid, formic acid, acetic acid, adipic acid, citric acid,
20 benzenesulfonic acid, toluenesulfonic acid, dodecylbenzenesulfonic acid and any other phenyl-substituted benzenesulfonic acids, nitric acid, terephthalic acid, isophthalic acid, stearic acid and other fatty acids, acid chlorides such as phenyl chloroformate, stearic acid chloride, acetoxy-BP-A, benzoyl chloride and
25 esters, semi-esters and bridged esters of the above-stated acids such as for example toluenesulfonic acid esters, phosphoric acid esters, phosphorous acid esters, phosphonic acid esters, dimethyl sulfate, boric acid esters,
30 arylboronic acid esters and other components which generate acid on exposure to water such as tri-iso-octylphosphine, Ultrinox 640 and BDP (bisphenol diphosphate oligomer).

Compounds which may preferably be considered here are orthophosphoric acid, phosphorous acid, pyrophosphoric acid, hypophosphoric acid, polyphosphoric acids, benzenephosphonic acid, sodium dihydrogenphosphate, boric acid, arylboronic acid, benzoic acid, salicylic acid, benzenesulfonic acid, toluenesulfonic acid, dodecylbenzenesulfonic acid and any other phenyl-substituted benzenesulfonic acids, acid chlorides such as phenyl chloroformate, stearic acid chloride, acetoxy-BP-A, benzoyl chloride and esters, semi-esters and bridged esters of the above-stated acids such as for example toluenesulfonic acid esters, phosphoric acid esters, phosphorous acid esters, phosphonic acid esters, boric acid esters, arylboronic acid esters and other components which generate acid on exposure to water such as tri-iso-octylphosphine, Ultranox 640 and BDP.

Compounds which may particularly preferably be considered are orthophosphoric acid, pyrophosphoric acid, polyphosphoric acids, benzenephosphonic acid, benzoic acid, benzenesulfonic acid, toluenesulfonic acid, dodecylbenzenesulfonic acid and any other phenyl-substituted benzenesulfonic acids and esters, semi-esters and bridged esters of the above-stated acids such as for example toluenesulfonic acid esters, phosphoric acid esters, phosphorous acid esters, phosphonic acid esters and other components which generate acid on exposure to water such as tri-iso-octylphosphine, Ultranox 640 and BDP.

Compounds which may very particularly preferably be used are orthophosphoric acid, pyrophosphoric acid, benzenesulfonic acid, toluenesulfonic acid, dodecylbenzenesulfonic acid and any other phenyl-

substituted benzenesulfonic acids and esters, semi-esters and bridged esters of the above-stated acids such as for example toluenesulfonic acid esters and phosphoric acid esters.

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The acidic components may be apportioned in solid, liquid or gaseous form. In a preferred method, the acidic component is continuously homogeneously incorporated into the product stream from which monomers are, for example, to
10 be removed in the production process directly once the desired final molecular weight has been achieved in order to begin evaporating the residual monomers immediately thereafter. In a particularly preferred method, incorporation of additives to improve individual product
15 properties is performed downstream from apportionment of the acid and stripping and not together with the stripping step because additives are often used which are volatile under a vacuum, which is essential to stripping, and the necessary concentrations in the polymer are then difficult
20 to establish.

The acidic components are preferably added in liquid form. Since the quantities to be apportioned are very small, solutions of the acidic components are preferably used.

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Suitable solvents are those which do not disrupt the process, are chemically inert and evaporate rapidly.

Properties of the resultant polymers may be modified with
30 conventional additives and additional substances (e.g. auxiliaries and reinforcing materials). The purpose of adding additives and added substances is to extend service life (for example hydrolysis or degradation stabilisers),

to improve colour stability (for example heat and UV stabilisers), to simplify processing (for example mould release agents, flow auxiliaries), to improve service characteristics (for example antistatic agents), to improve
5 flame retardancy, to influence visual appearance (for example organic colorants, pigments) or to adapt polymer properties to specific stresses (impact modifiers, finely divided minerals, fibrous materials, silica flour, glass fibres and carbon fibres). These may all be combined at
10 will in order to establish and obtain the desired properties. Such added substances and additives are described, for example, in "Plastics Additives", R. Gächter and H. Müller, Hanser Publishers 1983, in Additives for Plastics Handbook, John Murphy, Elsevier, Oxford 1999 or in
15 Plastics Additives Handbook Hans Zweifel, Hanser, Munich 2001.

These additives and added substances may be added to the polymer melt individually or in any desired mixtures or in
20 two or more different mixtures and in particular directly on isolation of the polymer or alternatively after melting pelletised material in a "compounding" step.

The additives and added substances or mixtures thereof may
25 here be added to the polymer melt as a solid, i.e. as a powder, or as a melt and also in the form of solutions in suitable solvents. Another apportionment method is to use masterbatches or mixtures of masterbatches of the additives or mixtures of additives.

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These substances are preferably added to the finished polymer using known apportioning units, but, if required, they may also be added at another stage of the polymer

production process. Mixing with the polymer proceeds in apparatus known for this purpose, such as for example screw machines or static mixers.

