

A PROCESS FOR THE EXTRACTION, PURIFICATION AND
ENZYMATIC MODIFICATION OF SOY 7S GLOBULIN ALPHA'
SUBUNIT FOR USE AS HYPOCHOLESTEROLEMIZING AGENT

The present invention relates to a process for the extraction, purification and enzymatic modification of β -conglycinin α' subunit.

According to the invention, β -conglycinin is selectively extracted from ground, defatted soy, then precipitated by treatment with aqueous ethanol; the enriched fraction is then subjected to Metal Affinity Chromatography (MAC) in denaturant conditions to obtain the α' subunit. The latter is treated with chymotrypsin, then subjected to a further affinity chromatography step to recover the amino-terminal region of this polypeptide (MW 28,000 Da).

TECHNICAL BACKGROUND

10 The known cholesterol lowering properties of soy and derivatives thereof are related with the content in isoflavones (Kirk et al., 1998) and in proteins (Anderson et. al, 1995).

Soy proteins mainly consist of glycinins (11S fraction) and β -conglycinins (7S fraction), the latter consisting of three subunits, named α , α' and β (Thanh and Shibasaki, 1976). Studies carried out on soy proteins have established that the 7S fraction (Lovati et. al, 1992, 1996), particularly the α' subunit (Manzoni et. al, 1998) is capable of activating LDL receptor and is therefore the main responsible for the reduction of cholesterol plasma levels. In fact, treatment of an hepatic cell line with 7S globulin induces extensive degradation of the α and α' subunits and stimulation of LDL receptor activity, whereas β subunits are not degraded and the receptor is not activated. Moreover, soy mutants in which 7S fraction lacks α' subunit are not able to modify the receptor activity, even at high concentrations.

As a consequence of these experimental observations, methods are

needed to obtain β -conglycinin in the pure form, as well as recovering and purifying the α' subunit, from which specific amino acidic sequences could subsequently be obtained by enzymatic treatment, without making use of peptide synthesis.

- 5 The process suggested by Than et al. (1975 and 1976) and subsequently modified by O'Keefe et al. (1991) allows to separate glycinins and β -conglycinins based on their different solubilities at different pH; however, cross-contamination is still high and gel filtration or affinity chromatography are required, which are costly and difficult to carry out on an industrial scale.
- 10 Also the modification suggested by Nagano et al. (1992), although allowing to increase the fractions purity, is still an expensive method which can be used only on laboratory scale.

 Recently, Wu et al. (1999) have described a method for separating glycinins and conglycinins on a pilot-plant scale. Glycinins are precipitated by
15 two subsequent aqueous extractions at pH 8.5, followed by treatment of the supernatant with a 0.98 g/L bisulfite solution, while conglycinins are precipitated by adding 0.25 M NaCl to the mother liquors from the glycinins precipitation, then adjusting pH to 4.8. The process allows to treat high amounts of starting material and also provides high yields in protein, but the
20 fractions purity is still unsatisfactory; β -conglycinin, in particular, undergoes degradation, apparently during diafiltration with water, which is a treatment necessary to reduce the bisulfite ions excess and to remove salts.

 The above cited methods not only do not yield pure β -conglycinin, but above all do not envisage separation and purification of the α' subunit.

- 25 According to the invention, a solid fraction enriched in β -conglycinin is prepared by extracting a defatted ground soy in an aqueous medium according to conventional procedures and subsequently precipitating the supernatant with aqueous ethanol; the resulting fraction is then purified by Metal Affinity

Chromatography (MAC) in denaturant conditions to yield the pure α' subunit, which is subjected to enzymatic treatment with chymotrypsin to obtain the amino-terminal region which has apparently the highest LDL receptor-activating activity.

5 SUMMARY OF THE INVENTION

The present invention provides a process for the selective extraction, purification and enzymatic modification of soy β -conglycinin α' subunit, which process comprises the following steps:

- 10 a) extraction of a defatted ground soy with a sodium bisulfite aqueous solution at slightly acidic pH to obtain a β -conglycinin -enriched soluble protein fraction;
- b) precipitation of the β -conglycinin fraction from step a) by treatment with ethanol;
- 15 c) purification of the precipitated fraction from step b) by Metal Affinity Chromatography (MAC) under denaturant conditions, to isolate the α' subunit; and
- d) precipitation of the α' subunit with organic solvents.

20 The process further comprising a step of enzymatic treatment of the α' subunit with a proteolytic enzyme and further purification by MAC chromatography, wherein the said step is carried out after step d).

