CLAIMS:

1. A process for converting mixed waste plastic (MWP) into petrochemicals, comprising feeding mixed waste plastic (MWP) to a pyrolysis reactor, converting said MWP into a gaseous stream and a liquid stream, and further processing said gaseous stream into petrochemicals, said process further comprising the steps of:

i) feeding said liquid stream, together with a hydrocracker feed, to a hydrocracking unit, said hydrocracker feed comprising crude distillation bottoms from atmospheric distillation and/or vacuum distillation;

ii) converting said liquid stream, together with said hydrocracker feed, through hydrocracking into at least one gaseous stream and a liquid stream:

iii) further processing said at least one gaseous stream into petrochemicals, wherein in step i) said liquid stream from said pyrolysis reactor is first separated into a liquid stream having a high aromatics content and a liquid stream having a low aromatics content, wherein said liquid stream having a low aromatics content is then sent to said hydrocracking unit and wherein said liquid stream having a high aromatics content by-passes said hydrocracking unit.

2. A process according to claim 1, further comprising combining said gaseous stream originating from said pyrolysis reactor with said at least one gaseous stream originating from said hydrocracking unit and further processing the combined gaseous stream into petrochemicals.

3. A process according to any one or more of the claims 1-2, wherein said pyrolysis reaction is carried out such that 90% of said liquid stream coming from said pyrolysis reactor boils below 350 °C.

4. A process according to any one or more of the preceding claims, wherein said gaseous stream from said pyrolysis reactor and said at least one gaseous stream originating from said hydrocracking unit are further processed in one or more processing units chosen from the group of steam cracking unit, propane dehydrogenation unit, butane dehydrogenation unit and combined propane/butane

dehydrogenation unit.

5. A process according to claim 4, wherein said gaseous stream from said pyrolysis reactor and said at least one gaseous stream originating from said hydrocracking unit are further processed in steam cracking unit and one or more processing units chosen from the group of propane dehydrogenation unit, butane dehydrogenation unit and combined propane/butane dehydrogenation unit.

6. A process according to claims 4-5, further comprising separating said gaseous stream from said pyrolysis reactor and/or and said at least one gaseous stream originating from said hydrocracking unit into a lights fraction, a C2 fraction, a C3 fraction and a C4 fraction before further processing.

7. A process according to any one or more of the claims 4-6, further comprising feeding said C2 fraction to said steam cracking unit, said C3 fraction to said propane dehydrogenation unit and said C4 fraction to said butane dehydrogenation unit, respectively.

8. A process according to any one or more of the claims 1-7, further comprising no hydrogenation of any liquid stream coming from said pyrolysis reactor to free it from chlorine, before carrying out step i).

9. A process according to any one or more of the claims 1-8, further comprising feeding mixed waste plastic (MWP) to a separator for PVC removal before feeding the MWP to said pyrolysis reactor, wherein the thus obtained segregated PVC stream is preferably thermally dehydrochlorinated at temperatures of up to 450 °C and preferably fed to said pyrolysis reactor.

10. A process according to any one or more of the claims 1-9, further comprising mixing said liquid stream and said hydrocracker feed in such a proportion by weight or volume which results in the combined mixture prior to entering the hydrocracking unit or its feed heaters having an S value measured as per ASTMD7157-12 of greater than 1.