Examples

Determination of stated analytical characteristics:

5 Rel. viscosity:

Relative viscosity is determined as the quotient of the viscosity of the solvent and the viscosity of the polymer dissolved in this solvent. It is measured in

- 10 dichloromethane at 25°C at a concentration of 5 g/l of solution.

Residual monomer content:

- 15 Residual monomer content is determined by dissolving the sample in dichloromethane and then precipitating it with acetone/methanol. Once the precipitated polymer has been separated, the filtrate is evaporated. The residual monomers are quantified by reverse-phase chromatography in
- 20 a 0.04% phosphoric acid/acetonitrile mobile solvent gradient. Detection is by UV means.

YI:

- 25 The YI value is determined to ASTM E 313 on injection moulded samples 4 mm in thickness. The injection moulding temperature is 300°C.

- 30 The same polycarbonate, produced by the transesterification process, is used for all the Examples. The data are stated in Table 1. In order to be able to achieve and compare the stripping effect, the polycarbonate pellets are sprayed prior to use with such a quantity of 1% phosphoric acid and

homogenised at room temperature in a tumble dryer that the concentration of 100% phosphoric acid relative to the polycarbonate is 5 ppm.

- 5 Likewise in all the Examples, the pellets were melted at 290°C at a rate of 50 kg/h in a melting extruder (model ZSK 32 MC, Coperion Werner & Pfleiderer) in order to be introduced directly thereafter into the stripping apparatus.

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Example 1:

- The melt produced in the melting extruder was supplied to a device according to DE 4 447 422 C2 with a rotor diameter
15 of 620 mm and a ratio of rotor diameter-to-length of 0.8, which was operated at a rotational speed of 1.3 revolutions per minute at 290°C and 1 mbar absolute. The filling level was adjusted such that an average residence time of 20 minutes was obtained. The melt was discharged with a gear
20 pump via a nozzle, shaped into bristles, cooled and pelletised. The data obtained are shown in Table 1.

Comparative Example 1:

- 25 As Example 1, but using an apparatus according to DE 4 447 422 C2 with a rotor diameter of 620 mm and rotor diameter-to-length ratio of 3. The rotational speed, pressure and temperature were as in Example 1, but the average residence time was 90 minutes.

30

Comparative Example 2:

The melt produced in the melting extruder was conveyed into a model ZSK 40 degassing screw machine from Werner & Pfleiderer with a screw diameter of 40 mm and a ratio of external to root diameter of the screws of 1.55. The degassing screw machine, which was operated at a wall temperature of 300°C, had two degassing zones. The first degassing zone was operated at atmospheric pressure. 0.25% by mass of nitrogen, relative to the quantity of melt, was apportioned before the second degassing zone. The pressure in the second degassing zone was 2 mbar absolute. The melt was discharged via a nozzle, shaped into a plurality of strands, cooled and pelletised. The data obtained are shown in Table 1.

Comparative Example 3:

The melt produced in the melting extruder is passed into a strand evaporator, which was heated to 290°C and was at a vacuum of 1 mbar absolute. The melt was here subdivided into strands by means of a spinneret plate with 150 bores, each of a diameter of 3 mm, the strands free-falling for 3 m in the cabinet. The melt coalesced on the base and was discharged with a gear pump via a nozzle, shaped into a plurality of strands, cooled and pelletised. The data obtained are shown in Table 1.

Table 1:

	Relative viscosity	DPC [ppm]	BPA [ppm]	Phenol [ppm]	YI
Initial product	1.204	520	11	76	1.9
Example 1	1.208	50	5	49	2.3
Comparative Example 1	1.211	45	6	55	3.4
Comparative Example 2	1.205	175	8	67	2.5
Comparative Example 3	1.205	220	8	70	2.4

Claims:

1. A process for stripping volatile constituents from polymer melts comprising introducing the melt into a horizontally oriented cylindrical device having a length to diameter ratio of 0.6 to 2.5 that contains a plurality of perforated disks rotating about a common horizontally oriented, externally driven shaft bringing the melt and disks into contact in a manner calculated to constantly renew the surface of the melt to be stripped, wherein the perforated disks have equal-sized holes having a common size A conforming to $A = x \left(\frac{\eta}{\text{kg}^2 \text{ m}^{-5} \text{ s}^{-2}} \right)^{1/3}$ wherein x is $2 \cdot 10^{-3}$ to $3 \cdot 10^{-2}$ and η is the kinematic melt viscosity in Pas.
2. The process according to claim 1 wherein the shaft is perforated and hollow.
3. The process according to claim 1 where the device further contains stators having horizontal cross bars, the stators positioned between the disks.
4. Stripping apparatus comprising a horizontally arranged, cylindrical housing, a rotor comprising circular perforated disks which are mounted on a central shaft and connected together with a horizontally arranged, perforated hollow cylinder, wherein the length-to-diameter ratio of the first cylinder is between 0.6 and 2.5.