25 The present invention also provides polypeptide fragments of soy β -conglycinin α' subunit obtainable with the process of the present invention. The soy β -conglycinin α' subunit may be for use as a medicament. The present invention also provides amino-terminal polypeptide fragment obtainable according to process of the present invention. The amino-terminal polypeptide fragment may be for use as a medicament.

The present invention provides a use of the polypeptide fragments of the β -conglycinin α' subunit from soy for the preparation of medicament for the treatment of hyperlipidemias. The present invention also provides a use of the polypeptide fragment for the preparation of medicaments for the treatment of hyperlipidemias.

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Pharmaceutical compositions containing the polypeptide fragments of the present invention, alone or in combination with other active ingredients, in admixture with suitable carriers is provided.

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The present invention provides supplements or alimentary products containing the polypeptide fragments of the invention.

The present invention also provides β -conglycinin -enriched fraction and α' subunit from soy obtainable with the process of the present invention.

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BRIEF DESCRIPTION OF DRAWINGS

Figure 1 shows a process flow of β -conglycinin enrichment.

Figure 2 shows a process flow of α' subunit precipitation.

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DETAILED DISCLOSURE OF THE INVENTION

The present invention relates to a process for the selective extraction, purification and enzymatic modification of soy β -conglycinin α' subunit, which process comprises the following steps:

- 5 a) extraction of a defatted ground with a sodium bisulfite aqueous solution at slightly acidic pH to obtain a β -conglycinin -enriched soluble protein fraction;
- b) precipitation of the β -conglycinin fraction from step a) by treatment with ethanol;
- 10 c) purification of the precipitated fraction from step b) by Metal Affinity Chromatography (MAC) under denaturant conditions, to isolate the α' subunit;
- d) enzymatic treatment of the α' subunit from step c) with a proteolytic enzyme and further purification by MAC chromatography;
- 15 e) precipitation of the α' subunit with organic solvents.

β -Conglycinin is enriched as shown in Figure 1. The starting material is soy flour, defatted by removing the lipid fraction with solvents. The material is extracted with a sodium bisulfite aqueous solution at slightly acidic pH. A solution volume ranging from 14 to 16 times the weight of the starting material, preferably from 14.5 to 15.5 times, is used. The bisulfite concentration ranges from 0.80 to 1.20 g/L, preferably from 0.90 to 1.10 g/L, most preferably from 0.95 to 1.05 g/L. The extraction is carried out for a time ranging between 14 and 18 hours at a temperature ranging from -2 to 8°C. According to a preferred embodiment of the invention, the extraction is

carried out for 16 hours with 15 volumes of a 0.98 g/L bisulfite solution at pH 6.4, at temperatures ranging from 0 to 4°C.

Under these pH and temperature conditions, glycinins solubility is very low, therefore these precipitate together with other insoluble material. The precipitate is separated by centrifugation and the soluble fraction is treated with 35 - 60% (vol/vol) aqueous ethanol, preferably 40% aqueous ethanol, at temperatures ranging from 20 to 30°C, preferably at room temperature, 25°C. The supernatant is centrifuged off and the precipitate, mainly consisting of β -conglycinin, is freeze-dried. The resulting powder is subjected to the subsequent step (Figure 2).

The choice to separate and purify the α' subunit by means of MAC (Ostrove and Weiss, 1990) depends on its ability to coordinate metal ions such as Zn^{2+} and Ni^{2+} , as this subunit has higher histidine content than the α and β subunits (Thanh and Shibasaki, 1978).

A matrix conjugated with zinc or nickel, preferably zinc, is used. According to a preferred embodiment of the invention, the matrix consists of iminodiacetic acid-agarose. The freeze-dried protein material is suspended in a denaturing buffer consisting of 50 mM Tris, 0.5 M NaCl, pH 7.2 and containing 5 to 8 M urea, preferably 5 M. In these conditions, the α' subunit selectively binds to the matrix, and the α and β subunits can be removed by elution with the above buffer; the α' subunit is subsequently eluted with 0.1 M imidazole in the same buffer or in distilled water.

The protein fraction enriched in α' subunit is collected and treated with organic solvents which precipitate the proteins, preferably with cold acetone. Acetone is used in a volume ranging from 2 to 5 times the fraction volume, preferably 3 to 4 volumes, at a temperature ranging between -10 and -30°C, preferably between -15 and -25°C. According to a preferred embodiment of the invention, 3 volumes of acetone at -20°C are used. The resulting

precipitate is separated by centrifugation, resuspended in ethanol, preferably 95% ethanol, further centrifuged and freeze-dried. The lyophilizate contains 94% of protein material and is 10 times more enriched in the α' subunit than the starting material.

- 5 Table 1 shows the extraction yields in β -conglycinin and α' subunit from soy flour.

Table 1

Protein fraction	Starting material	Extraction yield (% by weight)
β -Conglycinin	Defatted flour	18.7
α' Subunit	β -Conglycinin	11.0
α' Subunit	Defatted flour	2.1

- 10 Polypeptide fragments of the α' subunit are prepared by subjecting the lyophilizate from the previous step to enzymatic treatment with a proteolytic enzyme. According to a preferred embodiment of the invention, the proteolytic enzyme is chymotrypsin and the resulting fragment mainly consists of the amino-terminal region having MW 28,000 Da.

- 15 The procedure is as follows: the lyophilizate from the previous step is dissolved at a concentration of 5 mg/ml in 0.2 M NH_4HCO_3 containing 1.6 M urea at pH ranging from 7.5 to 8.5. Chymotrypsin is added in a 1:10 to 1:50 ratio, preferably 1:25 w/w to the substrate, incubating at 37°C with stirring for 24 hours. A step on MAC is subsequently carried out, as described above.

- 20 The material eluted with imidazole contains three polypeptide fragments, the main having MW 28,000 Da, and constituting the N-terminal region of the α' subunit.

The administration of the α' subunit and of chymotrypsin fragment to rats (table 2) proved that both are capable of remarkably decreasing cholesterol and total triglycerids plasma levels. In particular, the chymotrypsin

fragment proved not only more effective than the other soy components, but also than clofibrate, in reducing cholesterol levels, and it afforded comparable results on triglycerids.

The results of the biological experimentation suggest that the products obtainable according to the process of the present invention, in particular the α' subunit and the fragments thereof, can be used as medicaments, in particular for the treatment of those pathologies which require lowering of cholesterol and/or triglycerids plasma levels. Said compounds will be used, alone or in combination with other active principles and in admixture with suitable carriers, for the preparation of pharmaceutical compositions, in particular for the treatment of hyperlipidemias. Furthermore, they can also be used for the preparation of supplements or food products for dietary regimens to be followed in the above mentioned conditions.

EXAMPLES

15 *First step: Purification of 7S globulin from soy*

The starting material was ground soy, defatted according to the Soxhlet method, using pentane as solvent.

Proteins were extracted with a 0.98 g/L NaHSO₃ solution in amounts 15 times the volume of the defatted ground soy, for 16 hours at temperatures ranging from 0 to 4°C, keeping pH at 6.4. After centrifugation, the supernatant was treated with 40% ethanol (vol/vol) at room temperature. The resulting precipitate, enriched in β -conglycinin and containing the α' subunit at a double concentration than the starting material, was freeze-dried.

Second step: Purification of the α' subunit

25 The β -conglycinin enriched fraction was resuspended in denaturing buffer (50 mM Tris, 0.5 M NaCl, pH 7.2) containing 5 M urea and purified by MAC on an agarose-iminodiacetic acid matrix (Sigma) conjugated with zinc. The unbound protein material was eluted with the same buffer as above,

whereas the bound protein material, mainly consisting of the α' subunit, was eluted with 0.1 M imidazole in the same buffer or in distilled water.

The α' subunit- enriched fractions were treated with 3-4 volumes of acetone at -20°C ; the resulting precipitate was suspended in 40% ethanol at room temperature, then centrifuged and freeze-dried. The resulting powder contains 94% of proteins and is 10 times more enriched in α' subunit than the starting material.

Third step: Enzymatic treatment of the α' subunit

The lyophilizate from the above step was dissolved at a concentration of 5 mg/ml in 0.2 M NH_4HCO_3 containing 1.6 M urea, at pH ranging from 7.5 to 8.5. The solution was then treated with chymotrypsin in a 1:25 w/w ratio to the protein substrate and incubated at 37°C with stirring for 24 hours, then purified by MAC as described above. The material retained by the resin and eluted with 0.1 M imidazole contains three polypeptide fragments, the major one having molecular weight 28,000 Da and consisting of the N-terminal region of the α' subunit.

BIOLOGICAL EXPERIMENTATION

Animals

Male rats CD SPF/VAF, weighing 75-100 g, were used. The animals were housed in makrolon cages (4-5 animals per cage) in environment with automatic control of light (12 hour light/ 12 hour darkness cycles), temperature ($21 \pm 1^{\circ}\text{C}$) and humidity ($60 \pm 5\%$).

Experimental protocol

After 7 day housing, the animals were randomly divided into seven groups of 20 rats each (Table 2). During 28 days, one group was fed with normal diet (cod. 014RF25C; Mucedola S.r.l., Settimo Milanese, MI, Italy), whereas the others were fed with hypercholesterolemic diet consisting of 1% cholesterol, 0.5% cholic acid and 25% hydrogenated coconut oil (batch

332000, preparation 01.09.2000; Laboratorio Dottori Piccioni, Gessate, MI, Italy), with access to water *ad libitum*. The diet was given daily (40 g, 09.00 a.m.) and the unconsumed amount was weighed. Treatment was carried out as follows.

- 5 Group 1 (control): animals fed with normal diet and treated orally for 28 days with a 0.5% carboxymethylcellulose solution.
- Group 2: animals fed with hypercholesterolemic diet and treated orally for 28 days with a 0.5% carboxymethylcellulose solution.
- 10 Group 3: animals fed with hypercholesterolemic diet and treated orally for 28 days with clofibrate at a dose of 200 mg/kg.
- Group 4: animals fed with hypercholesterolemic diet and treated orally for 28 days with the soy total protein extract (TPE) at a dose of 200 mg/kg.
- 15 Group 5: animals fed with hypercholesterolemic diet and treated orally for 28 days with β -conglycinin at a dose of 50 mg/kg.
- Group 6: animals fed with hypercholesterolemic diet and treated orally for 28 days with the α' subunit at a dose of 10
- 20 mg/kg.
- Group 7: animals fed with hypercholesterolemic diet and treated orally for 28 days with the α' subunit chymotrypsin fragment at a dose of 1 mg/kg.

25 Total cholesterol and triglycerids plasma levels were measured at the end of the 28 day treatment and after 16 hour fasting. The animals were anaesthetized with ethyl ether and blood was drawn from the inferior vena cava in tubes containing EDTA (1 mg/ml). After centrifugation for 15 min at 4°C at 3000 rpm, plasma was recovered, frozen and stored at -20°C until

measurements.

Total cholesterol and triglycerids plasma concentrations (reported in Table 2) were determined according to conventional enzymatic assays.

Table 2

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TREATMENT	Total cholesterol (mg/dL)	Total triglycerids (mg/dL)
GROUP 1	55.4±3	105.1±7.2
GROUP 2	284.1 ± 10.3	226.9 ± 12.6
GROUP 3	191.2 ± 8.0	139.1 ± 5.8
GROUP 4	236.1 ± 10.2	176.9 ± 8.1
GROUP 5	196.4 ± 7.6	146.7 ± 5.9
GROUP 6	182.2 ± 12.1	150.1 ± 9.8
GROUP 7	175.8 ± 7.9	140.3 ± 7.4

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CLAIMS

1. A process for the selective extraction, purification and enzymatic modification of soy β -conglyonin α' subunit, which process comprises the following steps:
 - 5 a) extraction of a defatted ground soy with a sodium bisulfite aqueous solution at slightly acidic pH to obtain a β -conglyonin -enriched soluble protein fraction;
 - b) precipitation of the β -conglyonin fraction from step a) by treatment with ethanol;
 - 10 c) purification of the precipitated fraction from step b) by Metal Affinity Chromatography (MAC) under denaturant conditions, to isolate the α' subunit; and
 - d) precipitation of the α' subunit with organic solvents.
2. The process as claimed in claim 1, the process further comprising a step of
15 enzymatic treatment of the α' subunit with a proteolytic enzyme and further purification by MAC chromatography, wherein the said step is carried out after step d).
3. A process as claimed in any one of claims 1 or 2 wherein the extraction is carried out with 15 volumes of a 0.98 g/L sodium bisulfite solution at pH
20 6.4.

4. A process as claimed in any one of claims 1 to 3 wherein precipitation of step b) is carried out with 40% ethanol.
5. A process as claimed in any one of claims 1 to 4 wherein MAC in step c) is carried out on a matrix conjugated with zinc or nickel.
- 5 6. A process as claimed in claim 5 wherein the matrix is conjugated with zinc.
7. A process as claimed in any one of claims 5 or 6 wherein the matrix consists of agarose-iminodiacetic acid.
8. A process as claimed in any one of claims 1 to 7 wherein the
10 denaturing agent used in MAC of step c) is urea.
9. A process as claimed in any one of claims 2 to 8 wherein the proteolytic enzyme for the enzymatic treatment is chymotrypsin.
10. A process as claimed in any one of claims 1 to 9 wherein precipitating solvent for the α' subunit in step d) is acetone.
- 15 11. A process as claimed in any one of claims 1 to 10 wherein the β -conglycinin -enriched fraction and the α' subunit are stabilized by freeze-drying.